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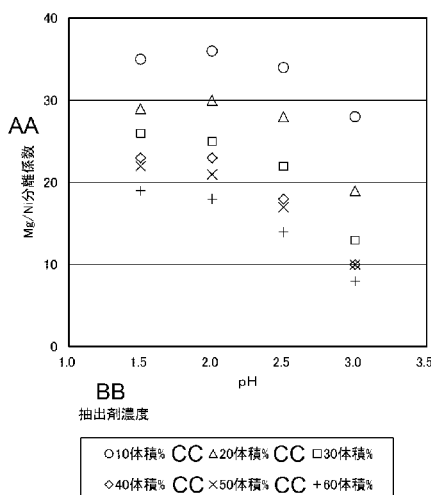


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(54) Title: SOLVENT EXTRACTION METHOD

(54) 発明の名称: 溶媒抽出方法



AA Mg/Ni separation coefficient
BB Concentration of extraction agent
CC vol%

(57) Abstract: Provided is a solvent extraction method capable of selectively separating magnesium from an acidic aqueous solution of sulfuric acid. This solvent extraction method is for extracting magnesium in an organic solvent by bringing an acidic aqueous solution, of sulfuric acid, containing nickel, cobalt, and magnesium into contact with the organic solvent. As the organic solvent, one that is obtained by diluting an extraction agent containing an alkyl phosphonic acid ester with a diluent is used. The concentration of the extraction agent is 40-60 vol%, and the pH of the acidic aqueous



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solution of sulfuric acid is 1.5-2.0. Alternatively, the concentration of the extraction agent is 20-50 vol%, and the pH of the acidic aqueous solution of sulfuric acid is 2.0-2.5.

(57) 要約: 硫酸酸性水溶液からマグネシウムを選択的に分離できる溶媒抽出方法を提供する。ニッケル、コバルト、およびマグネシウムを含有する硫酸酸性水溶液と有機溶媒とを接触させて、マグネシウムを有機溶媒に抽出する溶媒抽出方法である。有機溶媒としてアルキルホスホン酸エステルからなる抽出剤を希釈剤で希釈したものをを用いる。抽出剤の濃度を40体積%以上、60体積%以下とし、かつ、硫酸酸性水溶液のpHを1.5以上、2.0以下とする。または、抽出剤の濃度を20体積%以上、50体積%以下とし、かつ、硫酸酸性水溶液のpHを2.0以上、2.5以下とする。

DESCRIPTION

TITLE OF INVENTION

SOLVENT EXTRACTION METHOD

TECHNICAL FIELD

[0001] The present invention relates to a solvent extraction method. More specifically, the present invention relates to a solvent extraction method to separate magnesium from an acidic aqueous solution of sulfuric acid containing nickel, cobalt, and magnesium.

BACKGROUND ART

[0002] Various positive electrode materials have been developed as a positive electrode material of a lithium-ion battery as a secondary battery. A nickel-cobalt-manganese (NCM)-based positive electrode material referred to as a ternary system and a nickel-cobalt-aluminum (NCA)-based positive electrode material referred to as a nickel-base have been recently gathering attention.

[0003] The positive electrode material containing nickel like the NCM-based positive electrode material and the NCA-based positive electrode material are manufactured by processing an aqueous solution containing a salt of a metal, such as nickel, with an alkali and performing a burning process on the obtained metallic hydroxide. The metal salt used as the raw material includes chloride (nickel chloride) and sulfate (nickel sulfate). The use of the chloride generates a chlorine gas in the burning process, and therefore a firing furnace is likely to be corroded. Therefore, the sulfate is generally used as the metal salt.

[0004] The sulfate is, for example, manufactured by nickel smelting using a nickel oxide ore as a raw material. The nickel-oxidized ore usually contains a cobalt oxide. Therefore, the nickel smelting obtains an acidic aqueous solution of sulfuric acid containing nickel and cobalt. There may be a case where this acidic aqueous solution of sulfuric acid contains magnesium as impurities.

[0005] Manufacturing the positive electrode material with the acidic aqueous solution of sulfuric acid containing the magnesium as the raw material results in containing the magnesium as the impurities in the positive electrode material. A lithium-ion battery using the positive electrode material possibly deteriorates battery properties, such as a charge/discharge capacity. Accordingly, preliminarily removing the magnesium from the acidic aqueous solution of sulfuric acid is desired.

[0006] Patent Document 1 discloses that a solvent extraction method separates and recovers a nickel sulfate aqueous solution and a cobalt sulfate aqueous solution from an acidic aqueous solution of sulfuric acid containing nickel and cobalt. Use of a monothiophosphinic acid compound as an extractant allows obtaining a cobalt sulfate aqueous solution that hardly contains

magnesium. However, the magnesium is contained in the nickel sulfate aqueous solution. Thus, selectively separating the magnesium from the acidic aqueous solution of sulfuric acid containing the nickel and the magnesium is difficult.

Citation list

Patent document

[0007] Patent Document 1: Japanese Patent No. 4225514

SUMMARY OF INVENTION

[0008] In consideration of the circumstances, the present invention seeks to provide a solvent extraction method that allows selectively separating magnesium from an acidic aqueous solution of sulfuric acid containing nickel, cobalt, and magnesium.

[0009] A solvent extraction method according to a first invention includes: bringing an acidic aqueous solution of sulfuric acid containing nickel, cobalt, and magnesium in contact with an organic solvent to extract the magnesium into the organic solvent; and using the organic solvent produced by diluting an extractant made of bis(2-ethylhexyl) hydrogen phosphate with a diluent. A concentration of the extractant in the organic solvent is set to 40 volume% or more and 60 volume% or less and a pH of the acidic aqueous solution of sulfuric acid is set to 1.5 or more and 2.0 or less.

In a solvent extraction method according to a second invention, which is in the first invention, the concentration of the extractant in the organic solvent is set to 40 volume% or more and 50 volume% or less.

[0009a] According to another aspect, the present invention provides a solvent extraction method comprising: bringing an acidic aqueous solution of sulfuric acid containing nickel, cobalt, and magnesium in contact with an organic solvent to extract the magnesium into the organic solvent; and wherein the organic solvent is produced by diluting an extractant made of bis(2-ethylhexyl) hydrogen phosphate with a diluent, wherein a concentration of the extractant in the organic solvent is set to 40 volume% or more and 60 volume% or less and a pH of the acidic aqueous solution of sulfuric acid is set to 1.5 or more and 2.0 or less.

Advantageous effects of invention

[0010] The present invention allows selectively separating the magnesium from the acidic aqueous solution of sulfuric acid containing the nickel, the cobalt, and the magnesium.

BRIEF DESCRIPTION OF DRAWINGS

- [0011] Fig. 1 is a graph showing a nickel extraction rate.
Fig. 2 is a graph showing a cobalt extraction rate.
Fig. 3 is a graph showing a magnesium extraction rate.
Fig. 4 is a graph showing a Mg/Co separation factor.
Fig. 5 is a graph showing a Mg/Ni separation factor.

DESCRIPTION OF EMBODIMENTS

[0012] Next, one embodiment of the present invention will be described.

A solvent extraction method of this embodiment brings an acidic aqueous solution of sulfuric acid containing nickel, cobalt, and magnesium in contact with an organic solvent to extract the magnesium into the organic solvent. While the nickel and the cobalt are caused to remain in a water phase, the magnesium is extracted to an organic phase to selectively separate the magnesium.

[0013] A device used for the solvent extraction is not specifically limited. A solvent extraction device includes a mixer-settler extractor.

[0014] As the organic solvent, a solvent produced by diluting an extractant with a diluent is employed. Alkylphosphonic acid ester is used as the extractant. The alkylphosphonic acid ester includes bis(2-ethylhexyl) hydrogen phosphate (D2EHPA), 2-ethylhexyl hydrogen-2-ethylhexylphosphonate (PC-88A), and Diisooctylphosphinic acid (CYANEX272). Among these substances, the bis(2-ethylhexyl) hydrogen phosphate is preferably used as the extractant.

[0015] As long as the extractant can be dissolved, the diluent is not specifically limited. As examples of the diluent, a naphthene-based solvent and an aromatic-based solvent can be employed.

[0016] The alkylphosphonic acid ester is one kind of an acid extractant. Taking only an action as the acid extractant into consideration, an extraction reaction is a pure acid-base reaction. An amount of substance of the extractant contributing to the extraction reaction is determined according to a concentration and a valence of an element to be extracted in the aqueous solution. In a case where the extraction reaction to all the elements is the acid-base reaction, a separation factor between the elements does not depend on the concentration of the extractant in the organic solvent.

[0017] Note that the alkylphosphonic acid ester also acts as a chelate extractant. The alkylphosphonic acid ester contains phosphorus and oxygen in molecules. In addition to the acid-base reaction, an element that forms a coordinate bond with phosphorus or oxygen is extracted by formation of a chelate compound. Increasing the concentration of the extractant in the organic

solvent promotes the formation of the chelate compound. Among the elements in the aqueous solution, an element that facilitates the formation of the chelate compound increases an extraction rate compared with that of an element that is less likely to form the chelate compound.

[0018] A formation trend of the chelate compound by nickel, cobalt, and magnesium is in the order of nickel > cobalt \approx magnesium. That is, the nickel preferentially forms the chelate compound. As the concentration of the extractant increases, the extraction of the nickel is promoted compared with that of the magnesium, and therefore a separation factor of the magnesium relative to the nickel (hereinafter referred to as a "Mg/Ni separation factor") decreases.

Meanwhile, the formation trends of the chelate compound of the cobalt and the magnesium are approximately the same. Accordingly, the concentration of the extractant hardly affects the separation factor of the magnesium relative to the cobalt (hereinafter referred to as a "Mg/Co separation factor"). Accordingly, as the concentration of the extractant decreases, the Mg/Ni separation factor can be increased, thereby ensuring efficiently separating the magnesium chemically.

[0019] However, the decrease in the concentration of the extractant reduces a reaction volume, resulting in decrease in the extraction rate of the magnesium. Industrially, some extent of the magnesium extraction rate needs to be maintained. Therefore, the concentration of the extractant is adjusted to ensure maintaining a desired magnesium extraction rate.

[0020] Appropriately adjusting the concentration of the extractant allows increasing the extraction rate of the magnesium while the extraction rates of the nickel and the cobalt are suppressed to be low. Specifically, the concentration of the extractant is preferably adjusted to be from 20 to 60 volume%. This allows selectively separating the magnesium from the acidic aqueous solution of sulfuric acid containing the nickel, the cobalt, and the magnesium.

[0021] In the acidic aqueous solution of sulfuric acid processed by the solvent extraction method according to this embodiment, the magnesium concentration decreases. Therefore, the acidic aqueous solution of sulfuric acid can be used as, for example, a raw material of a positive electrode material, such as an NCM-based positive electrode material and an NCA-based positive electrode material.

[0022] Note that the solvent extraction method according to this embodiment extracts the magnesium as impurities in the organic solvent. In a case where the nickel and the cobalt, which are the objective metals, are extracted in the organic solvent, the objective metals in the organic phase need to be back-extracted in a water phase in a post-process. In a case where a large amount of the objective metals is contained in the acidic aqueous solution of sulfuric acid, a large amount of an agent used for the back extraction, such as alkali and acid, is required. In contrast to this, since the objective metals remain in the water phase in this embodiment, the operation of back-extracting the objective metals is unnecessary. Additionally, since the magnesium extracted in the organic phase is a trace, usage of the agent used for the back extraction of the magnesium can be reduced.

Examples

[0023] Next, the examples will be described.

First, an acidic aqueous solution of sulfuric acid containing nickel, cobalt, and magnesium was prepared as a raw solution. A nickel concentration is 120 g/L, a cobalt concentration is 5 g/L, and a magnesium concentration is 5 g/L in the acidic aqueous solution of

sulfuric acid.

[0024] Next, an extractant was diluted with a diluent to prepare an organic solvent. Bis(2-ethylhexyl) hydrogen phosphate (BAYSOLVEX D2EHPA manufactured by LANXESS Corporation) was used as the extractant. A naphthene-based solvent (Teclean N20 manufactured by JXTG Nippon Oil & Energy Corporation) was used as the diluent. Six kinds of organic solvents whose concentrations of the extractants were different were prepared. The concentrations of the extractants in the respective organic solvents are 10 volume%, 20 volume%, 30 volume%, 40 volume%, 50 volume%, and 60 volume%.

[0025] 20 ml of the raw solution and 20 ml of the organic solvent were put in a 50 ml beaker and stirred for 20 minutes. During the stirring, a sulfuric acid or sodium hydroxide aqueous solution was added, and a pH of a water phase (acidic aqueous solution of sulfuric acid) was adjusted to be any of 1.5, 2.0, 2.5, and 3.0. Note that a final additive amount of the sulfuric acid and the sodium hydroxide aqueous solutions was 1 ml or less.

[0026] After ending the stirring, the mixed liquid was left for phase separation and the water phase (acidic aqueous solution of sulfuric acid) and an organic phase (organic solvent) were each recovered. A nickel concentration, a cobalt concentration, and a magnesium concentration of the water phase and the organic phase were analyzed by ICP optical emission spectrometer. Respective masses of the nickel, the cobalt, and the magnesium in the organic phase were obtained from analysis values. Extraction rates of the nickel, the cobalt, and the magnesium were each calculated by dividing the mass in the organic phase by a mass in the raw solution. Distribution ratios of the nickel, the cobalt, and the magnesium were each calculated by dividing the concentration in the organic phase by the concentration in the water phase. Then, the distribution ratio of the magnesium was divided by the distribution ratio of the cobalt to obtain a Mg/Co separation factor. The distribution ratio of the magnesium was divided by the distribution ratio of the nickel to obtain a Mg/Ni separation factor.

[0027] Table 1 and Fig. 1 show the extraction rate of the nickel. Table 2 and Fig. 2 show the extraction rate of the cobalt. Table 3 and Fig. 3 show the extraction rate of the magnesium. Table 4 and Fig. 4 show the Mg/Co separation factor. Table 5 and Fig. 5 show the Mg/Ni separation factor.

[0028]

[Table 1]

Ni Extraction Rate [%]

pH	Extractant concentration [volume%]					
	10	20	30	40	50	60
1.5	0.01	0.04	0.10	0.18	0.31	0.53

2.0	0.06	0.15	0.58	0.92	1.26	2.00
2.5	0.19	0.48	1.50	2.50	3.41	4.75
3.0	0.39	1.08	2.90	5.17	6.67	9.17

[0029]

[Table 2]

Co Extraction Rate [%]

pH	Extractant concentration [volume%]					
	10	20	30	40	50	60
1.5	0.1	0.2	0.4	0.7	1.1	1.6
2.0	0.4	0.8	2.5	3.6	4.5	6.2
2.5	1.3	2.8	6.8	9.1	11.2	13.6
3.0	3.7	7.0	12.8	17.8	20.4	23.1

[0030]

[Table 3]

Mg Extraction Rate [%]

pH	Extractant concentration [volume%]					
	10	20	30	40	50	60
1.5	0	1	3	4	6	9
2.0	2	4	13	17	21	27
2.5	6	12	26	32	37	42
3.0	10	18	28	36	41	46

[0031]

[Table 4]

Mg/Co Separation Factor

pH	Extractant concentration [volume%]					
	10	20	30	40	50	60
1.5	5.5	5.9	6.0	6.1	5.8	5.9
2.0	5.7	5.8	5.8	5.6	5.7	5.6
2.5	4.9	4.8	4.7	4.7	4.6	4.6
3.0	2.9	2.8	2.7	2.6	2.8	2.8

[0032]

[Table 5]

Mg/Ni Separation Factor

pH	Extractant concentration [volume%]					
	10	20	30	40	50	60
1.5	35	29	26	23	22	19
2.0	36	30	25	23	21	18
2.5	34	28	22	18	17	14
3.0	28	19	13	10	10	8

[0033] As seen from Fig. 1 to Fig. 3, as the pH increases, the extraction rate of each metallic element increases. In the case of the nickel and the cobalt, as the pH increases, the extraction rate increases in an accelerated manner. Meanwhile, in the case of the magnesium, especially setting the concentration of the extractant to 30 volume% or more asymptotically increases the extraction rate as the pH increases. Accordingly, it is predicted that the low pH improves separation efficiency of the magnesium from the nickel and the cobalt.

[0034] The separation factors back up the above-described prediction. As seen from Fig. 4, the lower the pH is, the higher the Mg/Co separation factor becomes. Additionally, as seen from Fig. 5, as the pH decreases, the Mg/Ni separation factor tends to be high. Accordingly, it can be said that the decrease in pH facilitates separating the magnesium from the nickel and the cobalt.

[0035] As seen from Fig. 4, the concentration of the extractant hardly affects the Mg/Co separation factor. Meanwhile, as seen from Fig. 5, the Mg/Ni separation factor depends on the concentration of the extractant. The lower the concentration of the extractant is, the higher the Mg/Ni separation factor becomes. That is, as the concentration of the extractant lowers, the separation of the magnesium from the nickel and the cobalt is facilitated.

[0036] However, as seen from Fig. 3, the lower the concentration of the extractant is, the lower the extraction rate of the magnesium becomes. When the extraction rate of the magnesium is excessively low, it is not realistic to industrially separate the magnesium from the acidic aqueous solution of sulfuric acid.

[0037] Therefore, it is preferred that the concentration of the extractant is set to be 40 volume% or more and the pH of the acidic aqueous solution of sulfuric acid is set to be 1.5 or more, the concentration of the extractant is set to be 20 volume% or more and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.0 or more, or the concentration of the extractant is set to be 10 volume% or more and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.5 or more. Doing so allows obtaining the extraction rate of the magnesium of 4% or more. Additionally, it is more preferred that the concentration of the extractant is set to be 30 volume% or more and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.0 or more, or the concentration of the extractant is set to be 20 volume% or more and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.5 or more. Doing so allows obtaining the extraction rate of the magnesium of 10% or more.

[0038] As seen from Fig. 4, from a perspective of separating the magnesium from the cobalt, the pH of the acidic aqueous solution of sulfuric acid is preferably set to be 2.5 or less. Doing so allows obtaining the Mg/Co separation factor of 4 or more.

[0039] As seen from Fig. 5, from a perspective of separating the magnesium from the nickel, it is preferred that the concentration of the extractant is set to be 50 volume% or less and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.5 or less, or the concentration of the extractant is set to be 60 volume% or less and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.0 or less. Doing so allows obtaining the Mg/Ni separation factor of 15 or more. Additionally, it is more preferred that the concentration of the extractant is set to be 30 volume% or less and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.5 or less, or the concentration of the extractant is set to be 50 volume% or less and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.0 or less. Doing so allows obtaining the Mg/Ni separation factor of 20 or more.

[0040] In conclusion, it is preferred that the concentration of the extractant is set to be 40 to 60 volume% and the pH of the acidic aqueous solution of sulfuric acid is set to be 1.5 to 2.0, or the concentration of the extractant is set to be 20 to 50 volume% and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.0 to 2.5. Doing so allows obtaining the extraction rate of the magnesium of 4% or more, the Mg/Co separation factor of 4 or more, and the Mg/Ni separation factor of 15 or more.

[0041] It is more preferred that the concentration of the extractant is set to be 40 to 50 volume% and the pH of the acidic aqueous solution of sulfuric acid is set to be 1.5 to 2.0, or the concentration of the extractant is set to be 20 to 30 volume% and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.0 to 2.5. Doing so allows obtaining the extraction rate of the magnesium of 4% or more, the Mg/Co separation factor of 4 or more, and the Mg/Ni separation factor of 20 or more.

[0042] It is further preferred that concentration of the extractant is set to be 30 to 50 volume% and the pH of the acidic aqueous solution of sulfuric acid is set to be 2.0 to 2.5. Doing so allows obtaining the extraction rate of the magnesium of 10% or more, the Mg/Co separation factor of 4 or more, and the Mg/Ni separation factor of 15 or more.

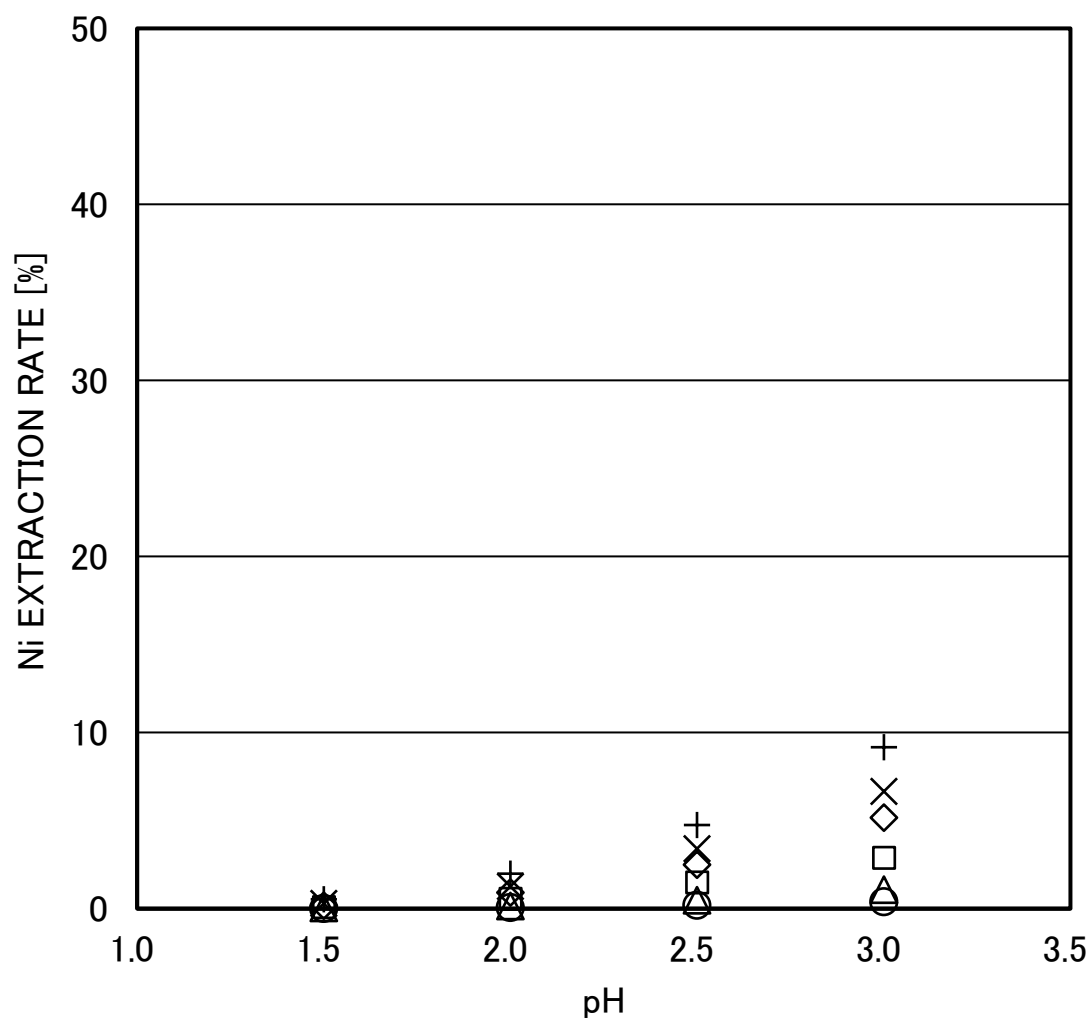
[0043] Throughout this specification and the claims which follow, unless the context requires otherwise, the word "comprise", and variations such as "comprises" or "comprising", will be understood to imply the inclusion of a stated integer or step or group of integers or steps but not the exclusion of any other integer or step or group of integers or steps.

[0044] The reference in this specification to any prior publication (or information derived from it), or to any matter which is known, is not, and should not be taken as, an acknowledgement or admission or any form of suggestion that that prior publication (or information derived from it) or known matter forms part of the common general knowledge in the field of endeavour to which this specification relates.

The claims defining the invention are as follows:

1. A solvent extraction method comprising:
bringing an acidic aqueous solution of sulfuric acid containing nickel, cobalt, and magnesium in contact with an organic solvent to extract the magnesium into the organic solvent;
and
wherein the organic solvent is produced by diluting an extractant made of bis(2-ethylhexyl) hydrogen phosphate with a diluent, wherein
a concentration of the extractant in the organic solvent is set to 40 volume% or more and 60 volume% or less and a pH of the acidic aqueous solution of sulfuric acid is set to 1.5 or more and 2.0 or less.
2. The solvent extraction method according to claim 1, wherein
the concentration of the extractant in the organic solvent is set to 40 volume% or more and 50 volume% or less.

Fig.1



EXTRACTANT CONCENTRATION

○ 10 volume%

△ 20 volume%

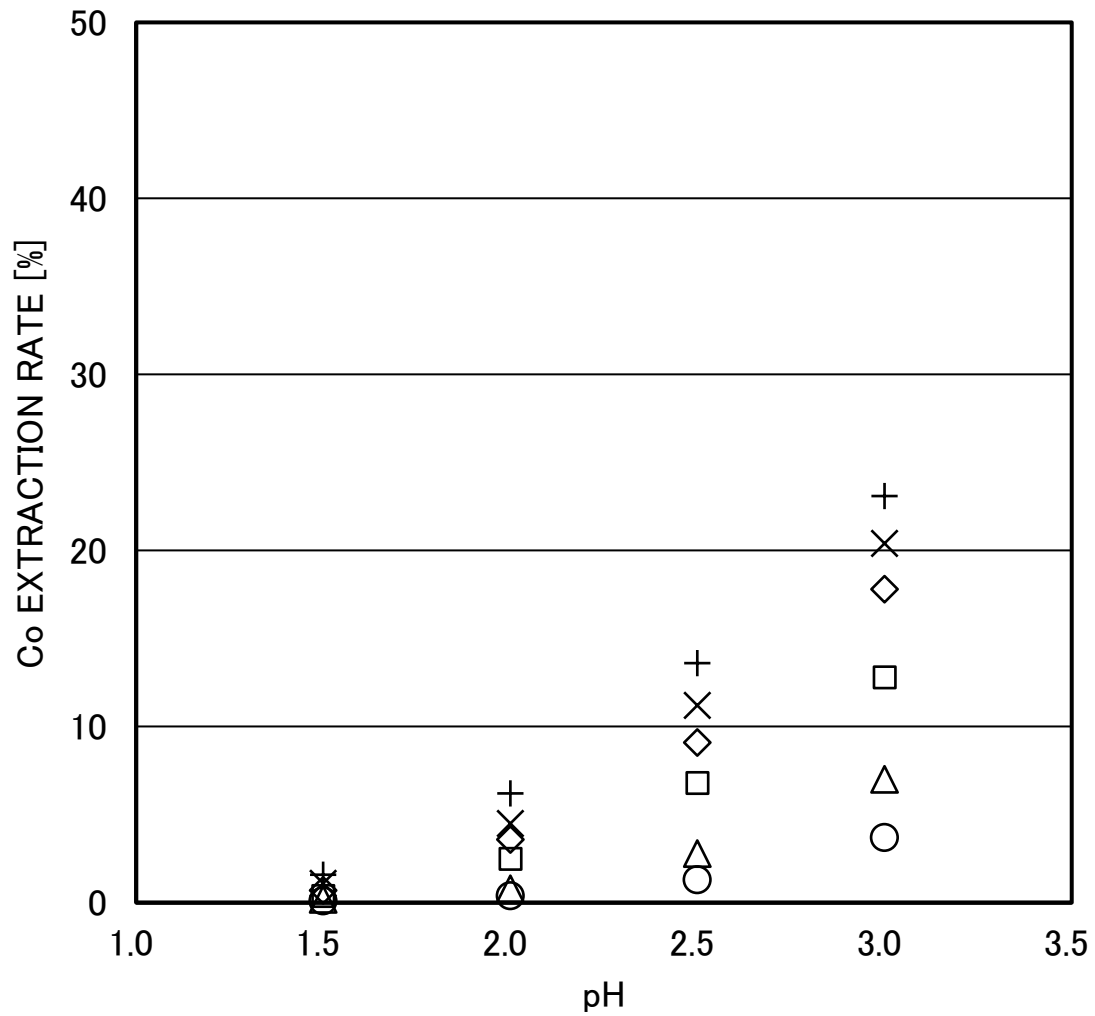
□ 30 volume%

◇ 40 volume%

× 50 volume%

+ 60 volume%

Fig.2



EXTRACTANT CONCENTRATION

○ 10 volume%

△ 20 volume%

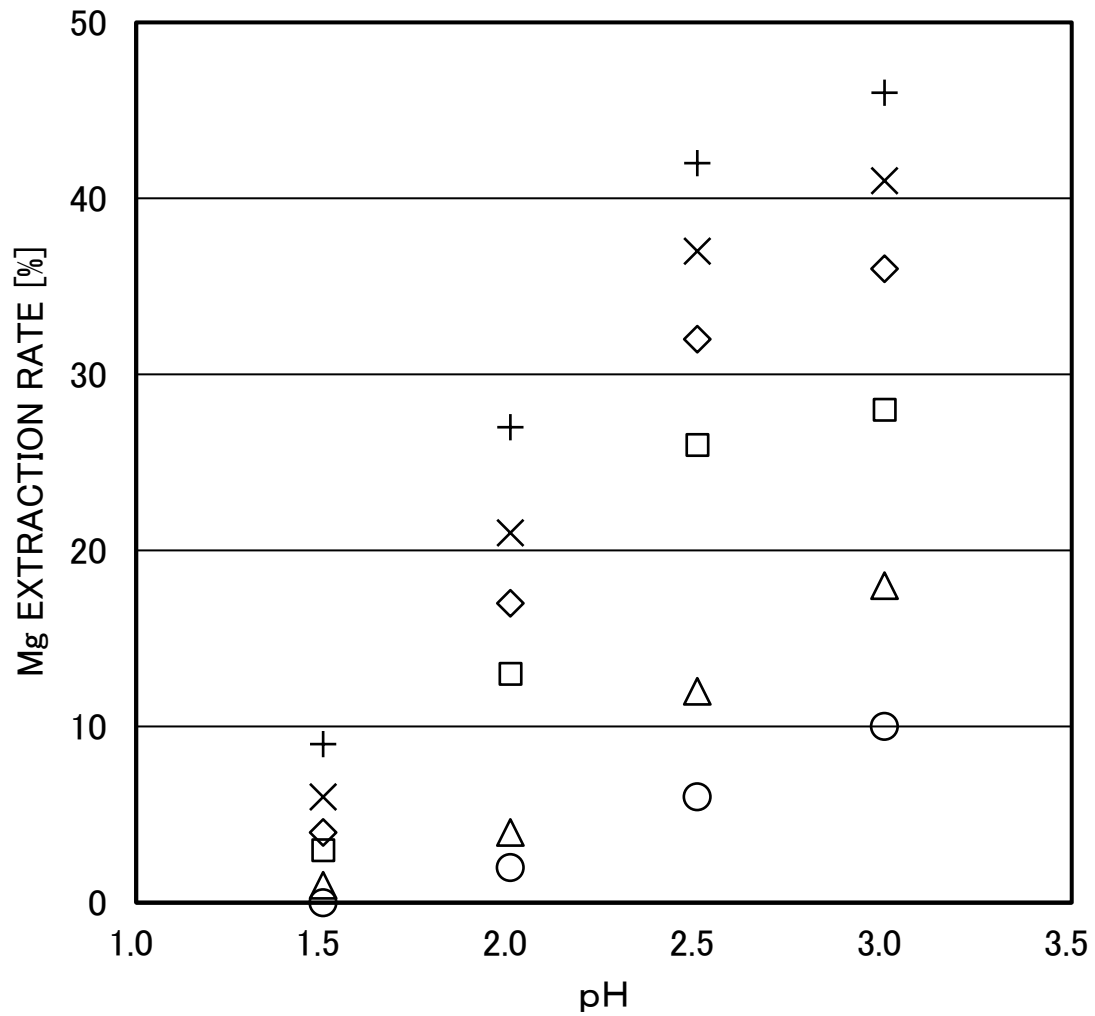
□ 30 volume%

◇ 40 volume%

× 50 volume%

+ 60 volume%

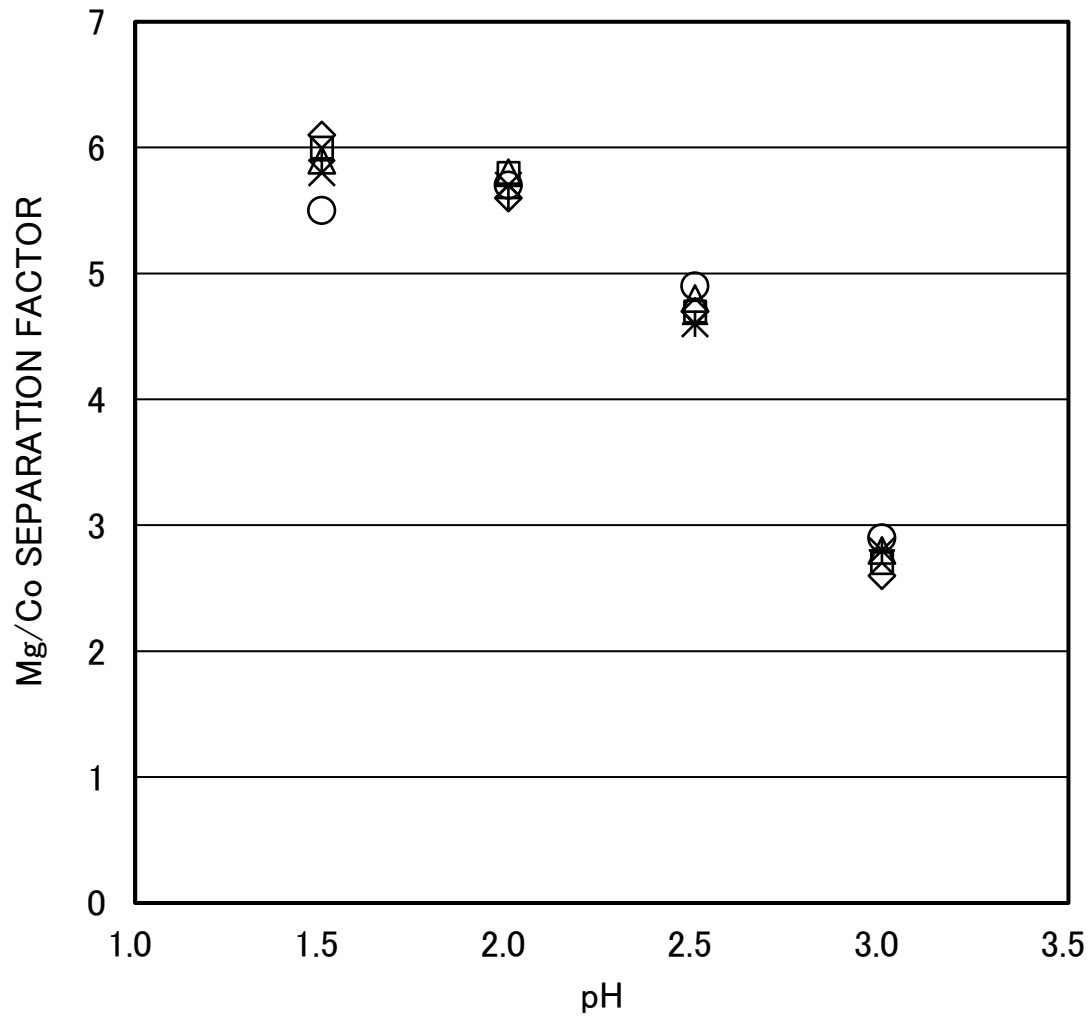
Fig.3



EXTRACTANT CONCENTRATION

○ 10 volume%	△ 20 volume%	□ 30 volume%
◇ 40 volume%	× 50 volume%	+ 60 volume%

Fig.4



EXTRACTANT CONCENTRATION

○ 10 volume%

△ 20 volume%

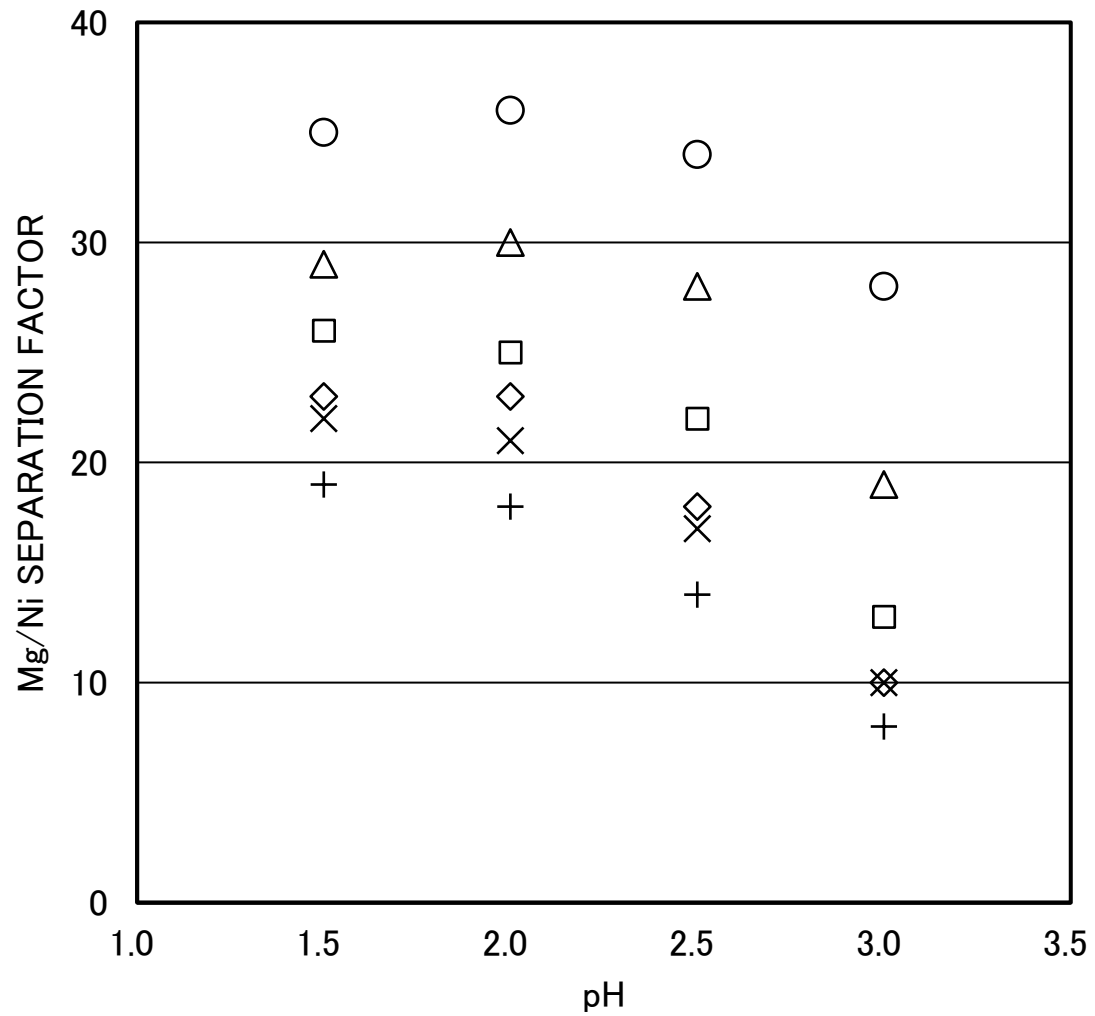
□ 30 volume%

◇ 40 volume%

× 50 volume%

+ 60 volume%

Fig.5



EXTRACTANT CONCENTRATION

○ 10 volume%

△ 20 volume%

□ 30 volume%

◇ 40 volume%

× 50 volume%

+ 60 volume%