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NONPIGMENTARY TITANIUM DIOXIDE POWDERS

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(57) Claim

1. A process for preparing free flowing powders of nonpigmentary titanium dioxide granular aggregates useful in the manufacture of glass and ceramic products consisting of:

forming a filter cake comprised of free water and flocculated pigmentary titanium dioxide particles by dewatering a flocculated slurry of pigmentary titanium dioxide particles, said pigmentary particles being prepared by oxidation of titanium tetrachloride in a vapor phase;

preparing solid preforms comprised of said free water and said flocculated pigmentary titanium dioxide particles from said filter cake by breaking or extruding said filter cake to form said solid preforms;

drying said solid preforms to reduce said free water contained therein; and

subjecting said dried solid preforms to comminution to effect a reduction in size of said solid preforms to provide said free flowing powders of nonpigmentary titanium dioxide granular aggregates said free flowing powders having bulk densities ranging from about 0.5 g/cc to about 3.5

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g/cc and wherein at least about 75 weight percent of the nonpigmentary granular aggregates comprising said free flowing powders range in size from a minimum limiting particle size of about 150 microns to a maximum limiting particle size of about 1700 microns.

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(21) International Application Number: PCT/US89/03717 (22) International Filing Date: 31 August 1989 (31.08.89) (30) Priority data: 244,676 15 September 1988 (15.09.88) US (71) Applicant: KERR-McGEE CHEMICAL CORPORATION [US/US]; Kerr-McGee Center, Oklahoma City, OK 73125 (US). (72) Inventors: STORY, Phillip, M. ; 13225 W. Memorial Road, Yukon, OK 73099 (US). BRAND, John, R. ; 3901 Cindy Road, Oklahoma City, OK 73132 (US). (74) Agents: WARD, John, P. et al.; Kerr-McGee Center, Oklahoma City, OK 73125 (US).		(81) Designated States: AT (European patent), AU, BE (European patent), BR, CH (European patent), DE (European patent), FI, FR (European patent), GB (European patent), IT (European patent), JP, KR, LU (European patent), NL (European patent), NO, SE (European patent), SU. Published <i>With international search report.</i> <i>With amended claims and statement.</i>
(54) Title: NONPIGMENTARY TITANIUM DIOXIDE POWDERS (57) Abstract The present invention is directed to a process for preparing free flowing powders of nonpigmentary titanium dioxide granular aggregates. The process comprises the providing of dried preforms of flocculated pigmentary titanium dioxide and the comminution thereof to powders of granular aggregates of enhanced bulk density and predetermined particle size.		

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Nonpigmentary Titanium Dioxide Powders

Field of the Invention

The present invention relates to a process for preparing free flowing powders suitable for use in the manufacture of glass and ceramic products. Particularly, the invention is directed to a process for preparing free flowing titanium dioxide powders comprised of granular aggregates of a size larger than pigmentary titanium dioxide and which powders are readily dispersible in glass and ceramic melts.

10 Background of the Invention

Nonpigmentary titanium dioxide is used in the manufacture of various glass and ceramic products for a wide variety of purposes. For example, it is employed in the manufacture of glass frit used in producing vitreous enamel and glaze type coatings and in the manufacture of glass ceramics employed in missile radomes and microwave transmitters. In the former application, the titanium dioxide functions as both an opacifying agent and to enhance the acid resistance of the coatings while in the latter application, it functions as a nucleating agent to effect the nucleation and growth of the major crystalline phases of the glass. Other properties of various glass and ceramic compositions which can be effected through the use of titanium dioxide are those of thermal expansion, chemical durability, refractive index, and the like.

In general, it is believed that the commercially available nonpigmentary titanium dioxides currently employed in the glass and ceramic industries are those produced by the well-known sulfate process. This belief is premised on the fact that nonpigmentary titanium

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dioxide products readily can be produced through the manipulation of either the crystallization step or calcination step, or both, employed in the sulfate process. Such belief is supported by the disclosures
5 found in U.S. Patent No. 3,434,853 issued on March 25, 1969. According to this patent, a nonpigmentary titanium dioxide granular material can be produced by calcining, at a temperature of from 800°C to 1000°C, a
10 titanium hydrate prepared by hydrolyzing a titanium sulfate solution of low titanium concentration at low temperatures to form nodules of aggregated titanium dioxide particles and thereafter, subdividing these nodules into granules. The granules are described as
15 being free flowing and capable of undergoing rapid melting and thorough dispersion when incorporated into a molten glass batch composition.

In contrast, pigmentary titanium dioxide produced by the chloride process, the second major commercial process employed for the manufacture of titanium
20 dioxide, often is unsuited for use in glass and ceramic manufacture. Typically, pigmentary titanium dioxide is so fine and of such low bulk density that it tends to float upon the surface of the glass melt and, as a result, is easily lost through dusting as it is
25 carried out of the glass making vessel by the hot air convection currents generated in the vessel. Fine particle size pigmentary titanium dioxide also tends to form agglomerates in the molten glass batch which agglomerates do not melt properly and which sink to the
30 bottom of the vessel where they form a sintered mass in the glass melt.

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Summary of the Invention

The present invention relates to a process for preparing free flowing powders comprised of nonpigmentary titanium dioxide granular aggregates for use in the manufacture of glass and ceramics.

The process of this invention comprises a sequence of multiple steps the first of which comprises providing solid preforms of flocculated pigmentary titanium dioxide, said preforms having a free water content ranging from about 25 to about 50 weight percent based on the total weight of the preforms. In a second step of the process, the solid preforms are subjected to drying at elevated temperatures whereby the free water content of the preforms is reduced to a level of less than about 5 weight percent. Finally, the dried preforms are comminuted to effect a reduction in size of the preforms and produce a free flowing powder of nonpigmentary titanium dioxide granular aggregates. The free flowing powder is characterized by a bulk density ranging broadly from about 0.5 to about 3.5 g./cc. It is comprised of nonpigmentary titanium dioxide granular aggregates, a substantial portion of which range in size from a minimum limiting particle size of about 150 microns to a maximum limiting particle size of about 1700 microns.

In a further embodiment of the invention the free flowing powder can be subjected to size enlargement where the maximum limiting particle size remains at about 1700 microns but wherein the particle size distribution of the granular aggregates is narrowed by agglomeration of those granular aggregates having particle sizes smaller than about 150 microns.

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Detailed Description of the Invention

The surprising discovery now has been made of a process for conveniently and economically converting pigmentary titanium dioxide into free flowing powders of nonpigmentary titanium dioxide granular aggregates. Broadly, the present invention comprises providing solid preforms of pigmentary titanium dioxide, drying the preforms to reduce the free water content thereof and thereafter subjecting the dried preforms to comminution to produce the free flowing powders of nonpigmentary titanium dioxide granular aggregates.

The present invention is particularly suited to the conversion of pigmentary titanium dioxide produced by way of the so-called "chloride process". Broadly, the chloride process comprises chlorinating a titaniferous ore to produce titanium tetrachloride and then oxidizing the titanium tetrachloride, in the vapor phase, to produce a hot, solids-gaseous reaction mixture. Typically, this hot, solids-gaseous reaction mixture will comprise particulate, pigmentary titanium dioxide suspended in a gaseous mixture of unreacted titanium tetrachloride, chlorine, oxygen and hydrogen. The hot solids-gaseous reaction stream further may contain an inert refractory material, such as sand, of a particle size larger than that of the pigmentary titanium dioxide being produced. In general, this inert refractory material is added to the reaction vessel in which the vapor phase oxidation is conducted to prevent or substantially minimize the deposition of the particulate pigmentary titanium dioxide on the inner surfaces of the reaction vessel.

The hot solids-gaseous reaction mixture exiting the reaction vessel is rapidly cooled to prevent any further

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growth of the particulate pigmentary titanium dioxide product and this reaction mixture then separated into its solids and gaseous constituents. Various means have been employed to effect this separation although, typically, cyclones and bag filters are the most widely used means. To improve the economics of the chloride process, the unreacted titanium tetrachloride and chloride components usually are recovered and recycled for reuse in the process.

10 The separated and recovered particulate pigmentary titanium dioxide and any inert refractory material which may have been employed in the oxidation step then are dispersed in water in a suitable vessel to form a slurry having a solid pigmentary titanium dioxide content of
15 from about 25 to about 70 weight percent and preferably from about 30 to about 50 weight percent. In general, good dispersion of the pigmentary titanium dioxide in this slurry is achieved at slurry pH's of below about 4 and above about 8. To maintain this good dispersion and
20 prevent flocculation of the dispersed pigmentary titanium dioxide during the subsequent milling and classification steps employed in the chloride process, it is usual practice to add to the slurry a stabilizing amount of either an appropriate mineral acid or inorganic base.
25 A stabilizing amount will comprise any amount capable of maintaining the slurry pH below about 4 or above about 8. Representative of useful mineral acids are hydrochloric and sulfuric acids while useful inorganic bases include any of the well-known hydroxides, bicarbonates
30 and carbonates of ammonia and the alkali and alkaline earth metals. Representative examples of such base materials include sodium hydroxide, potassium hydroxide,

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ammonium hydroxide, calcium hydroxide, sodium carbonate, sodium bicarbonate, potassium carbonate, and the like.

To further enhance the stability of the above
5 described slurry it also is usual practice to add to the
slurry an additional dispersant material. This additional dispersant material can include any of the
various primary, secondary and tertiary amines employed
for such purposes as well as various water soluble
10 phosphates and particularly the phosphates of sodium,
potassium, lithium and ammonia. Particularly useful
additional dispersant materials which can be employed
for improving the dispersion characteristics of the
slurry are the tripolyphosphates, hexametaphosphates and
15 tetraphosphates of sodium.

When the slurry comprises a mixture of pigmentary
titanium dioxide and an inert refractory material such
as sand, the slurry then is subjected to classification
to effect a separation of the larger particle size inert
20 refractory material from the finer particle size
pigmentary titanium dioxide contained in the slurry.

Following removal of the inert refractory material
from the slurry, the slurry is subjected to milling and
further classification. The slurry containing the
25 dispersed pigmentary titanium dioxide, then is floccu-
lated either by adjustment of the slurry pH to a value
in the range of from about 4 to about 8 by addition of
an acid or base such as disclosed hereinabove, or by the
addition of a flocculating agent. Suitable flocculating
30 agents include inorganic agents such as, for example,
magnesium sulfate and organic agents such as, for
example, polymeric polyacrylamides. Finally, the
flocculated slurry is washed to remove undesirable

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byproducts and salts and dewatered to yield a filter cake of flocculated pigmentary titanium dioxide.

Dewatering of the slurry readily can be accomplished by known techniques such as by filtration utilizing

5 conventional rotary vacuum drum, or disc filters, or pressure filters of the plate, leaf and disc type. The resulting filter cake of flocculated pigmentary titanium dioxide will contain from about 25 to about 50 weight percent of free water and from about 50 to about 75
10 weight percent of the flocculated pigmentary titanium dioxide based on the weight of the filter cake. The exact amount of free water content in the filter cake will depend upon the type of filtration apparatus employed.

15 In the conventional chloride process, the above filter cake would be dried and subjected to fluid energy milling to produce a finished pigmentary titanium dioxide having particle sizes in the range of from about 0.01 to about 0.5 microns and preferably in the range of
20 from about 0.2 to about 0.4 microns. Such pigmentary titanium dioxide is particularly useful in the preparation of various coating formulations. However, as noted hereinabove, such pigmentary titanium dioxide often is, due to its extremely small particle size and low bulk
25 density, unsuited for use in the manufacture of glass and ceramic products.

It now has been found that when the filter cake produced in the above generally described chloride process is treated in accordance with the process of
30 this invention, a nonpigmentary titanium dioxide product suitable for use in the manufacture of glass and ceramics can be produced. In accordance with the present invention, the above described filter cake first

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is converted into solid preforms either by breaking the filter cake into irregular shaped pieces or by extruding the filter cake into predetermined forms such as, for example, pellets, rods, and the like. The manner by which the filter cake is converted into these solid preforms and the particular shape or form of the solid preforms produced is not critical and, in general, will depend upon the free water content of the filter cake.

The solid preforms, which contain essentially the same free water content and weight percent of flocculated pigmentary titanium dioxide as the filter cake then are subjected to drying at elevated temperatures to reduce the free water content contained therein to a level of less than about 5 weight percent based on the weight of the dried solid preforms. Drying of the solid preforms to achieve such reduced levels of free water can be achieved using conventional drying apparatus such as, for example, well-known tunnel and belt drying apparatus. Generally, this drying of the solid preforms will be carried out at elevated temperatures ranging from about 125°C to about 700°C.

Following drying of the solid preforms, the solid preforms are reduced in size by comminution to provide the desired free flowing powder. The free flowing powder will comprise nonpigmentary titanium dioxide granular aggregates a substantial portion, e.g., at least 75 weight percent, and preferably, at least 85 weight percent of which will range in size from a minimum limiting particle size of about 150 microns (100 mesh) to a maximum limiting particle size of about 1700 microns (10 mesh). The free flowing powder further is characterized by exhibiting bulk densities ranging from about 0.5 g/cc to about 3.5 g/cc and preferably from

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about 0.8 g/cc to about 1.2 g/cc. Free flowing powders comprised of nonpigmentary titanium dioxide granular aggregates within the above disclosed size and bulk density ranges easily can be incorporated into a glass melt thus avoiding the hereinabove mentioned problems associated with the use of pigmentary titanium dioxide.

Comminution of the solid preforms to free flowing powders possessing the above disclosed characteristics readily can be achieved using a wide variety of crushing and grinding equipment. Particularly good results have been obtained using both smooth-roll and corrugated-roll crushing apparatus.

In a further embodiment of this invention, the free flowing powders of nonpigmentary titanium dioxide granular aggregates can be subjected to size enlargement to reduce the quantity of the smaller size granular aggregates contained therein. In this embodiment, the free flowing powders first are wetted with water in amounts ranging from about 0.25 to about 11.0 weight percent, and preferably from about 0.25 to about 5.0 weight percent, based on the weight of the powders. The wetted powders then are agglomerated by, for example, introducing the wetted powders into a conventional drum-type pelletizer. Within the drum-type pelletizer, a substantial portion of those granular aggregates ranging of a size smaller than about 150 microns (100 mesh) are converted into granular aggregates larger than about 150 microns. During this size enlargement, the maximum limiting particle size remains substantially the same, i.e., about 1700 microns (10 mesh). Typically, this size enlargement results in the production of free flowing powders wherein at least about 95 weight percent of the granular aggregates contained therein range in

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size from the minimum limiting particle size of about 150 microns to the maximum limiting particle size of about 1700 microns.

5 The following examples are presented for purposes of illustration only and are not to be construed as limiting the scope of the invention. All parts and percentages are by weight unless otherwise specified.

Examples 1 - 2

10 Two free flowing powders comprised of nonpigmentary titanium dioxide granular aggregates are prepared in accordance with the process of the present invention as follows:

15 To a laboratory scale roll crusher, equipped with two pairs of 9-inch by 12-inch chilled iron rollers and operated at a speed of 720 rpm, is fed a quantity of titanium dioxide substantially in the form of rod-shaped preforms measuring approximately $\frac{1}{4}$ inch by 1 to 2 inches. The preforms are produced by extrusion of a
20 highly viscous filter cake of flocculated pigmentary titanium dioxide produced by the chloride process described hereinabove and containing approximately 40 weight percent of free water. The preforms are dried at
25 an elevated temperature of about 180°C for a time sufficient to reduce the free water content of the preforms to a level of less than about 0.5 weight percent.

The dried preforms then are subjected to comminution by feeding the preforms to the above described roll
30 crusher at a rate of 425 pounds per hour. Screen analysis of the two free flowing powders prepared therefrom are determined using Tyler screen sieves and the results thereof are set forth in the Table below.

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Table I

Example No.	(a)		(b)	
	1		2	
Bulk Density, g/cc	1.23		1.21	
5 Dry Flow ^(c) , mm	4-6		4-6	
Size Distribution, cumulative Wt.% larger than:				
10 mesh	0.8		4.2	
10 20 mesh	33.6		39.4	
35 mesh	61.3		65.3	
65 mesh	71.4		75.3	
80 mesh	82.3		84.9	
100 mesh	85.7		87.8	
15 (a)	Roll crusher equipped with corrugated rolls.			
(b)	Roll crusher equipped with smooth rolls.			
(c)	Smallest diameter tube through which the sample will flow without assistance.			
20				
25	As disclosed hereinabove, powders of nonpigmentary titanium dioxide possessing bulk densities ranging from about 0.5 g/cc and 3.5 g/cc and comprised of granular aggregates, a substantial portion of which range in size from about +100 mesh (150 microns) to about -10 mesh			

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(1700 microns), easily can be incorporated into a glass melt. From the data set forth in Table I, it is clear that the nonpigmentary titanium dioxide powders (Examples 1 and 2) produced in accordance with this invention possess these characteristics. For example, the bulk densities of the powders of Examples 1 and 2 are 1.23 g/cc and 1/21 g/cc, respectively, values well within the bulk density range given above. Also, a substantial portion of the granular aggregates comprising these powders, e.g., 84.9 weight percent for the powder of Example 1 and 83.6 weight percent for the powder of Example 2, fall within the above disclosed particle size range. Thus, the nonpigmentary titanium dioxide powders prepared in Examples 1 and 2 above easily can be incorporated into a glass melt and their use readily avoids the difficulties associated with the use of pigmentary titanium dioxide, i.e., pigment losses from dusting and the formation of large agglomerates which tend to sink to the bottom of the glass melt where they can form sintered masses.

Examples 3 - 6

To demonstrate the further embodiment of the present invention, i.e., size enlargement, the free flowing powders of Examples 1 and 2 above are combined in equal portions into a powdery blend. Tyler screen analysis of this powdery blend indicates a particle size distribution for the granular aggregates contained in the blend as follows: 0.1 weight percent of the granular aggregates are larger than 10 mesh in size; 86.2 weight percent of the granular aggregates range from +100 mesh to -10 mesh in size; and 13.7 weight percent of the aggregates are smaller than 100 mesh in size.

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The above powdery blend is divided into four separate samples of equal proportions and each sample subjected to size enlargement by pelletization in a 14-inch drum pelletizer rotated at a speed of 30 rpm.

5 During each pelletizing operation water is sprayed into the pelletizer to agglomerate the finer granular aggregates contained in each sample. Data relating to the pelletized samples are set forth in Table II below.

10

15

Table II

Example Number	<u>Particle Size Distribution, Wt.%</u>			<u>Added H₂O, Wt.%</u>
	<u>+10 mesh</u>	<u>10-100 mesh</u>	<u>-100 mesh</u>	
3	0.1	98.9	1.0	11.0
20 4	0.0	99.4	0.6	4.5
5	0.0	98.4	1.6	4.0
6	0.0	95.0	5.0	2.0

25

A comparison of the particle size distribution data set forth in Table II for the pelletized samples with the particle size distribution data for the original
30 powdery blend disclose a significant reduction having been effected in the quantity of granular aggregates smaller than 100 mesh in size. Furthermore, it is clear from the above data that this reduction is achieved

while the quantity of granular aggregates larger than 10 mesh remains substantially the same or, with regard to Examples 4 - 6, actually decreases.

25 Example 7

30 An enamel glass frit composition comprising 8.7 parts of feldspar, 11.4 parts of borax, 25.5 parts of sand, 14.1 parts of soda ash, 5.1 parts of sodium nitrate, 7.8 parts of red lead, 5.1 parts of zinc oxide,

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20

Comparative Example

For comparative purposes, a conventional pigmentary titanium dioxide is used in the dry blended glass composition of Example 7 in place of a nonpigmentary titanium dioxide powder produced in accordance with the process of this invention. Upon melting of this dry blended glass composition, not all of the added pigmentary titanium dioxide will dissolve. At least a portion of the pigmentary titanium dioxide will rise to the surface of the glass melt while a further portion remains undissolved and suspended in the glass melt. The resulting product is a nonhomogenous glass mixture containing numerous sintered black masses of pigmentary titanium dioxide suspended therein.

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From the above description and examples, it is clearly shown that the process of this invention is capable of producing titanium dioxide powder products well suited for use in glass and ceramic manufacture.

5 These titanium dioxide powder products have higher bulk densities and are comprised of granular aggregates of a size larger than the particles of pigmentary titanium dioxide. These characteristics render the titanium
10 dioxide powder products produced in accordance with this invention readily dispersible in glass and ceramic melts and, thus, avoiding the problems associated with the use of convention pigmentary titanium dioxide powders.

While the present invention has been described in respect to what at present is considered to be the
15 preferred embodiments, it will be understood that changes and modifications can be made therein without departing from the true scope thereof as defined in the appended claims.

20

AMENDED CLAIMS

[received by the International Bureau
on 15 February 1990 (15.02.90);
original claims 1, 6, 10, 12 and 13 amended;
other claims unchanged (5 pages)]

1. A process for preparing free flowing powders of nonpigmentary titanium dioxide granular aggregates useful in the manufacture of glass and ceramic products consisting of:
 - forming a filter cake comprised of free water and flocculated pigmentary titanium dioxide particles by dewatering a flocculated slurry of pigmentary titanium dioxide particles, said pigmentary particles being prepared by oxidation of titanium tetrachloride in a vapor phase;
 - preparing solid preforms comprised of said free water and said flocculated pigmentary titanium dioxide particles from said filter cake by breaking or extruding said filter cake to form said solid preforms;
 - drying said solid preforms to reduce said free water contained therein; and
 - subjecting said dried solid preforms to comminution to effect a reduction in size of said solid preforms to provide said free flowing powders of nonpigmentary titanium dioxide granular aggregates said free flowing powders having bulk densities ranging from about 0.5 g/cc to about 3.5 g/cc and wherein at least about 75 weight percent of the nonpigmentary granular aggregates comprising said free flowing powders range in size from a minimum limiting particle size of about 150 microns to a maximum limiting particle size of about 1700 microns.
2. The process of claim 1 wherein said solid preforms contain from about 25 to about 50 weight percent of free water and from about 50 to about 75 weight



percent of said flocculated pigmentary titanium dioxide particles.

3. The process of claim 1 wherein said solid preforms are dried at elevated temperatures to reduce the free water content thereof to a level of less than about 5.0 weight percent based on the weight of the preforms.
4. The process of claim 3 wherein said solid preforms are dried at elevated temperatures ranging from about 125°C to about 700°C.
5. The process of claim 1 wherein said free flowing powders have bulk densities ranging from about 0.8 g/cc to about 1.2 g/cc.
6. The process of claim 1 wherein at least 85 weight percent of said nonpigmentary titanium dioxide granular aggregates comprising said free flowing powders range in size from about 150 microns to about 1700 microns.
- ~~7. The process of claim 1 further defined as comprising:
wetting said free flowing powders of nonpigmentary titanium dioxide granular aggregates; and
subjecting said wetted free flowing powders to agglomeration.~~
8. The process of claim 7 wherein said free flowing powders are wetted with from about 0.25 to about 11 weight percent of water, based on the weight of the free flowing powders.



~~9. The process of claim 8 wherein said free flowing powders are wetted with from about 0.25 to about 5.0 weight percent of water.~~

7. A process for preparing free flowing powders of nonpigmentary titanium dioxide granular aggregates consisting of:

forming a filter cake comprised of from about 25 to about 50 weight percent of free water and from about 50 to about 75 weight percent of flocculated pigmentary titanium dioxide particles by dewatering a flocculated slurry of pigmentary titanium dioxide particles, said pigmentary particles being prepared by oxidation of titanium tetrachloride in a vapor phase;

preparing solid preforms comprised of said free water and said flocculated pigmentary titanium dioxide particles, said preforms containing from about 25 to about 50 weight percent of said free water and from about 50 to about 75 weight percent of said flocculated pigmentary titanium dioxide particles based on the weight of said solid preforms said solid preforms being prepared from said filter cake by breaking or extruding said filter cake into said solid preforms;

drying said solid preforms at elevated temperatures to reduce the free water contained therein to levels of less than about 5.0 weight percent based on the weight of said solid preforms; and

subjecting said dried solid preforms to comminution to effect a reduction in size of said solid preforms to provide said free flowing powders of nonpigmentary titanium dioxide granular aggregates, said free flowing powders having bulk



densities ^{ranging} ~~in the range of~~ from about 0.5 g/cc to about 3.5 g/cc and wherein at least about 75 weight percent of the nonpigmentary granular aggregates comprising said free flowing powders range in size from a minimum limiting particle size of about 150 microns to a maximum limiting particle size of about 1700 microns.

8. The process of claim 7 wherein said free flowing powders have bulk densities ranging from about 0.8 g/cc to about 1.2 g/cc.

9. The process of claim 7 wherein said solid preforms are dried at elevated temperatures ranging from about 125°C to about 700°C.

10. The process of claim 7 wherein at least 85 weight percent of said nonpigmentary titanium dioxide granular aggregates comprising said free flowing powders range in size from about 150 microns to about 1700 microns.

11. The process of claim 7 further defined as comprising:

wetting said free flowing powders of nonpigmentary titanium dioxide granular aggregates with from about 0.25 to about 11 weight percent of water based on the weight of said free flowing powders; and

subjecting said wetted free flowing powders to agglomeration to provide free flowing powders of nonpigmentary titanium dioxide granular aggregates and wherein at least about 95 weight percent of said granular aggregates range in size from about 150 microns to about 1700 microns.



5 12. The process of claim 1, wherein said filter cake is
comprised of from about 25 to about 50 weight percent of
said free water and from about 50 to about 75 weight
percent of said flocculated pigmentary titanium dioxide
particles.

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DATED: 7 August, 1991

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INTERNATIONAL SEARCH REPORT

International Application No. PCT/US 89/03717

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all) ⁶		
According to International Patent Classification (IPC) or to both National Classification and IPC		
IPC5: C 01 G 23/08		
II. FIELDS SEARCHED		
Minimum Documentation Searched ⁷		
Classification System ¹	Classification Symbols	
IPC5	C 01 G	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in the Fields Searched ⁸		
III. DOCUMENTS CONSIDERED TO BE RELEVANT ⁹		
Category ¹⁰	Citation of Document, ¹¹ with indication, where appropriate, of the relevant passages ¹²	Relevant to Claim No. ¹³
X	DE, B, 1207363 (LAPORTE TITANIUM LIMITED) 23 December 1965, see column 4, line 19 - line 31; column 5, line 16 - line 33	1
	--	
A	US, A, 2899278 (E.D. LEWIS) 11 August 1959, see column 3, line 28 - line 41	1
	--	
A	DE, C2, 2534281 (TIOXIDE GROUP LTD.) 22 January 1987, see page 1, line 1 - line 7; page 2, line 22 - line 33	1
	--	
<p>¹⁴ Special categories of cited documents:</p> <p>"A" document defining the general state of the art which is not considered to be of particular relevance</p> <p>"E" earlier document but published on or after the international filing date</p> <p>"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>"O" document referring to an oral disclosure, use, exhibition or other means</p> <p>"P" document published prior to the international filing date but later than the priority date claimed</p> <p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step</p> <p>"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.</p> <p>"&" document member of the same patent family</p>		
IV. CERTIFICATION		
Date of the Actual Completion of the International Search	Date of Mailing of this International Search Report	
21st December 1989	19. 01. 90	
International Searching Authority	Signature of Authorized Officer	
EUROPEAN PATENT OFFICE	T.K. WILLIS	

ANNEX TO THE INTERNATIONAL SEARCH REPORT
ON INTERNATIONAL PATENT APPLICATION NO.

PCT/US 89/03717

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31673

This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report. The members are as contained in the European Patent Office EDP file on 08/11/89. The European Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

Patent document cited in search report	Publication date	Patent family members:	Publication date
DE-B- 1207363	23/12/65	NONE	
US-A- 2899278	11/08/59	NONE	
DE-C2- 2534281	22/01/87	NL-A- 7508727	12/02/76
		BE-A- 832284	09/02/76
		FR-A-B- 2281316	05/03/76
		AU-D- 82876/75	13/01/77
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