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DESCRIPTION

FIELD

[0001] The present invention relates to a method of enhancing soil using a composite formed of oligomeric lignin and char derived from lignocellulosic biomass by pyrolyzing feed in the presence of steam (hydrous thermolysis) to produce (1) a stream of water-soluble Hodge' carbonyls, (2) a stream of water insoluble-oligomeric lignin and (3) a stream of charcoal particulates .

BACKGROUND

[0002] Since the late seventies, many researchers and developers have concentrated on fast pyrolysis of biomass, also termed flash, ultra, rapid, and ablative pyrolysis of biomass. Most often - "flash pyrolysis consists of an operation wherein the dried, comminuted substantially organic fraction is combined with a particulate solid source of heat and a carrier gas which is nonreactive or non deleteriously reactive with respect to the product of pyrolysis under turbulent flow conditions in a flash pyrolysis zone maintained at a temperature from about 600°F to about 2000°F (315.6°C to 1093.3°C) by the flow of a solid particulate source of heat there through" as in US Patent No. 4,260,473 issued to H.S. Bauer.

[0003] Attempts have been made by Occidental Research Corporation to commercialize a waste flash pyrolysis process which failed.

[0004] Most initiatives involving fast pyrolysis, after those of Occidental Research Corporation, were aimed at the production of biomass-based homogeneous liquids, considered as potential liquid fuels in stationary applications. After about 25 years of effort, the commercial potential of liquid fuel often named "bio-oil" has not yet been fully realized, although some attempts for replacement of bunker C and heating oil #2 were reported.

[0005] "Bio-oils", as produced by fast pyrolysis, are not considered applicable as transportation fuels. They have heating values similar to that of the original biomass (but those are only approximately 60% of the higher heating value (HHV) of bunker C, on a volumetric basis). Thus, if these oils are not transportation fuels, then it is difficult to understand why dry and ground biomass is not burned directly (in a variety of boilers) instead of going through a rather costly pyrolysis step first to produce a new liquid boiler fuel - bio-oil. On the other hand, it seems, there can be a valid strategy to direct pyrolytic processing towards particular fractions or specific chemicals. For such a strategy, if adopted, critical requirements like homogeneity or a low water content, of importance in fuel applications, are no longer as relevant or a prerequisite.

[0006] International Publication No. WO2004/037747A2 relates to The Production And Use Of A Soil Amendment Made By The Combined Production Of Hydrogen, Sequestered Carbon And Utilizing Off Gases Containing Carbon Dioxide; and discloses a series of steps to provide an economical production of a carbon based fertilizer and soil amendment made during the capture of greenhouse gases from the combustion of fossil and non fossil fuels, using biomass and other carbonaceous sources through pyrolytic conversion to gases and charcoal, to allow for the further production of coproducts, such as hydrogen and ammonia; and the combination of hydrated ammonia, combustion flue gas exhaust, and charcoal, provide for the conversion of the charcoal into a valued added soil amendment to return essential trace minerals and plant nutrients to the soil.

[0007] US Patent No. 5,235,021 relates to resole resin products derived from fractionated organic and aqueous condensates made by fast-pyrolysis of biomass materials; and discloses a process for preparing phenol-formaldehyde resole resins by fractionating organic and aqueous condensates made by fast-pyrolysis of biomass materials while using a carrier gas to move feed into a reactor to produce phenolic-containing/neutrals in which portions of the phenol normally contained in said resins are replaced by a phenolic/neutral fractions extract obtained by fractionation.

[0008] US Patent No. 3,309,355 relates to Levoglucosan production by pyrolysis of cellulosic material; and discloses that levoglucosan is a chemical potentially useful as a raw material for the large scale production of explosives, propellants, plasticizers, surfactants, plastics, resins and other products.

[0009] The journal article Sagehashi M et al. Superheated steam pyrolysis of biomass elemental components and Sugi (Japanese cedar) for fuels and chemicals. Bioresource Technology. ELSEVIER BV. GB. vol. 97. No. 11. 1 July 2006; discloses that to develop a novel noncatalytic biomass refinery process that can be used as a portable process, superheated steam pyrolysis was investigated to produce both carbonized solid fuels and chemicals using a large-scale reactor.

[0010] Bridgwater A V (Ed) et al. Fast Pyrolysis Of Biomass: A Handbook; NEWBURY, CPL PRESS, GB; relates to Production, Properties And Use Of Wood Pyrolysis Oil, and discloses fast pyrolysis of biomass for producing fuels and chemicals.

[0011] From earlier work in the field, the following pyrolysis related products have been discovered:

1. 1. **Hodge' carbonyls** - the main biomass carbohydrate polymers, cellulose and hemicellulose (holocellulose) upon fast pyrolysis conditions, above 480 deg C, convert to carbohydrate fragments like hydroxyacetaldehyde, glyoxal, methylglyoxal, acetol, formaldehyde (Hodge' carbonyls). Those components have high water affinity and are water soluble. Hodge' carbonyls are finding applications in food industry, as a water base solvents, as pesticides, in formulations of silver-containing inkjet inks, as desulfurization

and odour removal agents, as polymer precursors (polyesters of high boiling points), in glycolic acid production etc.

2. **Oligomeric lignin** - the most abundant aromatic polymer in nature, lignin, under fast pyrolysis conditions, breaks down to oligomeric molecular fragments - "oligomeric lignin" containing circa 2-20 aromatic rings of molecular weight in the range of 400-2500 Daltons. This chemical fraction is water insoluble, odorless and rather non-volatile. There is a strong analogy/similarity between oligomeric lignin and humic acids. Humic acids are arguably the most important part of the soil. Both, oligomeric lignin and humic acids are products of lignin-polymer degradation. The exact chemical structures of both substances have not been established.
3. **Pyrolytic char:** See US Patent # 5,676,727 issued to Radlein - "The pyrolytic char, which as a by-product of the pyrolysis process, has a high content of oxygenated functional groups and, in fact, represents a partially activated carbon. It may, therefore, serve not only as an absorbent, but may also bind nitrogen directly by reaction with NH₂ groups".
4. **Pyrolytic water** - in all pyrolytic processing (of biomass) the main product is 'pyrolytic water' which is a product of thermal dehydration. The dehydration reactions can lead to highly undesired products like poly-aromatic hydrocarbons (PAH), soot and coke.

[0012] Methods of fast pyrolysis of biomass as practiced by emerging energy companies use an almost dry biomass feed and typically yield homogeneous "oils", commonly called bio-oils. The oils contain mainly a variety of carbonyls/acids, pyrolytic lignin and water. Char is considered as a by-product. The pyrolytic water yield (often underestimated by researchers) is typically over 12-16 wt % on a dry biomass basis. Such pyrolytic water yield indicates the occurrence of dehydration reactions taking place during pyrolysis.

[0013] As set forth in US Patent Application No. 2004/0108251, a criticism of fast pyrolysis schemes is the need to circulate very high volumes of inert gas in order to transport the inorganic heat supplying material at a mass ratio versus the carbonaceous feedstock in the range of 12:1 to 200:1.

[0014] When the recycle gas stream in such volumes is required to transport the sand and biomass - such transport of gas increases the size and complexity of the entire pyrolysis recovery system. The required expenditure of energy to operate recycle blowers and compressors makes the pyrolysis operation very noisy, energy inefficient and often troublesome. The fouling of blowers and compressors is a common occurrence reported by the industry.

[0015] Steam usage in fast pyrolysis towards energy products (fuels) was never considered because the steam-water usage dilutes the liquid fuel - bio-oil, causing phase separation, non-homogeneity, a lowering of BTU value, etc. However, for non-bio-oil targeted processing, as found out in this application, steam has a number of advantages. For example, steam

enhances the removal of non-volatile chemical species (oligomeric lignin) from the reaction/pyrolysis zone due to their enhanced volatility with steam. Steam also tends to minimize thermal dehydration/condensation reactions occurring during pyrolysis and during condensation steps lessening yields of pyrolytic water. Polyaromatic hydrocarbons (PAHs), soot and coke yields are minimized. Steam increases yields of Hodge' carbonyls. Volumes of highly explosive and poisonous gases are no longer in re-circulation.

[0016] It has been found that pyrolytic charcoal absorbs a melt of oligomeric lignin. It is an object to use such composite as a base in a variety of soil enhancers and fertilizer formulations.

[0017] Also disclosed is provision of thermal processing while minimizing dehydration reactions.

[0018] Also disclosed is provision of a simplified method of producing Hodge' carbonyls and oligomeric lignin in improved yields and at lower costs.

[0019] Also disclosed is improvement and utilization of properties of pyrolytic char as an absorbent.

[0020] Still another object of this invention is to provide a method of using oligomeric lignin and pyrolytic char in novel formulations of slow release, carbon containing fertilizers by combining them with commercial N, P, K fertilizers like liquid and gas ammonia, ureas, polyureas, or ammonium, sodium, potassium nitrates or carbonates and similar, including nitrogen and phosphorous rich sludges, manures, and litters.

[0021] Also disclosed is enhancement of the economic viability of biomass conversion processes, especially as an integral part of a "bio-refinery", by providing a method for utilization of different parts of liquid and solid products.

[0022] A still further object of this invention is to provide a new product formulae leading to economically viable, high value partially organic "N, P, K, - C" slow release fertilizers which also can return bio-carbon to the soil (carbon sequestration in form of solid organic carbon).

[0023] Also disclosed is provision of a water solution of Hodge' carbonyls, potential feedstock for transportation fuel production, by means of well known processes like steam co-reforming of methane, gasification towards Fischer-Tropsh synthesis (Sasol), NREL catalytic hydrogen production, aqueous phase reforming and other similar processes, see :

- Czernik, S., French R., Feik, C., Chornet E., - "Hydrogen by Catalytic Steam Reforming of Liquid By-Products from Biomass Thermo-Conversion Processes", Ind. Eng. Chem. Res. 41, 4209-4215 (2002) and
- G.W. Huber, J.A. Dumesic, - "An overview of aqueous-phase catalytic processes for production of hydrogen and alkanes in a biorefinery", Catalysis Today, 111, 119-132

(2006).

SUMMARY OF THE INVENTION

[0024] There is provided a method of enhancing soil using a composite formed of oligomeric lignin and char derived from lignocellulosic biomass by fast pyrolysis of a feed of said biomass in the presence of steam, as defined in the claims.

[0025] A plurality of product streams are produced at selected temperatures which include Hodge' carbonyls, oligomeric lignin and bio-char particulates.

[0026] The biomass feed is lignocellulosics. Steam or steam-inert gas mixture is used at pyrolysis temperatures of 430 to 550 deg C.

[0027] Examples of lignocellulosics are forest and agricultural biomass like wood chips, barks, straw, stalks, husks, chaff, hulls, grasses, shives, needles, vine prunings, yew clippings, waste paper, organosolve lignin and similar. At this instance the main product streams are:

1. 1. Oligomeric lignin (wet); - water-insoluble phase
2. 2. Water-rich phase containing Hodge' carbonyls, acetic and formic acids, and partially water-soluble phenolics - homologs of syringol and guaiacol.
3. 3. Bio-char (charcoal, bio-carbon, agrichar)

[0028] It is judged in this invention that the oligomeric lignin in combination with char can be used to procure bio-carbon rich, slow release "N, P, K - C" fertilizers, soil enhancers and similar solid-organic-carbon (SOC) containing products. The utilization of whole fast pyrolysis bio-oil, in a procurement of nitrogen-slow- release fertilizer is described in US Patent No. 5,676,727 issued to Radlein, Piskorz, and Majerski.

[0029] In another aspect of the invention there is provided a method of enhancing soil using a product of the fast pyrolysis of lignocellulosic biomass, comprising char mixed/combined with oligomeric lignin.

[0030] The product of the fast pyrolysis of lignocellulosic biomass feed, is oligomeric lignin in combination with bio- char to form a soil enhancer.

BRIEF DESCRIPTION OF THE DRAWINGS

[0031] Further features and advantages will be apparent from the following detailed description, given by way of example, taken in conjunction with the accompanying drawings, wherein:

Fig. 1 is a schematic drawing of an apparatus for fast hydrous pyrolysis of biomass; and

Fig. 2 is a flow diagram showing the process of Fig. 1.

DETAILED

DESCRIPTION

[0032] Referring to Fig. 1, the system used for the pyrolysis "in- steam" consists of a pyrolyzer 1 coupled to a feed source 3 and to a source of superheated steam 2. The steam and external heaters 9 heat the feed material to a temperature high enough so that degradation occurs. Energy input to the steam source 2 and to the pyrolyzer 1 can be effected by heaters 9 running on product gas, on propane/butane/natural gas, solid fuels or electricity. The product stream from the pyrolyzer 1 is directed to a cyclone separator 7 which separates the char and then to a scrubber 4 which removes all condensibles including water. The output from the scrubber 4 is directed to a surge tank 5 where product gas (mostly carbon monoxide and carbon dioxide) is removed.

[0033] The surge tank liquid slurry is directed by a pump 6 to a phase separation device 8 such as a hydrocyclone, or centrifuge yielding the stream of oligomeric lignin (heavier, tarry phase) 10 and the aqueous phase stream 12 containing Hodge' carbonyls/acids and water-soluble phenolics. A part of the aqueous stream 13, after extra cooling by heat exchanger 11, is directed to the scrubber 4.

[0034] The process of pyrolyzing biomass in the presence of superheated steam is shown in Fig. 2. Biomass feed is directed from the feed source 3 to the pyrolyzer 1 at step 20. At the same time superheated steam from the steam source 2 is directed to the pyrolyzer 1 at step 22. At step 24 heat from an external heat supply 9 is applied to heat the feed material to raise its temperature high enough so that degradation occurs. At step 26 the product streams are extracted and fed to a cyclone separator 7 which separates the char (bio-char) 28 and sends the remaining aerosol stream to the scrubber 4. At step 30 droplets, particulates, vapors are removed from the gas phase by the scrubber 4. The gas stream (mostly carbon monoxide and carbon dioxide) is extracted from the surge tank 5 at step 32 while at step 34 oligomeric lignin rich stream (tarry) and Hodge' carbonyls stream (watery) are collected. The separation of these two streams is achieved by directing all scrubber condensables from the surge tank 5 by pump 6 to decanter device 8. Oligomeric lignin and some char are removed from the decanter

8 at one end and an aqueous product stream **14** is removed at the other end. An additional cooling **11** is applied to the aqueous product stream **14** before it is returned to the scrubber **4** along line **13**.

[0035] There are a number of additional advantages of this processing. It is possible to process biomass having a high moisture content like leaves, branches, yard waste, brush. Also, agricultural residua of high ash and nitrogen content can be processed. It is well known that such feeds are not optimal for bio-oil-energy targeted thermal conversions.

[0036] There are additional engineering advantages of using steam in the present application. For example, there is no need for recycle gas clean-up devices like filters, electrostatic precipitators, packed bed scrubbers-demisters. Such devices put additional (parasitic) energy demands on blowers/compressors. The presence of steam-water modulates pyrophillic properties of char-solids facilitating its safe removal/transport. The self-cleaning attributes of steam are of importance in keeping the recovery train unblocked. There is general simplicity of operation that requires only a farm level of technical sophistication. There is no start-up liquid medium required. The high temperature steam equipment and accessories required have an off-the-shelf availability.

[0037] The technological consequences of using steam, apart from a lowering pyrolytic water yield, is a lower gas-product yield. Also, water improves the thermal stability of both liquid fractions. The presence of water minimizes phenol-formaldehyde-like condensation reactions and aldol condensation reactions.

Cellulosic pyrolysis

Example 1

[0038] The object of this example is to demonstrate an augmented yield of key Hodge' carbonyls, hydroxyacetaldehyde and glyoxal, resulting from the pyrolysis of Avicel cellulose in steam versus non-steam processing.

Table 1

Cellulose pyrolysis. Avicel.		
I. STEAM in use		
Yields of hydroxyacetaldehyde and glyoxal		
Wt%, on dry feed base		
Temperature deg C	Hydroxyacetaldehyde	Glyoxal
575	16.9	4.2
550	19.2	2.9
525	16.3	4.4

Cellulose pyrolysis. Avicel.		
I. STEAM in use		
Yields of hydroxyacetaldehyde and glyoxal		
Wt%, on dry feed base		
Temperature deg C	Hydroxyacetaldehyde	Glyoxal
II. NO STEAM in use		
Temperature deg C	Hydroxyacetaldehyde	Glyoxal
600	12.1	3.4
550	10.9	4.0
525	10.6	3.7
475	4.9	0.3

[0039] The yields of hydroxyacetaldehyde, in particular, are consistently larger when cellulose is processed in steam.

Example 2

[0040] The object of this example is to demonstrate the augmented yields of Hodge' carbonyls from bleached pulps

Table 2

Pyrolysis feed - bleached pulp (Tembec)		
Temperature - 550 deg C		
Yields, wt%, dry feed basis		
	Steam processing	Non-steam processing
Run #	220	222
Hydroxyacetaldehyde	18.0	10.7
Glyoxal	4.1	1.5
Acetol	2.0	2.0
Formaldehyde	5.1	3.6

[0041] Yields of key Hodge' carbonyls are consistently higher in steam processing.

Example 3

[0042] The objective of Example 3 is to demonstrate elevated-augmented yields of Hodge carbonyls in a specified temperature above 490 deg C.

Table 3

Pyrolysis feed - unbleached pulp and cellulosic sludge from clarifier (Tembec) Steam processing				
Yields, wt% dry basis				
Feed	Pulp	Pulp	Pulp	Sludge
Temperature, deg C	450	500	550	500
Glyoxal	Trace	2.1	1.8	0.9
Methylglyoxal	Trace	0.9	0.8	
Hydroxyacetaldehyde	6.4	12.0	12.0	11.0
Formaldehyde	6.7	7.7	5.9	
Acetol	2.8	4.7	Nd	2.5

[0043] The table illustrates, that cellulosic pulps and sludges can be pyrolyzed, preferably at 500-550 deg C, to yield Hodge' carbonyls

Lignocellulosics pyrolysis

Example 4

[0044] The objective of example 4 is to demonstrate elevated yields of Hodge' carbonyls and oligomeric lignin from lignocellulosics, when applying steam processing utilizing as a feed a British Columbia fir-spruce (softwood) mix

Table 4

Yields, wt %, dry basis		
Run #	224	226
Temperature, deg C	485	460
Atmosphere	Nitrogen	Steam, Nitrogen
Char	10.9	11.8
Oligomeric lignin	19.6	22.3
Glyoxal	0.8	1.4
Hydroxyacetaldehyde	12.5	15.0
Formaldehyde	2.2	2.4

[0045] Again, steam processing yielded relatively more Hodge' carbonyls and, also this time in the case of lignocellulosics more oligomeric lignin.

Example 5

[0046] Example 5 compares steam processing of hardwoods (beech) with processing without steam for different temperatures.

Apparent vapour residence time ~1 second

[0047]

Table 5

Yields, wt%, dry feed basis		
Temperature, deg C	435	425
Atmosphere	Nitrogen	Steam, Nitrogen
Char	15.1	10.9
Oligomeric lignin	16.5	23.0
Glyoxal	2.0	2.2
Hydroxyacetaldehyde	7.1	8.6
Temperature, deg C	485	475
Atmosphere	Nitrogen	Steam, Nitrogen
Char	9.3	8.3
Oligomeric lignin	18.0	28.0
Glyoxal	2.0	2.0
Hydroxyacetaldehyde	9.5	9.5
Temperature, deg C	530	545
Char	6.3	6.0
Oligomeric lignin	25.0	25.0
Hydroxyacetaldehyde	7.7	8.0
Levogluconan	2.2	1.0

[0048] Again, for hardwoods, steam processing increases yield of oligomeric lignin, particularly when processed at temperature of 475 deg C. Hodge carbonyls yield is affected only slightly.

Example 6

Rice straw processing

[0049] The object of this example is to illustrate the advantageous effects of steam use in limiting dehydration reaction (less pyrolytic water production) and elevated yields of overall pyrolytic condensables (water-less organics)

Table #6

Yields, Wt% dry, ash free basis		
Run #	236	238
Atmosphere	Nitrogen	Steam/Nitrogen
Temperature, deg C	490	475
Pyrolytic water	21.5	18.1
Organic condensables	37.9	43.2
Gases	19.0	16.6
Char	18.2	17.5

[0050] Steam processing lowered yields of pyrolytic water and gas.

Example 7

[0051] Oligomeric lignin (humus analog/precursor) and char yields are of interest when formulating proposed soil enhancers/fertilizers containing organic carbon.

[0052] The following table sets forth a summary of experimental work showing typical yields of chars and oligomeric lignin upon fast pyrolysis with steam processing at ~500 deg C.

Table 7

Yields, wt% (on moisture, ash free basis)		
Biomass	Pyrolytic CHAR	Oligomeric LIGNIN
Corn Bran	11	9
Corn Hulls	11	12
Corrugated Cardboard	12	12
Sugar Cane Bagasse	12	13.5
Giant Reed	14	14
Willow Coppice	12	17
Flax Straw	15	15

Yields, wt% (on moisture, ash free basis)		
Biomass	Pyrolytic CHAR	Oligomeric LIGNIN
Oats Hulls	13	18
Switch Grass	14	16
Hemp	16	16
Biomass	Pyrolytic CHAR	Oligomeric LIGNIN
Miscanthus	13	19
Corn Stover	15	20
Distiller's Grain	17	20
Flax Shives	16	22
Olive Pits	16	24
Coffee Waste	16	24
Sewage Sludge	20	34
Pine Brush	18	35
Pine Needles	25	29

Example 8

[0053] Example 8 deals with fast pyrolysis of a spruce-fir mix in steam. The products obtained, namely, charcoal and oligomeric lignin, were mixed together in weight proportion 30-70, respectively. At a temperature of ~ 45 deg C the oligomeric lignin melt was absorbed totally by the charcoal. The charcoal retained the original particle size. Its bulk density increased more than 3 times.

[0054] Such a dual product-component, charcoal + oligomeric lignin, can be considered as a flexible matrix in the formulation of fertilizers, a matrix in which a range of nutrients and additives could be included. Thus, a unique and valuable fertilizer for agricultural and horticultural applications can simply be specified and then formulated.

[0055] Judging from the examples 7 and 8 one can conclude that 20 to 50 % of biomass could be converted to a novel oligomeric lignin and char composite wherein the lignin and the char are physically combined. Such composite could be utilized as a novel soil enhancer, rich in SOC (soil organic carbon). Such composite can be utilized also (by adopting known-art) to formulate a variety of fertilizers with specified nitrogen, phosphorous, and potassium content. In particular, oligomeric lignin melt is suitable to be used as a coating of commercially available solid N,P,K fertilizers making them into a slow or controllable release type. A novel fertilizer formulae, this time, including an element carbon is described by the 4- letters "N,P,K and C".

Example 9

[0056] This example also deals with fast pyrolysis of a spruce-fir mix in steam. However, in this case a no cyclone with a condensing trapping unit is used in the recovery train to separate char particles.

Steam : biomass (dry) ratio 1:1.

The following two separate streams of products were targeted.

1. 1. Hodge carbonyls in a yield of 50wt% on a dry wood basis, in water. The water content of the actual product is ~50wt%.
2. 2. Char - oligomeric lignin solids. The charcoal particulates contain all oligomeric lignin in their bulk volume. The yield of char + oligomeric lignin on a dry biomass basis is 32wt%. As produced this stream is still wet with approximately 27wt% water.

[0057] The example teaches, that even more simplified processing, this time without cyclonic char particulate separation, could be adopted, if judged sufficient for a targeted products spectrum.

REFERENCES CITED IN THE DESCRIPTION

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Patentkrav

1. Fremgangsmåde til forøgelse af jord ved anvendelse af en komposit, der er dannet af oligomer lignin og trækul, der stammer fra lignocellulosisk biomasse
5 ved hurtig pyrolyse af en ladning fra nævnte biomasse ved tilstedeværelse af damp til at producere (i) en strøm af vandopløselige carbonyler stammende fra carbohydrat, (ii)) en strøm af vandopløseligt oligomer lignin og (iii) en strøm af trækul, hvor fremgangsmåden omfattende følgende trin:
 - 10 (a) udsættelse af den lignocellulosiske biomasse for overophedet damp i en pyrolysator, hvor biomassen opvarmes til en temperatur i området 430 - 550 ° C,
 - (b) hurtig pyrolysering af nævnte biomasse i pyrolyseren ved tilstedeværelse af overophedet damp,
 - 15 (c) nedbrydning af biomassen,
 - (d) opsamling af produktstrømme omfattende (i) den vandige strøm indeholdende nævnte carbonyler stammende fra carbohydrat, (ii) strømmen af vådt oligomer lignin og (iii) strømmen af trækul,
 - (e) fysisk at kombinere oligomer lignin og trækullet til dannelse af komposit-
 - 20 ten, og
 - (f) anvendelse af kompositten til at forbedre jorden.
2. Fremgangsmåde ifølge krav 1, hvor trin (c) til (d) omfatter:
 - 25 (c) nedbrydning af biomassen for at danne en strøm indeholdende trækul og en aerosolstrøm,
 - (d) (d1) adskille trækullet fra aerosolstrømmen i en cyklon, (d2) opdele aerosolstrømmen i en gasstrøm og en kondensabel strøm i et renseapparat, og (d3) dele den kondensable strøm i en faseseparationsindretning,
 - 30 i en centrifuge eller i en karaffel op i den vandige produktstrøm indeholdende carbonyler stammende fra carbohydrat og en tjæreproduktstrøm indeholdende oligomer lignin.

3. Fremgangsmåde ifølge krav 1 eller 2, hvor nævnte carbonyler omfatter mindst én blandt hydroxyacetaldehyd, glyceraldehyder, acetol, pyruvaldehyd, glyoxal, 5-hydroxymethylfurfural, furfuraler og formaldehyd.
- 5 4. Fremgangsmåde ifølge krav 1 eller 2, hvor den lignocellulosiske biomasse omfatter træflis, bark, halm, stængler, skaller, avne, bælge, græsser, skiver, nåle, vinbeskæringer, beskæringer af takstræ, affaldspapir eller organisk opløst lignin.
- 10 5. Fremgangsmåde ifølge krav 1, hvor lignocelluloserne er valgt fra skovbrug og landbrugsmæssigt produceret biomasse indbefattet spild og rester.
6. Fremgangsmåde ifølge krav 1, hvor nævnte trækul har et højt indhold af oxygenerede funktionelle grupper og fungerer ikke blot som en absorbent men
15 binder også nitrogen direkte ved reaktion med NH_2 -grupperne.

DRAWINGS



