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(54) **Titre :** PROCEDE VISANT A EMPECHER OU REDUIRE LES DEPOTS D'ALUMINOSILICATE LORS DE PROCEDES INDUSTRIELS
(54) **Title:** METHOD OF PREVENTING OR REDUCING ALUMINOSILICATE SCALE IN INDUSTRIAL PROCESSES

(57) **Abrésumé/Abstract:**

Materials and a method are provided whereby polymers with least 0.5 mole % of the pendant group or end group containing - Si (OR')₃ (where R' is H, an alkyl group, Na, K, or NH₄) are used to control aluminosilicate scaling in an industrial process having an alkaline process stream such as a pulping mill process stream. When materials of the present invention are added to the alkaline process stream, they reduce and even completely prevent formation of aluminosilicate scale on equipment surfaces such as evaporator walls and heating surfaces. The present materials are effective at treatment concentrations that make them economically practical.



Abstract

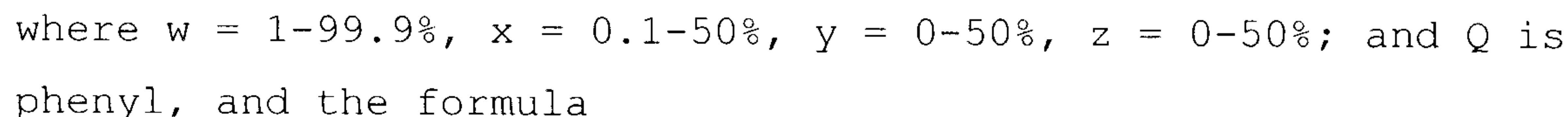
Materials and a method are provided whereby polymers with least 0.5 mole % of the pendant group or end group containing - Si (OR')₃ (where R' is H, an alkyl group, Na, K, or NH₄) are used to control aluminosilicate scaling in an industrial process having an alkaline process stream such as a pulping mill process stream. When materials of the present invention are added to the alkaline process stream, they reduce and even completely prevent formation of aluminosilicate scale on equipment surfaces such as evaporator walls and heating surfaces . The present materials are effective at treatment concentrations that make them economically practical.

This is a divisional application of Canadian patent application serial No. 2,597,082, filed on February 1, 2006.

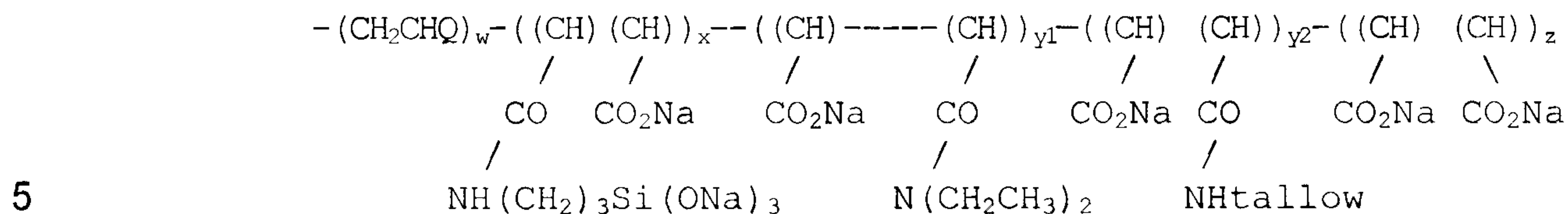
The invention describes materials and methods for preventing or inhibiting the formation of scale on or in equipment used in industrial processes having alkaline process streams.

$$\text{A-O-(CH}_2\text{CH}_2\text{O)}_x\text{(CH}_2\text{CH(CH}_3\text{)O)}_y\text{(CH}_2\text{CH}_2\text{O)}_z\text{-O-B} \quad (\text{Formula XI})$$

The subject matter of the parent application was directed to a composition for use in reducing aluminosilicate in an alkaline industrial process comprising a polymer from the formula



75365-246D1



where $w = 1-99.9\%$, $x = 0.1-50\%$, $y1+y2 = 0-50\%$, $y1$ and $y2 = 0-50\%$
 $z = 0-50\%$; and Q is phenyl.

However, it should be understood that the expression
 "the invention" and the like, as used herein, encompass the
 subject matter of both the parent and this divisional
 application.

Background of the Invention

The problem of scaling in and on process equipment used
 in industrial processes and particularly in those having an
 alkaline process stream is very well known. The scales present a
 significant problem when they build up on the surface of process
 equipment and cause a loss in the heat transfer coefficient.
 Thus, additional heat may be required to be provided to the
 evaporator equipment in these processes resulting in added cost.

An example of such an industrial process having an
 alkaline process stream is the Kraft recovery process for
 manufacturing paper which has been known for over 100 years and
 is eloquently described in many texts on the subject (see G.A.
 Smook "Handbook for Pulp and paper technologists , 3rd Edition).
 More recently the development of closed loop cycles in kraft
 paper mills has resulted in an increase in scaling problems in
 process equipment due to the build up of aluminum and silicon in
 the system as is described by P.N. Wannamaker and W.J. Frederick
 in "Application of solubility data to predicting the accumulation
 of aluminum and silicon in alkaline pulp mills", Minimum Effluent

75365-246D1

Mills Symposium, 1996, p303. It has, therefore, been a well recognized need to provide a method and compositions for inhibiting the formation of aluminosilicate scales in kraft pulp mills. US 5409571 describes the use of terpolymers of maleic
5 acid, acrylic acid and hypophosphorous acid as scale inhibitor for kraft pulp mills. This type of polymer is shown to be

WO 2006/086189

PCT/US2006/003525

calcium carbonate scales but has not been shown to be effective for aluminosilicate scales.

High Level Nuclear Waste (HLNW) facilities process radioactive-rich solid and liquid wastes in order to minimize waste volume and immobilize the hazardous material for long term storage. HLNW treatment is currently performed via two processes; one process is performed under acidic conditions and one under alkaline conditions. Under alkaline processing conditions, sodium aluminosilicate scale growth is a significant problem during the pretreatment stage, prior to waste vitrification.

Within the pretreatment facility, the waste is evaporated, filtered, ion exchanged and further evaporated. During evaporation, aluminosilicate scales can form on the surfaces of the evaporator walls and heating surfaces. Furthermore, transfer pipes can also become blocked due to the buildup of these scales and precipitates necessitating closure for maintenance.

20

The pretreated HLNW wastes go vitrification facilities. HLNW waste goes into a melter preparation vessel where silica and other glass-forming materials are added. The mixture is then heated and the molten mixture is then poured into large stainless steel containers, cooled and moved into temporary storage until a permanent storage location is selected.

From the vitrification unit operation, a portion of the Si-containing glass-forming materials are recycled back into the evaporator unit (during pretreatment). The dissolved aluminum, in the form of sodium aluminate, and sodium silicate species react slowly in solution to form complex hydrated sodium aluminosilicate species. Among these species are families of amorphous aluminosilicates (aluminosilicate hydrogel), zeolites, sodalites, and cancrinites collectively known as "sodium aluminosilicate". These nuclear waste streams

WO 2006/086189

PCT/US2006/003525

also contain high concentrations (up to 2M for each ion) of nitrate and nitrite ions, and very high concentrations (up to 16M in some sections of the tank) of OH⁻ ions. These factors greatly enhance the rate of formation of aluminosilicate scale. As a result, sodium aluminosilicate scale formed has a low solubility in the alkaline HLNW liquor.

Also, sodium aluminosilicate scale is considered to be an undesirable HLNW product due to the incorporation of radioactive lanthanides and actinides into the aluminosilicate scale cage structures and coprecipitation of sodium diuranate. (Peterson, R. A. and Pierce, R. A., (2000), *Sodium diuranate and sodium aluminosilicate precipitation testing results*, WSRC-TR-2000-00156, Westinghouse Savannah River Company, Aiken, SC.). It is therefore, desirable for HLNW facilities to minimize the volume of HLNW's including those resulting from aluminosilicate scales. Thus, it can be seen that, sodium aluminosilicate scale growth has a significant negative economic and operational impact on the treatment of nuclear wastes.

Therefore, it would be desirable to provide a solution to the sodium aluminosilicate scaling problem in the nuclear waste evaporators.

Attempts to solve the aforementioned problems have lead to limited success see Wilmarth and coworkers (Wilmarth, W. R., Mills, J. T. and Dukes, V. H., (2005), Removal of silicon from high-level waste streams via ferric flocculation, Separation Sci. Technol., 40, 1-11. These authors have examined the use of ferric nitrate to remove Si from solution in the form of a ferric precipitate, in order to reduce or eliminate the formation of aluminosilicate scale. Although this approach has some merit, there is still the disposal of the high-level ferric precipitate to deal with and an additional filtration unit operation is required. Also, W. R. Wilmarth and J. T. Mills "Results of Aluminosilicate Inhibitor Testing", WSRC-TR-2001-00230 have proposed using low

75365-246

molecular weight compounds as scale inhibitors for HLNW's but have found none to be satisfactory.

Thus there is a need for an economical and effective method for reducing aluminosilicate scale buildup on equipment
5 used in industrial processes where such buildup is a problem as for example, the Kraft pulp paper process and in nuclear waste treatment streams.

SUMMARY OF THE INVENTION

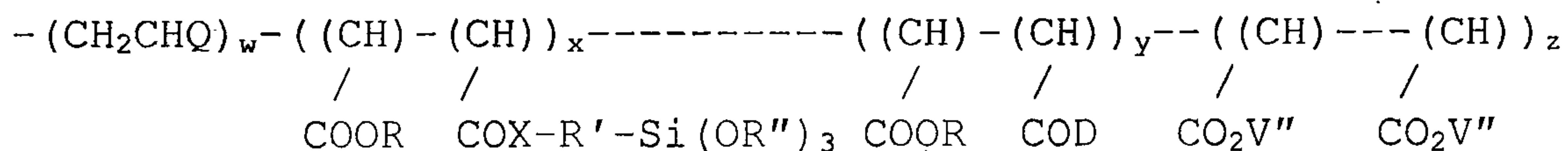
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The present invention solves the aforementioned problems and others by providing materials and a method whereby polymers having at least 0.5 mole % of the group $-\text{Si}(\text{OR}'')_3$ (where R'' is H, an alkyl group, Na, K, or NH_4) as an end group
15 or pendant thereto are used to reduce or eliminate aluminosilicate scaling in a process having an alkaline process stream such as a kraft pulping mill or a high level nuclear waste evaporation process treatment stream. When materials of the present invention are added to these
20 industrial process streams, they reduce and even completely prevent formation of aluminosilicate scale on the equipment surfaces. Moreover, the present materials are effective at treatment concentrations that make them economically practical.

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The present description describes the following invention aspects:

- i) a composition for use in reducing aluminosilicate scale in an alkaline industrial process comprising a polymer
5 according to the formula:



- where $w = 1-99.9 \%$, $x = 0.1-50\%$, $y = 0-50\%$, $z = 0-50\%$; and
10 $Q = \text{C1-C10 alkyl, aryl, amide, acrylate, ether, COXR}$ where $X=O$ or NH and $R = \text{H, Na, K, NH}_4, \text{C1-C10 alkyl or aryl, or any other substituent;}$ $X = \text{NH, NP}$ where $P = \text{C1-C3 alkyl or aryl, or O;}$
 $R' = \text{C1-10 alkyl, or aryl;}$ $V'' = \text{H, C1-C3 alkyl, aryl, Na, K or NH}_4$ or forms an anhydride ring; $R'' = \text{H, C1-C3 alkyl, aryl, Na, K or NH}_4$, and $D = \text{NR}_1\text{ or OR}_1$ wherein $R_1 = \text{H, C1-C20 alkyl, C1-C20 alkenyl or aryl,}$ with the proviso that all R, R'', V'' and R_1 groups do not have to be the same;
15

- ii) a composition for use in reducing aluminosilicate scale in an alkaline industrial process comprising a polymer
20 which is a polysaccharide having pendant thereto a group or an end group containing formula I:

Formula I

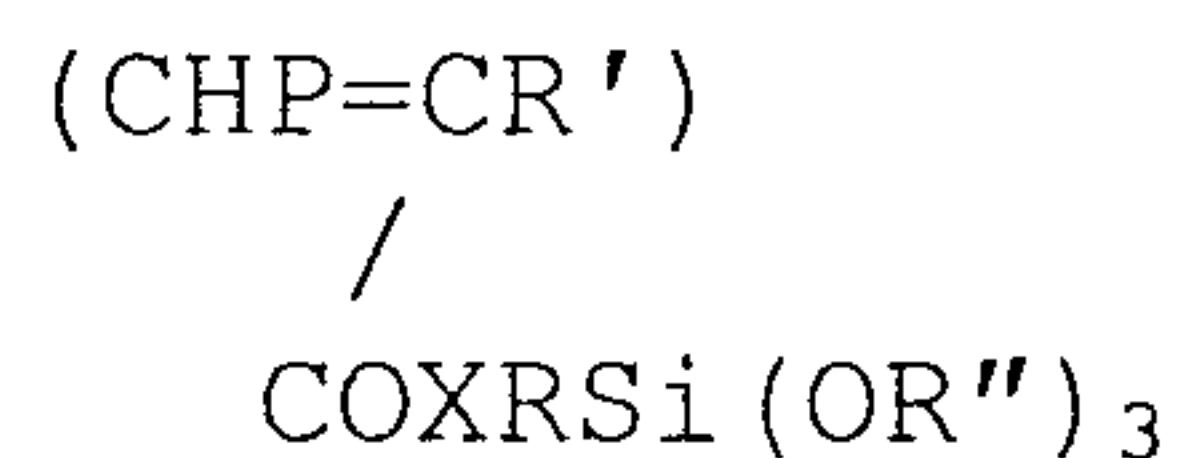


where $R'' = \text{Na, K or NH}_4$;

75365-246

iii) a composition for reducing aluminosilicate scale in an industrial process comprising a polymer which is a homopolymer or copolymer derived from an unsaturated monomer of formula V:

5 Formula V



where P = H, C1-C3 alkyl, -CO₂R'', -CONHR

10 R = C1-C10 alkyl, aryl,

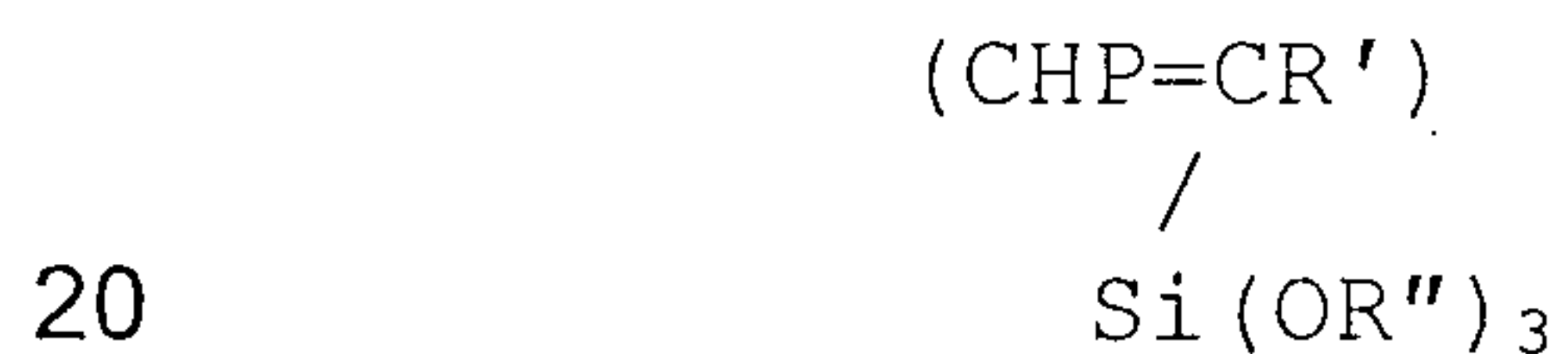
R' = H, C1-3 alkyl, or aryl

X = O, NH, or NR

R'' = H, C1-C3 alkyl, aryl, Na, K or NH₄;

iv) a composition for reducing aluminosilicate scale
15 in an industrial process comprising a homopolymer or copolymer derived from monomers of formula VI:

Formula VI



where P = H, C1-C3 alkyl, -CO₂R'', -CONHR

R = C1-C10 alkyl, aryl,

R' = H, C1-3 alkyl, or aryl

X = O, NH, or NR

75365-246

$$R'' = \text{Na, K or NH}_4;$$

v) a composition for reducing aluminosilicate scale in an industrial process comprising a polymer according to the formula XI:

5 Formula XI

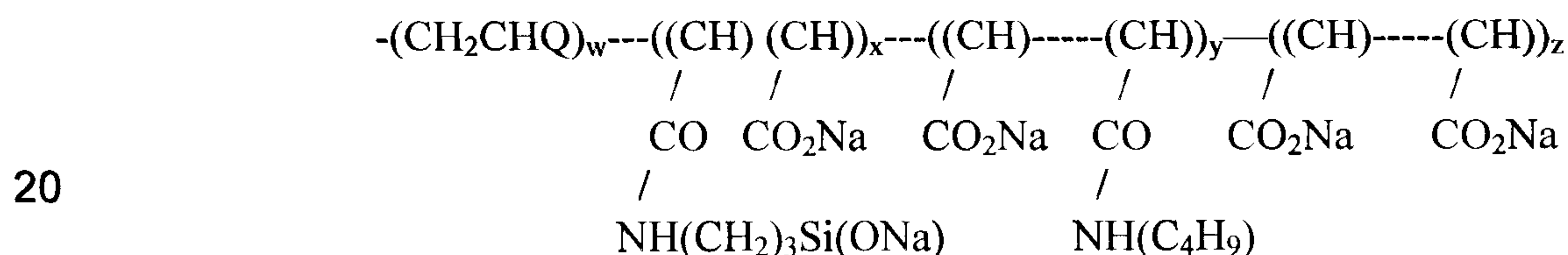


where $x = 5\text{-}100\%$, y and $z = 0\text{-}100\%$ and at least one A and / or B unit is a group containing the group --Si(OR'')_3 , where $R'' = \text{Na, K or NH}_4$;

vi) a composition for reducing aluminosilicate scale in an industrial process
 10 comprising a polymer which is the reaction product of poly(ethylene glycol)-block-poly(propylene glycol)-block-poly(ethylene) with 3-glycidoxypropyltrim ethoxysilane;

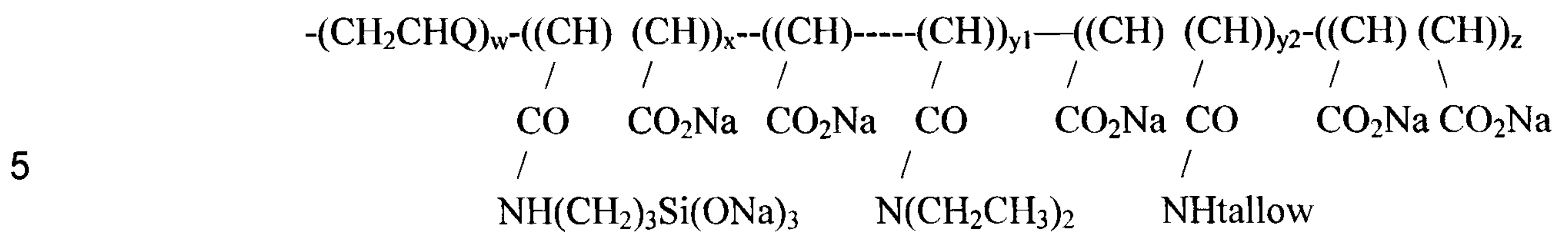
vii) a composition for reducing aluminosilicate scale in an industrial process comprising a polymer which is the reaction product of polyethyleneimine with 3-glycidoxypropyltrimethoxysilane; and

15 viii) a composition for use in reducing aluminosilicate scale in an alkaline industrial process comprising a polymer selected from the formula



where $w = 1\text{-}99.9\%$, $x = 0.1\text{-}50\%$, $y = 0\text{-}50\%$, $z = 0\text{-}50\%$; and Q is phenyl, and the formula

75365-246



where $w = 1-99.9\%$, $x = 0.1-50\%$, $y1+y2 = 0-50\%$, $y1$ and $y2 = 0-50\%$ $z = 0-50\%$; and Q is phenyl.

DETAILED DESCRIPTION OF THE INVENTION

10 The present invention is directed to a method and materials for the reduction of aluminosilicate containing scale in an industrial process having an alkaline process stream such as in the kraft pulp mill process streams or a high level nuclear waste treatment stream. The process stream to be treated can be any process stream having an alkaline condition and in which scaling occurs, e.g. black, green and white liquors of the kraft process or a high level

15 nuclear waste evaporation process stream.

The method comprises the step of adding to the process stream an aluminosilicate containing scale inhibiting amount

WO 2006/086189

PCT/US2006/003525

of a polymer having at least 5 mole % pendant thereto a group or end group containing $--Si(OR'')_3$ where $R'' = H, C1-C3$ alkyl, aryl, Na, K or NH_4 . The amount of $--Si(OR'')_3$ functionality present in the polymer will be an amount sufficient enough to achieve the desired results and can range from a little as 0.5 mole % of the total monomer groups present in the polymer to as much as 100 mole%. However it will be most economical to use the least amount necessary to yield the desired results. The polymers are preferably prepared initially as the silylether derivatives Polymer-- $Si(OR'')_3$ where $R'' = C1-C3$ alkyl, aryl, eg Polymer-- $Si(OCH_2CH_3)_3$ or Polymer-- $Si(OCH_3)_3$. The silylether derivatives may be added directly to the industrial process stream or they may be hydrolyzed to the silanol derivatives to form polymers of the following generic structures, Polymer-- $Si(OH)_3$, Polymer-- $Si(ONa)_3$, Polymer-- $Si(OK)_3$, and Polymer-- $Si(O NH_4)_3$ before addition to the process stream. It is a convenient feature of this invention that any of these forms may be added to the process stream. The molecular weight of the polymer should be at least about 500, most preferably at least about 1000.

In a preferred embodiment, the group containing $--Si(OR'')_3$ where $R'' = H, C1-C3$ alkyl, aryl, Na, K or NH_4 comprises a group according to $--G--R--X--R'--Si(OR'')_3$ where G = no group, NH, NR'' or O; R = no group, C=O, O, C1-C10 alkyl, or aryl; X = no group, NR, O, NH, amide, urethane, or urea; R' = no group, O, C1-C10 alkyl, or aryl; and $R'' = H, C1-C3$ alkyl, aryl, Na, K or NH_4 .

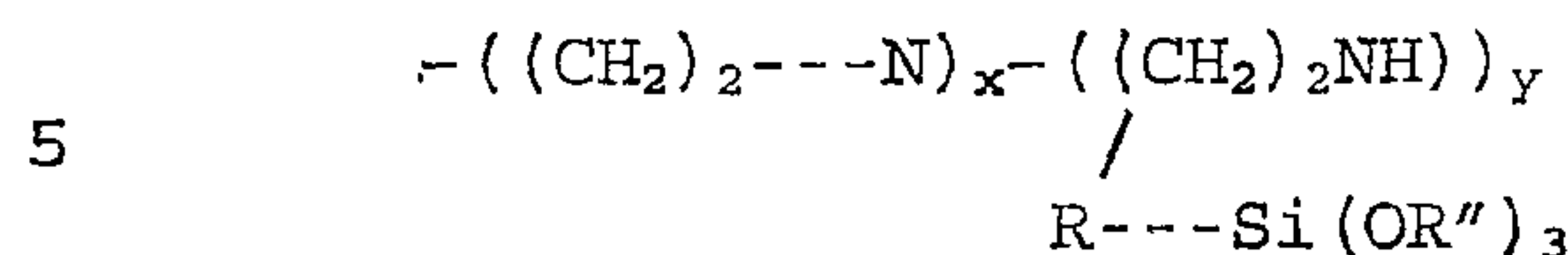
In one embodiment, the group is $--NH--R--X--R'--Si(OR'')_3$, where R = no group, O, C1-C10 alkyl, or aryl; X = O, NH, an amide, urethane, or urea; R' = no group, O, C1-C10 alkyl, or aryl; and $R'' = H, C1-C3$ alkyl, aryl, Na, K or NH_4 .

In another embodiment the polymer to which the group is pendant can comprise at least one nitrogen to which the pendant group is attached. Exemplary polymers comprising at least one nitrogen to which the pendant group is attached

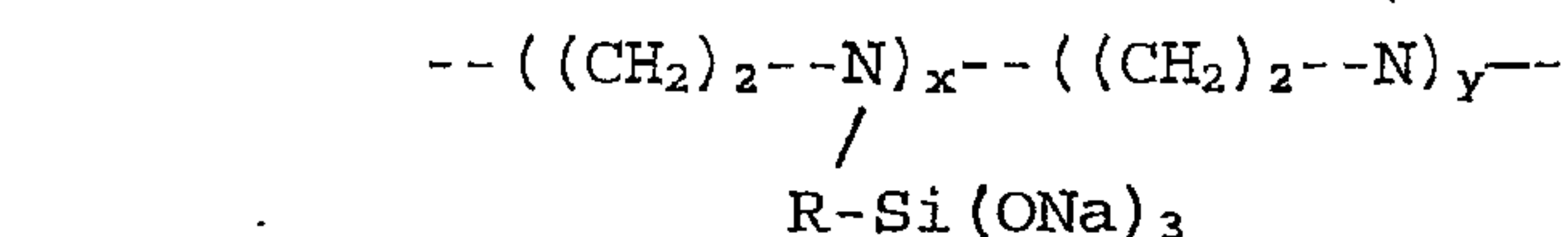
WO 2006/086189

PCT/US2006/003525

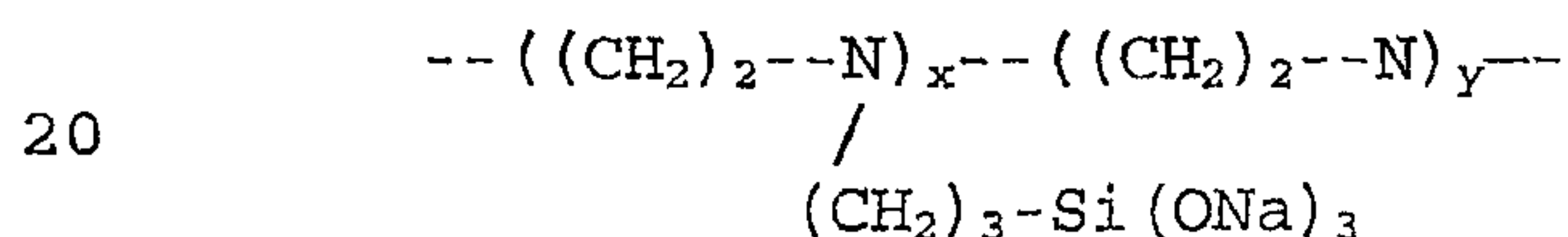
include, but are not limited to, a polymer according to the following formula:



where $x = 0.1\text{-}100\%$, $y = 99.9\text{-}0\%$; and $\text{R} =$ no group, C1-C10 alkyl, aryl, or ---COX-R' , where $\text{X} = \text{O}$ or NH and $\text{R}' =$ no group, C1-C10 alkyl or aryl; and $\text{R}'' = \text{H}$, C1-C3 alkyl, aryl, Na, K or NH_4 ; wherein polymers according to the formula:



where $x = 0.5\text{-}20\%$, $y = 99.5\text{-}80\%$ and $\text{R} = \text{C2-C6}$ are preferred, and wherein polymers according to the formula:

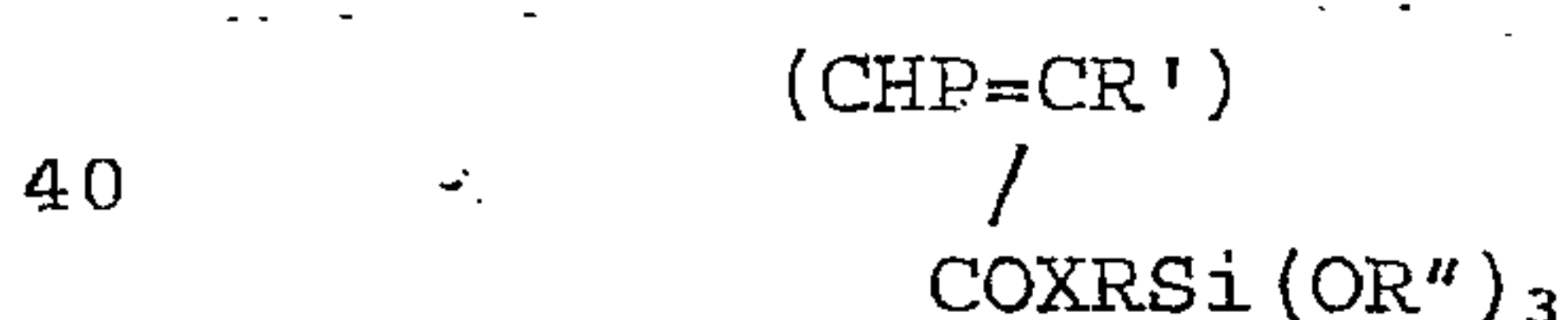


where $x = 0.5\text{-}20\%$, $y = 99.5\text{-}80\%$ are specific examples.

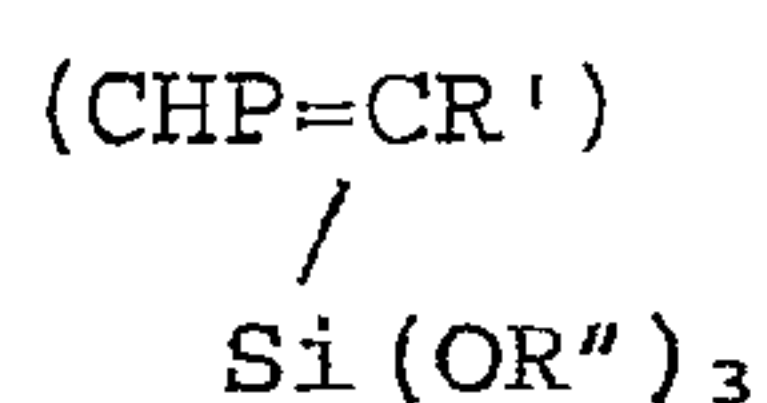
In another embodiment the polymer having pendant thereto a group or end group containing ---Si(OR'')_3 is derived from an unsaturated polymerizable monomer containing the group ---Si(OR'')_3 where $\text{R}'' = \text{H}$, C1-C10 alkyl, aryl, Na, K or NH_4 and is optionally copolymerized with one or more additional polymerizable monomer(s). Examples of such additional polymerizable monomers include but are not limited to vinylpyrrolidone, (meth)acrylamide, N-substituted acrylamides such as N-alkylacrylamides or acrylamidomethylpropanesulfonic acid, (meth)acrylic acid and salts or esters thereof, maleimides, vinyl acetate, acrylonitrile, and styrene. Particularly preferred unsaturated polymerizable monomers containing

---Si(OR'')_3 groups are monomers of formula V and VI.

Formula V:



Formula VI:



WO 2006/086189

PCT/US2006/003525

where $P = H, C1-C3 \text{ alkyl}, -CO_2R'', -CONHR$

$R = C1-C10 \text{ alkyl}, \text{aryl},$

$R' = H, C1-3 \text{ alkyl}, \text{or aryl}$

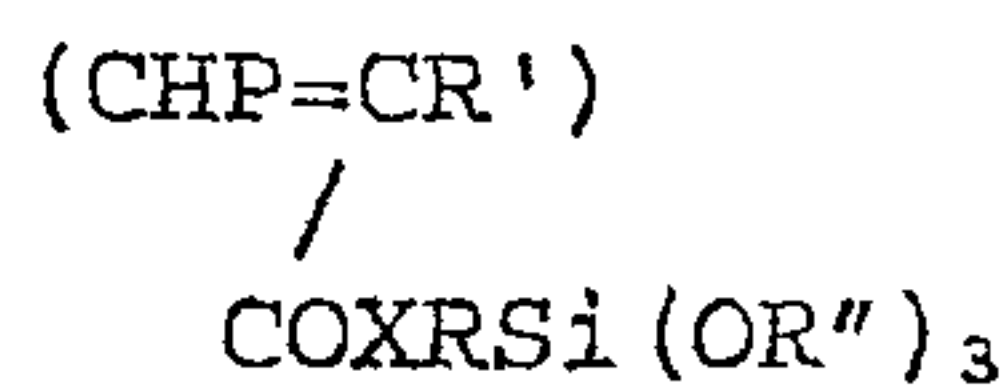
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$X = O, NH, \text{ or } NR$

$R'' = H, C1-C3 \text{ alkyl}, \text{aryl}, Na, K \text{ or } NH_4.$

Examples of such polymers include homo- and copolymers of trialkoxyvinylsilanes such as $CH_2=CHSi(OCH_2CH_3)_3$ and monomers of the formula VII:

10 Formula VII:



15 where $P = H, R = -CH_2CH_2CH_2-, R' = H, X = NH$ and $R'' = H, C1-C3 \text{ alkyl}, \text{aryl}, Na, K \text{ or } NH_4.$

Monomers of this type may be copolymerized with any other polymerizable monomers such as those described above.

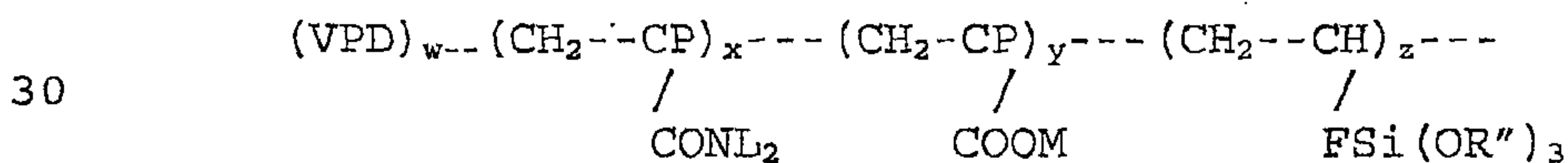
Particularly preferred copolymerizable monomers include

20 vinylpyrrolidone, (meth)acrylamide, N-substituted

(meth)acrylamides, (meth)acrylic acid and its salts or esters and maleimides. Particularly preferred are N-substituted acrylamides containing 4-20 carbon atoms such as N-

25 methylacrylamide, N,N-dimethylacrylamide, N-ethylacrylamide N-propylacrylamide, N-butylacrylamide, N-amylacrylamide, N-hexylacrylamide, N-penylacrylamide, N-octylacrylamide.

In a preferred embodiment a polymer according to the formula:



where $w=0-99\%$, $x=1-99\%$, $y=1-99\%$, $z=0.5-20\%$ and $M = H, Na,$

$K, NH_4;$ and $R'' = H, C1-10 \text{ alkyl}, \text{aryl}, Na, K \text{ or } NH_4; P = H \text{ or}$

35 $CH_3, L=H, \text{ or } C1-C10 \text{ alkyl}, \text{aryl or aralkyl},$

$F = -G-R-X-R'-Si(OR'')_3$ wherein $G = \text{no group}, NH, NR'' \text{ or } O;$

$R = \text{no group}, C=O, O, C1-C10 \text{ alkyl}, \text{ or aryl}; X = \text{no group}, NR,$

$O, NH, \text{ amide}, \text{urethane}, \text{ or urea}; R' = \text{no group}, O, C1-C10$

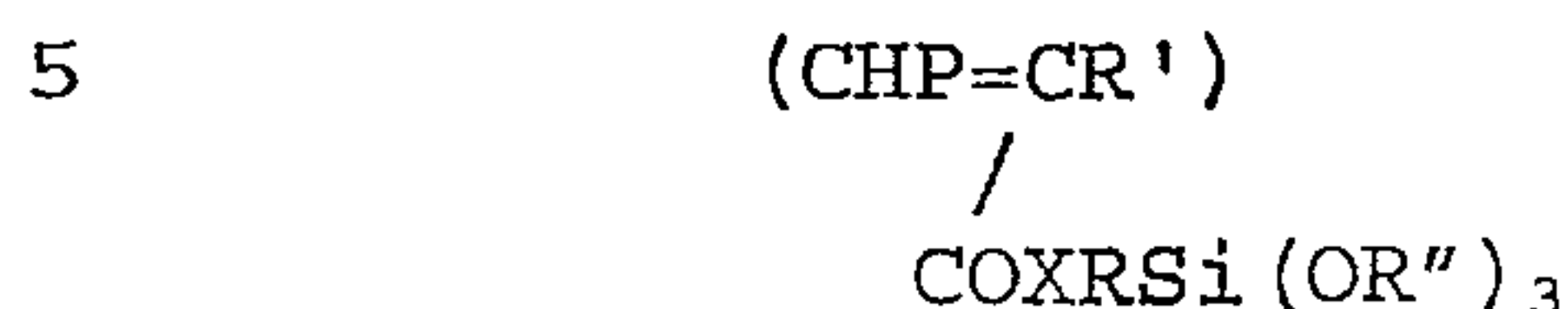
$\text{alkyl}, \text{ or aryl}; \text{ and } R'' = H, C1-C3 \text{ alkyl}, \text{aryl}, Na, K \text{ or } NH_4 \text{ and}$

WO 2006/086189

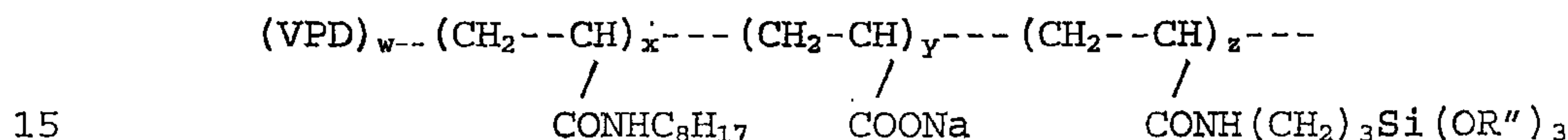
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VPD is a moiety derived from substituted or unsubstituted vinylpyrrolidone monomer. Exemplary polymers are homo- or copolymers of one or more comonomers of formulae VII:

Formula VII:

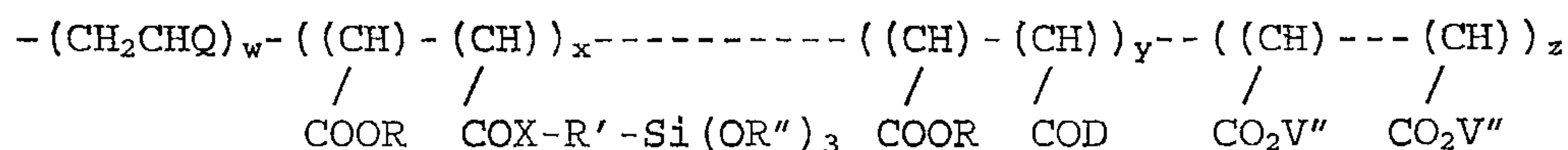


where P = H, R = -CH₂CH₂CH₂-, R' = H, X = NH and
R'' = H, C1-C3 alkyl, aryl, Na, K or NH₄ wherein
polymers according to the following formula:

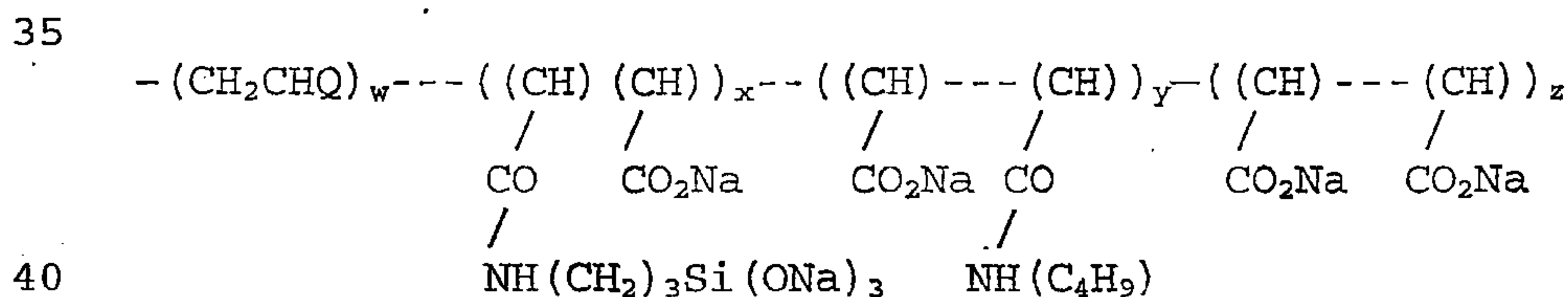


wherein w = 0-90%, x=0-50%, Y=0-90%, Z=2-50 mole % are
specific examples.

In another embodiment, a polymer according to the formula:



where w = 1-99.9 %, x = 0.1-50%, y = 0-50%, z = 0-50%; and
Q = C1-C10 alkyl, aryl, amide, acrylate, ether, COXR where X=O
or NH and R = H, Na, K, NH₄, C1-C10 alkyl or aryl, or any other
substituent; X = NH, NP where P= C1-C3 alkyl or aryl, or O;
R' = C1-10 alkyl, or aryl; V'' = H, C1-C3 alkyl, aryl, Na, K or
NH₄ or forms an anhydride ring; R'' = H, C1-C3 alkyl, aryl, Na,
K or NH₄, and D= NR₁₂ or OR₁ wherein R₁ = H, C1-C20 alkyl, C1-
C20 alkenyl or aryl, with the proviso that all R, R'', V'' and
R₁ groups do not have to be the same, is used, and wherein
polymers according to the formulae:

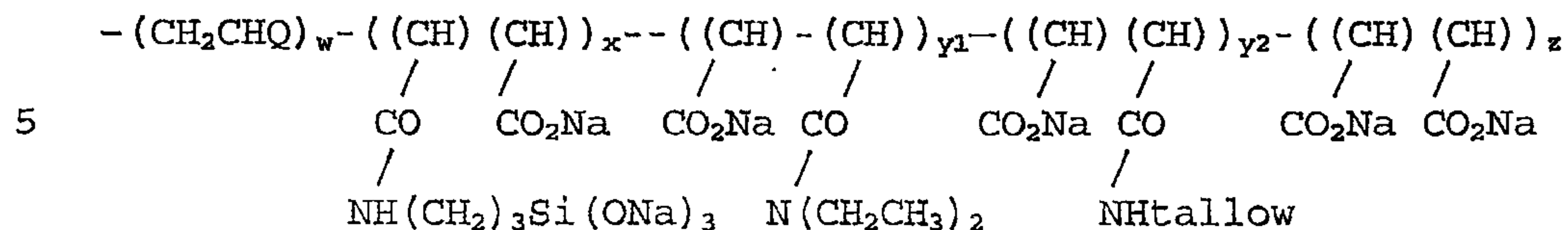


where w =1-99.9%, x=0.1-50%, y=0-50%, z=0-50%; and

WO 2006/086189

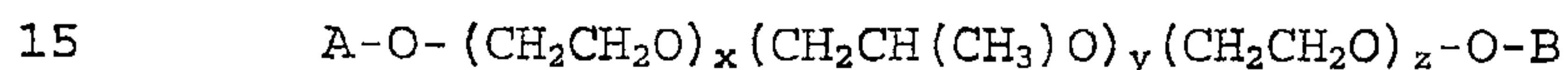
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Q is phenyl, and:



where $w = 1-99.9\%$, $x = 0.1-50\%$, $y1+y2 = 0-50\%$, $y1$ and $y2 = 0-50\%$
 $z = 0-50\%$; and Q is phenyl are specific examples.

In another embodiment a polymer according to the formula:



where $x = 5-100\%$ (as mole %), y and $z = 0-100\%$ and at least one A and/or B unit is a group containing the group $--\text{Si}(\text{OR}'')_3$, where $R'' = \text{H}$, C1-C3 alkyl, aryl, Na, K or NH_4 , is used. Exemplary such polymers include;

$A-O-(\text{CH}_2\text{CH}_2\text{O})_x(\text{CH}_2\text{CH}(\text{CH}_3)\text{O})_y(\text{CH}_2\text{CH}_2\text{O})_z-O-B$ in which A and/or B = $\text{R}-\text{Si}(\text{OR}'')_3$, and $x = 5 - 50\%$, $y = 5 - 95\%$ and $z = 0 - 50\%$ i.e. a copolymer of ethylene oxide and propylene oxide substituted with $-\text{Si}(\text{OR}'')_3$ groups, and
 $A-O-(\text{CH}_2\text{CH}_2\text{O})_x(\text{CH}_2\text{CH}(\text{CH}_3)\text{O})_y(\text{CH}_2\text{CH}_2\text{O})_z-O-B$ in which A and/or B = $\text{R}-\text{Si}(\text{OR}'')_3$, $x = 100\%$, $y = 0\%$ and $z = 0\%$ i.e., a homopolymer of polyethylene oxide substituted with $\text{R}-\text{Si}(\text{OR}'')_3$ groups is used.

In another embodiment a polymer prepared from a polysaccharide or polysaccharide derivative is used. Any polysaccharide to which the pendant $--\text{Si}(\text{OR}'')_3$ groups can be attached may be employed. Preferably the polysaccharide should be soluble in the industrial process stream such as a kraft pulping mill process streams liquor or the high level nuclear waste process stream. Polysaccharides useful in this invention include but are not limited to cellulose and its derivatives, such as hydroxyethylcellulose, hydroxypropylcellulose, methylcellulose, hydroxybutylcellulose, carboxymethylcellulose, starch and starch derivatives such as cationic starch, guar, dextran, dextrans, xanthan, agar,

WO 2006/086189

PCT/US2006/003525

carrageenan and the like. Particularly preferred are starch and cellulose derivatives wherein the reaction product of hydroxyethylcellulose with 3-glycidoxypropyltrimethoxysilane is a specific example.

5

The polymers used in the invention can be made in a variety of ways. For example, they can be made by polymerizing a monomer containing the group $--Si(OR'')_3$, where $R'' = H$, C1-C3 alkyl, aryl, Na, K or NH_4 , such as for example a silane monomer, or copolymerizing such a monomer with one or more co-

monomers. Suitable silane monomers for use in the present invention include, but are not limited to vinyltriethoxysilane, vinyltrimethoxysilane, allyltriethoxysilane, butenyltriethoxysilane, gamma-N-

acrylamidopropyltriethoxysilane, p-triethoxysilylstyrene, 2-(methyltrimethoxysilyl) acrylic acid, 2-

(methyltrimethoxysilyl)-1,4 butadiene, N-triethoxysilylpropyl-maleimide and other reaction products of maleic anhydride and other unsaturated anhydrides with amino

compounds containing the $--Si(OR'')_3$ group. These monomers can be hydrolyzed by aqueous base, either before or after

polymerization. Suitable co-monomers for use in the present invention include, but are not limited to, vinyl acetate, acrylonitrile, styrene, (meth)acrylic acid and its esters or

salts, (meth)acrylamide and substituted acrylamides such as acrylamidomethylpropanesulfonic acid, N-methylacrylamide, N,N-

dimethylacrylamide, N-ethylacrylamide N-propylacrylamide, N-butylacrylamide, N-amylacrylamide, N-hexylacrylamide, N-

phenylacrylamide, N-octylacrylamide. The copolymers can also

be graft copolymers such as polyacrylic acid-g-

poly(vinyltriethoxysilane) and poly(vinyl acetate-co-crotonic acid) -g- poly(vinyltriethoxysilane). These polymers can be

made in a variety of solvents. Solvents suitable for such use include, but are not limited to, acetone, tetrahydrofuran,

toluene, xylene, etc. In some cases the polymer is soluble in the reaction solvent and is recovered by stripping off the

WO 2006/086189

PCT/US2006/003525

solvent. Alternatively, if the polymer is not soluble in the reaction solvent, the product is recovered by filtration. Suitable initiators for use in the present invention include, but are not limited to, 2,2'-azobis(2,4-dimethylvaleronitrile) and 2,2'-azobisisobutyronitrile, benzoyl peroxide, and cumene hydroperoxide.

In another embodiment of the present invention, polymers useful in the invention can be made by reacting a compound containing a $--Si(OR'')_3$ group as well as a reactive group that reacts with either a pendant group or backbone atom of an existing polymer. For example, polyamines and polysaccharides can be reacted with a variety of compounds containing $--Si(OR'')_3$ groups to give polymers which can be used for the invention. Suitable reactive groups include, but are not limited to an alkyl halide group, such as for example, chloropropyl, bromoethyl, chloromethyl, and bromoundecyl. The compound containing $--Si(OR'')_3$ can contain an epoxy functionality such as glycidoxypropyl, 1,2-epoxyamyl, 1,2-epoxydecyl or 3,4-epoxycyclohexylethyl. 3-glycidoxypropyltrimethoxysilane is a particularly preferred compound.

The reactive group can also be a combination of a hydroxyl group and a halide, such as 3-chloro-2-hydroxypropyl. The reactive moiety can also contain an isocyanate group, such as isocyanatopropyl, or isocyanatomethyl that react to form a urea linkage. In addition, silanes containing anhydride groups, such as triethoxysilylpropylsuccinic anhydride are suitable for use in making the polymers for the present invention. The reactions can be carried out either neat or in a suitable solvent. In addition, other functional groups such as alkyl groups can be added by reacting other amino groups or nitrogen atoms on the polymer with alkyl halides, epoxides or isocyanates. The polyamines can be made by a variety of methods. They can be made by a ring opening polymerization of aziridine or similar compounds. They also can be made by condensation reactions of amines such as ammonia, methylamine,

WO 2006/086189

PCT/US2006/003525

dimethylamine, ethylenediamine etc. with reactive compounds such as 1,2-dichloroethane, epichlorohydrin, epibromohydrin and similar compounds.

5 Polymers containing anhydride groups can be reacted with a variety of compounds containing $-\text{Si}(\text{OR})_3$ to make polymers suitable for use in the present invention. Suitable anhydride containing polymers include copolymers of maleic anhydride with ethylenically unsaturated monomers such as styrene, ethylene, alpha olefins such as octadecene, meth(acrylamide),
10 (meth)acrylic acid, acrylate esters such as methyl (meth)acrylate, ethyl (meth)acrylate, butyl acrylate and methylvinylether. The polymer can also be a graft copolymer such as poly(1,4-butadiene)-g-maleic anhydride or polyethylene-g-maleic anhydride and the like. Other suitable
15 anhydride monomers include, but are not limited to, itaconic and citraconic anhydrides. Suitable reactive silane compounds include, but are not limited to γ -aminopropyltriethoxysilane, bis(gamma-triethoxysilylpropyl)amine, N-phenyl-gamma aminopropyltriethoxysilane, p-aminophenyltriethoxysilane, 3-
20 (m-aminophenoxypropyl)-trimethoxysilane, and gamma-aminobutyltriethoxysilane. Other functional groups can be added to the polymer by reacting it with amines, alcohols and other compounds. In a preferred polymer for use in the present invention, maleic anhydride is the anhydride and the
25 co-monomer is styrene. A preferred silane is gamma-aminopropyltriethoxysilane. It is also advantageous to react some of the anhydride groups with another amine such as diethylamine.

The same type of amino compound containing an $-\text{Si}(\text{OR})_3$
30 group can be reacted with polymers containing a pendant isocyanate group, such as copolymers of for example, isopropenyldimethylbenzylisocyanate and vinyl isocyanate, with co-monomers including, but not limited to, vinyl acetate, styrene, acrylic acid, and acrylamide. These polymers can also
35 be reacted with other compounds such as amines to enhance performance.

WO 2006/086189

PCT/US2006/003525

Isocyanate functional compounds with an $--Si(OR'')_3$ group such as gamma-isocyanatopropyltrimethoxysilane can also be reacted with polymers containing hydroxyl groups such as hydrolyzed poly(vinyl acetate) and copolymers of vinyl acetate with other monomers. Other hydroxyl containing polymers suitable for use include, but are not limited to, polysaccharides and polymers containing N-methylolacrylamide.

In the present process, the amount of polymer added to the process stream can depend on the composition of the industrial process stream (e.g. a Kraft pulping mill process or high level nuclear waste streams liquor involved and generally all that is required is an aluminosilicate containing scale inhibiting amount thereof. In general the polymer is preferably added to the process stream in economically and practically favorable concentrations. A preferred concentration is one that is greater than about 0 ppm to about 300 ppm, more preferably in a concentration that is greater than about 0 ppm to about 50 ppm and most preferably the polymer is added to the process stream in a concentration that is greater than about 0 ppm to about 10 ppm.

The polymer can be added directly to any industrial process stream where scaling can occur, e.g. in the black liquor evaporators of the kraft pulp milling process, and in green and white liquor process streams of that process. It is preferred, however to add the polymer to a charge stream or recycle stream or liquor leading to the black liquor evaporator. While the polymer can be added to the industrial process stream at any time during the process, it is preferable to add it at any convenient point in the process before or during application of heat. Usually, the polymer is added immediately before the evaporator.

Examples

High Level Nuclear Waste

Comparative Example A

WO 2006/086189

PCT/US2006/003525

Preparation of the reaction product of styrene/maleic anhydride copolymer with butylamine (Comparative Polymer A) is as follows: 10.0 g of dry styrene/maleic anhydride copolymer (SMA), with a mole ratio of styrene to maleic anhydride of about 1.1 and M_w about 16,000, is suspended in 100 ml of toluene. A solution of 1.72 g of butylamine in 10 ml of toluene is added at ambient temperature. The mixture is refluxed for 3 hr. The solid product is filtered off, washed, and dried. This gives a polymer containing 53 mole% styrene, 24 mole% N-butyl half amide from maleic anhydride, and 23 mole% maleic anhydride.

Comparative Example B

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Preparation of the reaction product of SMA with tallow amine and diethylamine (Comparative Polymer B) is as follows: 100.0 g of dry SMA, with a mole ratio of styrene to maleic anhydride of about 1.1 and M_w about 16,000, is suspended in 941.7 g of toluene. A solution of 25.2 g tallow amine and 27.5 g diethylamine in 35.2 g toluene is added at ambient temperature and the mixture is then refluxed for 30 min. The resulting toluene slurry is cooled to room temperature and then added with mixing to about 700 ml of 2% aqueous caustic. The toluene layer is separated and the residual toluene in the aqueous phase is removed by distillation. The aqueous solution is further purified by ultrafiltration using a 0.2 μm hydrophilic polyethersulfone filter and then freeze dried to obtain the dry polymer. This gives a polymer containing 53 mole% styrene, 38 mole% N-diethyl half amide from maleic anhydride, and 9 mole% N-tallow half amide from maleic anhydride.

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Comparative Example C

WO 2006/086189

PCT/US2006/003525

Preparation of a copolymer of N-tert-octylacrylamide and acrylic acid (Comparative Polymer C) is as follows: 2.81 g Acrylic acid, 2.52 g N-tert-octylacrylamide, and 0.14 g 2-mercaptoethanol are dissolved in 12.5 g DMF and 13.87 g dioxane and purged with nitrogen. The mixture is heated to 75° C and 0.16 g 2,2'-azobis(2,4-dimethylvaleronitrile) in 3 g dioxane is added. After 6 hr at 75° C, the mixture is cooled, giving the desired polymer in solution. This gives a polymer containing 73.7 mole% acrylic acid and 26.3 mole% N-tert-octylacrylamide.

Example 1 - Polymer i

Preparation of the reaction product of SMA with butylamine and (3-aminopropyl)triethoxysilane to give a polymer with 1 mole% silane containing monomer units (Polymer i) is as follows: 10.0 g of dry SMA, with a mole ratio of styrene to maleic anhydride of about 1.0 and M_w about 16,000, is suspended in 100 ml of toluene. A solution of 1.72 g of butylamine and 0.21 g of (3-aminopropyl)triethoxysilane in 10 ml of toluene is added at ambient temperature. The mixture is refluxed for 3 hr. The solid product is filtered off, washed, and dried. This gives a polymer containing 53 mole% styrene, 23.9 mole% N-butyl half amide from maleic anhydride, 1 mole% N-(3-triethoxysilyl)propyl half amide from maleic anhydride, and 22.1 mole% maleic anhydride.

Example 2 - Polymer ii

Preparation of the reaction product of SMA with butylamine and (3-aminopropyl)triethoxysilane to give a polymer with 3.8 mole% silane containing monomer units (Polymer ii) is as follows: 10.0 g of dry SMA, with a mole ratio of styrene to maleic anhydride of about 1.1 and M_w about 16,000, is suspended in 100 ml of toluene. A solution of 1.72 g of butylamine and 0.83 g of (3-aminopropyl)triethoxysilane

WO 2006/086189

PCT/US2006/003525

in 10 ml of toluene is added at ambient temperature. The mixture is refluxed for 3 hr. The solid product is filtered off, washed, and dried. This gives a polymer containing 53 mole% styrene, 23.9 mole% N-butyl half amide from maleic anhydride, 3.8 mole% N-(3-triethoxysilyl)propyl half amide from maleic anhydride, and 19.3 mole% maleic anhydride.

Example 3 - Polymer iii

Preparation of the reaction product of SMA with butylamine and (3-aminopropyl)triethoxysilane to give a polymer with 7.6 mole% silane containing monomer units (Polymer iii) is as follows: 10.0 g of dry SMA, with a mole ratio of styrene to maleic anhydride of about 1.1 and M_w about 16,000, is suspended in 100 ml of toluene. A solution of 1.72 g of butylamine and 1.66 g of (3-aminopropyl)triethoxysilane in 10 ml of toluene is added at ambient temperature. The mixture is refluxed for 3 hr. The solid product is filtered off, washed, and dried. This gives a polymer containing 53 mole% styrene, 23.9 mole% N-butyl half amide from maleic anhydride, 7.6 mole% N-(3-triethoxysilyl)propyl half amide from maleic anhydride, and 15.5 mole% maleic anhydride.

Example 4 - Polymer iv

Preparation of the reaction product of SMA with tallow amine, diethylamine, and (3-aminopropyl)triethoxysilane to give a polymer with 3.8 mole% silane containing monomer units (Polymer iv) is as follows: 100.0 g of dry SMA, with a mole ratio of styrene to maleic anhydride of about 1.1 and M_w about 16,000, is suspended in 941.7 g of toluene. A solution of 25.2 g tallow amine, 24.8 g diethylamine, and 8.3 g (3-aminopropyl)triethoxysilane in 38.9 g toluene is added at ambient temperature and the mixture is then refluxed for 30 min. The resulting toluene slurry is cooled to room temperature and then added with mixing to about 700 ml of 2%

WO 2006/086189

PCT/US2006/003525

aqueous caustic. The toluene layer is separated and the residual toluene in the aqueous phase is removed by distillation. The aqueous solution is further purified by ultrafiltration using a 0.2 μ m hydrophilic polyethersulfone filter and then freeze dried to obtain the dry polymer. This gives a polymer containing 53 mole% styrene, 3.8 mole% N-(3-triethoxysilyl)propyl half amide from maleic anhydride, 9.4 mole% N-tallow half amide of maleic anhydride, and 33.8 mole% N,N-diethyl half amide of maleic anhydride.

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Example 5 - Polymer v

Preparation of the reaction product of SMA with tallow amine, diethylamine, and (3-aminopropyl)triethoxysilane to give a polymer with 7.5 mole% silane containing monomer units (Polymer v) is as follows: 100.0 g of dry SMA, with a mole ratio of styrene to maleic anhydride of about 1.1 and M_w about 16,000, is suspended in 941.7 g of toluene. A solution of 20.2 g tallow amine, 23.4 g diethylamine, and 16.7 g (3-aminopropyl)triethoxysilane in 40.2 g toluene is added at ambient temperature and the mixture is then refluxed for 30 min. The resulting toluene slurry is cooled to room temperature and then added with mixing to about 700 ml of 2% aqueous caustic. The toluene layer is separated and the residual toluene in the aqueous phase is removed by distillation. The aqueous solution is further purified by ultrafiltration using a 0.2 μ m hydrophilic polyethersulfone filter and then freeze dried to obtain the dry polymer. This gives a polymer containing 53 mole% styrene, 7.5 mole% N-(3-triethoxysilyl)propyl half amide from maleic anhydride, 7.5 mole% N-tallow half amide of maleic anhydride, and 30 mole% N,N-diethyl half amide of maleic anhydride.

35 Example 6 - Polymer vi

WO 2006/086189

PCT/US2006/003525

Preparation of the reaction product of SMA with tallow amine, diethylamine, and (3-aminopropyl)triethoxysilane to give a polymer with 3.8 mole% silane containing monomer units (Polymer vi) is as follows: 100.0 g of dry SMA, with a mole ratio of styrene to maleic anhydride of about 1.1 and M_w about 16,000, is suspended in 941.7 g of toluene. A solution of 10.1 g tallow amine, 28.9 g diethylamine, and 8.3 g (3-aminopropyl)triethoxysilane in 31.3 g toluene is added at ambient temperature and the mixture is then refluxed for 30 min. The resulting toluene slurry is cooled to room temperature and then added with mixing to about 700 ml of 2% aqueous caustic. The toluene layer is separated and the residual toluene in the aqueous phase is removed by distillation. The aqueous solution is further purified by ultrafiltration using a 0.2 μ m hydrophilic polyethersulfone filter and then freeze dried to obtain the dry polymer. This gives a polymer containing 53 mole% styrene, 3.8 mole% N-(3-triethoxysilyl)propyl half amide from maleic anhydride, 3.8 mole% N-tallow half amide of maleic anhydride, and 39.4 mole% N,N-diethyl half amide of maleic anhydride.

Example 7

Preparation of N-(3-triethoxysilyl)propylacrylamide (TESPA) is as follows: 197.4 g of (3-aminopropyl)triethoxysilane and 89.9 g of triethylamine are dissolved in 330 g THF, purged with nitrogen, and cooled to 0° C. With mixing, 83.9 g of acryloyl chloride is added dropwise, and after the addition the mixture is heated to 40° C for 2 hr. The mixture is cooled to room temperature and the salt filtered out. The resulting solution of TESP (42% in THF) is used as is without further purification.

Example 8 - Polymer vii

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WO 2006/086189

PCT/US2006/003525

Preparation of the tetrapolymer of N-tert-octylacrylamide, acrylic acid, 1-vinyl-2-pyrrolidinone, and TESPAs to give a polymer containing 5 mole% silane containing monomer units (Polymer vii) is as follows: 1.89 g of 1-Vinyl-2-pyrrolidinone, 0.66 g acrylic acid, 2.21 g N-tert-octylacrylamide, 1.30 g TESPAs (42% in THF), and 0.14 g 2-mercaptoethanol are dissolved in 14 g DMF and 11.64 g dioxane and purged with nitrogen. The mixture is heated to 75° C and 0.16 g 2,2'-azobis(2,4-dimethylvaleronitrile) in 3 g dioxane is added. After 6 hr at 75° C, the mixture is cooled, giving the desired polymer in solution. The polymer is further purified by precipitation with isopropyl alcohol, washed, and dried. This gives a polymer containing 42.5 mole% 1-vinyl-2-pyrrolidinone, 22.5 mole% acrylic acid, 5 mole% TESPAs, and 30 mole% N-tert-octylacrylamide.

Example 9 - Polymer viii

Preparation of the copolymer of 1-vinyl-2-pyrrolidinone and TESPAs to give a polymer containing 5 mole% silane containing monomer units (Polymer viii) is as follows: 4.69 g of 1-Vinyl-2-pyrrolidinone, 1.44 g TESPAs (42% in THF), and 0.14 g 2-mercaptoethanol are dissolved in 12.5 g DMF and 13.07 g dioxane and purged with nitrogen. The mixture is heated to 75° C and 0.16 g 2,2'-azobis(2,4-dimethylvaleronitrile) in 3 g dioxane is added. After 6 hr at 75° C, the mixture is cooled, giving the desired polymer in solution with 15% concentration. This gives a polymer containing 95 mole% 1-vinyl-2-pyrrolidinone and 5 mole% TESPAs.

Example 10 - Polymer ix

Preparation of the terpolymer of N-tert-octylacrylamide, acrylic acid, and TESPAs to give a polymer containing 5 mole% silane containing monomer units (Polymer ix) is as follows: 2.46 g Acrylic acid, 2.21 g N-tert-octylacrylamide, 1.56 g

WO 2006/086189

PCT/US2006/003525

TESPA (42% in THF), and 0.14 g 2-mercaptoethanol are dissolved in 12.5 g DMF and 12.97 g dioxane and purged with nitrogen. The mixture is heated to 75° C and 0.16 g 2,2'-azobis(2,4-dimethylvaleronitrile) in 3 g dioxane is added. After 6 hr at 75° C, the mixture is cooled, giving the desired polymer in solution with 15% concentration. This gives a polymer containing 70 mole% acrylic acid, 5 mole% TESP, and 25 mole% N-tert-octylacrylamide.

Example 11 - Polymer x

Preparation of the reaction product of polyethylene oxide with 3-glycidoxypropyltrimethoxysilane to give a polymer containing 2.2 mole% silane containing monomer units (Polymer x) is as follows: 20.0 g of polyethyleneoxide (M_n about 2000) is dissolved in 10.0 g DMSO and purged with nitrogen. To this mixture is added 2.63 g 3-glycidoxypropyltrimethoxysilane, followed by 1.36 g of 45% KOH. The resulting mixture is heated to 80° C for 1 hr, giving the desired polymer in solution with 65.8% concentration. This gives a polymer containing about 97.8 mole% ethylene oxide and 2.2 mole% 3-glycidoxypropyltrimethoxysilane.

Example 12 - Polymer xi

Preparation of the reaction product of poly(ethylene glycol)-block-poly(propylene glycol)-block-poly(ethylene glycol) with 3-glycidoxypropyltrimethoxysilane to give a polymer containing 3.1 mole% silane containing monomer units (Polymer xi) is as follows: 30.0 g of poly(ethylene glycol)-block-poly(propylene glycol)-block-poly(ethylene glycol) (with 50 wt% ethylene oxide and M_n about 1900) is mixed with 4.52 g 3-glycidoxypropyltrimethoxysilane under nitrogen. 2.34 g 45% KOH is added and the resulting mixture heated to 80° C for 1 hr, giving the desired polymer with 92.6% concentration. This gives a polymer containing about 55.1 mole% ethylene oxide,

WO 2006/086189

PCT/US2006/003525

41.8 mole% propylene oxide, and 3.1 mole% 3-glycidoxypropyltrimethoxysilane.

Example 13 - Polymer xii

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Preparation of the reaction product of poly(ethylene glycol)-block-poly(propylene glycol)-block-poly(ethylene glycol) with 3-glycidoxypropyltrimethoxysilane to give a polymer containing 3.0 mole% silane containing monomer units (Polymer xii) is as follows: 30.0 g of poly(ethylene glycol)-block-poly(propylene glycol)-block-poly(ethylene glycol) (with 10 wt% ethylene oxide and M_n about 2000) is mixed with 4.3 g 3-glycidoxypropyltrimethoxysilane under nitrogen. 2.22 g 45% KOH is added and the resulting mixture heated to 80° C for 1 hr, giving the desired polymer with 92.9% concentration. This gives a polymer containing about 12.3 mole% ethylene oxide, 84.7 mole% propylene oxide, and 3.0 mole% 3-glycidoxypropyltrimethoxysilane.

20 Example 14 - Polymer xiii

Preparation of the reaction product of polyethylenimine with 3-glycidoxypropyltrimethoxysilane to give a polymer containing 0.5 mole% silane containing monomer units (Polymer xiii) is as follows: 25.4 g Polyethylenimine (M_w about 25,000) is mixed with 0.7 g 3-glycidoxypropyltrimethoxysilane, and the resulting mixture is heated at 70° C for 16 hr, giving the desired polymer as a soft friable gel.

30 Example 15 - Polymer xiv

Preparation of the reaction product of polyethylenimine with 3-glycidoxypropyltrimethoxysilane to give a polymer containing 1.0 mole% silane containing monomer units (Polymer xiv) is as follows: 25.72 g Polyethylenimine (M_w about 25,000) is mixed with 1.43 g 3-glycidoxypropyltrimethoxysilane, and

WO 2006/086189

PCT/US2006/003525

the resulting mixture is heated at 70° C for 16 hr, giving the desired polymer as a soft friable gel.

Example 16 - Polymer xv

5

Preparation of the reaction product of polyethylenimine with 3-glycidoxypropyltrimethoxysilane to give a polymer containing 2.0 mole% silane containing monomer units (Polymer xv) is as follows: 11.39 g Polyethylenimine (M_w about 25,000) is mixed with 1.28 g 3-glycidoxypropyltrimethoxysilane, and the resulting mixture is heated at 70° C for 16 hr, giving the desired polymer as a soft friable gel.

Example 17 - Polymer xvi

15

Preparation of the reaction product of polyethylenimine with 3-glycidoxypropyltrimethoxysilane to give a polymer containing 4.0 mole% silane containing monomer units (Polymer xvi) is as follows: 10.0 g Polyethylenimine (M_w about 25,000) is mixed with 2.29 g 3-glycidoxypropyltrimethoxysilane, and the resulting mixture is heated at 70° C for 16 hr, giving the desired polymer as a soft friable gel.

Example 18 - Polymer xvii

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Preparation of the reaction product of hydroxyethyl cellulose with 3-glycidoxypropyltrimethoxysilane to give a polymer containing a high (~30 mole%) silane containing monomer units (Polymer xvii) is as follows: 8.0 g dry hydroxyethyl cellulose (molecular weight 24,000-27,000) is mixed with 2.0 g 3-glycidoxypropyltrimethoxysilane in 5 g acetone. The acetone is removed by evaporation and the resulting mixture heated at 100° C for 16 hr, giving the desired polymer.

35 Table 1 Summary of Polymers Used in Scale Inhibition Testing

WO 2006/086189

PCT/US2006/003525

Example	Polymer	Composition	Mole% Silane*
Comparative A	Comparative A	Reaction product of SMA with butylamine	0
Comparative B	Comparative B	Reaction product of SMA with tallow amine and diethylamine	0
Comparative C	Comparative C	Copolymer of N-tert-octylamide and acrylic acid	0
	Comparative D	Polyethylenimine (M_w ~25,000) obtained from Aldrich	0
	Comparative E	Polyvinylpyrrolidone (M_w ~10,000) from Aldrich	0
1	i	Reaction product of SMA with butylamine and (3- aminopropyl)triethoxysilane	1
2	ii	reaction product of SMA with butylamine and (3- aminopropyl)triethoxysilane	3.8
3	iii	reaction product of SMA with butylamine and (3- aminopropyl)triethoxysilane	7.6
4	iv	Reaction product of SMA with tallow amine, diethylamine, and (3-aminopropyl)triethoxysilane	3.8
5	v	reaction product of SMA with tallow amine, diethylamine, and (3-aminopropyl)triethoxysilane	7.5
6	vi	reaction product of SMA with tallow amine, diethylamine, and (3-aminopropyl)triethoxysilane	3.8
7	vii	tetrapolymer of N-tert- octylacrylamide, acrylic acid, 1-vinyl-2-pyrrolidinone, and TESPA	5
8	viii	copolymer of 1-vinyl-2- pyrrolidinone and TESP	5
9	ix	terpolymer of N-tert- octylacrylamide, acrylic acid, and TESP	5
10	x	reaction product of polyethylene oxide with 3- glycidoxypropyltrimethoxysilane	2.2
11	xi	reaction product of poly(ethylene glycol)-block- poly(propylene glycol)-block- poly(ethylene glycol) with 3- glycidoxypropyltrimethoxysilane	3.1
12	xii	reaction product of poly(ethylene glycol)-block- poly(propylene glycol)-block- poly(ethylene glycol) with 3- glycidoxypropyltrimethoxysilane	3.0
13	xiii	reaction product of	0.5

WO 2006/086189

PCT/US2006/003525

		polyethylenimine with 3-glycidoxypropyltrimethoxysilane	
14	xiv	reaction product of polyethylenimine with 3-glycidoxypropyltrimethoxysilane	1
15	xv	reaction product of polyethylenimine with 3-glycidoxypropyltrimethoxysilane	2
16	xvi	the reaction product of polyethylenimine with 3-glycidoxypropyltrimethoxysilane	4
17	xvii	the reaction product of hydroxyethyl cellulose with 3-glycidoxypropyltrimethoxysilane	-30

*Mole% of monomer units in the polymer containing the silane functional group.

5 Example 19

Test Procedure

10 A synthetic high level nuclear waste liquor is made by adding sodium carbonate, sodium sulfate, sodium hydroxide, sodium aluminate solution (made by digesting alumina trihydrate in caustic), sodium silicate, sodium nitrate, and sodium nitrite to deionized water. The final composition of the liquor is shown in Table 2

15

Table 2

Species	Concentration (mole/l)
NaOH	4.5
NaNO ₃	1.0
NaNO ₂	1.0
Na ₂ CO ₃	0.25
Na ₂ SO ₄	0.25
Alumina Trihydrate	0.5
SiO ₂	0.01

20 All of the polymer samples are dissolved in 2% aqueous NaOH prior to addition to the nuclear waste liquor, hydrolyzing any anhydride and trialkoxysilane groups that have not previously been reacted, transforming the trialkoxysilane groups into silanol groups or the sodium

WO 2006/086189

PCT/US2006/003525

salts. Into a 125 ml polyethylene bottle, are placed the scale reducing additive (if used) as a 0.5% solution in 2% aqueous NaOH for the lower doses and for the higher doses a 3% solution is used. 120 ml of the above stock synthetic high level nuclear waste solution is then added to the bottle with mixing. The sealed bottle is heated with agitation at 102° C for 18±2 hours. Up to 24 such tests (bottles) are done at one time. At the end of the 18 hours, the bottles are opened and the solution is filtered (0.45 µm filter). Considerable aluminosilicate scale is observed to form as loose aluminosilicate in the liquor (which may have initially formed on the polyethylene surfaces). In the examples below, the weight of scale formed in the test is expressed as a percentage of the average weight of scale that formed on two comparative blank tests (i.e. no additive used) that are part of the same set of tests.

Using the test procedure outlined above, a series of SMA type polymers reacted with butylamine and containing varying amounts of silane are examined for aluminosilicate scale inhibition activity and the results are reported in Table 3.

Table 3

Polymer	Mole% Silane	Dosage, mg/l	Total Scale Formed, % vs. Blank
Comparative A	0	10	104.4
Comparative A	0	50	103.9
i	1	10	69.4
i	1	50	72.6
ii	3.8	10	63.3
ii	3.8	50	37.1
iii	7.6	10	5.2
iii	7.6	50	1.0

Example 20

Using the test procedure as outlined in Example 19, a series of SMA polymers reacted with tallow amine and

WO 2006/086189

PCT/US2006/003525

diethylamine and containing varying amounts of silane are examined for scale inhibition activity and the results are reported in Table 4.

5 Table 4

Polymer	Mole% Silane	Dosage, mg/l	Total Scale Formed, % vs. Blank
Comparative B	0	10	87.4
Comparative B	0	50	95.8
iv	3.8	10	59.2
iv	3.8	50	54.9
v	7.5	10	2.8
v	7.5	50	0
vi	3.8	10	49.6
vi	3.8	50	66.8

Example 21

- 10 Using the test procedure as outlined in Example 19, a series of polymers made with the silane containing monomer TESPA are examined for scale inhibition activity and the results are reported in Table 5.

15 Table 5

Polymer	Mole% Silane	Dosage, mg/l	Total Scale Formed, % vs. Blank
Comparative C	0	10	102.8
Comparative C	0	50	104.2
Comparative E	0	10	93.5
Comparative E	0	50	101.2
vii	5	10	3.1
vii	5	50	2.9
viii	5	10	1.6
viii	5	50	2.7
ix	5	10	2.7
ix	5	50	1.1

Example 22

WO 2006/086189

PCT/US2006/003525

Using the test procedure as outlined in Example 19, a series of polyether type polymers containing varying amounts of silane are examined for scale inhibition activity and the results are reported in Table 6.

5

Table 6

Polymer	Mole% Silane	Dosage, mg/l	Total Scale Formed, % vs. Blank
x	2.2	10	68.0
x	2.2	50	6.2
x	2.2	300	2.2
xi	3.1	10	21.0
xi	3.1	50	1.0
xi	3.1	300	1.9
xii	3.0	10	23.3
xii	3.0	50	6.2
xii	3.0	300	0.7

Example 23

10

Using the test procedure as outlined in Example 19, a series of polyethylenimine type polymers containing varying amounts of silane are examined for scale inhibition activity and the results are reported in Table 7.

15

Table 7

Polymer	Mole% Silane	Dosage, mg/l	Total Scale Formed, % vs. Blank
Comparative D	0	10	102.0
Comparative D	0	50	105.5
Comparative D	0	300	112.8
xiii	0.5	10	43.3
xiii	0.5	50	1.6
xiii	0.5	300	0
xiv	1	10	4.2
xiv	1	50	0
xiv	1	300	0.1
xv	2	10	0
xv	2	50	0
xv	2	300	0
xvi	4	10	0
xvi	4	50	0

WO 2006/086189

PCT/US2006/003525

xvi	4	300	0
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Example 24

Using the test procedure as outlined in Example 19, a
 5 hydroxyethyl cellulose derivative containing silane is
 examined for scale inhibition activity and the results are
 reported in Table 8.

Table 8

10

Polymer	Mole% Silane	Dosage, mg/l	Total Scale Formed, % vs. Blank
xvii	~30	10	17.5
xvii	~30	50	3.0
xvii	~30	300	16.9

Kraft pulp mill scale inhibition testing

15 Example 25

In order to simulate the conditions found in a typical
 kraft pulp mill black liquor a synthetic process liquor
 simulating a typical black liquor is prepared in the following
 20 way.

A basic aluminate solution is prepared according to the
 recipe below by adding the aluminate and NaOH solution to the
 water and stirring overnight. The solution is then filtered
 25 through a 3- μ m filter membrane (Pall Versapor-3000 T w/wa, 47
 mm) :

	Na ₂ O.Al ₂ O ₃ .3 H ₂ O	100.0 g
	50% NaOH	146.6 g
30	Deionized water	753.4 g

	Total	1000.0 g

This basic aluminate solution is used to prepare a
 35 simulated kraft black liquor solution according to the recipe
 and procedure below. Sodium acetate is added to achieve the

WO 2006/086189

PCT/US2006/003525

desired sodium ion concentration. Amounts are in grams and percentages are w/w unless otherwise indicated.

	Sodium carbonate	121.9
5	Sodium sulfate	32.7
	Sodium thiosulfate	36.4
	Sodium hydrosulfide, 60%	70.9
	Sodium acetate	445.3
	50% sodium hydroxide	290.7
10	29.55% SiO ₂	14.0
	Basic aluminate solution	25.1
	Deionized water	1746

15	Total	2783 g = 2.30 liter

Calculated concentration:

	[CO ₃ ²⁻] = 0.5 M
	[SO ₄ ²⁻] = 0.1 M
	[S ₂ O ₃ ²⁻] = 0.1 M
20	[SH ⁻] = 0.33 M
	[Na ⁺] = 5.7 M
	[OH ⁻] = 1.6 M
	[Si] = 0.03 M
25	[Al] = 0.01 M

The solution is prepared by adding the sodium carbonate, sodium sulfate, sodium thiosulfate, sodium hydrosulfide, and sodium acetate to the water with rapid stirring. After 30 min stirring, the solution is filtered through a coarse glass frit to remove minor amounts of insoluble material. The sodium hydroxide solution, silica solution, and finally basic aluminate solution is added, with stirring after each addition. The solution is used immediately as described below.

For each of Examples 26 to 33, respective polymer solutions of polymers iii (Example 3), v (Example 5), vii (Example 8), viii (Example 9), x (Example 11), xi (Example 12), xvi (Example 17) and xvii (Example 18) are pre-diluted to 1% (w/w) active concentration in 2% NaOH solution prior to use.

The amount of 1.45 g of a polymer solution, (or 1.45 g of water for the control test), is added to a labeled 4-oz HDPE wide-mouth jar. Then 145 g (120 ml) of simulated kraft black liquor solution is added to each jar before capping and shaking. Each jar then contained a "test solution". The polymer dose is 100 ppm.

WO 2006/086189

PCT/US2006/003525

The caps on the jars are then loosened so as to be able to relieve pressure, and the jars placed on the floor of a 102 °C oven to simulate heating in a kraft process liquor. After 1.5 hr the caps are tightened and the jars placed on a rotisserie placed inside the oven. After turning on the rotisserie in the oven overnight (16.5 hr), each sample is filtered using a pre-weighed 3-µm filter membrane (Pall Versapor-3000 T w/wa, 47 mm). Each membrane plus any collected solid is washed with about 5-ml water and placed on a 2.5-inch diameter watch glass. A steel tray containing all the watch glasses and membranes is placed in a 102 °C oven for 30 min to dry the filtered solids. Each membrane plus solid is weighed and the weight of the solid calculated by difference. % Scale inhibition is then calculated in the following manner:

% Scale inhibition =

$$100 \times \frac{\text{Weight of scale formed with polymer present}}{\text{Weight of scale formed with polymer absent}}$$

The results of testing polymers in examples 26-33 at 100 ppm are shown in Table 9.

Table 9.

Example	Polymer	% Scale Reduction
26	iii	10.3
27	v	27.5
28	vii	98.0
29	viii	65.1
30	x	96.1
31	xi	96.5
32	xvi	6.2
33	xvii	28.7

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CLAIMS:

1. A composition for reducing aluminosilicate scale in an industrial process comprising a polymer which is the reaction product of poly(ethylene glycol)-block-poly(propylene glycol)-
5 block-poly(ethylene) with 3-glycydoxypropyltrimethoxysilane.
2. A composition for reducing aluminosilicate scale in an industrial process comprising a polymer which is the reaction product of polyethyleneimine with 3-glycydoxypropyltrimethoxysilane.