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(54) Titre : MANGANATE DE LITHIUM, PROCEDE DE PRODUCTION, ET PILE AU LITHIUM PRODUITE D'APRES CE PROCEDE
(54) Title: LITHIUM MANGANATE, PROCESS FOR PRODUCING THE SAME, AND LITHIUM BATTERY USING THE SAME



(57) Abrégé/Abstract:

A lithium manganate useful as an active material of the positive plate of a lithium cell, a method for producing the same, a positive plate for a lithium cell comprising an active material of lithium manganate, and a lithium cell are provided. The lithium manganate is cubic particles and the particles have pores therein. Therefore lithium cell comprising such an active material of lithium manganate has a high initial discharge capacity of over 95 mAh/g and an excellent cycle characteristic.

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(21) 国際出願番号 PCT/JP98/05798 (22) 国際出願日 1998年12月22日(22.12.98) (30) 優先権データ 特願平9/365563 1997年12月22日(22.12.97) JP (71) 出願人 (米国を除くすべての指定国について) 石原産業株式会社 (ISHIHARA SANGYO KAISHA, LTD.)[JP/JP] 〒550-0002 大阪府大阪市西区江戸堀一丁目3番15号 Osaka, (JP) (72) 発明者 ; および (75) 発明者 / 出願人 (米国についてのみ) 吹田徳雄(SUITA, Tokuo)[JP/JP] 宮崎裕光(MIYAZAKI, Hiromitsu)[JP/JP] 〒512-0912 三重県四日市市三重9-2-3 城山寮 Mie, (JP) (74) 代理人 弁理士 浅村 皓, 外(ASAMURA, Kiyoshi et al.) 〒100-0004 東京都千代田区大手町2丁目2番1号 新大手町ビル331 Tokyo, (JP)		(81) 指定国 AU, BR, CA, CN, ID, IL, IN, JP, KR, MX, SG, US, 欧州特許 (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE). 添付公開書類 国際調査報告書
(54)Title: LITHIUM MANGANATE, METHOD OF PRODUCING THE SAME, AND LITHIUM CELL PRODUCED BY THE METHOD (54)発明の名称 マンガン酸リチウム及びその製造方法ならびにそれを用いてなるリチウム電池 (57) Abstract A lithium manganate useful as an active material of the positive plate of a lithium cell, a method for producing the same, a positive plate for a lithium cell comprising an active material of lithium manganate, and a lithium cell are provided. The lithium manganate is cubic particles and the particles have pores therein. Therefore lithium cell comprising such an active material of lithium manganate has a high initial discharge capacity of over 95 mAh/g and an excellent cycle characteristic.		

DESCRIPTION

LITHIUM MANGANATE, PROCESS FOR PRODUCING THE SAME, AND
LITHIUM BATTERY USING THE SAME

TECHNICAL FIELD

The present invention relates to lithium
manganate which is a compound useful as an active material
for positive electrode for lithium battery, a process for
5 producing the same, a positive electrode for lithium
battery using the same as an active material for positive
electrode, and a lithium battery.

BACKGROUND ART

Lithium manganate is a compound represented by
10 the formula $\text{Li}_x\text{Mn}_y\text{O}_4$, and representative are spinel type
 LiMn_2O_4 , $\text{Li}_{4/3}\text{Mn}_{5/3}\text{O}_4$ and the like. For obtaining such
lithium manganates, a process of firing a mixture of a
manganese compound and a lithium compound at a temperature
of about 800°C is employed.

15 DISCLOSURE OF INVENTION

Lithium manganate obtained by the above conven-
tional process is apt to become a sintered body in which
non-uniform sintering occurs between particles because a
mixture of a manganese compound and a lithium compound is
20 fired at about 800°C for the purpose of adjustment of
valence of manganese or diminishment of by-products. Thus,
there is a problem that size of particles cannot be

controlled. Moreover, since a mixture of a manganese compound and a lithium compound is inferior in reactivity even when it is fired at high temperatures, uniform composition can hardly be obtained and there are many
5 lattice defects. In order to avoid these problems, firing or mechanical grinding must be repeated many times.

Furthermore, lithium secondary batteries which use lithium manganate obtained by the above process as an active material for positive electrodes are not only low in
10 initial charge and discharge capacity, but also show conspicuous reduction in capacity with repetition of charge and discharge. This is because crystals of lithium manganate are collapsed at the time of charging and discharging, which is considered to be caused by the
15 presence of lattice defects and the low lithium ion conductivity.

For the solution of the above problems, there is proposed a process which comprises impregnating a porous manganese dioxide with lithium acetate, lithium nitrate or
20 lithium hydroxide and obtaining a product of uniform composition at low temperatures (for example, "Electrochemistry (Denki Kagaku)", 63, 941 (1995)), but this process is still not sufficient.

The inventors have conducted intensive research
25 in an attempt to obtain lithium manganate useful as active materials for positive electrodes of lithium batteries. As a result, it has been found that lithium secondary batteries in which is used an active material for positive

electrodes which comprises lithium manganate having a cubic particle form and containing voids in the particles are high in initial charge and discharge capacity and excellent in cycle characteristics after repetition of charge and discharge. After additional investigations, the present invention has been accomplished. That is, the present invention relates to a lithium manganate which has a cubic particle form and provides an initial discharge capacity of at least 95 mAh/g when it is used as an active material for positive electrodes of lithium batteries. Furthermore, the present invention relates to a process for the advantageous production of the lithium manganate, and the first process is characterized by including a step of reacting a manganese compound with an alkali to obtain a manganese hydroxide, a step of oxidizing the hydroxide in an aqueous medium or a gaseous phase to obtain a manganese oxide, a step of reacting the manganese oxide with a lithium compound in an aqueous medium to obtain a lithium manganate precursor, and a step of firing the precursor with heating to obtain lithium manganate. The second process is characterized by including a step of reacting a manganese compound with an alkali to obtain a manganese hydroxide, a step of oxidizing the hydroxide in an aqueous medium or a gaseous phase to obtain a manganese oxide, a step of reacting the manganese oxide with an acid in an aqueous medium to substitute proton for a part of manganese to obtain a proton-substituted manganese oxide, a step of reacting the proton-substituted manganese oxide with a

lithium compound in an aqueous medium to obtain a lithium
manganate precursor, and a step of firing the precursor
with heating to obtain lithium manganate. The present
invention further relates to a positive electrode for
5 lithium battery in which the above lithium manganate is
used as an active material for the positive electrode and
to a lithium battery using the positive electrode.

BRIEF DESCRIPTION OF DRAWINGS

FIG. 1 is an X-ray diffraction chart of sample a.
10 FIG. 2 is an X-ray diffraction chart of sample A.
FIG. 3 is a scanning electron microphotograph
(50,000 × magnification) showing the particle structure of
sample A.

FIG. 4 is a scanning electron microphotograph
15 (50,000 × magnification) showing the particle structure of
sample C.

FIG. 5 is a transmission electron microphotograph
(1,500,000 × magnification) showing the particle structure
of sample A.

20 FIG. 6 is an electron diffraction photograph of
sample A.

FIG. 7 is a scanning electron microphotograph
(50,000 × magnification) showing the particle structure of
sample L.

25 BEST MODE FOR CARRYING OUT THE INVENTION

The present invention relates to a lithium

manganate which has a cubic particle form and contains voids in the particles and provides an initial discharge capacity of at least 95 mAh/g, preferably at least 100 mAh/g when it is used as an active material for positive electrodes of lithium batteries. The lithium manganate may be a single phase or may be a mixture containing lithium manganate and impurities coming from the production steps, such as manganese oxide, as far as the above-mentioned discharge capacity is at least 95 mAh/g. If the discharge capacity is lower than the above range, amount of lithium manganate necessary for obtaining batteries of desired capacity increases and this is industrially not preferred. Lithium manganate in the present invention is a compound represented by the formula $\text{Li}_x\text{Mn}_y\text{O}_4$, and the values of x and y in the formula are preferably in the range of 0.3-1.5 expressed by the value of x/y. As preferred compositions, mention may be made of, for example, spinel type LiMn_2O_4 and $\text{Li}_{4/3}\text{Mn}_{5/3}\text{O}_4$ and layered rock-salt type LiMnO_2 .

The cubic particle form means cubic form such as a die or rectangular parallelopiped form, and the particles include those having angles, namely, apexes or sides which are partially removed. All of the individual particles are not needed to have the same form, and as far as they are mainly composed of cubic particles, amorphous particles may partially be contained.

The presence of voids in the particles can be confirmed by measuring void content, and when the void content is 0.005 ml/g or more, it can be admitted that the

particles have voids. The void content is preferably 0.01-1.5 ml/g and more preferably 0.01-0.7 ml/g.

Furthermore, that the initial discharge capacity is at least 95 mAh/g when the lithium manganate is used as an active material for positive electrodes of lithium batteries can be easily confirmed by conducting the measurement in the state of battery and under the measuring conditions mentioned hereinafter.

By employing the above construction, the lithium secondary batteries which contain the lithium manganate of the present invention as an active material of positive electrodes are high in initial charge and discharge capacity and excellent in cycle characteristics.

Specific surface area of the lithium manganate is preferably 1-100 m²/g, more preferably 1-30 m²/g. Since this range is preferred for insertion reaction of lithium, when the lithium manganate is used for positive electrodes of lithium batteries, no collapse of crystals occurs at the time of charging and discharging, and battery characteristics are excellent. The particle diameter is preferably 0.01-10 μm, more preferably 0.05-5 μm. The particle diameter can be measured by reading the maximum length of the individual particles in an electron microphotograph.

With regard to the process for producing lithium manganate according to the present invention, the first production process is characterized by including ① a step of reacting a manganese compound with an alkali to obtain a manganese hydroxide, ② a step of oxidizing the hydroxide in

an aqueous medium or a gaseous phase to obtain a manganese oxide, ③ a step of reacting the manganese oxide with a lithium compound in water to obtain a lithium manganate precursor, and ④ a step of firing the precursor with heating to obtain a lithium manganate. The second production process is characterized by including ① a step of reacting a manganese compound with an alkali to obtain a manganese hydroxide, ② a step of oxidizing the hydroxide in an aqueous medium or a gaseous phase to obtain a manganese oxide, ②' a step of reacting the manganese oxide with an acid in an aqueous medium to substitute proton for a part of manganese to obtain a proton-substituted manganese oxide, ③ a step of reacting the proton-substituted manganese oxide with a lithium compound in an aqueous medium to obtain a lithium manganate precursor, and ④ a step of firing the precursor with heating to obtain a lithium manganate.

The step ① is a step of reacting a manganese compound with an alkali to obtain a manganese hydroxide. The reaction of a manganese compound with an alkali can be carried out by reacting a water-soluble manganese compound with an alkali in an aqueous medium or by reacting a manganese solution containing Mn^{2+} , Mn^{3+} and/or Mn^{4+} ion obtained by dissolving a hardly water-soluble manganese compound in an acid with an alkali in an aqueous medium. The former process of reacting a water-soluble manganese compound with an alkali in an aqueous medium is more preferred. As the water-soluble manganese compounds, there

may be used water-soluble inorganic manganese compounds such as manganese sulfate, manganese chloride and manganese nitrate and water-soluble organic manganese compounds such as manganese acetate. As the hardly water-soluble manganese compounds, there may be used MnO_2 and hydrates thereof, Mn_2O_3 and hydrates thereof, manganese oxides such as MnO and Mn_3O_4 , and organic manganese compounds such as manganese alkoxides. As the acids used, mention may be made of inorganic acids such as sulfuric acid, hydrochloric acid and nitric acid, and organic acids such as acetic acid and formic acid. As the alkalis, there may be used alkali hydroxides such as sodium hydroxide, potassium hydroxide and lithium hydroxide, ammonia compounds such as ammonia gas and aqueous ammonia, and alkali carbonate compounds such as sodium carbonate, potassium carbonate, lithium carbonate and ammonium carbonate. The reaction can be carried out in an atmosphere of either air or inert gas, but is preferably carried out in an inert gas atmosphere for the purpose of controlling the oxidation level of the manganese hydroxide. Reaction temperature is preferably 10-80°C for controlling the particle form.

The resulting manganese hydroxide may be filtered or washed, if necessary.

The next step ② is a step of oxidizing the manganese hydroxide obtained in the step ① in an aqueous medium or a gaseous phase to obtain a manganese oxide. The oxidization in an aqueous medium can be carried out by blowing air, oxygen or ozone into an aqueous medium

containing the manganese hydroxide or adding aqueous hydrogen peroxide or a peroxodisulfate to the aqueous medium. For example, potassium peroxodisulfate can be used as the peroxodisulfate. Oxidizing temperature in the aqueous medium is preferably 10°C to boiling point, more preferably room temperature to 90°C. The oxidization in a gaseous phase can be carried out by filtering or washing the aqueous medium containing the manganese hydroxide, if necessary, and then drying the manganese hydroxide in the air. Oxidizing temperature in the gaseous phase is preferably room temperature to 300°C, more preferably 50-130°C. In the present invention, it is preferred that the manganese hydroxide obtained in the step ① is (i) oxidized in an aqueous medium or (ii) first partially oxidized in the aqueous medium and then oxidized in a gaseous phase. The degree of oxidation of the manganese hydroxide can be optionally set, but it is considered that when the oxidation degree is small, oxides, hydrated oxides or hydroxides of manganese of bivalence, trivalence and tetravalence are present in the manganese oxide. Manganese oxides of preferred state in the present invention comprise $2\text{MnO} \cdot \text{MnO}_2$ as a main component with the molar ratio $\text{Mn}^{2+}/\text{Mn}^{4+}$ being in the range of 1-3. More preferred are manganese oxides which have a specific surface area of 10-40 m^2/g , a void content of 0.08-0.3 ml/g , and a particle diameter of about 0.08-0.15 μm , and these manganese oxides readily react with lithium compound in the next step ③ because of the large specific surface area and the high void content.

Such manganese oxides having a large specific surface area and a high void content can be obtained by employing the above-mentioned preferred oxidizing conditions. In the step ①, while the manganese compound is reacted with the
5 alkali, for example, while the alkali is added to an aqueous solution of a manganese compound, the oxidization may be carried out with air, oxygen, ozone, aqueous hydrogen peroxide, or peroxodisulfate.

The step ②' is a step of reacting the manganese
10 oxide obtained in the step ② with an acid in an aqueous medium to obtain a proton-substituted manganese oxide resulting from substitution of proton for a part of manganese, and the proton-substituted manganese oxide is high in reactivity with the lithium compound in the
15 subsequent step ③ of obtaining a lithium manganate precursor, and this is preferred.

As the acid, there may be used any of inorganic acids such as hydrochloric acid, sulfuric acid, nitric acid, hydrofluoric acid and the like, and water-soluble
20 organic acids such as acetic acid, formic acid and the like. Among them, inorganic acids such as hydrochloric acid, sulfuric acid, nitric acid and hydrofluoric acid are preferred because these are industrially advantageous. The temperature at which the manganese oxide is reacted with
25 acid is preferably in the range of room temperature to 90°C, more preferably in the range of 40-70°C.

The thus obtained manganese oxide may be filtered, washed or dried, if necessary.

The step ③ is a step of reacting the manganese oxide or the proton-substituted manganese oxide obtained in the step ② or ②' with a lithium compound in an aqueous medium to obtain a lithium manganate precursor. As the
5 lithium compound, there may be used lithium hydroxide, lithium carbonate or the like, and lithium hydroxide is preferred because it is superior in reactivity. The reaction proceeds by mixing the lithium compound and the manganese oxide in an aqueous medium and keeping the
10 temperature at 50°C or higher. The temperature is more preferably 100°C or higher, further preferably 100-250°C, and most preferably 100-180°C. When the reaction is carried out at a temperature of 100°C or higher, it is preferred to put the lithium compound and the manganese oxide in an
15 autoclave and subject them to hydrothermal treatment under saturated steam pressure or under pressurization. Furthermore, when the lithium compound and the manganese oxide are mixed in an aqueous medium and the mixture is heated, dried and solidified with evaporating the aqueous medium at 50°C
20 or higher (evaporation to dryness), concentration of the lithium compound in the aqueous medium increases with evaporation of the aqueous medium, and, as a result, the lithium manganate precursor is readily produced upon the reaction of the lithium compound and the manganese oxide,
25 and this is preferred. The lithium manganate precursor obtained in the step ③ varies in composition depending on the reaction conditions, but is considered to be a mixture containing mainly a solid solution of $2\text{MnO} \cdot \text{MnO}_2$ and

$\text{Li}_2\text{O} \cdot \text{MnO} \cdot \text{MnO}_2$, LiMn_2O_4 , LiMnO_2 or the like. This can be confirmed by X-ray diffraction.

When the reaction in the step ③ is carried out with feeding an oxidizing agent by batch-wise or continuous
5 process, reactivity with the lithium compound increases, and this is preferred. The batch-wise process is a process which comprises repeating the following operations (1)-(3) until the reaction reaches the desired level: (1) feeding a given amount of an oxidizing agent to the reaction system,
10 then (2) carrying out the reaction with suspending the feeding of the oxidizing agent until the fed oxidizing agent has been consumed, and (3) measuring the reacting weights of the manganese compound and the lithium compound. The batch-wise process is preferred for accurately control-
15 ling the reacting weights of the manganese oxide and the lithium compound. The continuous process is a process of carrying out the reaction until it reaches the desired reaction level by continuously feeding the oxidizing agent to the reaction system with measuring the reaction level of
20 the manganese oxide and the lithium compound. The continuous process is economically preferred for carrying out the reaction in industrial scale. Moreover, it is preferred to carry out the reaction using at least one oxidizing agent selected from air, oxygen, ozone, aqueous
25 hydrogen peroxide and peroxodisulfate because the reactivity of the lithium compound and the manganese oxide is improved. As the peroxodisulfate, for example, potassium peroxodisulfate can be used.

In order to perform the step ③ by hydrothermal treatment and feeding the oxidizing agent by the batch-wise process, prior to the hydrothermal treatment, air, oxygen or ozone can be blown into the mixture of the lithium compound and the manganese oxide or aqueous hydrogen peroxide or peroxodisulfate can be added to the mixture and, further, oxygen can be fed. Furthermore, in the course of the hydrothermal treatment, the temperature is once lowered, and air, oxygen or ozone may be blown into the mixture of the lithium compound and the manganese oxide or aqueous hydrogen peroxide or peroxodisulfate may be added to the mixture and, further, oxygen may be fed. In the case of the continuous process, the hydrothermal treatment is carried out with continuously feeding oxygen gas under pressure. The reacting weights of the manganese oxide and the lithium compound can be obtained by taking a small amount of the reaction mixture and measuring by neutralization titration the alkali concentration of the solution from which solid matter has been removed.

The lithium manganate precursor obtained in the step ③ may further be oxidized by blowing air, oxygen or ozone into the solution containing the lithium manganate precursor or adding aqueous hydrogen peroxide or peroxodisulfate to the solution. Furthermore, if necessary, the solution may be filtered, washed or dried. The drying temperature can be optionally set within the range of lower than the temperature at which the lithium manganate precursor is converted to a lithium manganate,

and is suitably 50-200°C.

The step ④ is a step of heating and firing the lithium manganate precursor obtained in the step ③ to obtain a lithium manganate. The temperature for heating and firing is in the range of from the temperature at which the precursor is converted to the lithium manganate to the temperature at which the specific surface area of the resulting lithium manganate reaches 1 m²/g or less. It is considered that the temperature for heating and firing may vary depending on the composition and particle size of the precursor and the firing atmosphere, but is generally 250-840°C, and is preferably 280-700°C for obtaining fine lithium manganate of good crystallinity, and more preferably 300-600°C. Furthermore, a range of 650-800°C is preferred for obtaining lithium manganate of large particle diameter. If the firing temperature is higher than the above range, lithium in the resulting lithium manganate readily vaporizes. The firing atmosphere is not limited as far as it is oxygen-containing atmosphere such as air, and the oxygen partial pressure can be optionally set.

Next, the present invention relates to a positive electrode for lithium batteries which uses the above-mentioned lithium manganate as an active material for the positive electrode, and further relates to a lithium battery made using this positive electrode. The lithium batteries in the present invention include primary batteries using lithium metal for negative electrodes, chargeable and dischargeable secondary batteries using

lithium metal for negative electrodes, and chargeable and dischargeable lithium ion secondary batteries using a carbon material, a tin compound, lithium titanate and the like for negative electrodes.

5 In the case of coin-shaped batteries, the positive electrode for lithium batteries can be obtained by adding carbon conductive agents such as acetylene black, carbon and graphite powders and binders such as polytetrafluoroethylene resin and polyvinylidene fluoride to the
10 lithium manganate powders of the present invention, kneading them, and molding the kneaded product into a pellet. In the case of cylindrical or rectangular batteries, the positive electrode can be obtained by adding the above additives and, besides, organic solvents such as N-
15 methylpyrrolidone to the lithium manganate powders of the present invention, kneading them to prepare a paste, coating the paste on a metallic current collector such as an aluminum foil, and drying the coat.

 As electrolytes of lithium battery, there may be
20 used those which are prepared by dissolving lithium ion in a polar organic solvent which is neither oxidized nor reduced at a potential in a range wider than the electrochemically stable range, namely, the potential range in which the battery works as a lithium battery. Examples of
25 the polar organic solvent are propylene carbonate, ethylene carbonate, diethyl carbonate, dimethoxyethane, tetrahydrofuran, γ -butyrolactone, and mixtures thereof. As a solute for lithium ion source, there may be used lithium

perchlorate, lithium hexafluorophosphate, lithium tetrafluoroborate, and the like. Furthermore, a porous polypropylene film or polyethylene film is put as a separator between electrodes.

5 As examples of the battery, mention may be made of coin-shaped battery made by disposing a separator between a pellet-like positive electrode and a negative electrode, press-bonding them to a sealed can with a propylene gasket, pouring an electrolyte therein, and
10 sealing it, and a cylindrical battery made by coating a positive electrode material and a negative electrode material on metallic current collectors, rolling them with a separator therebetween, inserting them into a battery can with a gasket, pouring an electrolyte therein, and sealing
15 the can. Moreover, there are three-electrode type batteries which are used especially for the measurement of electrochemical characteristics. These batteries in which a reference electrode is disposed in addition to a positive electrode and a negative electrode evaluate electrochemical
20 characteristics of the respective electrodes by controlling the potential of the positive and negative electrodes in respect to the reference electrode.

 The performance of the lithium manganate as a positive electrode material can be evaluated by construct-
25 ing a lithium battery in the above-mentioned manner, charging and discharging the battery at a suitable potential and current, and measuring the electric capacity. Furthermore, cycle characteristics can be judged from the

change in electric capacity caused by repetition of charge and discharge.

EXAMPLE

Examples of the present invention are shown below, but the present invention is never limited to these examples.

Example 1

(Synthesis of manganese hydroxide)

815 g of manganese sulfate (86% by weight as MnSO_4) was dissolved in water to prepare 6.179 liters of a solution. This aqueous manganese sulfate solution was charged in a glass reaction vessel of 10 liters, and, with stirring, 2.321 liters of sodium hydroxide of 4 mols/l in concentration was added to and dispersed in the aqueous solution over a period of 1 hour in a nitrogen atmosphere with keeping the temperature at $15 \pm 5^\circ\text{C}$ to obtain a manganese hydroxide.

(Synthesis of manganese oxide)

The resulting slurry containing manganese hydroxide was heated to 60°C , and air was blown thereinto for 1 hour to oxidize the manganese hydroxide in an aqueous medium, followed by aging for 1 hour with blowing nitrogen gas in place of the air and thereafter filtering and washing with water. The resulting filter cake was dried at 110°C for 12 hours to carry out gas phase oxidation to

obtain a manganese oxide. This manganese oxide was large in specific surface area and void content and was mainly composed of $2\text{MnO} \cdot \text{MnO}_2$.

(Synthesis of lithium manganate precursor)

5 The resulting manganese oxide (240 g in terms of Mn) was dispersed in water to prepare a slurry. Pure water and 0.920 liter of lithium hydroxide of 3.206 mols/l in concentration were added to the slurry to obtain 2.40 liters of a liquid. This was charged in a glass reaction
10 vessel of 3 liters and heated to 80°C , and reaction was carried out for 3 hours with blowing air thereinto. The evaporated water was replenished and then a part of the slurry was taken and alkali concentration thereof was measured to find that 18.8% by weight of the added lithium
15 reacted with the manganese oxide. The slurry was charged in an autoclave and subjected to hydrothermal treatment at 130°C for 2 hours. The slurry was cooled to 80°C and then alkali concentration in the slurry was measured in the same manner as above to find that 57.1% by weight of the added
20 lithium reacted with the manganese oxide. Air was blown into this slurry for 2 hours, and the slurry was again subjected to hydrothermal treatment at 130°C for 2 hours to obtain a slurry of a lithium manganate precursor (sample a) by batch-wise process. After the slurry was cooled to 80°C ,
25 the alkali concentration was measured in the same manner as above to find that 74.1% by weight of the added lithium reacted with the manganese oxide. The molar ratio of Li to

Mn in sample a was 0.50.

An X-ray diffraction chart of the sample a is shown in FIG. 1. From FIG. 1, it was recognized that the lithium manganate precursor of sample a was a mixture
5 mainly comprising a solid solution of $2\text{MnO} \cdot \text{MnO}_2$ and $\text{Li}_2\text{O} \cdot \text{MnO} \cdot \text{MnO}_2$, LiMn_2O_4 , LiMnO_2 and the like.

(Synthesis of lithium manganate)

Air was blown into the resulting precursor slurry for 2 hours, followed by filtration. Washing was not
10 carried out. The filter cake was dried at 110°C , and then fired at 500°C for 3 hours in the air to obtain a lithium manganate (sample A) of the present invention.

Example 2

(Synthesis of manganese hydroxide)

15 A manganese hydroxide was obtained in the same manner as in Example 1.

(Synthesis of manganese oxide)

A manganese oxide was obtained in the same manner as in Example 1.

20 (Synthesis of lithium manganate precursor)

The resulting manganese oxide (240 g in terms of Mn) was dispersed in water to prepare a slurry. Pure water and 0.870 liter of lithium hydroxide of 3.206 mols/l in concentration were added to the slurry to obtain 2.40

liters of a liquid. This was charged in a glass reaction vessel of 3 liters and heated to 80°C, and reaction was carried out for 3 hours with blowing air thereinto. The evaporated water was replenished and then a part of the
5 slurry was taken, and alkali concentration thereof was measured to find that 16.4% by weight of the added lithium reacted with the manganese oxide. The slurry was charged in an autoclave and subjected to hydrothermal treatment at 150°C for 2 hours. The slurry was cooled to 80°C and then
10 alkali concentration in the slurry was measured in the same manner as above to find that 61.1% by weight of the added lithium reacted with the manganese oxide. Air was blown into this slurry for 2 hours, and the slurry was again subjected to hydrothermal treatment at 150°C for 2 hours to
15 obtain a slurry of a lithium manganate precursor (sample b) by batch-wise process. After the slurry was cooled to 80°C, the alkali concentration was measured in the same manner as above to find that 78.3% by weight of the added lithium reacted with the manganese oxide. The molar ratio of Li to
20 Mn in the sample b was 0.50.

(Synthesis of lithium manganate)

Air was blown into the resulting precursor slurry for 2 hours, followed by filtration. Washing was not carried out. The filter cake was dried at 110°C, and then
25 fired at 500°C for 3 hours in the air to obtain a lithium manganate (sample B) of the present invention.

Example 3

(Synthesis of manganese hydroxide)

A manganese hydroxide was obtained in the same manner as in Example 1.

5 (Synthesis of manganese oxide)

A manganese oxide was obtained in the same manner as in Example 1.

(Synthesis of lithium manganate precursor)

The resulting manganese oxide (186.5 g in terms
10 of Mn) was dispersed in water to prepare a slurry. Pure water and 0.746 liter of lithium hydroxide of 3.000 mols/l in concentration were added to the slurry to obtain 2.40 liters of a liquid. This was charged in a glass reaction vessel of 3 liters and heated to 80°C, and reaction was
15 carried out for 3 hours with blowing air thereinto. The evaporated water was replenished and then a part of the slurry was taken, and alkali concentration thereof was measured to find that 13.8% by weight of the added lithium reacted with the manganese oxide. The slurry was charged
20 in an autoclave and subjected to hydrothermal treatment at 180°C for 2 hours. The slurry was cooled to 80°C and then alkali concentration in the slurry was measured in the same manner as above to find that 55.5% by weight of the added lithium reacted with the manganese oxide. Air was blown
25 into this slurry for 2 hours, and the slurry was again subjected to hydrothermal treatment at 180°C for 2 hours to

obtain a slurry of a lithium manganate precursor (sample c) by batch-wise process. After the slurry was cooled to 80°C, the alkali concentration was measured in the same manner as above to find that 79.1% by weight of the added lithium
5 reacted with the manganese oxide. The molar ratio of Li to Mn in the sample c was 0.52.

(Synthesis of lithium manganate)

Air was blown into the resulting precursor slurry for 2 hours, followed by filtration. Washing was not
10 carried out. The filter cake was dried at 110°C, and then fired at 500°C for 3 hours in the air to obtain a lithium manganate (sample C) of the present invention.

Example 4

(Synthesis of manganese hydroxide)

15 A manganese hydroxide was obtained in the same manner as in Example 1.

(Synthesis of manganese oxide)

The resulting slurry containing manganese hydroxide was heated to 60°C, and air was blown thereinto
20 for 1 hour to oxidize the manganese hydroxide in an aqueous medium, followed by aging for 1 hour with blowing nitrogen gas in place of the air and thereafter filtering and washing with water. The resulting filter cake was dried at 200°C for 12 hours to carry out gas phase oxidation to
25 obtain a manganese oxide. This manganese oxide was large

in specific surface area and void content and was mainly composed of $2\text{MnO} \cdot \text{MnO}_2$.

(Synthesis of lithium manganate precursor)

The resulting manganese oxide (186.5 g in terms
5 of Mn) was dispersed in water to prepare a slurry. Pure water and 0.746 liter of lithium hydroxide of 3.000 mols/l in concentration were added to the slurry to obtain 2.40 liters of a liquid. This was charged in an autoclave and subjected to hydrothermal treatment at 180°C for 2 hours.
10 The slurry was cooled to 80°C and a part of the slurry was taken and alkali concentration thereof was measured to find that 31.9% by weight of the added lithium reacted with the manganese oxide. Air was blown into this slurry for 2 hours, and the slurry was again subjected to hydrothermal
15 treatment at 180°C for 2 hours. The slurry was cooled to 80°C and alkali concentration thereof was measured in the same manner as above to find that 56.6% by weight of the added lithium reacted with the manganese oxide. Air was blown into this slurry for 2 hours, and the slurry was
20 again subjected to hydrothermal treatment at 180°C for 2 hours to obtain a slurry of a lithium manganate precursor (sample d) by batch-wise process. After the slurry was cooled to 80°C , the alkali concentration thereof was measured in the same manner as above to find that 75.8% by
25 weight of the added lithium reacted with the manganese oxide. The molar ratio of Li to Mn in sample d was 0.50.

(Synthesis of lithium manganate)

Air was blown into the resulting precursor slurry for 2 hours, followed by filtration. Washing was not carried out. The filter cake was dried at 50°C, and a part thereof was fired at 500°C, 700°C or 800°C for 3 hours in the air to obtain lithium manganates (samples D, E and F) of the present invention.

Example 5

(Synthesis of manganese hydroxide)

1146 g of manganese chloride tetrahydrate (99% by weight as $\text{MnCl}_2 \cdot 4\text{H}_2\text{O}$) was dissolved in water to prepare 7.153 liters of a solution. This aqueous manganese chloride solution was charged in a glass reaction vessel of 10 liters, and, with stirring, 1.847 liters of sodium hydroxide of 6.209 mols/l in concentration was added to and dispersed in the aqueous solution over a period of 1 hour in a nitrogen atmosphere with keeping the temperature at $15 \pm 5^\circ\text{C}$ to obtain a manganese hydroxide.

(Synthesis of manganese oxide)

The resulting slurry containing manganese hydroxide was heated to 60°C, and air was blown thereinto for 7 hours to oxidize the manganese hydroxide in an aqueous medium, followed by filtration, washing with water and re-pulping to obtain a slurry of manganese oxide. This manganese oxide had a large specific surface area and a high void content and was mainly composed of $2\text{MnO} \cdot \text{MnO}_2$.

(Synthesis of lithium manganate precursor)

To the resulting manganese oxide slurry (186.5 g in terms of Mn) were added pure water and 0.746 liter of lithium hydroxide of 3.000 mols/l in concentration to
5 obtain 2.40 liters of a liquid. This was charged in a glass reaction vessel of 3 liters and heated to 80°C, and reaction was carried out for 3 hours with blowing air thereinto. The evaporated water was replenished and then a part of the slurry was taken and alkali concentration
10 thereof was measured to find that 9.58% by weight of the added lithium reacted with the manganese oxide. The slurry was charged in an autoclave and subjected to hydrothermal treatment at 180°C for 2 hours. The slurry was cooled to 80°C and then a part of the slurry was taken and alkali
15 concentration of the slurry was measured to find that 64.6% by weight of the added lithium reacted with the manganese oxide. Air was blown into this slurry for 2 hours, and the slurry was again subjected to hydrothermal treatment at 180°C for 2 hours to obtain a slurry of a lithium manganate
20 precursor (sample g) by batch-wise process. After the slurry was cooled to 80°C, the alkali concentration was measured in the same manner as above to find that 75.8% by weight of the added lithium reacted with the manganese oxide. The molar ratio of Li to Mn in sample g was 0.50.

25 (Synthesis of lithium manganate)

Air was blown into the resulting precursor slurry for 2 hours, followed by filtration. Washing was not

carried out. The filter cake was dried at 50°C, and then fired at 500°C for 3 hours in the air to obtain a lithium manganate (sample G) of the present invention.

Example 6

5 (Synthesis of manganese hydroxide)

A manganese hydroxide was obtained in the same manner as in Example 1.

(Synthesis of manganese oxide)

10 A manganese oxide was obtained in the same manner as in Example 1.

(Synthesis of lithium manganate precursor)

0.304 liter of lithium hydroxide of 3.000 mols/l in concentration was added to the resulting manganese oxide (100 g in terms of Mn), followed by thoroughly mixing them
15 with stirring. Then, the mixture was evaporated to dryness at 110°C to obtain a lithium manganate precursor (sample h).

(Synthesis of lithium manganate)

The sample h was finely ground using a small-sized grinder and then fired at 750°C for 3 hours in the air
20 to obtain a lithium manganate (sample H) of the present invention.

Example 7

(Synthesis of manganese hydroxide)

A manganese hydroxide was obtained in the same manner as in Example 1.

5 (Synthesis of manganese oxide)

A manganese oxide was obtained in the same manner as in Example 1.

(Synthesis of lithium manganate precursor)

The resulting manganese oxide (324 g in terms of
10 Mn) was dispersed in water to prepare a slurry. Pure water
and 0.966 liter of lithium hydroxide solution of 3.655
mols/l in concentration were added to the slurry to obtain
2.40 liters of a liquid. This was charged in a glass
reaction vessel of 3 liters, and reaction was carried out
15 for 13 hours with heating to 90°C, and with blowing 1
liter/min of oxygen gas thereinto to obtain a lithium
manganate precursor (sample i). The evaporated water was
replenished and then a part of the slurry was taken and
alkali concentration thereof was measured to find that
20 89.4% by weight of the added lithium reacted with the
manganese oxide. The molar ratio of Li to Mn in the sample
i was 0.54.

(Synthesis of lithium manganate)

The resulting precursor slurry was filtered.
25 Washing was not carried out. The filter cake was dried at

110°C, and then fired at 750°C for 3 hours in the air to obtain a lithium manganate (sample I) of the present invention.

Example 8

5 (Synthesis of manganese hydroxide)

A manganese hydroxide was obtained in the same manner as in Example 1.

(Synthesis of manganese oxide)

The resulting slurry containing manganese
10 hydroxide was heated to 60°C. This slurry had a pH of 8.3. The manganese hydroxide was oxidized in the slurry with blowing 2 liters/min of oxygen gas into the slurry until pH reached 6. Successively, with blowing oxygen gas into the slurry, a sodium hydroxide solution of 2 mols/liter in
15 concentration was added to adjust the pH to 9, followed by heating to 90°C, aging for 2 hours with keeping the pH at 9, filtrating and washing with water. The resulting filter cake was dispersed in pure water to obtain a slurry of 100 g/l in concentration in terms of Mn. This slurry had a pH
20 of 10.7. With stirring, an aqueous hydrochloric acid solution of 1 mol/l in concentration was added to and dispersed in the slurry at room temperature to adjust the pH to 6. With keeping the pH at 6, reaction was carried out for 3 hours, followed by filtration, washing with water
25 and drying at 70°C for 15 hours in the air to obtain a manganese oxide. This manganese oxide had a large specific

surface area and a high void content and was mainly composed of $2\text{MnO} \cdot \text{MnO}_2$.

(Synthesis of lithium manganate precursor)

The resulting manganese oxide (312 g in terms of
5 Mn) was dispersed in water to prepare a slurry. Pure water
and 0.877 liter of lithium hydroxide solution of 3.655
mols/l in concentration were added to the slurry to obtain
2.40 liters of a liquid. This was charged in a glass
reaction vessel of 3 liters, and reaction was carried out
10 for 6 hours with heating to 90°C , and with blowing 1
liter/min of oxygen gas thereinto to obtain a lithium
manganate precursor (sample j). The evaporated water was
replenished and then a part of the slurry was taken and
alkali concentration thereof was measured to find that
15 89.8% by weight of the added lithium reacted with the
manganese oxide. The molar ratio of Li to Mn in the sample
j was 0.51.

(Synthesis of lithium manganate)

The resulting precursor slurry was filtered.
20 Washing was not carried out. The filter cake was dried at
 110°C , and then fired at 750°C for 3 hours in the air to
obtain a lithium manganate (sample J) of the present
invention.

Example 9

(Synthesis of manganese hydroxide)

815 g of manganese sulfate (86% by weight as MnSO_4) was dissolved in water to prepare 6.179 liters of a solution. This aqueous manganese sulfate solution was charged in a glass reaction vessel of 10 liters, and, with stirring, the solution was heated to 60°C in a nitrogen atmosphere. With keeping 60°C , 2.321 liters of sodium hydroxide of 4 mols/l in concentration was added to and dispersed in the aqueous solution over a period of 1 hour to obtain a manganese hydroxide.

(Synthesis of manganese oxide)

The resulting slurry containing manganese hydroxide had a pH of 8.3. With blowing 2 liters/min of oxygen gas into the slurry, the manganese hydroxide was oxidized in the slurry until pH reached 6, followed by filtration and washing with water. The resulting filter cake was dispersed in pure water to prepare a slurry of 100 g/l in terms of Mn, which was charged in a glass reaction vessel of 5 liters and heated to 60°C . 1.329 liters of aqueous hydrochloric acid solution of 1 mol/l in concentration was added to and dispersed in the slurry, and, thereafter, reaction was carried out for 3 hours to replace a part of Mn^{2+} contained in the produced $2\text{MnO}\cdot\text{MnO}_2$ with proton, followed by filtration and washing with water. By the acid treatment, color of the slurry changed from light brown to blackish brown. The slurry after completion of

the reaction had a pH of 4.6.

(Synthesis of lithium manganate precursor)

The resulting manganese oxide (312 g in terms of Mn) was dispersed in water to prepare a slurry. To this
5 slurry were added pure water and 0.841 liter of lithium hydroxide solution of 3.655 mols/l in concentration to obtain 2.40 liters of a liquid. This was charged in a glass reaction vessel of 3 liters, and reaction was carried out for 1 hour with heating to 90°C and with blowing 1
10 liter/min of oxygen gas thereinto. The evaporated water was replenished and then a part of the slurry was taken and alkali concentration thereof was measured to find that 55.6% by weight of the added lithium reacted with the manganese oxide. The slurry was charged in an autoclave
15 and subjected to hydrothermal treatment at 130°C for 3 hours. The slurry was cooled to 90°C and then alkali concentration of the slurry was measured in the same manner as above to find that 76.9% by weight of the added lithium reacted with the manganese oxide. With blowing 1 liter/min
20 of oxygen gas into this slurry, reaction was carried out at 90°C for 2 hours to obtain a lithium manganate precursor (sample k). In the same manner as above, the alkali concentration of the slurry was measured to find that 93.7% by weight of the added lithium reacted with the manganese
25 oxide. The molar ratio of Li to Mn in sample k was 0.51.

(Synthesis of lithium manganate)

The resulting precursor slurry was filtered. Washing was not carried out. The filter cake was dried at 110°C, and then fired at 750°C for 3 hours in the air to
5 obtain a lithium manganate (sample K) of the present invention.

Comparative Example 1

(Synthesis of lithium manganate)

50 g of reagent grade manganese dioxide (95% by
10 weight as MnO_2 ; manufactured by Kanto Kagaku Co., Ltd.) was mixed with lithium hydroxide monohydrate at a molar ratio of Li/Mn of 0.505. The mixture was thoroughly mixed and ground by a small-sized grinder, and then charged in an alumina crucible and fired at 750°C for 3 hours in the air
15 to obtain a lithium manganate (sample L) of a comparative sample.

Comparative Example 2

(Synthesis of manganese hydroxide)

A manganese hydroxide was obtained in the same
20 manner as in Example 1.

(Synthesis of manganese oxide)

A manganese oxide was obtained in the same manner as in Example 1.

(Synthesis of lithium manganate)

The resulting manganese oxide (50 g in terms of Mn) was mixed with lithium hydroxide monohydrate at a molar ratio of Li/Mn of 0.505. The mixture was thoroughly mixed
5 and ground by a small-sized grinder, and then charged in an alumina crucible and fired at 750°C for 3 hours in the air to obtain a lithium manganate (sample M) of a comparative sample.

Properties of the resulting samples A-M were
10 measured and are shown in Table 1. It was confirmed by observation with an electron microscope that particle form of the lithium manganates of the present invention was cubic. (As examples, scanning electron microphotographs of samples A and C are shown in FIGS. 3 and 4.) The samples
15 partially contained amorphous particles, but amount of the amorphous particles was slight. On the other hand, the comparative sample M contained partially cubic particles, but the proportion of amorphous particles in this sample was very high as in the comparative sample L. Furthermore,
20 the lithium manganates of the present invention were recognized to be excellent in crystallinity in view of the results that a spot-like diffraction pattern was obtained in electron diffraction (as an example, an electron diffraction photograph of sample A is shown in FIG. 6),
25 that a single lattice image was shown in observation by an ultra-high magnification transmission type electron microscope (transmission electron microphotograph of sample A is shown in FIG. 5 as an example), and that the lithium

manganates had a single composition of LiMn_2O_4 as a result of X-ray diffraction (X-ray diffraction chart of sample A is shown in FIG. 2 as an example).

Furthermore, measurement of specific surface area by BET method and that of void content by nitrogen adsorption were conducted. BELLSOAP-28 manufactured by Japan Bell Co., Ltd. was used for the measurement of the void content. The results of measurements are shown in Table 1. It can be seen from Table 1 that samples A-K had satisfactory specific surface area and had voids in the particles.

Next, charge and discharge characteristics and cycle characteristics of lithium secondary batteries using samples A-M as active materials of positive electrodes were evaluated. The batteries were of triple-electrode cells, and charge and discharge were repeated.

The batteries and measuring conditions will be explained.

Each of the samples, a graphite powder as a conductive agent and polytetrafluoroethylene resin as a binder were mixed at a ratio of 3:2:1, and the mixture was kneaded in an agate mortar. The kneaded product was molded into circular form of 14 mm in diameter to obtain a pellet. Weight of the pellet was 50 mg. This was put between meshes made of metallic titanium, followed by pressing under a pressure of 150 kg/cm^2 to obtain a positive electrode.

Separately, metallic lithium of 0.5 mm thick was

molded into circular form of 14 mm in diameter, and this was put between meshes made of metallic nickel, followed by press-bonding to obtain a negative electrode. Furthermore, a metallic lithium foil of 0.1 mm thick was wound around a
5 metallic nickel wire so that the foil was in a size of a grain of rice, thereby to obtain a reference electrode. As a non-aqueous electrolyte, there was used a mixed solution of 1,2-dimethoxyethane and propylene carbonate (1:1 in volume ratio) in which lithium perchlorate was dissolved at
10 a concentration of 1 mol/l. The electrodes were arranged in the order of positive electrode, reference electrode and negative electrode, and a porous polypropylene film was put between them as a separator.

The measurement of charge and discharge cycle was
15 carried out at a constant current setting the voltage range at 4.3 V to 3.5 V and the charge and discharge current at 0.26 mA (about 1 cycle/day). The initial discharge capacity, the discharge capacity at 10th cycle and the capacity retention rate at that time are shown in Table 1.
20 The capacity was per 1 g of the active material of positive electrode.

Table 1 Initial discharge capacity and cycle characteristics of batteries using the lithium manganate as active material of positive electrode

Sample	Particle diameter (μm)	Particle form	Specific surface area (m^2/g)	Void content (ml/g)	Initial discharge capacity (mAh/g)	Discharge capacity at 10th cycle (mAh/g)	Capacity retention rate (%)
A	0.08~0.1	Cubic	20.0	0.140	117.0	114.3	97.7
B	0.08~0.2	Cubic	16.5	0.106	123.5	118.0	95.5
C	0.1~0.2	Cubic	10.6	0.069	118.9	114.0	95.9
D	0.1~0.2	Cubic	10.3	0.085	111.8	107.8	96.4
E	0.1~0.6	Cubic+ Amorphous	4.1	0.018	124.0	113.8	91.8
F	0.5~0.6	Cubic+ Amorphous	1.7	0.010	123.0	110.6	90.0
G	0.1~0.2	Cubic	12.3	0.083	120.3	114.8	95.4
H	0.1~0.25	Cubic+ Amorphous	3.9	0.025	126.6	120.7	95.3
I	0.2~0.6	Cubic+ Amorphous	3.6	0.010	117.1	115.2	98.4
J	0.2~0.4	Cubic	6.0	0.014	130.6	126.8	96.8
K	0.4~0.5	Cubic	3.5	0.010	130.2	124.6	95.7
L	0.1~	Amorphous	1.5	0.007	91.4	87.2	95.4
M	0.2~0.4	Cubic+ Amorphous	2.8	0.006	68.2	66.0	96.9

As shown in Table 1, the lithium manganates of the present invention showed a high initial discharge capacity of at least 95 mAh/g and, besides, provided excellent cycle characteristics.

dry process was apt to have defects in crystal structure, which cause deterioration of crystallinity with repetition of charge and discharge, resulting in decrease of cycle capacity.

5 Moreover, lithium manganate is smaller in diffusion coefficient of lithium ion as compared with lithium cobaltate having a layered rock salt structure which has been practically used as active material for positive electrode of lithium ion secondary batteries. On
10 the other hand, the lithium manganate of the present invention has cubic particle form and contains voids in the particles, and thus is excellent in crystallinity. That is, it has conditions advantageous for insertion of lithium, and, hence, is preferred for attaining improvement
15 of current density.

INDUSTRIAL APPLICABILITY

The lithium manganate of the present invention has a cubic particle form and contains voids in the particles, and, therefore, lithium batteries using it as a
20 positive electrode material show a high initial discharge capacity and furthermore are excellent in cycle characteristics. In addition, the production process of the present invention is a process according to which lithium manganates having the above features can be advantageously
25 produced.

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CLAIMS:

1. A process for producing a lithium manganate, which method comprises:

reacting a manganese compound with an alkali to
5 obtain a manganese hydroxide;

oxidizing the hydroxide in an aqueous medium or a gaseous phase to obtain a manganese oxide;

reacting the manganese oxide with a lithium compound in an aqueous medium to obtain a lithium manganate
10 precursor; and

firing the precursor to obtain the lithium manganate.

2. A process for producing a lithium manganate, which method comprises:

15 reacting a manganese compound with an alkali to obtain a manganese hydroxide;

oxidizing the hydroxide in an aqueous medium or a gaseous phase to obtain a manganese oxide;

20 reacting the manganese oxide with an acid in an aqueous medium to substitute a proton for a part of manganese to obtain a proton-substituted manganese oxide;

reacting the proton-substituted manganese oxide with a lithium compound in an aqueous medium to obtain a lithium manganate precursor; and

25 firing the precursor to obtain the lithium manganate.

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3. The process according to claim 2, wherein the acid is at least one member selected from hydrochloric acid, sulfuric acid, nitric acid and hydrofluoric acid.

4. The process according to any one of claims 1 to 3,
5 wherein the manganese oxide or the proton-substituted manganese oxide is reacted with the lithium compound in the aqueous medium at a temperature of 50°C or higher to obtain the lithium manganate precursor.

5. The process according to any one of claims 1 to 3,
10 wherein the manganese oxide or the proton-substituted manganese oxide is reacted with the lithium compound in the aqueous medium at a temperature of 100 to 250°C to obtain the lithium manganate precursor.

6. The process according to any one of claims 1 to 5,
15 wherein the lithium manganate precursor is fired at a temperature of 250 to 840°C.

7. The process according to any one of claims 1 to 6, wherein the manganese compound reacted with the alkali is a water-soluble manganese compound.

20 8. The process according to claim 7, wherein the water-soluble manganese compound is selected from manganese sulfate, manganese chloride, manganese nitrate and manganese acetate.

9. The process according to any one of claims 1 to 8,
25 wherein the alkali is selected from sodium hydroxide, potassium hydroxide, lithium hydroxide, ammonia gas, aqueous ammonia, sodium carbonate, potassium carbonate, lithium carbonate and ammonium carbonate.

10. The process according to any one of claims 1 to 9,
30 wherein the manganese oxide or the proton-substituted

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manganese oxide and the lithium compound are subjected to hydro-thermal treatment in the aqueous medium in the step of reacting the manganese oxide or proton-substituted manganese oxide with the lithium compound in the aqueous medium to
5 obtain the lithium manganate precursor.

11. The process according to any one of claims 1 to 10, wherein the lithium compound is lithium hydroxide.

12. The process according to any one of
10 claims 1 to 11, wherein an oxidizing agent is fed in a reactor in a batch-wise or continuous manner in the step of reacting the manganese oxide or proton-substituted manganese oxide with the lithium compound in the aqueous medium to obtain the lithium manganate precursor.

15 13. The process according to claims 12, wherein the oxidizing agent is at least one member selected from air, oxygen, ozone, aqueous hydrogen peroxide and peroxodisulfate.

14. A process for producing lithium manganate of the
20 formula $\text{Li}_x\text{Mn}_y\text{O}_4$ in which x and y have such values that x/y is from 0.3 to 1.5, having a cubic particle form, containing voids in particles at a content of 0.01 to 0.7 ml/g and providing an initial discharge capacity of at least 95 mAh/g when used as an active material for a
25 positive electrode of a lithium battery, which process comprises:

(1) (a) reacting a water-soluble manganese compound with an alkali in an aqueous medium or (b) reacting a manganese solution containing at least one of Mn^{2+} , Mn^{3+} and
30 Mn^{4+} ions obtained by dissolving a hardly water-soluble manganese compound selected from the group consisting of MnO_2 ,

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hydrates thereof, Mn_2O_3 , hydrates thereof, MnO , Mn_3O_4 and organic manganese compounds in an acid, with an alkali in an aqueous medium, each at a temperature of from 10 to 80°C, thereby obtaining manganese hydroxide;

5 (2) oxidizing the manganese hydroxide obtained in the step (1), (a) in the aqueous medium by blowing air, oxygen or ozone into the aqueous medium or adding aqueous hydrogen peroxide or a peroxodisulfate to the aqueous medium, at a temperature of from 10 to 90°C or (b) in a
10 gaseous phase by filtering or washing an aqueous medium containing the manganese hydroxide and drying the manganese hydroxide in air at a temperature of from room temperature to 300°C, thereby obtaining manganese oxide comprising
15 $2\text{MnO} \cdot \text{MnO}_2$ with a $\text{Mn}^{2+}/\text{Mn}^{4+}$ molar ratio in the range of 1-3 and having a specific surface area of 10-40 m^2/g , a void content of 0.08-0.3 ml/g and a particle diameter of 0.08-0.15 μm ;

 (3) reacting the manganese oxide obtained in the step (2) with a lithium compound selected from the group consisting of lithium hydroxide and lithium carbonate in an
20 aqueous medium at a temperature of 50 to 250°C, thereby obtaining a lithium manganate precursor that contains a solid solution of (i) $2\text{MnO} \cdot \text{MnO}_2$ and (ii) at least one of $\text{Li}_2\text{O} \cdot \text{MnO} \cdot \text{MnO}_2$, LiMn_2O_4 and LiMnO_2 ; and

 (4) firing the lithium manganate precursor
25 obtained in the step (3) at a temperature of 250 to 840°C, thereby obtaining the desired lithium manganate.

15. The process according to claim 14, wherein the reaction of the step (3) is conducted at a temperature of 100 to 250°C in an autoclave to carry out a hydrothermal
30 treatment at least once under saturated steam pressure or under pressurization.

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16. The process according to claim 14 or 15, wherein the reaction of the step (3) is conducted using at least one oxidizing agent of air, oxygen, ozone, aqueous hydrogen peroxide and peroxodisulfate.

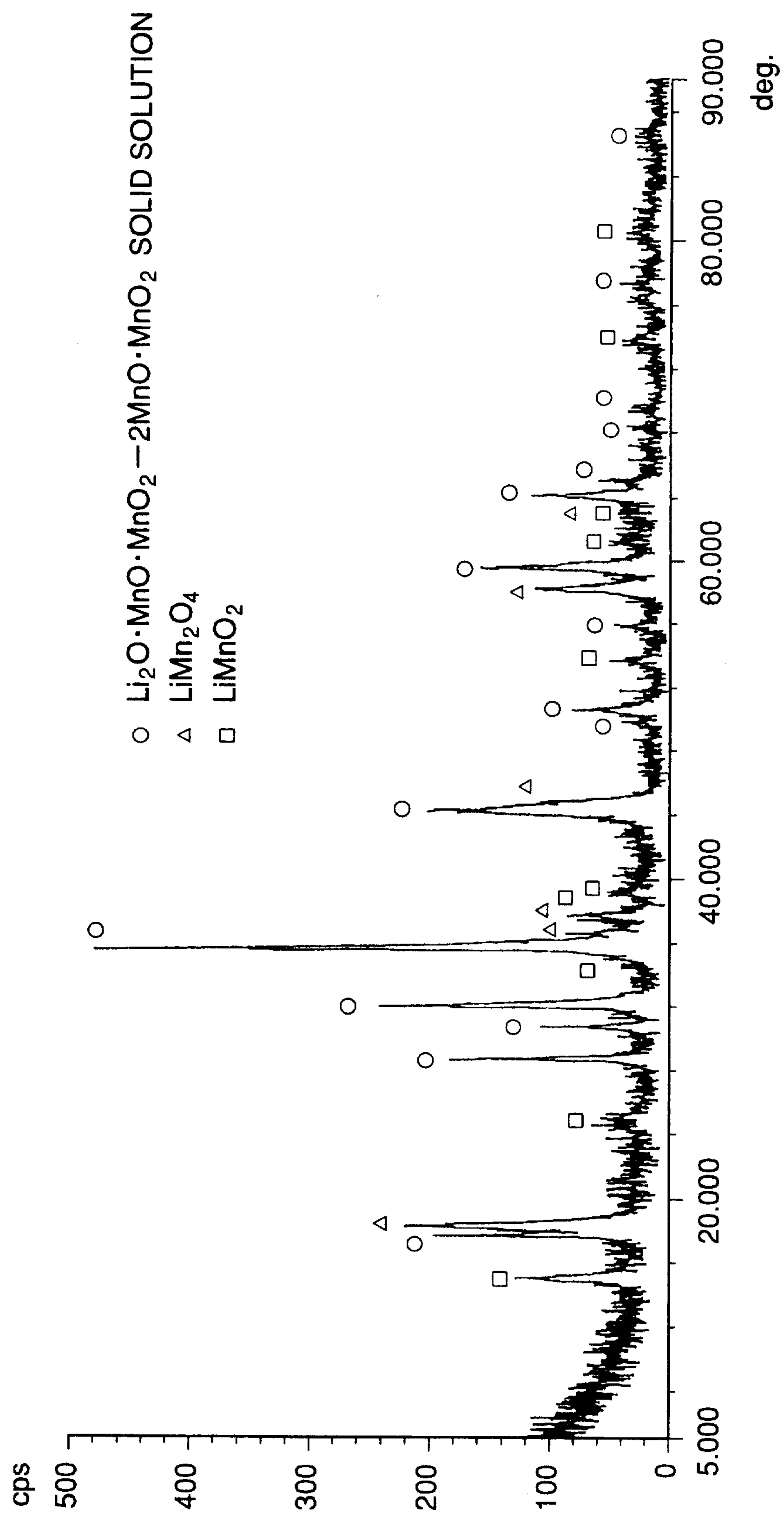
FETHERSTONHAUGH & CO.

OTTAWA, CANADA

PATENT AGENTS

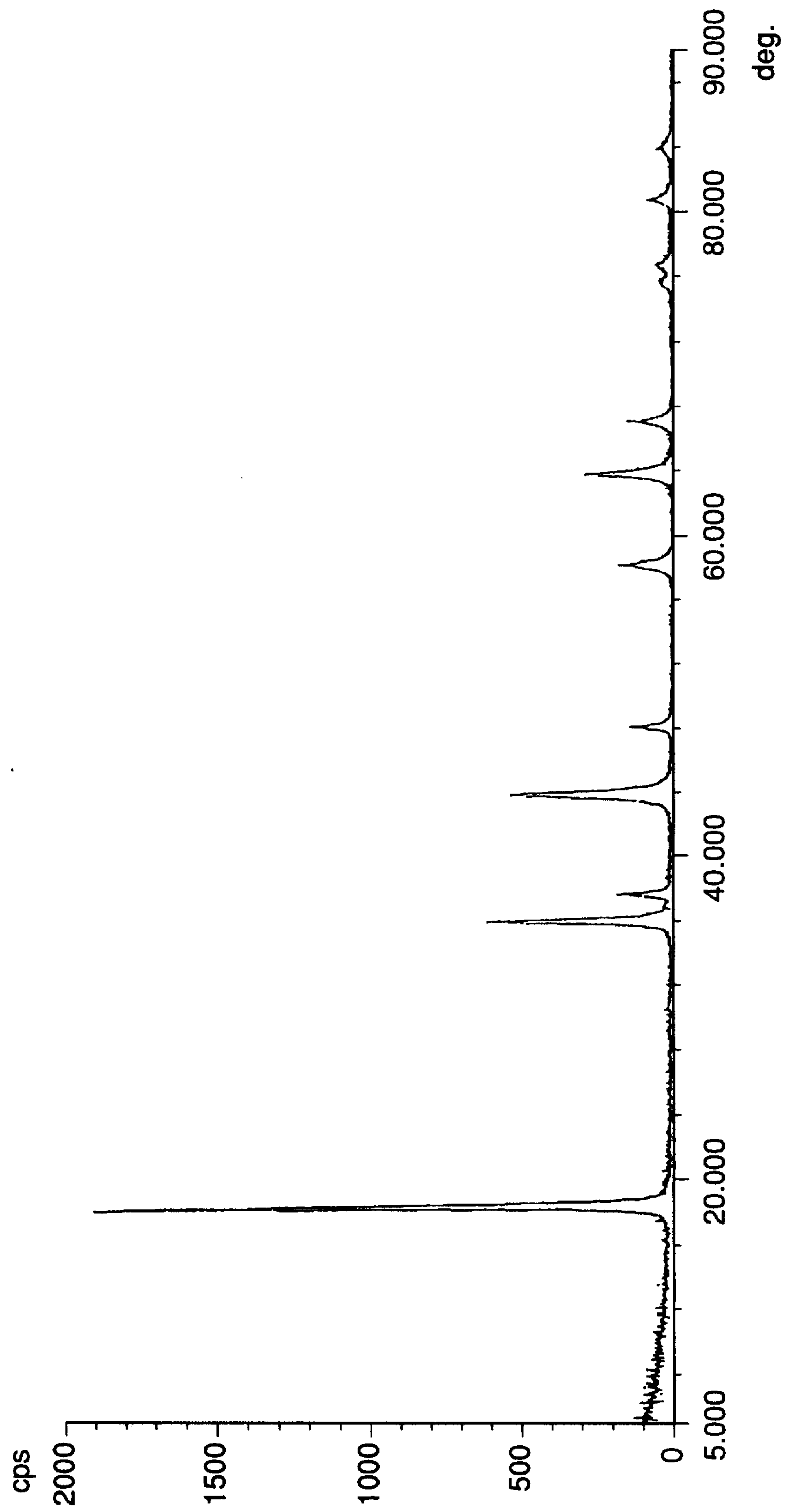
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FIG. 1



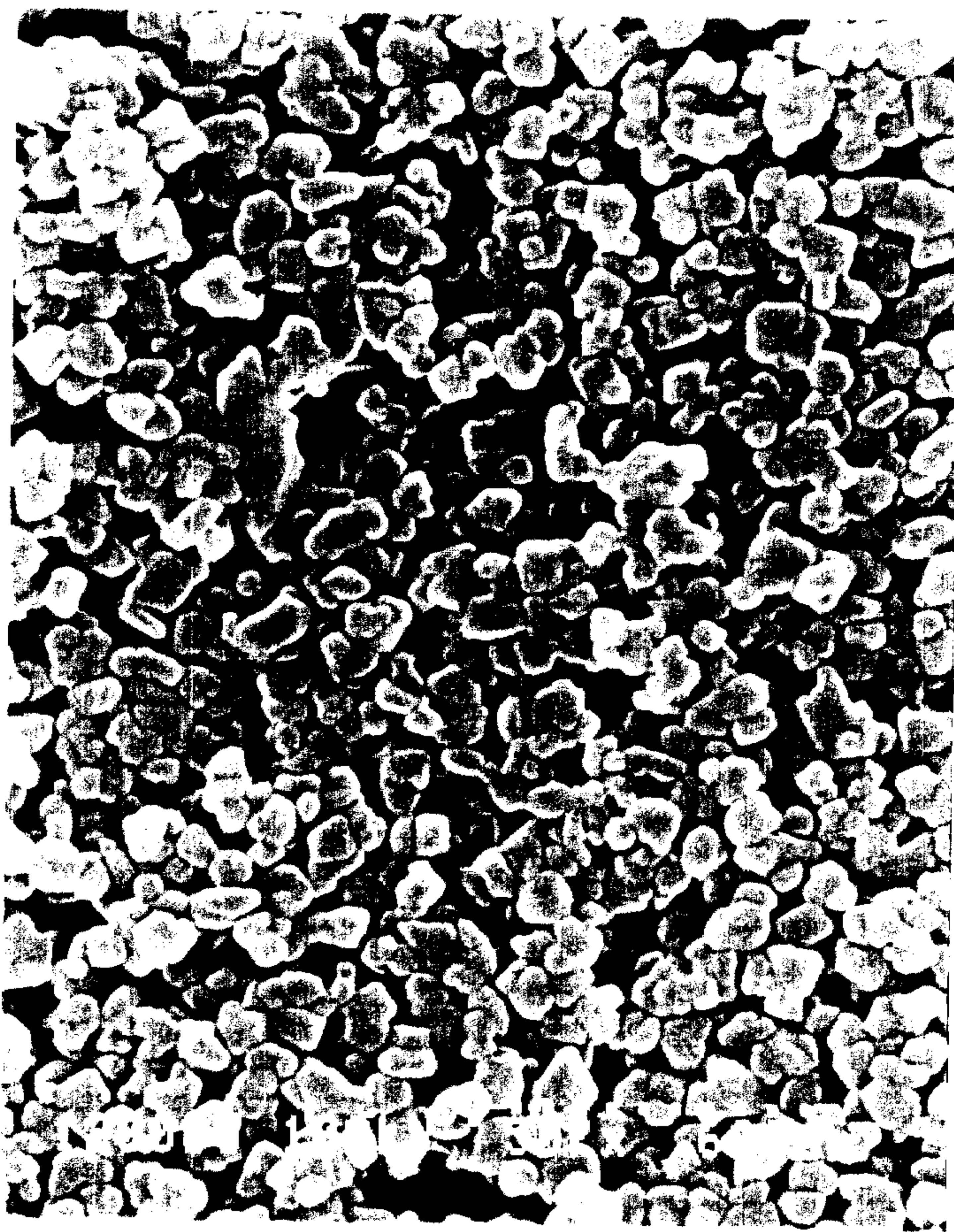
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FIG. 2



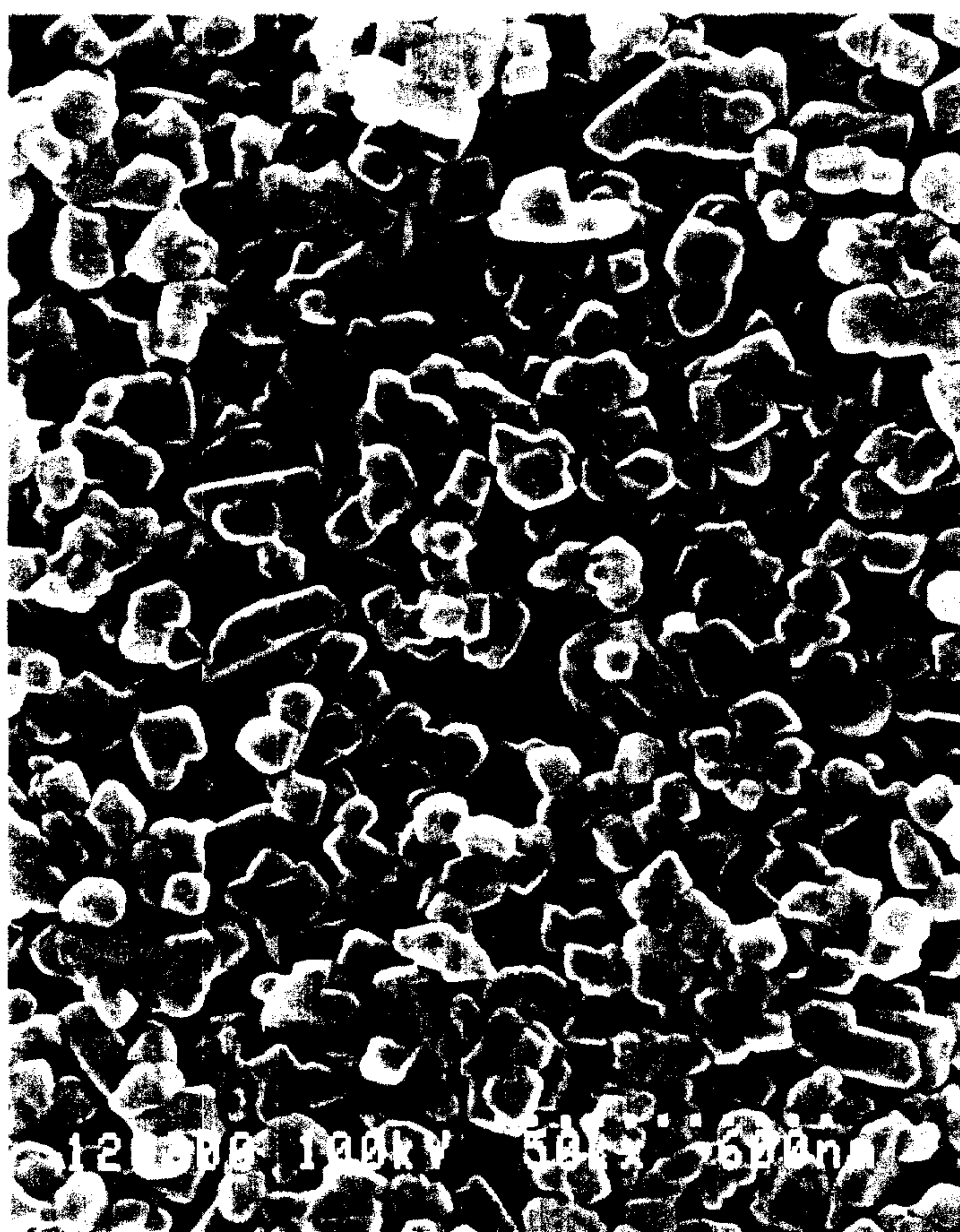
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FIG. 3



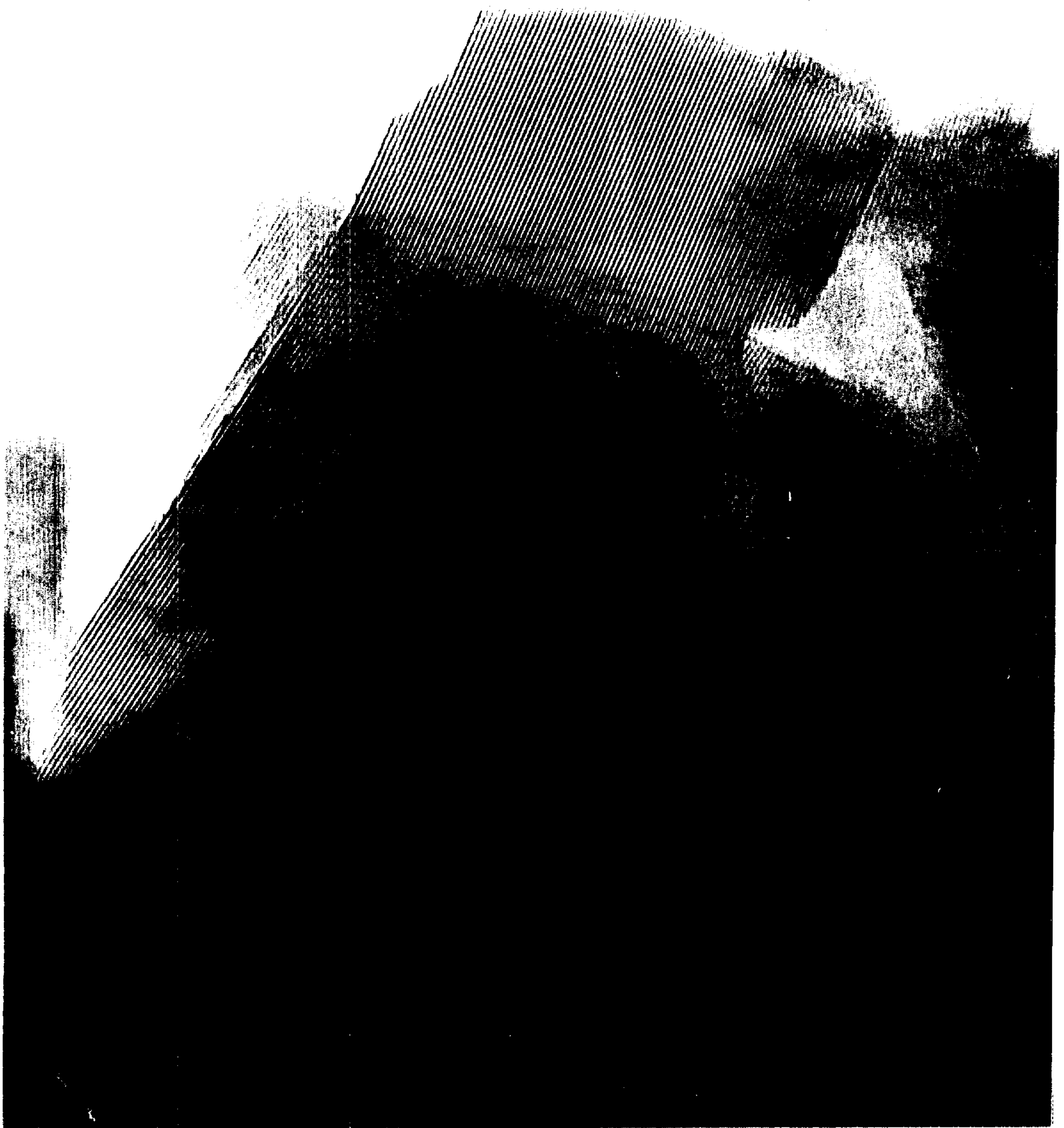
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FIG. 4



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FIG. 5



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FIG. 6



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FIG. 7



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