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(54) Title: HIGH MOLECULAR WEIGHT PERFLUOROCYCLOBUTANE POLYMERS AND METHOD OF MAKING

(57) Abstract: This invention relates to high molecular weight perfluorocyclobutane polymers and methods of polymerizing trifluorovinyl monomers to form high molecular weight perfluorocyclobutane polymers in the presence of a catalyst or initiator.

**High Molecular Weight Perfluorocyclobutane Polymers  
and Method of Making**

**Technical Field**

This invention relates to high molecular weight perfluorocyclobutane polymers and methods of polymerizing trifluorovinyl monomers to form such polymers in the presence of a catalyst or initiator.

**Background**

A number of references disclose the thermal polymerization of trifluorovinyl-containing monomers, typically bis-trifluorovinyl monomers, to form perfluorocyclobutylene polymers, including U.S. Patents Nos. 5,037,917, 5,159,038, 5,364,917, 5,066,746, 5,159,037, 5,023,380, 5,162,468, 5,037,919, 5,198,513, 5,021,602, 5,210,265, 5,037,918, 5,159,036, 5,246,782, 5,409,777, and 5,364,547, the teachings of which are incorporated herein by reference. Disclosed reaction conditions involve heating monomers to temperatures of typically about 150-210°C for several hours. The resulting polymers "preferably have a molecular weight of from about 300 to about 30,000." (5,037,917 at col. 2, ln. 38).

U.S. Pat. Nos. 5,037,918 and 5,159,036 disclose the use of "crosslinking initiating means" on perfluorocyclobutane polymers, subsequent to a completed step of polymerization, to obtain crosslinked polymer gels. Such crosslinking is further described in co-owned U.S. Pat. No. 5,246,782, at col. 3 ln 48 – col. 4, ln. 28 and at col. 11, lns. 11-31.

**Disclosure of Invention**

Briefly, the present invention provides high molecular weight perfluorocyclobutane polymers and methods of polymerizing trifluorovinyl containing

monomers to form high molecular weight perfluorocyclobutane polymers in the presence of a catalyst or initiator.

In this document:

“C(number)” refers to a chemical moiety containing the indicated number of 5 carbon atoms; and

“substituted” when used without reference to a particular substituent, means substituted by conventional substituents which do not interfere with the desired product or process, *e.g.*, substituents can be alkyl, alkoxy, aryl, phenyl, halo (F, Cl, Br, I), cyano, nitro, etc.

10

### Detailed Description

The present invention provides high molecular weight perfluorocyclobutane polymers and methods of polymerizing trifluorovinyl containing monomers to form high molecular weight perfluorocyclobutane polymers in the presence of a catalyst or 15 initiator.

Monomers useful in the method of the present invention contain two or more polymerizable trifluorovinyl groups. Monomers are preferably of the formula  $\text{CF}_2=\text{CF}-\text{X}-\text{R}^1-\text{X}-\text{CF}=\text{CF}_2$ , where each  $-\text{X}-$  is independently selected from the group consisting of:  $-\text{O}-$ ,  $-\text{S}-$ ,  $-\text{SO}-$ ,  $-\text{SO}_2-$ ,  $-\text{CO}-$ ,  $-\text{NH}-$ , and  $-\text{NR}^2-$ , wherein  $\text{R}^2$  is C1-C25 20 substituted or unsubstituted, saturated or unsaturated alkyl or aryl and  $\text{R}^1$  is a substituted or unsubstituted C1-C30 aryl or alkyl moiety which may additionally comprise heteroatoms. Preferably X is oxygen. Preferably,  $\text{R}^1$  is a C1-C16 aryl or alkyl moiety. Suitable monomers disclosed in the background references cited above may be used. Mixtures of monomers may additionally be used. PCFB oligomers or 25 lower molecular weight PFCB polymers can also be used in place of or along with monomers to produce higher molecular weight polymers according to the present invention. Monomers containing three or more polymerizable trifluorovinyl groups may be added to create branch points.

We have found that the use of initiators or catalysts can result in a higher 30 molecular weight polymer. Preferred initiators or catalysts include salts comprising

fluorine-containing anions, more preferably anions selected from F<sup>-</sup>, BF<sub>4</sub><sup>-</sup>, PF<sub>6</sub><sup>-</sup> and

SbF<sub>6</sub><sup>-</sup>, more preferably F<sup>-</sup> or PF<sub>6</sub><sup>-</sup> and most preferably PF<sub>6</sub><sup>-</sup>. Useful initiators or

catalysts include alkylammonium, alkylsulfonium or alkylphosphonium salts and salts  
of organometallic complex cations. Preferred initiators or catalysts include

5 alkylammonium salts. Most-preferred initiators or catalysts include (alkyl)<sub>4</sub>N<sup>+</sup>PF<sub>6</sub><sup>-</sup>,  
wherein the alkyl group is a C1-C8 alkyl group, including (CH<sub>3</sub>)<sub>4</sub>N<sup>+</sup>PF<sub>6</sub><sup>-</sup> and (n-  
C<sub>3</sub>H<sub>7</sub>)<sub>4</sub>N<sup>+</sup>PF<sub>6</sub><sup>-</sup> (available from Aldrich Chemical Co., Milwaukee, WI). Without  
wishing to be bound by theory, it is believed that preferred initiators or catalysts include  
fluoride generators.

10 Polymerization involves joining trifluorovinyl groups of different monomer  
molecules to form linking perfluorocyclobutylene (PFCB) groups. Any suitable  
reaction conditions and equipment may be used, including batch or continuous  
processes. Suitable conditions and equipment disclosed in the background references  
cited above may be used. In addition, the present method has the advantage of allowing  
15 the use of lower reaction temperatures.

In the present method, the initiator or catalyst is preferably added to the reaction  
mixture (comprising monomers, oligomers, or combinations thereof) prior to heating  
the reaction mixture to reaction temperature or after the reaction mixture reaches  
reaction temperature, during polymerization. The initiator or catalyst is preferably

20 added to the reaction mixture before it reaches reaction temperature or more preferably  
before heating. Reaction temperature may be between 100 and 300°C but is more  
typically between 120 and 250°C and preferably 150-200°C. Reaction time is typically  
1-24 hours. Solvent may be added. Addition of solvent may improve the activity of the  
initiator or catalyst by solvating initiator or catalyst.

25 Crosslinkers or branching agents containing three or more reactive trifluorovinyl  
groups may be added. Exemplary agents include tris(trifluorovinyloxyaryl)alkanes such  
as 1,1,1-tris(4'-trifluorovinyloxyphenyl)ethane and others cited in U.S. Patent Nos.  
5,037,918 and 5,159,036, incorporated herein by reference. Preferably the polymer  
according to the present invention is not crosslinked after polymerization and no  
30 crosslinking step is carried out after polymerization.

The resulting polymers have typical weight average molecular weights of two to eight or more times higher than the same polymerization performed without added initiator or catalyst. For comparison, polymers made under typical conditions of about 200°C for about 72 hours demonstrate typical weight average molecular weights of 5 about 60,000. Preferably polymers of the present invention (made without added crosslinking or branching agents) have a weight average molecular weight (Mw) of 100,000 or greater, more preferably 130,000 or greater, more preferably 160,000 or greater, and most preferably 190,000 or greater.

This invention is useful in the manufacture of high molecular weight PFCB 10 polymers.

Objects and advantages of this invention are further illustrated by the following examples. The particular materials and amounts thereof recited in these examples, as well as other conditions and details, should not be construed to unduly limit this invention.

15

### Examples

In the examples, all parts, ratios and percentages are by weight unless otherwise indicated. Unless otherwise noted, all chemicals and reagents were obtained or may be available from Aldrich Chemical Co., Milwaukee, WI.

20

#### **Example 1C (Comparative)**

4,4'-bis(trifluorovinyloxy)(described in U.S. Patent No. 5,037,917, Example 1.)("Monomer A") was added to a covered, glass interior, controlled-temperature reactor, heated to 200°C and maintained at that temperature for 72 hours under nitrogen 25 atmosphere. The polymer was extracted with THF and precipitated in methanol. The yield was approximately 95 weight percent (wt %). The resulting perfluorocyclobutane (PFCB) arylether polymer had weight average molecular weight (Mw) of 58,000 as measured by GPC in THF solvent using a polystyrene standard.

**Example 2**

A thermally-controlled vessel was charged with 90 wt % of Monomer A and 10 wt % of (n-propyl)<sub>4</sub>NPF<sub>6</sub> (available from Aldrich Chemical Co., Milwaukee, WI).

5 The vessel was brought to 180°C and maintained at that temperature for 16 hours under nitrogen atmosphere. The polymer was extracted with THF and precipitated in methanol. The yield was again approximately 95 weight percent (wt %). The resulting PFCB arylether polymer had a Mw of 190,000 and a mono-modal molecular weight distribution.

10

**Example 3**

The procedure of Example 2 was repeated at a higher reaction temperature of 200°C. The resulting polymer was swellable but mostly insoluble in THF. When the polymer was extracted with THF and precipitated in methanol, a fraction of less than 5 wt % of the total polymer was recovered having a Mw of approximately 190,000.

15

Thus it is concluded that the remainder of the polymer had a Mw of greater than 190,000.

**Example 4**

The procedure of Example 2 was repeated, replacing (n-propyl)<sub>4</sub>NPF<sub>6</sub> with 20 (methyl)<sub>4</sub>NPF<sub>6</sub> (available from Aldrich Chemical Co., Milwaukee, WI). The polymer was extracted with THF and precipitated in methanol. The yield of PFCB arylether polymer was again approximately 95 weight percent (wt %). The polymer had a Mw of 180,000 and a mono-modal molecular weight distribution.

25

**Example 5C (Comparative)**

A thermally-controlled vessel was charged with Monomer A and brought to 118°C and maintained at that temperature for 16 hours under nitrogen atmosphere. The polymer was extracted with THF and precipitated in methanol. The yield was again approximately 95 weight percent (wt %). The resulting PFCB arylether polymer had a 30 Mw of 2,000 and a mono-modal molecular weight distribution.

**Example 6**

A thermally-controlled vessel was charged with 95 wt % of Monomer A and 5 wt % of  $[\text{Ir}(\text{cyclooctadiene})(\text{triphenylphosphine})_2]\text{PF}_6$ . The vessel was brought to 118°C and maintained at that temperature for 16 hours under nitrogen atmosphere. The polymer was extracted with THF and precipitated in methanol. The yield was again approximately 95 weight percent (wt %). The resulting PFCB arylether polymer had a Mw of 16,300 and a mono-modal molecular weight distribution.

**Example 7C (Comparative)**

10 A thermally-controlled vessel was charged with Monomer A and brought to 160°C and maintained at that temperature for 16 hours under nitrogen atmosphere. The polymer was extracted with THF and precipitated in methanol. The yield was again approximately 95 weight percent (wt %). The resulting PFCB arylether polymer had a Mw of 14,700 and a mono-modal molecular weight distribution.

15

**Example 8**

A thermally-controlled vessel was charged with 95 wt % of Monomer A and 5 wt % of  $(\text{n-propyl})_4\text{NPF}_6$  (available from Aldrich Chemical Co., Milwaukee, WI). The vessel was brought to 160°C and maintained at that temperature for 16 hours under 20 nitrogen atmosphere. The polymer was extracted with THF and precipitated in methanol. The yield was again approximately 95 weight percent (wt %). The resulting PFCB arylether polymer had a Mw of 46,900 and a mono-modal molecular weight distribution.

25

**Example 9C (Comparative)**

A thermally-controlled vessel was charged with Monomer A and brought to 180°C and maintained at that temperature for 48 hours under nitrogen atmosphere. The polymer was extracted with THF and precipitated in methanol. The yield was again approximately 95 weight percent (wt %). The resulting PFCB arylether polymer had a 30 Mw of 40,000 and a mono-modal molecular weight distribution.

**Example 10**

A thermally-controlled vessel was charged with 95 wt % of Monomer A and 10 wt % of (Me)<sub>4</sub>NF (available from Aldrich Chemical Co., Milwaukee, WI). The vessel was brought to 180°C and maintained at that temperature for 48 hours under 5 nitrogen atmosphere. The polymer was extracted with THF and precipitated in methanol. The yield was approximately 90 weight percent (wt %). The resulting PFCB arylether polymer had a Mw of 66,000 and a mono-modal molecular weight distribution.

10 Various modifications and alterations of this invention will become apparent to those skilled in the art without departing from the scope and principles of this invention. It should be understood that this invention is not to be unduly limited to the illustrative embodiments set forth hereinabove.

We claim:

1. A method of making a perfluorocyclobutane (PFCB) polymer comprising a step of polymerizing a monomer comprising two or more trifluorovinyl groups in the presence of an initiator or catalyst.  
5
2. The method according to claim 1 wherein said initiator or catalyst is selected from the group consisting of salts comprising fluorine-containing anions.  
10
3. The method according to claim 1 wherein said initiator or catalyst is selected from the group consisting of salts comprising anions selected from the group consisting of  $\text{F}^-$ ,  $\text{BF}_4^-$ ,  $\text{PF}_6^-$  and  $\text{SbF}_6^-$ .  
15
4. The method according to claim 1, 2 or 3 wherein said initiator or catalyst is selected from the group consisting of salts of alkyl- or arylammonium, alkyl- or arylsulfonium, alkyl- or arylphosphonium and organometallic complex cations.  
20
5. The method according to claim 1, 2 or 3 wherein said initiator or catalyst is selected from the group consisting salts of alkylammonium cations.  
25
6. The method according to claim 1 wherein said initiator or catalyst has the formula  $(\text{R})_4\text{N}^+\text{PF}_6^-$ , wherein R is a C1-C8 alkyl group.  
7. The method according to claim 1 wherein said initiator or catalyst is  $(\text{CH}_3)_4\text{N}^+\text{F}^-$   
8. The method according to any of claims 1 - 7 wherein said monomers are selected from the group consisting of monomers of the formula  $\text{CF}_2=\text{CF-X- R}^1\text{-X-CF=CF}_2$ ,  
30 wherein each  $-\text{X-}$  is independently selected from the group consisting of:  $-\text{O-}$ ,  $-\text{S-}$ ,  $-\text{SO-}$ ,  $-\text{SO}_2-$ ,  $-\text{CO-}$ ,  $-\text{NH-}$ , and  $-\text{NR}^2-$ , wherein each  $\text{R}^2$  is independently

selected from C1-C25 substituted or unsubstituted, saturated or unsaturated alkyl or aryl;

wherein R<sup>1</sup> is a substituted or unsubstituted C1-C30 aryl or alkyl moiety which may additionally comprise heteroatoms.

5

9. The method according to claim 8 wherein -X- is -O-.

10. The method according to claim 8 wherein R<sup>1</sup> is a C1-C16 aryl or alkyl moiety.

10 11. The method according to claim 8 wherein said monomers include 4,4'-bis(trifluorovinyloxy)biphenyl.

12. A perfluorocyclobutane (PFCB) polymer made according to the method of any of claims 1 – 11.

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13. A perfluorocyclobutane (PFCB) polymer according to claim 12 having a weight average molecular weight (Mw) of 100,000 or greater.

# INTERNATIONAL SEARCH REPORT

International Application No  
PCT/US 01/19523

**A. CLASSIFICATION OF SUBJECT MATTER**  
IPC 7 C08F16/32

According to International Patent Classification (IPC) or to both national classification and IPC

**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 C08F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

WPI Data

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category <sup>a</sup>	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	WO 90 15082 A (THE DOW CHEMICAL CO.) 13 December 1990 (1990-12-13) cited in the application -----	
A	WO 90 15044 A (THE DOW CHEMICAL CO.) 13 December 1990 (1990-12-13) cited in the application -----	

Further documents are listed in the continuation of box C.

Patent family members are listed in annex.

<sup>a</sup> Special categories of cited documents :

- \*A\* document defining the general state of the art which is not considered to be of particular relevance
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\*X\* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

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**INTERNATIONAL SEARCH REPORT**

Information on patent family members

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 PCT/US 01/19523

Patent document cited in search report		Publication date		Patent family member(s)	Publication date
WO 9015082	A	13-12-1990	US	5037917 A	06-08-1991
			US	5037918 A	06-08-1991
			AT	112575 T	15-10-1994
			AU	619125 B2	16-01-1992
			AU	5926590 A	07-01-1991
			CA	2031185 A1	10-12-1990
			DE	69013120 D1	10-11-1994
			DE	69013120 T2	11-05-1995
			EP	0428708 A1	29-05-1991
			JP	3022921 B2	21-03-2000
			JP	4500388 T	23-01-1992
			KR	191390 B1	15-06-1999
			NO	177824 B	21-08-1995
			US	5364547 A	15-11-1994
			WO	9015082 A1	13-12-1990
			US	5364917 A	15-11-1994
			US	5066746 A	19-11-1991
			US	5159038 A	27-10-1992
			US	5159037 A	27-10-1992
			US	5159036 A	27-10-1992
-----	-----	-----	-----	-----	-----
WO 9015044	A	13-12-1990	US	5021602 A	04-06-1991
			AU	5834290 A	07-01-1991
			CA	2030800 A1	10-12-1990
			EP	0429618 A1	05-06-1991
			JP	4500364 T	23-01-1992
			NO	910516 A	03-04-1991
			WO	9015044 A2	13-12-1990
			US	5210265 A	11-05-1993
-----	-----	-----	-----	-----	-----