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Fortsættes ...

DESCRIPTION

[0001] This group of inventions relates to shell-and-tube heat-exchanging devices, in particular to shell-and-tube condensers, and can be used in energy, oil processing, oil chemistry, chemical, gas and other industries. A heat exchanger having the features of the preamble of claim 1 is known from US 2011/0083619.

[0002] There are many technological solutions relating to heat-exchange devices. Their common feature is a shell that houses a bundle of heat exchange tubes, fixed in place with tube plates, distribution chambers, input and output channels for the shell-side heat carrier, and input and output channels for the tubes. New solutions are suggested all the time, designed to improve these devices, their exploitation properties in particular, including shall-and-tube condensers.

[0003] There is a shell-and-tube condenser, wherein heat-exchange tubes are made of polytetrafluorethylene (PTFE) or from metal with PTFE layer sprayed on the surface [CN1078802, priority date 1.12.1971, publication date 24.11.1993;] MPC: F28D7/10, F28D7/10].

[0004] There exists a shell-and-tube condenser, which comprises guiding spacers, and along the entire length of the shell, in its lower part, there is a tube with perforations and a rod of appropriate diameter inside the tube [SU409445, priority date 1.12.1971, publication date 30.11.1973; MPC: F28D7/00. F28F9/00].

[0005] A shell-and-tube condenser, wherein it includes a shell, containing a bundle of heat-exchange tubes, fixed in place with tube plates located on butt surfaces of the shell, an inlet and an outlet connecting tubes for the tube heat carrier, connecting tubes for the heat carrier inside the tubes, wherein the heat exchange tubes carry grooves on the outer surface [UA74177, priority date 24.02.2012, publication date: 25.10.2012, MPC F28F1/10] was chosen as the prototype for this group of inventions.

[0006] A drawback of the prototype is the high level of risk of decreasing heat transfer coefficient between the heat carriers inside the tubes and on the shell side due to the fact that the design of the tubes does not provide for efficient reduction of the condensate film forming on the outer surface, and it also permits formation of crystalline structures of poorly soluble compounds on the inner surface, the low heat conductivity of which considerably increases thermal resistance coefficient and thus impairs efficiency of the shell-and-tube condenser.

[0007] The technological problem that this group of inventions targets is increasing the total heat conductivity coefficient between the heat carriers inside the tubes and in the shell space.

[0008] The technological result that this group of inventions strives to achieve is decreasing the risk of increased thermal resistance between the heat carriers inside the tubes and in the

shell space of shell-and-tube condensers.

[0009] The substance of the shell-and-tube condenser from the invention is defined in claim 1.

[0010] Further embodiments of the invention are defined in the dependent claims.

[0011] The hydrophobic material ensures a water-repelling coating, thanks to which the condensate rolls off the outer surface. The hydrophobic material can be characterised by an interfacial angle. The interfacial angle in the 90°-150° ensures highest water-repelling characteristics of the outer surface of the heat exchange tube. Materials of this quality include synthetic polyamides or polymers, nylon, teflon, or polytetrafluorethylene.

[0012] The shortening space between the guiding spacers ensures that the heat carrier moves along the shell space with a permanent, optimal velocity, within the 65-120 m/sec. The heat carrier in the shell space, introduced to the condenser- via the inlet- in the form of steam, condenses while moving from the inlet to the outlet and from run to another. As fluid has a smaller volume than steam, the total volume of heat carrier in the shell space decreases, so that as steam continues to spread in the shell space, pressure during further runs of the system drops, and, in the end, steam velocity also decreases. Due to this main principle of the shortening distance between the guiding spacers average velocity of the steam is maintained constant for the duration of each pass of the heat carrier in the shell space. Consequently, the pass of the heat carrier in this case is the distance between two adjacent guiding spacers where steam moves along a straight line, normally to the tubes. Constant average velocity of the steam for each pass of the shell space heat carrier is ensured by a constant ratio of the average volumetric steam discharge during every pass of the heat carrier in the shell space to the sectional area of a particular pass of the heat carrier in the shell space.

[0013] That ratio is calculated with the following formula.

$$\left\{ \begin{array}{l} \frac{D'_1 + D''_1}{2F_1} = \frac{D'_2 + D''_2}{2F_2} = \frac{D'_{n-1} + D''_{n-1}}{2F_n} = \dots = \frac{D'_n}{F_n} \\ \sum_{i=1}^n (D'_i - D''_i) = D_{\text{total}} \\ \sum_{i=1}^n F_i = F \end{array} \right.$$

[0014] Where:

D'I is volumetric discharge of steam at the start of pass 1 of the shell space, m³/h

D''I is a volumetric discharge of steam at the end of pass 1 of the shell space, m³/h

F_i is a sectional area of a pass of the heat carrier in the shell space m^2

F is the total Sectional area of all passes, m^2

N is the total number of passes.

[0015] An extra means for maintaining constant velocity of the heat carrier in the shell space, especially in turning areas, that can be used is decreasing the area of the window between consecutive guiding spacers in comparison with the preceding ones.

[0016] The heat exchange tube of the shell-and-tube condenser carries grooves on its outer surface, which provides for the creation of sloping areas. This reduces the thickness of the condensate film that forms on the outer surface of the heat exchange tube, or keeps breaking it. The grooves can be of different shape and can be directed differently; they can form circular, helical, or polyhedral depressions. They can be produced by cutting, shearing, knurling or punching. according to the invention, have roundings with the radius measuring 0.04-0.1 of the outer diameter of the heat exchange tube, while the radius of roundings of the sloping areas of the outer surface may measure 0.3-2 of the outer diameter of the heat exchange tube. The depth of grooves can be 0.1-3 mm, while the distance between any two adjacent grooves depend on the outer diameter of the heat exchange tube; it can be greater or smaller than the diameter of the heat exchange tube; however, it must not exceed the diameter of heat exchange tubes by more than 10-fold.

[0017] Materials with a high adhesion resistance ensures that a coating with a low coefficient of friction forms on the inner surface of the heat exchange tubes, which prevents adhesion and deposition of salts and other impurities present in heat carrier inside the tubes. Materials with high adhesion resistance can include synthetic polyamides, polymers or fluorine-containing materials, Teflon, polytetrafluorethylene or different metallic sprays. These materials can also be applied as a coating in combination with one another on the inner surface of the tubes: a metallic spray can become the bottom layer, while a fluorine-containing material would become the top layer. Polytetrafluorethylene or Teflon permint application of a very thin coating (starting at 0.1 micron), preventing additional growth of thermal resistance between the heat carriers in the tubes and in the shell space.

[0018] The heat exchange tube made in accordance with the second version carries ribs on the inner surface, promoting formation of turbulent eddies, which break the laminar flow of the heat carrier inside the tubes, thus reducing the probability of salt and other impurities deposition on the inner surface of heat exchanger tubes. Turbulent eddies also promote abrasive interaction between the salts and other impurities on the crystalline structures of poorly soluble compounds, already formed on the inner surface of the tubes, that helps to clean tubes from existing deposits.

[0019] Ribs can be of different shape: circular, diamond-shape, rectangular etc. Ribs can be positioned at assigned points, be of assigned height, which would depend on diameter and thickness of the walls of the tubes, flow velocity and properties of the heat carrier in the tubes and on presence of salts and other impurities in them. To reduce the risk of salt deposition between ribs and, consequently, reduce the risk of increasing thermal resistance between the heat carriers inside the tubes and in the shell space, the ribs can be spaced at regular intervals, 0.1-10 external diameters of the heat exchange tube between them. The height of the ribs can measure 0.1-10 mm. The width of the ribs can measure 0.5-10 mm.

[0020] Circular ribs can be made by milling, knurling or shearing. Diamond-shape ribs can be produced by either cutting or punching criss-cross helical grooves on the inner surface of the tubes, while rectangular ribs can be made by cutting or punching criss-crossing straight-line longitudinal and transverse grooves on the inner surface of tubes.

[0021] Ribs can also be fabricated by inserts set inside the tube and/or fastened to its inner surface. They can have a shape of ribs, helical bands, rings or corrugated components. To fortify eddies in the heat carrier flow inside the tubes, the inserts can be perforated through, while their surface can be coated with a high adhesion resistance material.

[0022] Ribs on the inner surface of a heat exchange tube can be fabricated as counterparts of the grooves on the outside surface. For instance ribs on the inner surface of a tube can be fabricated in the process of knurling the grooves on the outer surface of that tube, which imparts some extra reliability and simplifies the manufacturing of heat exchange tubes.

[0023] This group of inventions offers a combination of substantial features,

- the distance between the guiding spacers of the shell-and-tube condenser decreases from the inlet to outlet of the shell space heat carrier, ensuring permanent velocity of the heat carrier in the shell space, which provides for efficient removal of condensate drops from the outer surface of heat exchange tubes by a flow of non-condensed heat carrier throughout the entire shell space.
- the outer surface of heat exchange tubes is coated with a hydrophobic material, which reduces adhesion of condensate drops to the outer surface of heat exchange tubes.
- the inner surface of the heat exchange tubes is coated with a material with a high adhesion resistance coefficient, which reduces molecular interaction between particles of salt and the inner surface of the tubes, hindering formation of crystalline deposits of poorly soluble compounds on the inner surface of the heat exchange tubes.
- heat exchange tubes carry ribs on their inner surface, which generate eddies in the heat carrier flow inside the tubes, which break crystalline deposits on the surface of heat exchange tubes.

[0024] This combination of specific characteristics of this group of inventions ensures effective removal of condensate drops from the outer surface of heat exchange tubes, reduce adhesion

of condensate drops at the outer surface of the tubes, hindering formation of crystalline deposits of poorly soluble compounds on the inner surface of the tubes or breaking those such deposits that have already formed, which ensures that the desired technological result is achieved: the risk of growing thermal resistance between the heat carriers inside the tubes and in the shell space is reduced, while the heat transfer coefficient between the said heat carriers is amplified.

[0025] These characteristics of the proposed group of inventions are known, described in various science and technology publications, however, they usually aim at a different technological result, such as improving wear resistance of heat exchange tubes (polytetrafluorethylene coating) or extending the duration of contact between heat carriers inside the tubes and in the shell space. Moreover, the combination of the said characteristics with one another is not known from the state of art, also their combination with the presence of grooves on the outer surface and of ribs on the inner surfaces of heat exchange tubes is also unknown. The design of a device that includes coating of heat exchange tubes with a hydrophobic material, grooves and ribs on the surfaces of heat exchange tubes and the gradually decreasing distance between guiding spacers achieve a synergic effect: a significantly increased heat transfer coefficient between the heat carriers inside and outside the tubes of the shell-and-tube condenser, including due to the reduced thermal resistance coefficient between the heat carriers inside and outside the tubes.

[0026] This synergic effect is achieved due to the fact that the heat carrier in the shell space, condensed during the heat exchange process, forms only a very thin film on the outer surfaces of the heat exchange tubes covered with a hydrophobic material; consequently it forms droplets, most of which roll down from arcuate areas of the tubes into circular grooves, while those drops that stay on the arcuate surfaces of the tubes are carried away by the heat carrier flow in the shell space. Velocity of the flow is maintained due to the distance between the guiding spacers decreasing from the inlet of the shell space heat carrier to its outlet. Particles of salt in the heat carrier inside the tubes are repelled by the inner surface of the tubes, which is coated with a high adhesion resistance material. They interact with ribs, forming eddies, which have an abrasive effect on previously formed salt deposits, breaking them very efficiently.

[0027] To illustrate the synergic effect achieved, effects of application of one or another characteristic separately or combined were analysed. It is known from available information that grooves on heat exchanger tubes increase heat transfer coefficient by 1.5-1.9 times, that having heat transfer tubes coated with hydrophobic material increases that coefficient by 2.6-3.2 times, that gradually decreasing the distance between the guiding spacers increases it by 1.1-1.2 times, having heat transfer tubes coated inside with a high adhesion resistance material, by 1.8-2.4 times (depending on exploitation time), presence of ribs increase it by 1.4-1.6 times. In practice, application of this group of inventions increases heat transfer coefficient by 6.2-13.4 times. This result exceeds by several times the forecast total effect of combined application of the said characteristics calculated on the basis of the above theoretical data. This confirms that a synergic effect can be achieved.

[0028] This group of inventions is illustrated with the following diagrams.

Fig. 1. The shell-and-tube condenser with a one-way feed of a heat carrier into the shell, and a condensate cooler. Overall view. Longitudinal section.

Fig. 2. The shell-and-tube condenser with a one-way flow of a heat carrier in the shell space without a condensate cooler. Overall view. Longitudinal section.

Fig. 3. The shell-and-tube condenser with a two-way feed of a heat carrier in the shell without a condensate cooler. Overall view. Longitudinal section.

Fig. 4. A heat exchange tube of the shell-and-tube condenser with circular grooves on the outer surface. Overall view.

Fig. 5. A heat exchange tube of the shell-and-tube condenser with helical grooves on the outer surface. Overall view.

Fig. 6. A heat exchange tube of the shell-and-tube condenser with circular grooves on the outer surface and corresponding circular ribs on the inner surface. Longitudinal section.

Fig. 7. A heat exchange tube of the shell-and-tube condenser with circular grooves on the outer surface and diamond-shape ribs on the inner surface. Longitudinal section.

Fig. 8. A heat exchange tube of the shell-and-tube condenser with a helical groove on the outer surface and a corresponding diamond-shape ribs on the inner surface. Longitudinal section.

Fig. 9. A heat exchange tube of the shell-and-tube condenser with circular grooves on the outer surface and inserts in the shape of perforated rings. Longitudinal section.

[0029] The shell-and-tube condenser includes shell 1, distribution chamber 2 and turn chamber 3. Shell 1 houses a bundle of heat exchange tubes 4, fastened in place with tube plates 5, guiding spacers 6, shell side heat carrier inlet 7, outlet 8, tube-inside heat carrier inlet 9, outlet 10. The distance S_n between the spacers 6 decreases from inlet 7 to outlet 8, so that $S_n > S_{n+1}$. Heat exchange tubes 4 are coated with a hydrophobic material and carry grooves 11, due to which arcuate convex sections 12 form on the outer surface 4 of the tubes.

[0030] Shell-and-tube condenser operates as follows.

[0031] A coolant at a temperature below the steam saturation temperature is fed into the tubes at the temperature below the steam saturation temperature in the shell space 1 via inlet 9. The coolant circulates from inlet 9 to the distribution chamber 2, then, via heat exchange tubes 4 and the turn chamber 3 back to the distribution chamber 2 and outlet 10. The heat carrier in the shell space, that is to be cooled down, enters the shell space 1 via inlet 7. Coming into contact with the outer surface of tubes 4, it begins to partly condensate, flowing towards outlet

8. Droplets 13 of condensate form on the outer surface of the heat exchange tubes, most of which roll off arcuate segments 12 down into grooves 11. Residual condensate 14 is carried away by the flow of uncondensed shell space heat carrier, velocity of which is maintained by gradually decreasing the distance between the consecutive spacers 6 from inlet 7 of the shell space heat carrier to its outlet 8.

[0032] According the second version, tubes 4 of the shell-and-tube condenser carry - in addition to the first version- ribs 15; also the inner surface of the tubes is coated with a high adhesion resistance material.

[0033] This shell-and-tube condenser operates in a manner similar to the first version. Only a small quantity of salt particles 16 present in the coolant precipitates on the inner surface of tubes 4 thanks to the coat of a high adhesion resistance material on these surfaces, forming only the thin layer 17 of salt deposit. The coolant, interacting with ribs 15, generates eddies, which also impede deposition of salt 16 on the inner surface of the heat exchange tubes and breaks the previously formed layer 17 of salt by abrasion caused by the flow of the coolant and particles of salt 16 present in the coolant.

[0034] Thanks to the above arrangements, the film of condensate that forms on the outer surface of heat exchange tubes is thin and, on the other hand, fewer salt deposits form on the inner surface of the tubes. This achieves the desired technological result: cutting down the risk of increased thermal resistance between the heat carriers inside and outside the tubes, while increasing the overall heat exchange coefficient between the heat carriers in the tubes and in the shell space. Due to the decreased contact surface required, tube bank can be made smaller and of lighter weight, rendering the entire shell-and-tube condenser smaller and of lighter weight.

REFERENCES CITED IN THE DESCRIPTION

Cited references

This list of references cited by the applicant is for the reader's convenience only. It does not form part of the European patent document. Even though great care has been taken in compiling the references, errors or omissions cannot be excluded and the EPO disclaims all liability in this regard.

Patent documents cited in the description

- US20110083619A [0001]
- CN1078802 [0003]
- SU409445 [0004]
- UA74177 [0005]

PATENTKRAV

1. Skal- og rørkondensator, bestående af en skal (1), der rummer et bundt varmevekslingsrør (4), som bærer riller (11) på deres udvendige flade og fastgjort på stedet med rørplader (5), indløb (7, 9) og udløb (8, 10) til skal rum og skalumsvarmebærere, hvor skal- og rørkondensatoren omfatter afstandsstykker (6),
- kendetegnet ved, at**
- den udvendige flade af varmevekslingsrør bærer en coating af et hydrofobt materiale, og hvor afstanden mellem afstandsstykkerne (6) aftager fra indløbet (7) til skalumsvarmebæreren til dens udløb (8), riller (11) på varmevekslingsrørenes udvendige flader har en runding med en radius på 0,04-0,1 af den udvendige diameter på varmevekslingsrøret (4) og rillerne (11) er cirkelformede og placeret ved 0,1 - 10 gange rørets (4) udvendige diameter fra hinanden.
2. Skal- og rørkondensator ifølge krav 1, hvor varmevekslingsrørene (4) bærer ribber (15) på deres indvendige flader og en coating af et materiale med lav vedhæftningsmodstand.
3. Skal- og rørkondensator ifølge krav 2, hvor coatingen på rørets (4) udvendige flade er fremstillet af et materiale, der sikrer grænsefladevinklen i intervallet 90° - 150°.
4. Skal- og rørkondensator ifølge krav 1, hvor røret (4) er coatet på indersiden med et fluorholdigt materiale og/eller sprayet metal.
5. Skal- og rørkondensator ifølge krav 1, hvor ribberne (15) på den indvendige flade svarer til rillerne (11) på den udvendige flade.
6. Skal- og rørkondensator ifølge krav 5, hvor ribberne (15) er cirkelformede.
7. Skal- og rørkondensator ifølge krav 5, hvor ribber (15) er placeret ved 0,1 - 10 gange rørets (4) udvendige diameter fra hinanden.
8. Skal- og rørkondensator ifølge krav 5, hvor højden på ribberne (15) på den indvendige flade måler 0,5-10 mm.

9. Anvendelse af en skal- og rørkondensator ifølge et hvilket som helst af de foregående krav, hvor en konstant gennemsnitshastighed for damp under hver passage af skalrumsvarmebæreren bevares ved at reducere afstanden mellem afstandsstykkerne.
- 5 10. Anvendelse af en skal- og rørkondensator ifølge krav 9, hvor et konstant forhold mellem den gennemsnitlige volumenstrøm for damp for hver passage af skalrumsvarmebæreren og skalrumsvarmebærerens tværsnitsområde af den passende bevares ved at reducere afstanden mellem afstandsstykkerne.

DRAWINGS

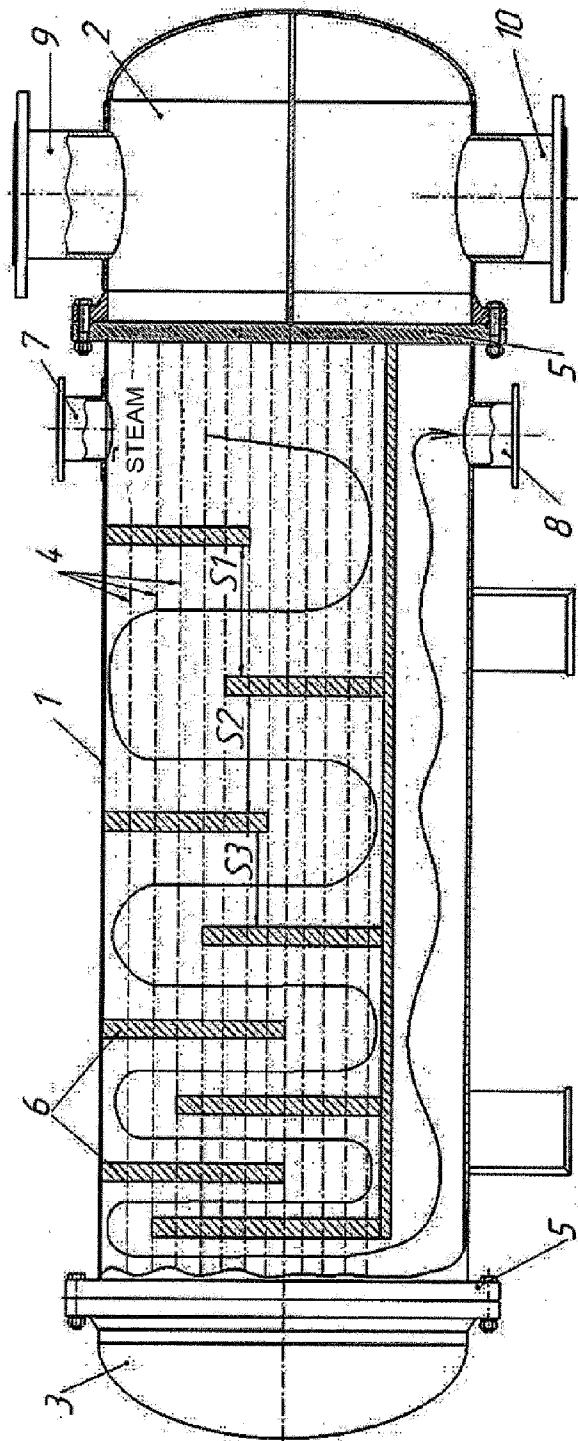


FIG. 1

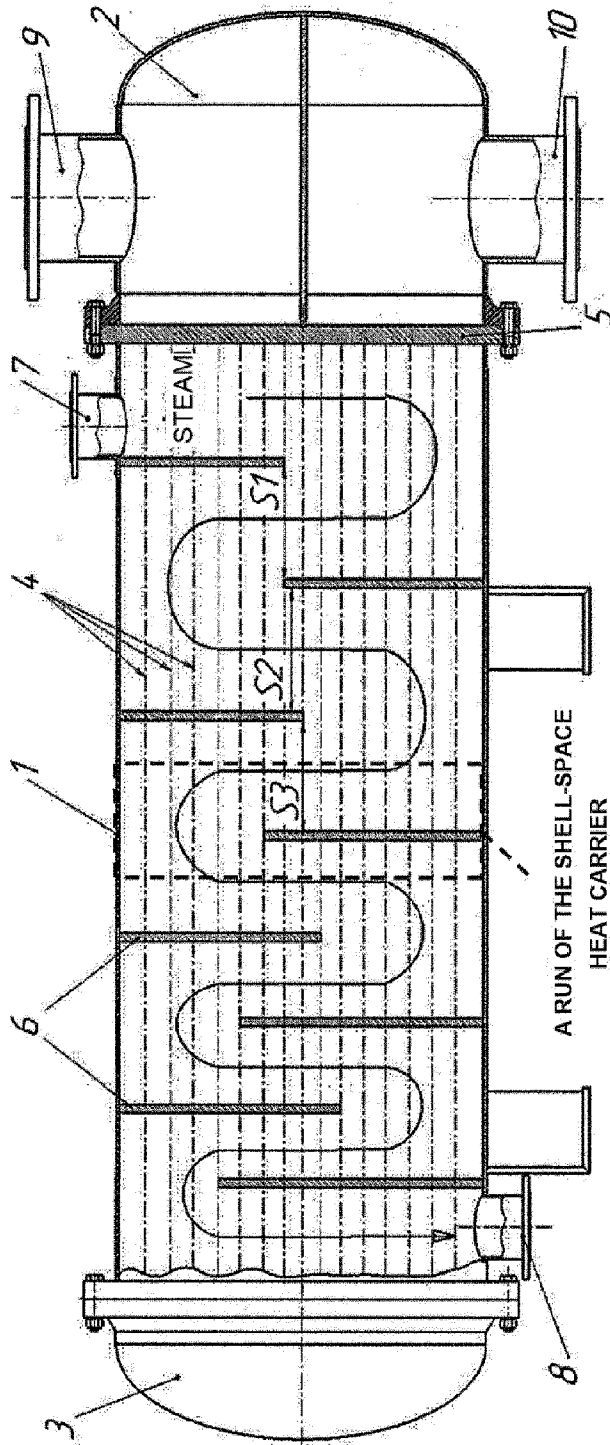


FIG. 2

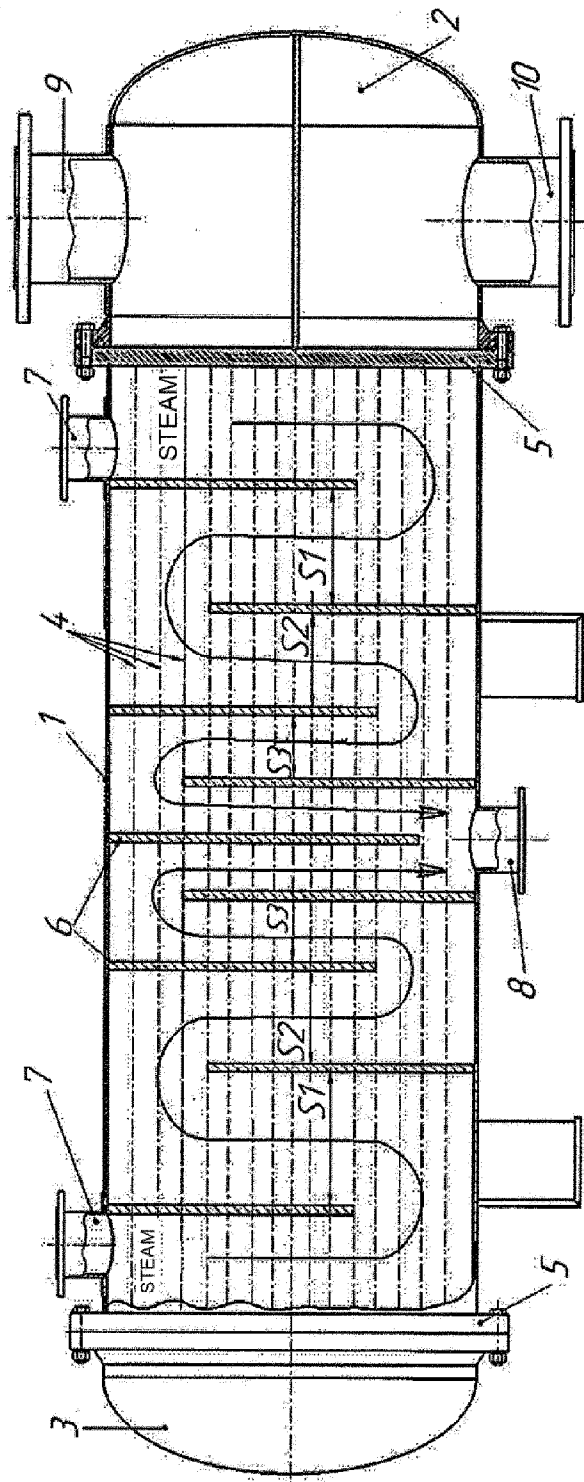


FIG. 3

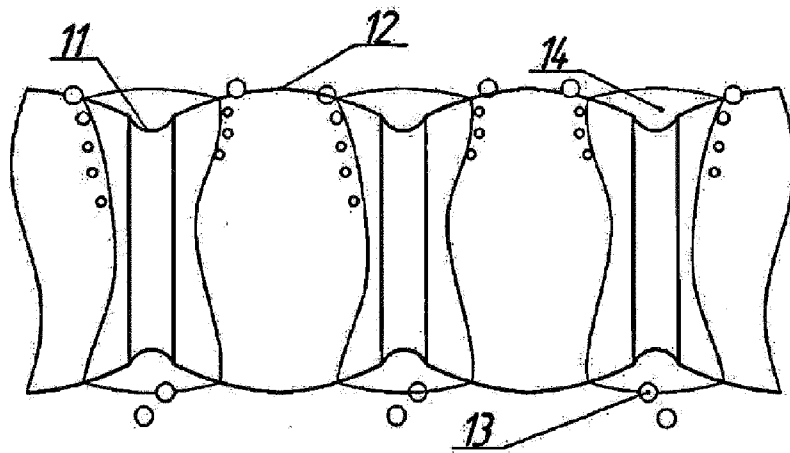


FIG. 4

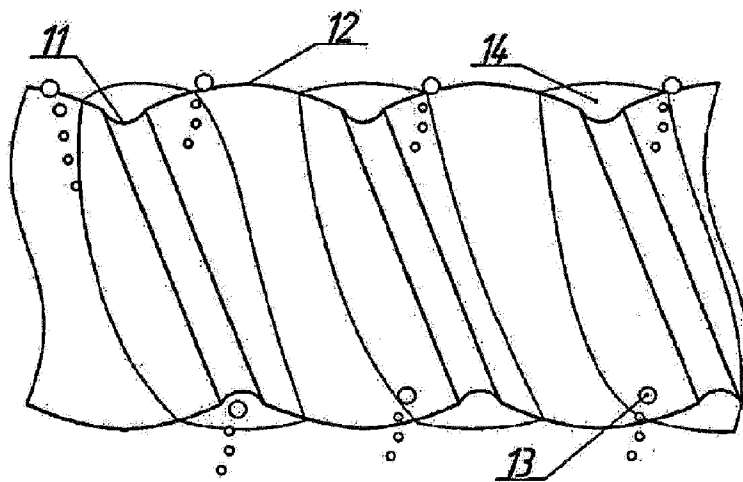


FIG. 5

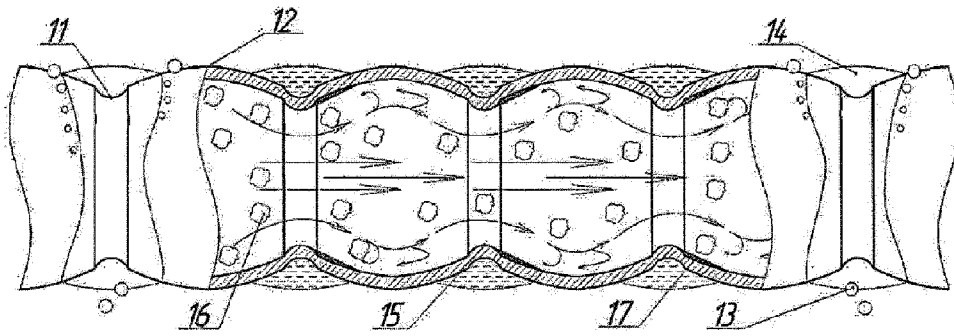


FIG. 6

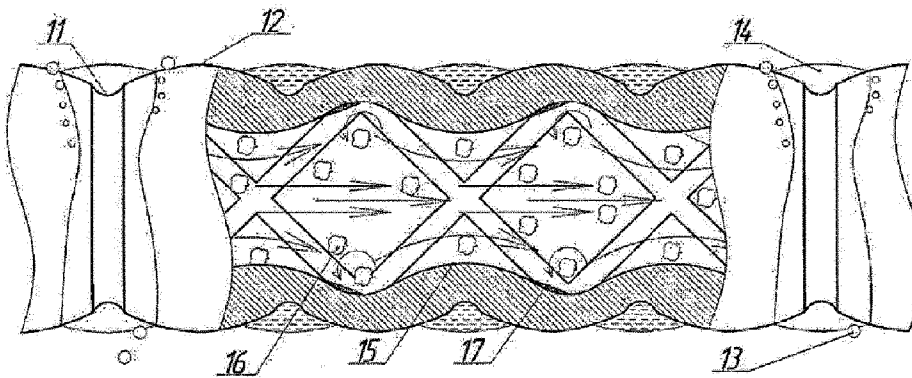


FIG. 7

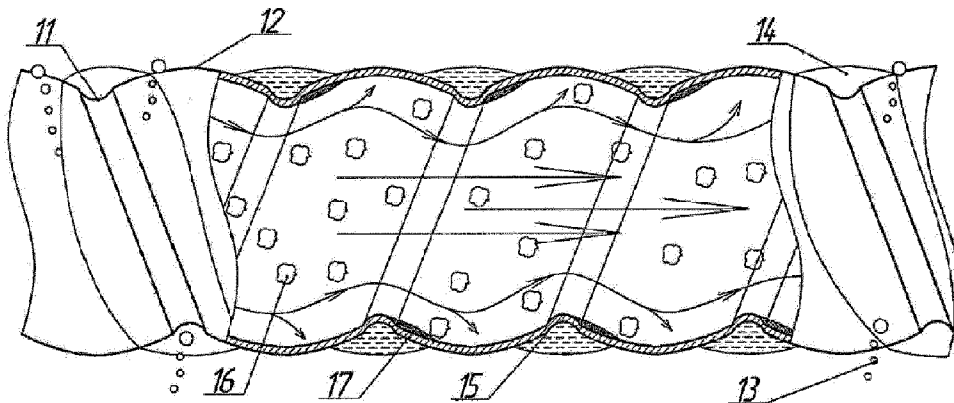


FIG. 8

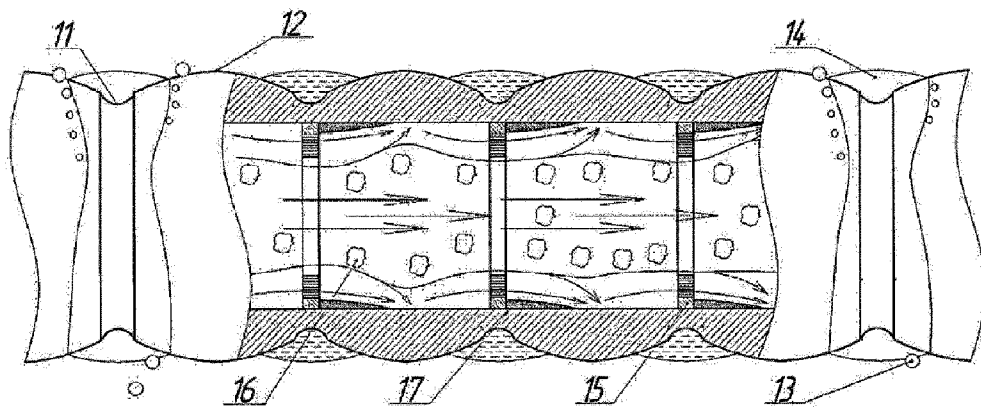


FIG. 9