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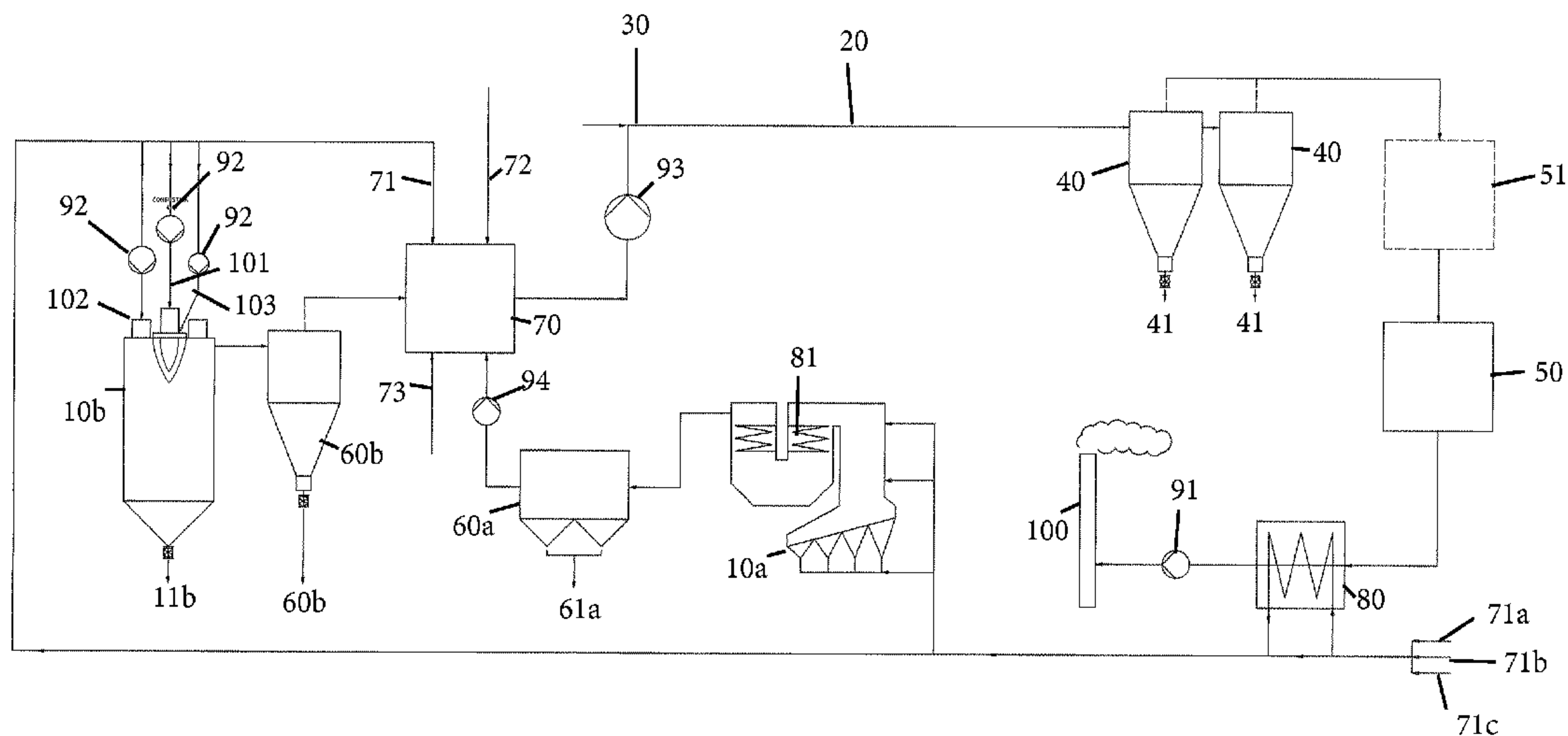
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(54) Titre : APPAREIL ET PROCEDE DE SECHAGE CONTINU DE PRODUITS EN VRAC
(54) Title: APPARATUS AND METHOD FOR CONTINUOUSLY DRYING BULK GOODS

Fig. 1



(57) **Abrégé/Abstract:**

The present invention relates to an apparatus for drying bulk goods and a method for continuously drying bulk goods. In particular, the invention relates to an apparatus as well as a method for drying wood fibers.

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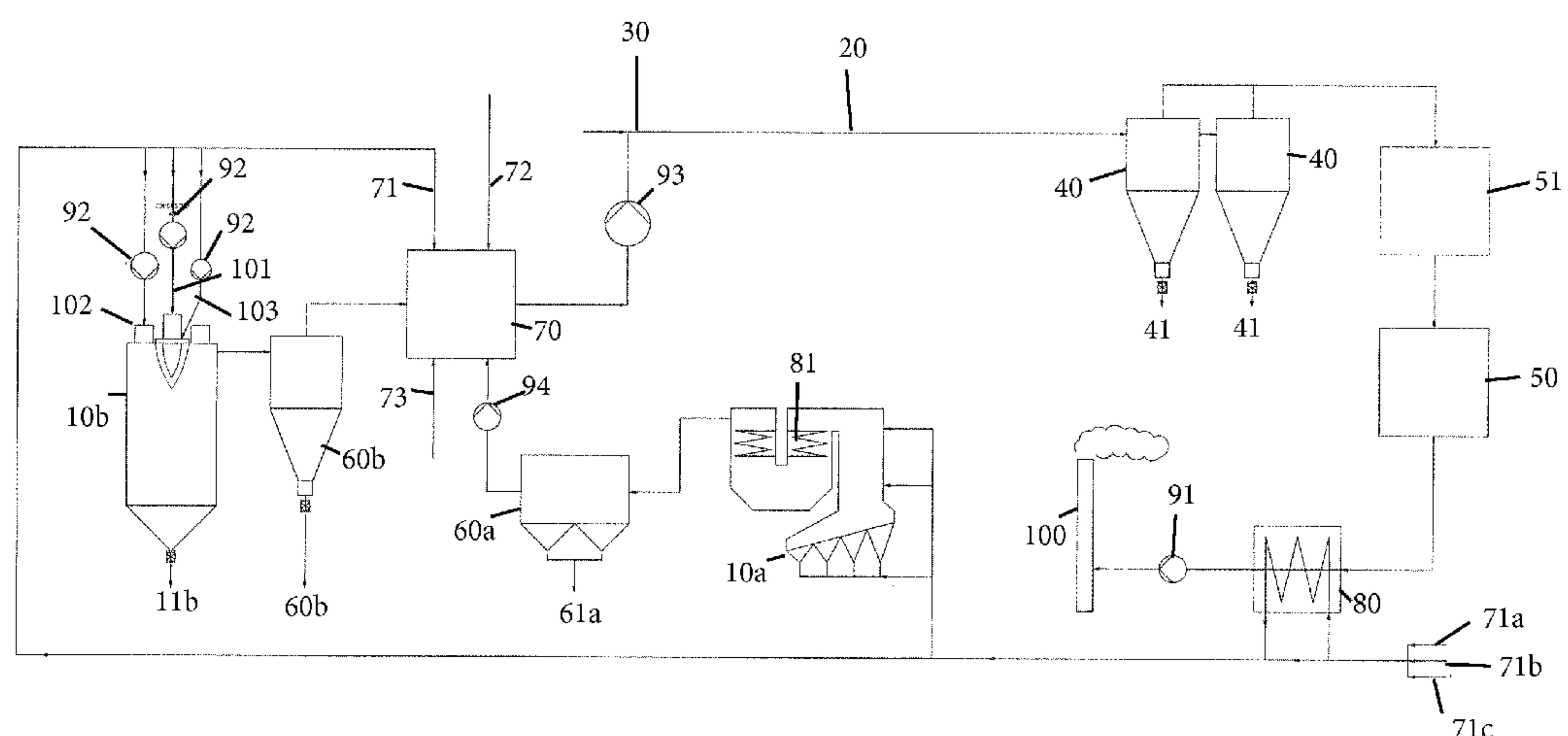
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(54) Title: APPARATUS AND METHOD FOR CONTINUOUSLY DRYING BULK GOODS

Fig. 1



(57) Abstract: The present invention relates to an apparatus for drying bulk goods and a method for continuously drying bulk goods. In particular, the invention relates to an apparatus as well as a method for drying wood fibers.

WO 2018/224130 A1

Apparatus and method for continuously drying bulk goods

5 The present invention relates to an apparatus for drying bulk goods and a method for continuously drying bulk goods. In particular, the invention relates to an apparatus as well as a method for drying wood fibers.

10 From the state of the art, numerous methods for manufacture of wood-fiber-boards are known, and which wood-fibers are produced from boiled wood chips. These boiled wood chips are supplied to a so-called refiner wherein the wood chips are processed by means of grinding discs to form fibers. The fibers are removed from the refiner by means of steam and transported via a line known as "blow-line" to a drying tube. Air is blown through the drying tube at elevated temperatures in order to dry the fibers.

15 In a drying tube, usually the moisture content of the wood fibers is reduced from 100% to e.g. 8 – 11%.

In the methods known from the state of the art, the fibers can be provided with an adhesive in the blow-line before entering the drying tube, in the alternative, the dry fibers are applied with adhesive after their removal from the dryer.

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Examples for the method described in the foregoing can e.g. be found disclosed in WO 03/013808 A1 or WO 03/013809 A1.

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WO 2015/056174 A2 describes a process for obtaining glued fibers suitable for a production of fiberboards, wherein the fibers are carried in an air stream for the removal of high density containments from the dried fibers by means of gravity, and said dried fibers are glued.

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EP 0 876 887 B1 refers to a method for the manufacture of a board from lignocellulosic material, comprising disintegration of the material, gluing, drying in two stages, forming to a mat and hot pressing the same to a ready board, where exhaust air from drying and pressing is used in a heat energy plant. The air used for drying the disintegrated lignocellulosic material is indirectly heated via heat exchangers, which are provided with thermal energy by means of a combustion furnace. The humid exhaust air, which results when drying the disintegrated lignocellulosic material is fed to the combustion furnace.

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The drawback of the method described in the foregoing is, however, that the heat exchangers used to heat the drying gases with the exhaust of the combustion furnace are often subject to inspection since solids contained in the exhaust gases precipitate in the heat exchangers thus reducing the standing time of the system. Due to the fact that the wet drying gases are post-combusted in the combustion furnace, the efficiency of the combustion process is additionally reduced.

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The objective of the present invention therefore is to overcome the disadvantages known from the prior art and to provide a reliable method for drying bulk material, especially wood fibers and/or wood chips.

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The aforementioned objective is solved by the apparatus as described in claim 1 as well as the method described in claim 15. The respective dependent claims describe advantageous embodiments.

5 Accordingly, the present invention relates to an apparatus for drying bulk goods, in particular of wood fibers and/or wood chips, comprising

at least one hot gas generator, producing hot gases used as drying gases in at least one dryer,

10 at least one dryer, in particular a flash tube type dryer, said at least one dryer is aligned downstream of said at least one hot gas generator and directly supplied with hot gases produced by said at least one hot gas generator,

at least one blow-line entering the at least one dryer,

at least one apparatus for separating the bulk goods from the drying gases which is aligned downstream of the at least one dryer,

15 wherein downstream of the at least one apparatus for separating the bulk goods from the drying gases at least one heat exchanger is provided which uses the separated drying gases to indirectly heat at least a part of the gases being fed to the at least one hot gas generator as combustion air.

20 According to the present invention at least one heat exchanger, that is one heat exchanger or more than one heat exchangers, such as e.g. two, three or more heat exchangers are provided in the apparatus according to the invention. If more than one heat exchanger is provided in the apparatus according to the present invention, the heat exchangers can be provided at
25 different positions within the apparatus and thus aligned subsequently (i.e. one heat exchanger is aligned downstream from an earlier aligned heat exchanger). In addition or in the alternative, two or more exchangers also can be operated in parallel at the same position within the apparatus according to the invention.

30 The hot exhaust gases produced by the at least one hot gas generator directly are used as drying gases in the apparatus according to the invention. In contrast to the methods known from the state of the art, heat exchangers which are provided directly downstream of the hot gas generator are omitted.

Due to the fact that the hot gases produced by said at least one hot gas generator directly are used for drying the bulk material, not only a higher drying efficiency can be achieved, but only one drying circuit is necessary. This eliminates the need of one or more heat exchangers, which often are subject to inspection. Thus in addition a contamination of the – not existing heat exchangers – is eliminated. Accordingly, the up-time of the inventive apparatus can be increased. In addition, the at least one heat exchanger aligned downstream of the separation device is used to pre-heat gases used as combustion gases (such as e.g. primary air, secondary air and/or tertiary air) before entering the at least one hot gas generator. Accordingly, a large part of the thermal energy contained in the drying gases can be recuperated and returned to the drying system before the cooled drying gases are released into the environment. Accordingly the energetic efficiency of the whole system can be further increased.

In a preferred embodiment, at least one further heat exchanger is provided upstream and/or downstream of the above described (first) at least one heat exchanger which uses the separated drying gases to indirectly heat a thermal fluid, such as e.g. water and/or thermal oil. These fluids can be used to transport thermal energy wherever needed in the system according to the invention or to any other part of the plant.

For example, said at least one additional heat exchanger can be a heat exchanger which uses a thermal oil as heat exchange medium. This heat exchanger can be aligned downstream of the above described first heat exchangers used for preheating the combustion air for the at least one hot gas generator. Of course it is also possible to align more than one of the thermal oil heat exchangers in the series and/or in parallel.

Furthermore, it is also possible to use at least one additional heat exchanger which uses water as heat exchange medium in addition to the first type of heat exchanger (used for preheating the combustion air for the at least one hot gas generator), and – if present – in addition to the above described at least one heat exchanger working with thermal oil as heat exchange medium.

In a preferred embodiment, this type of heat exchanger is the last in the row

of the heat exchangers and is present, before the treated drying gases are released into the environment.

5 In any case it is preferred that – regardless of how many heat exchangers of the same or different type are used – the drying gases are cooled only to a temperature that contained water vapours do not condense.

Preferably, the drying gases are not cooled in a way that entrained moisture condensates.

10

According to a preferred embodiment, at least one cleaning device for cleaning the hot gases produced by said at least one hot gas generator is provided in between the at least one hot gas generator and the at least one dryer, so that the exhaust gases produced by said at least one hot gas generator are passed through the at least one cleaning device for cleaning the hot gases.

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By means of the cleaning device, an effective removal of e.g. solids, contained within the hot gases produced by the at least one hot gas generator is possible. Accordingly, a deposition of said solid particles contained within the hot gases, e.g. fume gases, in the bulk good should be dried can effectively be suppressed. Therefore, less pollution of the bulk good is possible. Furthermore, a deposition of such solid particles in the subsequently aligned dryer is additionally suppressed. Accordingly, less maintenance of the dryer is necessary. The cleaning device provided in between the hot gas generator and a dryer therefore attributes to an enhanced service time of the apparatus of the invention. In addition, the degree of efficiency of the dryer can be maintained at high levels, a better drying efficiency of the bulk good is achieved. Thus, the apparatus according to the invention is superior to the ones known from the prior art, since overall a better efficiency results.

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The specific embodiment as described in the foregoing therefore solves the problem known from the prior art, that the hot gases produced from the hot gas generator comprise high amounts of solid particles, such as soot, carbon black, etc. resulting from the combustion process in the burner. Furthermore, solid pollutants are comprised in these fume gases. Accordingly, there has

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5 been a prejudice in the prior art, that the fume gases produced by the hot gas generator cannot directly be used as drying gases for drying bulk goods, since it has been feared that the bulk goods could be polluted by the solid particles contained in the hot fume gases. Therefore, in the prior art, always heat exchangers have been aligned downstream of the hot gas generators in order to heat drying gases used for drying of the bulk goods. However, if the exhaust gases of the hot gas generator are used to indirectly heat the drying gases by means heat exchangers, it is observed that the heat exchanger negatively can be effected by deposition inside the solid heat exchangers. 10 These depositions result from a high content of solids and be burned exhaust gases.

15 Accordingly, the preferred embodiment described in the foregoing contributes to the elimination of a need of a heat exchanger. Furthermore, the exhaust gases preferably can directly be used to dry the bulk goods. Accordingly, no energetic losses are observed. In addition, the cleaning of heat exchangers, once depositions have occurred can be avoided.

20 In an especially preferred embodiment, said at least one cleaning device for cleaning the hot gases is selected for the group consisting of a hot gas cyclone and an electrostatic precipitator, preferably a dry type electrostatic precipitator.

25 The at least one hot gas generator preferably is at least one solid fired hot gas generator, preferably a grate fired hot gas generator, a fluidized bed combustion hot gas generator and/or a stoker fired hot gas generator; and/or at least one multi-fuel burner.

30 It is also possible to combine two or more hot gas generators, which can be operated in parallel or in series.

35 According to another preferred embodiment the apparatus according to the invention is characterized in that said at least one hot gas generator comprises at least one solid fired hot gas generator. A solid fired hot gas generator allows the combustion of combustible organic material in any particular form, such as e.g. bulky wooden goods, particulate wooden goods or even wooden

dusts. As examples for a solid fired hot gas generators grate fired hot gas generators, fluidized bed combustion hot gas generators and/or stoker fired hot gas generators are possible which also can be present in combination. However, also multi-fuel burners known from the state of the art are possible.

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If more than one hot gas generator is present in the apparatus according to the invention, preferably both a solid fired hot gas generator and a multi-fuel burner are present. Accordingly, the apparatus is most flexible as far as possible fuels to cover the energetic need is concerned.

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The presence of a multi-fuel burner e.g. allows the combustion of fossil fuels such as gas or light oil, or dust-like solids such as wooden dust which can occur as side product in the drying process or in a following production of chipboards. The fuels can be used alone or in combination with each other. E.g. a mixture of wood dust and light oil or a mixture of wood dust and gas can be used.

15

A solid fired hot gas generator according to the present invention is enabled to combust solid materials, which cannot be combusted in the multi-fuel burner systems as described in the foregoing. Therefore, an alternative energetic supply concept of the apparatus according to the present invention is possible. With the solid fired hot gas generator, all materials which cannot be used in the production of e.g. wooden particle or fiberboards, can be energetically recycled. Examples of such materials are e.g. barks, production wastes of particle boards, wooden chips, packing material and/or waste wood.

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Furthermore, it is also possible to co-operate said solid fired hot gas generator in parallel or independent with a multi-fuel burner, i.e. the solid fired hot gas generator can be operated simultaneously or alternatively to the multi-fuel burner. This allows for a very flexible adjusting of the apparatus as far as the energetic supply is concerned. Also in case that the apparatus demands a peak amount of thermal energy the multi-fuel burner can help to deliver additional and quickly available thermal energy in addition to the solid fired hot gas generator.

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According to another preferred embodiment the apparatus according to the invention is characterized in that at least one hot gas generator comprises at least one multi-fuel burner and at least one solid fired hot gas generator which are aligned in parallel, said at least one multi-fuel burner comprises a combustion chamber with a muffle in which a fuel/combustion air mixture is ignited and burned and a combustion chamber ceiling, said combustion chamber ceiling comprising

- at least one inlet for combustion air into the muffle,
- an outer nozzle ring forming an inlet for a cooling gas surrounding the muffle and
- an inner nozzle ring forming an inlet for a cooling gas inside the muffle providing a laminar flow of cooling gas along the muffle.

A special feature underlying the present invention is that at least said inner and an outer nozzle ring being separately controllable and said inner nozzle ring being fed with gas exhausted by the at least one solid fired hot gas generator, with ambient air and/or with gas resulting from external production processes, such as press exhaust gases, saw exhaust gases, sanding line exhaust gases and/or exhaust gases from a glue production line.

According to this principle, the muffle, in which the fuel/combustion air mixture is ignited, can effectively be cooled. Due to the fact, that the air, entering through the inner nozzle ring preferably comprises considerably minor oxygen content, the formation of nitrous oxides can be reduced.

This advantage enables that post-burner-treatment of the exhaust gas, in order to reduce nitrous oxide, such as e.g. the injection of urea etc. can be reduced or even omitted and leads to considerably less complex apparatuses, which are easier to operate.

In addition and in a preferred embodiment, the gases used to supply the inner nozzle ring of the multi-fuel burner as described above can also be used to be fed into the multi-fuel burner through the outer nozzle ring.

The inventive apparatus is preferably characterized in that said at least one hot gas generator is fed with combustion gases which directly are derived

from external process steps such as press exhaust gases, saw exhaust gases, sanding line exhaust gases and/or exhaust gases from a glue production line. These external gases can be used as combustion air, cooling air, muffle cooling air, primary air, secondary air, tertiary air, and/or recirculation air within said at least one hot gas generator. Accordingly, the overall emission of an apparatus, which is integrated in an alignment for the production of wooden boards, can be reduced. Furthermore, reduction of emission sources is possible since these sources are thermally disposed within the at least one hot gas generator. Both a reduction of total mass flow of emissions and a reduction of total volume flow of exhaust gases therefore is possible. Especially advantageous is the increase of efficiency by the use of preheated combustion air.

In a particularly preferred embodiment of the inventive apparatus or method the cooling air supply to the hot gas generator is achieved via an interior and an exterior nozzle ring in the ceiling of the combustion chamber. It is particularly preferred, that these nozzle rings can be controlled separately from each other. Preferably, the inner nozzle ring and/or the outer nozzle ring are provided with a pre-adjusted entering angle for the respective fuel which is in the range between approximately 0, preferably 10 and approximately 60 degrees. Due to this construction of the cooling air supply respectively of the ceiling of the combustion chamber and the particular air supply in the combustion chamber as well as the guiding of the secondary air and the condensation deriving there from, combustion in the combustion chamber is achieved in a particularly advantageous manner.

According to an additionally preferred embodiment, between the at least one hot gas generator and the at least one dryer a mixing chamber is aligned which allows for the mixing of the hot gases of the at least one hot gas generator with further external gases which preferably are pre-heated and/or ambient air.

According to a further preferred embodiment according to the present invention downstream of said at least one apparatus for separating the bulk goods from drying gases at least one device for cleaning the drying gases exiting the at least one apparatus for separating the bulk goods from the

drying gases is provided, said at least one device for cleaning the drying gases being preferably provided upstream of the at least one heat exchanger. These cleaning devices can e.g. be regenerative thermal oxidizers (RTO) and/or wet electrostatic precipitators (WESP).

5

By incorporating devices for cleaning the drying gases such as e.g. RTOs and/or WESPs, a combustion or oxidation of contained volatile organic compounds (VOC) contained in the drying gases is possible. Accordingly, the emissions produced by the apparatus according to the present invention are by far lower than comparable emissions by drying apparatus according to the state of the art. Furthermore, the cleaning devices which are located downstream of the at least one apparatus for separating the bulk goods from drying gases also can be used in order to eliminate pollutants which can be produced during the combustion process taking place in the hot gas generator.

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According to this specific embodiment, the apparatus allows for a highly efficient drying of bulk goods with a minimum of harmful emissions.

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Furthermore, it is advantageous if downstream of the at least one apparatus for separating the bulk goods from drying gases (40), preferably in between the at least one apparatus for separating the bulk goods from drying gases at least one solids separator for separating solids from the drying gases is provided.

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Accordingly, e.g. dust particles etc. resulting from the dried bulk goods can be separated from the drying gases.

30

Downstream of said at least one heat exchange, at least one exhaust fan can be provided. In a particular preferred embodiment the exhaust fan directly is provided before a chimney used to exit the drying gases into the surrounding so that the complete system is operated in suction mode.

35

The present invention furthermore provides an arrangement for the manufacturing of wooden material boards, comprising at least one crushing device, at

least one drying device and at least one pressing device. The drying device of this arrangement is configured as the apparatus described in the foregoing.

Furthermore, the present invention relates to a method for continuously drying bulk goods, in particular wood fibers and/or wood chips in at least one dryer, in particular a flash tube type dryer, which is supplied with bulk goods via a blow-line entering the at least one dryer and with hot gases produced by at least one hot gas generator, said bulk good – after exiting the at least one dryer – being separated from the drying gases by means of at least one apparatus for separating the bulk goods from the drying gases which is aligned downstream of the at least one dryer, wherein after separation of the bulk goods from the drying gases the drying gases are fed to at least one heat exchanger which uses the thermal energy of the drying gases to indirectly heat at least a part of the gases being fed to the at least one hot gas generator as combustion air.

According to the present invention, the bulk goods enter the dryer via a blow-line. Preferably, the blow-line opens into the center of the drying tube, which e.g. can have a diameter of up to 5 m, such as e.g. 2,60 m. Drying gases are blown through the drying tube at a temperature of e.g. 100 – 300°C, preferable 130 – 240°C. Accordingly, the moisture can be reduced from 100% to 8 – 11% moisture content in the bulk good.

The bulk goods to be dried especially can be wooden fibers which are obtained by grinding wood chips in a refiner. The fibers can be removed from the refiner by means of steam and transported to the dryer via the blow-line. The steam pressure used to transport the fibers can be approximately 10 bar, the temperature of the steam can be approximately set to 150 – 160°C.

The grinding process of wooden chips and the transportation of the resulting fibers via the blow-line is conventionally known from the prior art.

An adhesive can be added to the fibers in the blow-line. However, it is also possible to omit the step of adding an adhesive.

The dryer can be especially in form of a flash dryer. This type of dryer includes a long tube, which can be e.g. up to 300 m long. The fibers are transported by means of a stream of drying gases by which according to the present invention are the exhaust gases of a hot gas generator.

5

According to a preferred embodiment, said exhaust gases produced by at least one hot gas generator are passed through at least one cleaning device for cleaning the hot gases before entering the at least one dryer, wherein the hot gases are cleaned, wherein said at least one cleaning device for cleaning the hot gases is preferably selected for the group consisting of a hot gas cyclone and an electrostatic precipitator, preferably a dry type electrostatic precipitator.

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Furthermore, it is possible that said at least one hot gas generator comprises at least one solid fired hot gas generator, preferably a grate fired hot gas generator, a fluidized bed combustion hot gas generator and/or a stoker fired hot gas generator which is fired with biomass, in particular wood biomass; and/or at least one multi-fuel burner.

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In an especially preferred embodiment, the at least one multi-fuel burner comprising a combustion chamber with a muffle in which a fuel/combustion air mixture is ignited and burned and a combustion chamber ceiling, said combustion chamber ceiling comprising

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- at least one inlet (101) which is fed with combustion air,
- an outer nozzle ring (102) which is fed with a cooling gas surrounding the muffle and
- an inner nozzle ring (103) which is fed with a cooling gas for providing inside the muffle a laminar flow of cooling gas along the muffle,

25

said inner and outer nozzle ring (102) being separately controllable.

30

In the embodiment described in the foregoing, the inner and/or the outer nozzle ring can have an entering angle between approximately 0 and approximately 60 degrees, preferably in between 10 and 60 degrees, which angle is preferably adjustable depending on the fuel used.

35

Furthermore, it is possible, that between the at least one hot gas generator and the at least one dryer the hot gases of the at least one hot gas generator are mixed with further external gases which preferably are pre-heated and/or ambient air.

5

Especially, between the at least one apparatus for separating the bulk goods from drying gases and the at least one device for cleaning the drying gases exiting the at least one apparatus for separating the bulk goods at least one additional cleaning step for separating solids from the drying gases is carried out.

10

Furthermore, gases which are fed to the at least one hot gas generator as combustion air are indirectly heated by means of at least one heat exchanger which uses the thermal energy contained in the gases downstream of the at least one device for cleaning the drying gases.

15

Finally, the drying gases can be propelled by means of at least one exhaust fan which is provided downstream of said at least one device for cleaning the drying gases.

20

The present invention is further specified in the following figure without restricting the invention to the specified details.

Figure 1 shows an apparatus according to the present invention, in which a method according to the present invention can be implemented.

25

The drying apparatus according to Figure 1 comprises a dryer 20, which in the present case is a flash tube. Wood fibers, which are to be dried within the dryer 20 are entered into the tube dryer by means of a blow-line 30. The fibers are blown into the tube dryer with superheated steam which expands into the tube 20. Hot air is blown through the dryer tube 20 which by means of fan 93. This hot air is provided from a mixing chamber 70, which is used to optionally mix hot gases resulting from hot gas generators 10a, 10b with further gases.

30

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The apparatus as displayed in Figure 1 comprises two hot gas generators, namely a grate fired hot gas generator 10a and a multi-fuel burner 10b. The exhaust gases of both types of hot gas generators flow into the mixing chamber 70. Depending on the energetically need or on fuels available, the grate fired hot gas generator 10a and the multi-fuel burner 10b can be operated in parallel or in the alternative. Before entering the mixing chamber 70, the hot gases produced by the grate fired hot gas generator 10a and the multi-fuel burner 10b are cleaned by cleaning devices. In Figure 1, dry type electrostatic filter 61a is located downstream of the grate fired hot gas generator 10a, whereas a hot gas cyclone 60b is located downstream of the multi-fuel burner 11b. However, it is also possible that for each type of hot gas generator the same type of cleaning device is used.

The grate fired hot gas generator 10a optionally encompasses a thermal oil casing 81 in which the thermal energy produced by the grate fired hot gas generator 10a can be used for external process.

The multi-fuel burner 10b comprises a muffle, in which the combustion is taken place. The gases 71a, 71b and 71c can be used as primary air and fed into the muffle as combustion air. Inside the muffle, a combustion air/fuel mixture is ignited and combusted. The mixing of the primary air and the fuel is not displayed in Figure 1. The primary air is added at inlet 101 into the multi-fuel burner 10b.

Furthermore, the multi-fuel burner 10b encompasses an outer nozzle ring 102, into which cooling air for the muffle can be entered.

In addition, a further muffle cooling air stream 103 can be provided directly to the muffle.

The air streams added to the multi-fuel burner 10b can respectively be propelled by means of adjustable fans 92.

Solids, which are extracted from the hot gases produced by either the grate fired hot gas generator 10a or the multi-fuel burner 10b, such as carbon black and/or soot can be extracted from the cleaning devices via a dust exit 61a or

61b, respectively. Also the multi-fuel burner 10b encompasses an exit 11b in which solids, which precipitate inside the multi-fuel burner 10b during the combustion process can be extracted.

5 The cleaned hot gases from the hot gas generators 10a and 10b, respectively, are entered into the mixing chamber 70. Into the mixing chamber, external gas streams such as e.g. preheated ambient air 71a, polluted exhaust air (such as e.g. from external processes) or exhaust air 71c can be entered.

10 Additionally, the same gases also can be entered into the mixing chamber 70 at ambient temperature at 72. Also the addition of ambient air (fresh air 73) is possible.

15 The hot gases produced by the hot gas generators can be conveyed by means of a fan 94 towards the mixing chamber.

By the ratio of the different air streams, the volume and/or the temperature of the gases transported to the tube dryer 20 can be adjusted.

20 After the drying gas/fiber mixture leaves the flash tube 20, the fibers are extracted from the gas stream by means of at least one cyclone, such as the two subsequently aligned cyclones 40 as shown in Figure 1. The dried fibers leave the cyclones 40 at fiber exit 41.

25 The separated drying gases can be conducted to an optional separation device 51, in which solid particles can be extracted from the gas stream. Further, downstream the gases are treated in an emission control system, i.e. a cleaning device 50. This cleaning device can be e.g. a regenerative thermal oxidizer (RTO) or a wet electrostatic precipitator (WSEP). It is possible that
30 either one or both of the aforementioned devices are present.

The thus cleaned drying gases are then further conveyed to a heat exchanger 80 in which the entrained thermal energy of the drying gases is recuperated. Preferably, the drying gases are not cooled in a way that entrained moisture
35 condensates. The recuperated energy is transferred to a part of the gases 71a,

71b and 71c which are fed to the hot gas generators 10a and 10b as combustion air.

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In alternative and also preferred embodiments, an additional second heat exchanger which uses a thermal oil as heat exchange medium (not shown) can be aligned downstream of the heat exchanger 80.

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Additionally, a third heat exchanger which uses a water as heat exchange medium (not shown) can be aligned downstream of the second heat exchanger.

15

The gases are propelled by means of a fan 91 towards a chimney 100, wherein the cleaned gases are released into the environment. The second and third heat exchangers (if present) preferably are aligned upstream of fan 91 so that all heat exchangers can be operated in suction mode.

Claims

- 5 1. Apparatus for drying bulk goods, in particular of wood fibers and/or wood chips, comprising
- at least one hot gas generator (10a, 10b), producing hot gases used as drying gases in at least one dryer (20),
- 10 at least one dryer (20), in particular a flash tube type dryer, said at least one dryer (20) is aligned downstream of said at least one hot gas generator (10a, 10b) and directly supplied with hot gases produced by said at least one hot gas generator (10a, 10b),
- at least one blow-line (30) entering the at least one dryer (20),
- 15 at least one apparatus for separating the bulk goods from the drying gases (40) which is aligned downstream of the at least one dryer (20),
- characterized in that
- downstream of the at least one apparatus for separating the bulk goods from the drying gases (40) at least one heat exchanger (80) is provided which uses the separated drying gases to indirectly heat at
- 20 least a part of the gases being fed to the at least one hot gas generator (10a, 10b) as combustion air.
- 25 2. Apparatus according to claim 1, characterized in that upstream and/or downstream of the least one heat exchanger (80) at least one further heat exchanger is provided which uses the separated drying gases to indirectly heat a thermal fluid.
- 30 3. Apparatus according to one of the preceding claims, characterized in that at least one cleaning device (60a, 60b) for cleaning the hot gases produced by said at least one hot gas generator (10a, 10b) is provided in between the at least one hot gas generator (10a, 10b) and the at least one dryer (20), so that the exhaust gases produced by said at least one hot gas generator (10a, 10b) are passed through the at least

one cleaning device (60a, 60b) for cleaning the hot gases.

4. Apparatus according to the preceding claim, characterized in that said at least one cleaning device (60a, 60b) for cleaning the hot gases is selected for the group consisting of a hot gas cyclone (60b) and an electrostatic precipitator, preferably a dry type electrostatic precipitator (60a).

5. Apparatus according to one of the preceding claims, characterized in that said at least one hot gas generator (10a, 10b) comprises at least one solid fired hot gas generator, preferably a grate fired hot gas generator (10a), a fluidized bed combustion hot gas generator and/or a stoker fired hot gas generator; and/or at least one multi-fuel burner (10b).

6. Apparatus according to the preceding claim, characterized in that said at least one hot gas generator (10a, 10b) comprises at least one solid fired hot gas generator (10a) and at least one multi-fuel burner (10b) which are operated in parallel.

7. Apparatus according to the preceding claim, characterized in that the at least one multi-fuel burner (10b) comprises a combustion chamber with a muffle in which a fuel/combustion air mixture is ignited and burned and a combustion chamber ceiling, said combustion chamber ceiling comprising

- at least one inlet (101) for combustion air into the muffle,
- an outer nozzle ring (102) (102) forming an inlet for a cooling gas surrounding the muffle and
- an inner nozzle ring (103) (103) forming an inlet for a cooling gas inside the muffle providing a laminar flow of cooling gas along the muffle,

said inner and outer nozzle ring (102) being separately controllable.

8. Apparatus according to the preceding claim, characterized in that the inner (103) and/or outer nozzle ring (102) comprises an entering angle

of approximately 0 degrees to approximately 60 degrees, preferably in between 10 to 60 degrees.

9. Apparatus according to one of the preceding claims, characterized in that between the at least one hot gas generator (10a, 10b) and the at least one dryer (20) a mixing chamber (70) is aligned which allows for the mixing of the hot gases of the at least one hot gas generator (10a, 10b) with further external gases (71, 72) which preferably are pre-heated and/or ambient air.
 10. Apparatus according to one of the preceding claims, characterized in that downstream of said at least one apparatus for separating the bulk goods from drying gases (40) at least one device for cleaning the drying gases (50) exiting the at least one apparatus for separating the bulk goods from the drying gases (40) is provided, said at least one device for cleaning the drying gases being preferably provided upstream of the at least one heat exchanger (80).
 11. Apparatus according to the preceding claim, characterized in that the at least one device for cleaning the drying gases (50) is selected from the group consisting of regenerative thermal oxidizers (RTO) and/or wet electrostatic precipitators (WESP).
 12. Apparatus according to one of the preceding claims, characterized in that downstream of the at least one apparatus for separating the bulk goods from drying gases (40), preferably in between the at least one apparatus for separating the bulk goods from drying gases (40) and the at least one device for cleaning the drying gases (50) at least one solids separator (51) for separating solids from the drying gases is provided.
 13. Apparatus according to one of the preceding claims, characterized in that a downstream of said at least one heat exchanger (80) at least one exhaust fan (91) is provided.
 14. Arrangement for the manufacturing of wooden material boards with at least one crushing device, at least one drying device and at least one pressing device, characterized in that a drying device according to the

apparatus of one of the preceding claims is provided.

15. Method for continuously drying bulk goods, in particular wood fibers and/or wood chips in at least one dryer (20), in particular a flash tube type dryer, which is supplied with bulk goods via a blow-line (30) entering the at least one dryer (20) and with hot gases produced by at least one hot gas generator (10a, 10b), said bulk good – after exiting the at least one dryer (20) – being separated from the drying gases by means of at least one apparatus for separating the bulk goods from the drying gases (40) which is aligned downstream of the at least one dryer (20),

characterized in that

after separation of the bulk goods from the drying gases the drying gases are fed to at least one heat exchanger (80) which uses the thermal energy of the drying gases to indirectly heat at least a part of the gases being fed to the at least one hot gas generator (10a, 10b) as combustion air.

16. Method according to claim 15, characterized in that said exhaust gases produced by at least one hot gas generator (10a, 10b) are passed through at least one cleaning device (60a, 60b) for cleaning the hot gases before entering the at least one dryer (20), wherein the hot gases are cleaned, wherein said at least one cleaning device (60a, 60b) for cleaning the hot gases is preferably selected for the group consisting of a hot gas cyclone (60b) and an electrostatic precipitator, preferably a dry type electrostatic precipitator (60a).

17. Method according to one of claims 15 to 16, characterized in that said at least one hot gas generator (10a, 10b) comprises at least one solid fired hot gas generator, preferably a grate fired hot gas generator (10a), a fluidized bed combustion hot gas generator and/or a stoker fired hot gas generator which is fired with biomass, in particular wood biomass; and/or at least one multi-fuel burner (10b).

18. Method according to one of claims 15 to 17, characterized in that the

at least one multi-fuel burner (10b) comprising a combustion chamber with a muffle in which a fuel/combustion air mixture is ignited and burned and a combustion chamber ceiling, said combustion chamber ceiling comprising

- 5 – at least one inlet (101) which is fed with combustion air,
- an outer nozzle ring (102) which is fed with a cooling gas surrounding the muffle and
- an inner nozzle ring (103) which is fed with a cooling gas for providing inside the muffle a laminar flow of cooling gas along the
- 10 muffle,

said inner and outer nozzle ring (102) being separately controllable.

19. Method according to the preceding claim, characterized in that the inner and/or the outer nozzle ring (102) has (have) an entering angle between approximately 0 and approximately 60 degrees, preferably in
15 between 10 and 60 degrees, which angle is preferably adjustable depending on the fuel used.
20. Method according to one of claims 15 to 19, characterized in that between the at least one hot gas generator (10a, 10b) and the at least
20 one dryer (20) the hot gases of the at least one hot gas generator (10a, 10b) are mixed with further external gases which preferably are pre-heated and/or ambient air.
21. Method according to one of claims 15 to 20, characterized in that in between the at least one apparatus for separating the bulk goods from
25 drying gases (40) and the at least one device for cleaning the drying gases exiting the at least one apparatus for separating the bulk goods at least one additional cleaning step for separating solids from the drying gases is carried out.
22. Method according to one of claims 15 to 21, characterized in that after
30 separation of the bulk goods from the drying gases the drying gases are cleaned by means of at least one device for cleaning the drying gases (50), which preferably is provided upstream of the at least one

heat exchanger (80).

- 5 23. Method according to the preceding claim, characterized in that the drying gases are cleaned by means of at least one regenerative thermal oxidizer (RTO) and/or at least one wet electrostatic precipitator (WESP).
- 10 24. Method according to one of claims 15 to 23, characterized in that downstream of the at least one apparatus for separating the bulk goods from drying gases (40), preferably in between the at least one apparatus for separating the bulk goods from drying gases (40) and the at least one device for cleaning the drying gases (50) solids are removed from the drying gases by means of at least one solids separator (51).
- 15 25. Method according to one of claims 15 to 24, characterized in that the drying gases are propelled by means of at least one exhaust fan (91) which is provided downstream of said at least one heat exchanger (80).

Fig. 1

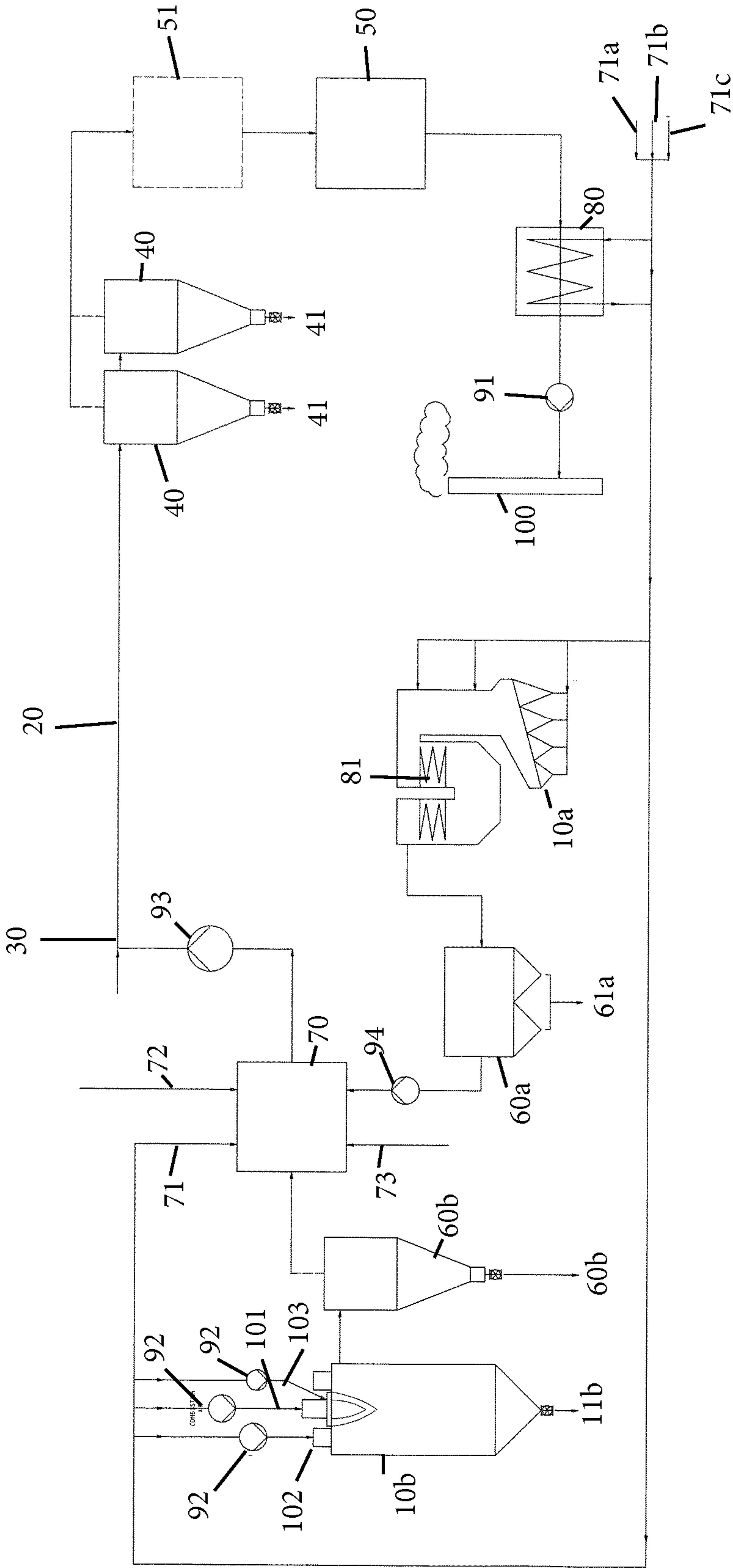


Fig. 1

