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(57)

ABSTRACT

There are described vinyl sequential copolymers (and processes for making them) comprising (a) at least 8. 5 wt-% preferably ≥ 20 wt-% of a higher itaconate diester (preferably dibutyl itaconate—DBI); (b) less than 23 wt-% acid monomer but also sufficient to have an acid value less than 150 mg KOH/g of polymer, (c) optionally with less than 50 wt-% of other itaconate monomers, and (d) optionally less than 77 wt-% of other monomers not (a) to (c). The DBI may be biorenewable. One embodiment is an aqueous dispersion of the vinyl sequential polymer of two phases: A) 40 to 90 wt-% of a vinyl polymer A with Tg from -50 to 30°C .; and B) 10 to 60 wt-% of a vinyl polymer B with Tg from 50 to 130°C .; where DBI is used to prepare A and/or B and polymer A has from 0.1 to 10 wt-% of at least one acid-functional olefinically unsaturated monomer.

POLYMER, PROCESS AND COMPOSITION

[0001] The present invention relates to polymers and polymeric materials obtained and/or obtainable from certain 2-methylidenebutanedioate diester monomers (also referred to herein as higher itaconate diesters) to a process for making such a polymers and their use to prepare for example coatings, inks and/or adhesives. It is preferred that polymers of the invention, and/or the higher itaconate diesters, are obtained from bio-renewable sources.

[0002] Many conventional polymers often suffer from undue sensitivity to water. This is especially true for water based polymer emulsions which can suffer from an increased water sensitivity compared to their solvent borne counterparts. A common way of countering this is to incorporate very hydrophobic monomers, such as butyl acrylate (BA) or 2-ethylhexyl acrylate (EHA). However, as homopolymers from these monomers have an extremely low Tg, incorporation of large amounts of these monomers produces a composition which is very often too soft (low Tg), yet is not sufficient hydrophobic if the amount of these monomer is sufficiently low to produce a satisfactory Tg. This might in turn be mitigated by introduction of high Tg, hydrophobic monomer such as styrene and the like. However polymer compositions comprising styrenic monomers, suffer from reduced outdoor durability because of the inherent UV sensitivity of styrene.

[0003] We have now surprisingly found that the dilemma described above can be solved. Good water resistance and low water sensitivity combined with high hardness and high elongation at break may be achieved by introducing higher ester itaconates such as dibutyl itaconate (DBI) as the hydrophobic monomer. Even though these monomers are very hydrophobic, the applicant has unexpectedly found that polymers made from higher itaconate esters do not suffer the same reduction in hardness typically observed for copolymers made from high concentrations of the typical hydrophobic monomers such as butyl acrylate (BA) and/or 2-ethyl hexyl acrylate (EHA).

[0004] Itaconate ester monomers have been described for very many years. However they have not been widely used to make commercial vinyl polymers because they are expensive and difficult to process. Prior art documents describe the use of itaconate esters only in general terms and typically describe or exemplify lower itaconate diesters such as dimethyl itaconate (DMI). The few documents which describe higher itaconate esters are described below.

[0005] U.S. Pat. No. 4,206,292 (Kureha Kagaku Kogyo Kabushiki Kaisha) describes a vinyl chloride resin coating with a smooth surface. The coating comprises: (1) 100 parts of vinyl chloride polymer; and (2) 0.1 to 30 parts of a polymer processing aid comprising: (A) 10 to 100 parts of a copolymer comprising 20 to 99% of an alkyl methacrylate, 1 to 70% of a dialkyl itaconate, and 0 to 60% of a copolymerizable monomer; and (B) 0 to 90 parts of a copolymer comprising 80 to 100% of an alkyl methacrylate, and 0 to 20% of a copolymerizable monomer. The vinyl chloride resins are not prepared from bio-based or other environmentally benign sources. The maximum amount of DBI that is used in the examples is 30% by weight.

[0006] U.S. Pat. No. 4,547,428 (Monsanto) describes a terpolymer comprising repeating units derived from an olefin, a diester of an addition polymerizable unsaturated dicarboxylic acid, and a solubilizing monomer which promotes compatibility between the terpolymer and a vinyl halide polymer. A granular form of the processing aid and a method for its

preparation are also disclosed. These polymers are not suitable for coating applications and the highest concentration of DBI in the examples is 17% by weight.

[0007] U.S. Pat. No. 4,588,776 (Monsanto) describes a polymer composition comprising a blend of a vinyl halide polymer and a particulate terpolymer having a molecular weight of at least 100,000 and a glass transition temperature of at least 50° C. The terpolymer comprises repeating units derived from an olefin, a diester of an addition polymerizable unsaturated dicarboxylic acid, and a solubilizing monomer which promotes compatibility of the terpolymer with the vinyl halide polymer. These polymers are used to prepare shaped plastic articles and not for coating applications. The maximum concentration of DBI used in the examples is 17% by weight.

[0008] U.S. Pat. No. 6,951,909 (3M) describes a polymerizable system comprises an organoborane, at least one polymerizable monomer, and a work-life extending agent. These compositions are not suitable for coating applications and the maximum concentration of DBI used in the examples is 17% by weight.

[0009] WO11/073,417 (DSM) discloses an aqueous emulsion comprising at least a vinyl polymer, said vinyl polymer comprising: a) 45 to 99 wt-% of itaconate ester monomers having formula (I), wherein R and R' are independently an alkyl or an aryl group; b) 0.1 to 15 wt-% of ionic or potentially ionic unsaturated monomers; c) 0 to 54 wt-% of unsaturated monomers, different from a) and b); and 0.9 to 54.9 wt-% by weight of total monomers of a chaser monomer composition added subsequently and polymerised after the polymerisation of monomers a), b) and c); wherein a)+b)+c) and the chaser monomer composition add up to 100 wt-%; and wherein the aqueous emulsion contains less than 0.5 wt-% free itaconate ester monomers of formula I based on the total weight of the aqueous emulsion. Although it is a stated object of the invention to provide a vinyl polymer with a high total concentration of itaconate ester monomers (see page 2, lines 14 to 17) in practise the larger proportion of such itaconate esters are lower itaconate esters (i.e. esters of small alkyl groups such as DMI). This document does not teach that it would be desirable to use a high concentration of higher itaconate esters (i.e. esters of large alkyl groups such as DBI). Indeed '417 states that itaconate esters are difficult to process (see page 2, lines 23 to 25) which combined with the teaching of the examples demotivates a reader to incorporate large amounts of hydrophobic higher itaconate esters like DBI in a copolymer.

[0010] The only examples in '417 that describe use of a DBI monomer are Examples 2, 4, 5 and 6. The amounts of DBI and other monomers used to prepare these Examples is given in Table A below. It can be seen that DBI is used as co-monomer only at a low concentrations in the final copolymer prepared in these Examples (at a maximum of 22.7 wt-%) which are each also prepared with significant amounts of another hydrophobic monomer butyl acrylate (BA). A styrene chaser monomer is always present in the final product (at least 1,5 wt-%). These examples teach away from using DBI or other higher itaconate esters to replace common hydrophobic monomers such as BA, EHA and/or styrene. No significant improvement is seen in film properties such as hardness and water sensitivity of the copolymers prepared in this document.

[0011] GB1009486 (Borden) describes a latex of composite polymeric particles where the core and shell may comprise a copolymer of a vinylidene chloride and an ester of an alpha

unsaturated aliphatic acid (the amount of ester in the shell being greater than the core). One example (Example 3) describes use of dibutyl itaconate (DBI) as the ester in an total amount of 17% by weight of total monomers (5% in the outer shell and 12% in an inner non core layer). These composite multi-layer polymer particles address a problem of providing a water vapour barrier coating for paper and the like and they use much lower amounts of DBI than the present invention.

TABLE A

(prior art DBI examples from WO11/073417)												
Example of '417	Composition	Monomers/wt-% (1 d.p.)										Total Itaconate
		AA	BA	MMA	Plex 652	DAAM	MAA	DMI	DBI	S (chaser)		
Ex 2	Initial feed	2.0	28.0	—	—	—	—	45.0	25.0	—	60.0	
	Single phase copolymer	1.8	25.2	—	—	—	—	40.5	22.5	10.0	63.0	
Ex 4	First feed	4.4	32.4	13.2	—	—	—	20.0	30.0	—	50.0	
	Second feed	5.0	11.0	34.0	—	—	—	45.0	5.0	—	50.0	
	Sequential copolymer	4.1	25.5	15.8	—	—	—	22.7	22.7	9.1	45.4	
Ex 5	First feed	4.2	30.0	9.5	8.4	—	—	19.1	28.7	—	47.8	
	Second feed	4.7	9.3	28.8	9.5	—	—	42.9	4.7	—	47.6	
	Sequential copolymer	3.9	23.6	12.2	7.9	—	—	21.8	21.8	8.7	43.6	
Ex 6	Olg initial feed	35.4	—	—	—	8.0	5.0	51.6	—	—	51.6	
	Olg-plr initial feed	—	41.2	—	—	—	—	17.6	41.2	—	58.8	
	Polymer - oligomer	26.8	10.7 (inc 2.2 BA chaser)	—	—	6.1	3.8	42.7	8.5	1.5	51.2	

In Examples 2, 4 and 5 of WO11/073417 the chaser monomer was 100 wt-% styrene, in Example 6 the chaser monomer composition was a mixture of styrene (40 wt-%) and BA (60 wt %).

[0012] U.S. Pat. No. 3,766,112 describes a high gloss latex for floor polish comprising a chlorinated paraffin wax with a polyvinyl pyrrolidone protective colloid. Four monomer components used to prepare the colloid: styrene (70 to 85%), 2-ethylhexyl acrylate (EHA) (5 to 15%) (meth)acrylic acid (3 to 10%) and a fourth monomer (1 to 5%) all percentages by weight of total monomers of the polyvinyl pyrrolidone. One of the seven monomers suggested as the fourth monomer is DBI. These polymers address the problem of providing high gloss floor coatings and DBI is used in much lower amounts than in the present invention.

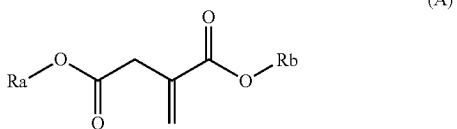
[0013] US2011-144265 (Durant Yvon) describes polymer particles prepared by polymerising esters of itaconic acid in the presence of seed particles to control particle size.

[0014] WO2002-068479 (3M) describes polymerisation of (meth)acrylic monomers using a two part initiator system of organoborane amine complex and an activator. One of the many different examples (Example 6) is prepared from a low amount of DBI (20% by weight) and this example does not use any other itaconate diester monomer.

[0015] WO 2007-026949 (Nippon Cat.) describes emulsion resin compositions that have a minimum film forming temperature (MFT) of $\leq 0^\circ\text{C}$. and are free of volatile organic compounds (VOC). These compositions are obtained by mixing a polymer with a high glass transition temperature (high Tg) with a polymer with low Tg. These polymers may be water dispersible and a wide variety of carboxy acid functional acid monomers are suggested to impart such water solubility including itaconic acid, mono-methyl itaconate ester and mono butyl itaconate ester (see page 12 lines 12 to

14). No other itaconic acid derived monomers are described and a reader of this document would have no reason to incorporate (non carboxy-acid functional) itaconate diester monomers.

[0016] The esters (including both mono and di-esters) of 2-methylidenebutanedioate (also referred to herein generically as itaconate esters) may be represented by Formula A:



where Ra and Rb can independently be H or any optionally substituted hydrocarbon moiety (such as any aliphatic, cycloaliphatic or aromatic moieties) provided that Ra and Rb are other than H (which is not an ester but itaconic acid).

[0017] It has been found that certain hydrophobic itaconate diesters (e.g. di esters of large alkyl groups) are difficult to use in conventional polymerisation processes (especially in aqueous emulsion polymerisation) and are also expensive. Therefore there has been a reluctance to use such hydrophobic higher itaconate esters at high concentrations in such processes.

[0018] It is an object of the present invention to solve some or all of the problems identified herein for example by providing polymeric materials made from larger amounts of higher itaconate esters (such as DBI) optionally together with other olefinically unsaturated monomers (also optionally from a biorenewable source). The resultant polymers may have various additional advantages as well as those already described herein such as good film forming at room temperature with the films having high flexibility (elasticity) and good resistance to blocking.

[0019] A second aspect of the present invention addresses the following problems in addition to or as well as those described herein. Traditional coatings may be unsatisfactory because the conventional coating films made from hard polymers possess little flexibility and when coated on substrates

which are not dimensionally stable (such as wood) the coating can tear and chip off. To improve the processing of dispersions of hard polymers large amounts of ingredients are added to assist film forming. When used in high concentrations these film formers are still present in the binder film in the coating and are released only gradually by conventional polymers at room temperature. This creates a high initial block resistance, which is the tendency of freshly applied coatings to block if they have dried for only a short time. High initial block resistance makes it virtually impossible to stack freshly coated substrates rapidly as when dried at room temperature their final block resistance is usually reached only after several days.

[0020] EP 387664 discloses an aqueous synthetic resin dispersion having a minimum film forming temperature below 50° C. containing an emulsion polymer with a core/shell structure consisting of A) 65-90% by weight of a weakly crosslinked core polymer having a glass transition temperature below 0° C. and an extension at break of at least 150% and B) 10-35% by weight of an essentially non-crosslinked shell polymer having a glass transition temperature below 60° C., the glass transition temperature of said core polymer being at least 10° C. below that of said shell polymer.

[0021] U.S. Pat. No. 5,021,469 discloses a binder, for water based gloss paints contains, dispersed in a aqueous phase, particles of a multiphase emulsion polymer made up of (a) core material having a glass transition temperature exceeding 40° C. and (b) a shell material having a glass transition temperature of less than 70° C.

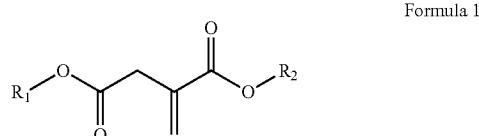
[0022] U.S. Pat. No. 4,654,397 discloses a process for the preparation of aqueous polymer dispersions which have a low film-forming temperature but still give films having a high block resistance, and the use of these polymer dispersions as binders for coating materials.

[0023] None of the above documents describe dispersions having the selected combination of features and integers as defined herein to produce the advantageous combination of properties as discussed herein.

[0024] This second aspect of the invention has as its preferred object to provide a physically-drying binder in the form of an aqueous synthetic resin dispersion which physically dries at low temperatures to give highly elastic films which are more or less non-tacky from the beginning. The emulsion polymers according to this second aspect of the invention address some or all of the problems described herein.

[0025] Therefore broadly in accordance with the present invention there is provided a copolymer (optionally a sequential copolymer) composition comprising (preferably consisting essentially of):

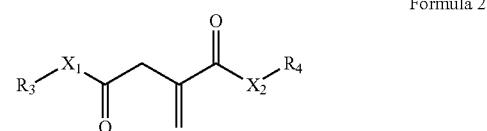
[0026] (a) greater than 8.5 wt-%, usefully ≥ 15 wt-%, preferably at least 20 wt-%, more preferably at least 24 wt-%, more preferably at least 30 wt-% for example at least 45 wt-% of at least one monomer represented by Formula 1



[0027] where both R₁ and R₂ independently represent an optionally substituted hydrocarbo moiety having from 4 to 10 carbon atoms.

[0028] (b) optionally at least one hydrophilic monomer preferably in an amount less than 23 wt-%, more preferably 0.5 to 15 wt-%, and also in an amount sufficient that the resultant polymer has an acid value of from 0 to 150 mg KOH/g, preferably less than 150 mg KOH/g, more preferably from 3 to 100 mg KOH per g of polymer,

[0029] (c) optionally less than 50 wt-%, for example from 0.01 to 10 wt-% and/or one or more monomers represented by Formula 2



[0030] (Formula 2 including itaconate diester monomers being other than those represented by Formula 1)

[0031] where R₃ and R₄ independently represent H or an optionally substituted hydrocarbo moiety having from 1 to 20 carbon atoms

[0032] X₁ and X₂ independently represents O or NR₅ where R₅ denotes H or an optionally substituted hydrocarbo moiety having from 1 to 20 carbon atoms with the proviso that when X₁ and/or X₂ are 0 then the respective R₃ and/or R₄ attached to the oxy group independently represent an optionally substituted hydrocarbo having from 1 to 3 carbon atoms

[0033] (d) optionally less than 80 wt-%, usefully less than 77 wt-%, preferably less than 75 wt-%, more preferably <70 wt-%, most preferably <65% wt-% of monomers other than components (a), (b) or (c).

[0034] where the weight percentages (also denoted herein as "% by weight" and/or "wt-%") of amounts of (a), (b) (c) (d) are calculated as a proportion of the total (weight) amount of (a)+(b)+(c)+(d) which thus totals 100%.

[0035] Copolymers of the invention may also be limited by one or more of the following optional provisos:

[0036] (I) when component (a) consists of DBI in an amount of less than 30% by weight of the total monomers then the copolymer is substantially free of any chloro groups; and

[0037] (II) when component (a) consists of DBI in an amount of less than 23% by weight of the total monomers then the copolymer is prepared by other than an emulsion polymerisation method in which a chaser monomer is used; and

[0038] (III) when component (a) consists of DBI in an amount of less than 23% by weight of the total monomers then if component (d) is present, component (d) is other than styrene or a mixture consisting of butyl acrylate (60 wt-% of mixture) and styrene (40 wt-% of mixture)

[0039] (IV) the copolymer is substantially free of styrene (preferably styrene free), more preferably component (d) if present is other than styrene or a mixture consisting

of butyl acrylate (60 wt-% of mixture) and styrene (40 wt-% of mixture), more preferably component (d) if present is other than styrene (S), butyl acrylate (BA), 2-ethyl hexyl acrylate (EHA) or mixtures thereof.

[0040] (V) is prepared by other than an emulsion polymerisation method in which a chaser monomer is used; and

[0041] (VI) the copolymer is prepared by other than an emulsion polymerisation method in which a chaser monomer is used optionally this proviso applying only when component (a) consists of DBI preferably in an amount of from 8.5 to 15% by weight of the total monomers (a)+(b)+(c)+(d).

[0042] (VII) when component (a) consists of DBI then component (a) is present in an amount other than 8.5 wt-%, 21.8 wt-%, 22.5 wt-% or 22.7 wt-% of the total monomer composition, preferably other than from 8 wt-% to 23 wt %,

[0043] (VIII) when component (a) consists of DBI then component (a) is present in an amount other than 4.7 wt-%, 5.0 wt-%, 8.5 wt-%, 21.8 wt-%, 22.5 wt-%, 22.7 wt-%, 25.0 wt-%, 28.7 wt-%, 30.0 wt-% or 41.2 wt-% of the total monomer composition, preferably other than from 4 wt-% to 42 wt %,

[0044] (IX) the copolymer is obtained other than from a polymerisation of a dimethyl itaconate (DMI) and dibutyl itaconate (DBI) in the respective weight ratio of 15 to 85 in the presence of poly diethyl itaconate seed polymer; more preferably the copolymer is obtained other than from polymerisation of dialkyl itaconate(s) in the presence of a poly diethyl itaconate seed polymer; most preferably the copolymer is obtained other than from polymerisation in the presence of a poly dialkyl itaconate seed polymer;

[0045] (X) if polymerisation of the copolymer occurs in the presence of an initiator system comprising organoborane amine complex and an activator then component (a) is present in an amount greater than 20 wt-%, preferably at least 24 wt-% of total monomers (a)+(b)+(c)+(d).

[0046] Preferably the copolymer of the invention is a sequential copolymer. As used herein the term sequential copolymer denotes a polymer obtained and/or obtainable by polymerisation of different polymer precursors (e.g. monomers) in sequence, for example in a living anionic polymerisation and/or emulsion polymerisation. A sequential polymer may be prepared in separate steps and/or in a single step for example by an all in one polymerisation where all the required ingredients are already present in the same vessel. Sequential copolymers of the invention may have any suitable distribution of monomers within the copolymer, for example be statistic, random, gradient, alternating, periodic and/or block copolymers.

[0047] Preferably the sequential copolymer composition is an emulsion copolymer (usefully an emulsion polymer prepared where no chaser monomer has been used), more preferably an aqueous emulsion copolymer, most preferably an aqueous coating composition.

[0048] Conveniently the composition is substantially free of polyvinyl chloride polymer and/or chlorinated paraffin wax, more preferably is substantially free of any monomer comprising chloro groups, most preferably is substantially free of any species comprising Cl whether as a substituent, atom, di-molecule, ion or otherwise

[0049] Broadly there is provided in a yet further aspect of the present invention a process for preparing a copolymer comprising the step of polymerising polymer precursors in a polymerisation method the polymer precursors comprising component (a), component (b) and optionally component (c) and/or component (d) as described above.

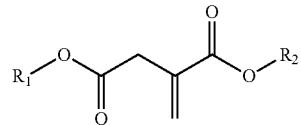
[0050] Preferably the polymerisation method is selected from an emulsion and/or suspension polymerisation. More preferably the copolymer is an emulsion copolymer.

[0051] Another aspect of the invention broadly provides for an optionally copolymer obtained and/or obtainable by a process of the present invention.

Hydrophobic Component (a) (Higher Itaconate Esters)

[0052] The present invention is particularly concerned with polymers obtained and/or obtainable from a narrow class of itaconate diester monomers selected from the broad disclosure of general itaconate esters of Formula A. Thus the hydrophobic component (a) comprises itaconate diester(s) of Formula 1:

Formula 1

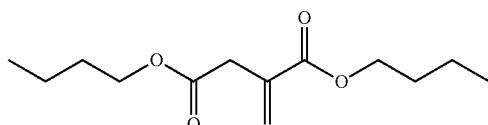


where both R₁ and R₂ independently represent an optionally substituted hydrocarbo moiety having from 4 to 10, preferably from 4 to 8, more preferably from 4 to 6, most preferably 4 carbon atoms.

[0053] The diesters of Formula 1 are also referred to herein as higher itaconate diesters.

[0054] Usefully R₁ and R₂ may independently represent optionally substituted C₄₋₁₀alkyl and/or C₄₋₁₀aryl, more usefully C₄₋₈alkyl and/or C₄₋₈aryl and most usefully C₄₋₆alkyl, even more usefully butyl (n-butyl being especially useful).

[0055] Whilst R₁ and R₂ may be different, more conveniently they represent identical moieties. Especially preferred examples of Formula 1 include those where R₁ and R₂ are identical, such di(benzyl)itaconate, di(phenyl)itaconate, di-n-butyl itaconate, di-i-butyl itaconate, and/or di-2-ethyl hexyl itaconate. Where R₁ and R₂ both represent n-butyl Formula 1 represents dibutyl 2-methylidenebutanedioate (also referred to herein as di(n-butyl)itaconate or DBI) which has the following structure:



[0056] DBI is the most preferred monomer for use as component (a) in the present invention.

[0057] Preferably component (a) is used in a total amount of at least 40%, and more preferably at least 50% by weight of the total monomers.

[0058] The itaconate functional component (a) is present in the compositions and/or copolymers of the invention in an amount of greater than 8.5% wt-%, usefully 15 wt-%, pref-

erably at least 20 wt-%, usefully at least 24 wt-%, more usefully at least 30 wt-%, even more usefully at least 35 wt-% and most usefully at least 40 wt-%, for example at least 50% based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0059] Conveniently the itaconate functional component (a) may be present in the compositions and/or copolymers of the invention in an amount of less than 80 wt-%, more conveniently less than 70 wt-%, even more conveniently less than 65 wt-%, most conveniently less than 58 wt-%, and for example less than 55 wt-%; based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0060] Preferably the itaconate functional component (a) may be present in the compositions and/or copolymers of the invention in an amount of from 20 to 80 wt-%, more preferably from 24 to 70 wt-%, even more preferably from 30 to 65 wt-%, most preferably from 35 to 65 wt-%, for example from 40 to 55 wt-% based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

Hydrophilic Component (b) (Acid Functional Monomers)

[0061] Suitable hydrophilic monomers of component (b) are those that are co-polymerisable with the hydrophobic monomer(s) of component (a) and are water soluble. Conveniently the at least one hydrophilic monomer of component (b) may comprise at least one activated unsaturated moiety as defined herein.

[0062] Usefully the hydrophilic monomer of component (b) is an acid functional ethylenically unsaturated monomer for example an acid functional acrylic monomer.

[0063] It will be understood that when referring to acid functional and/or acidic components herein this may relate to acidic moieties and/or potential acidic moieties which under the conditions of use may form acidic groups (e.g. anhydrides). An acid bearing monomer could be polymerised as the free acid or as a salt, e.g. the ammonium and/or alkali metal salt thereof. References herein to acids should therefore also be understood to include suitable salts and/or derivatives thereof (such as anhydrides and/or acid chlorides thereof).

[0064] Preferred hydrophilic monomers comprise, advantageously consist essentially of, at least one ethylenically unsaturated carboxylic acid although other acid groups such as optionally substituted organo phosphoric and/or sulphonnic acids may also be used.

[0065] Examples include phosphated alkyl (meth)acrylates, sulphonic acids (and derivatives thereof) of arylalkyl-alkenes, sulphonic acids (and derivatives thereof) of alkyl (meth)acrylates and/or other organo substituted sulphonic acids (such as acrylamidoalkyl sulfonic acids).

[0066] Preferred arylalkylene sulphonic acids are those where the arylalkylene moiety comprises optionally hydrocarbo substituted styrene, conveniently optionally C_{1-10} hydrocarbyl substituted styrene more conveniently optionally C_{1-4} alkyl substituted styrene. Useful acids are sulphonic acid substituted derivatives of styrenic compounds selected from the group consisting of styrene, α -methyl styrene, vinyl toluene, t-butyl styrene, di-methyl styrene and/or mixtures thereof. Especially preferred is styrene p-sulphonnic acid and its corresponding acid chloride styrene p-sulphonyl chloride.

[0067] Preferred phosphated organo acids comprise phosphated (meth)acrylates optionally substituted for example with one or more hydroxyl groups, for example phosphated hydroxy(meth)acrylates and C_{1-4} alkyl esters thereof.

[0068] Other preferred hydrophilic monomers of component (b) comprises partial acids of multivalent esters, more preferably half esters of diesters, most preferably mono acid half itaconate esters (i.e. those esters of Formula A where either R_a or R_b is H). Itaconic acid is also another example of a (di)acid functional monomer which is also suitable as component (b).

[0069] More preferred acids have one ethylenic group and one or two carboxy groups. Most preferably the acid(s) (and/or suitable acid derivative(s) thereof) are selected from the group consisting of: acrylic acid (and copolymerisable oligomers thereof), beta carboxy ethyl acrylate, citraconic acid, mesaconic acid, crotonic acid, fumaric acid, itaconic acid, maleic acid, methacrylic acid, methylene malonic acid, anhydrides thereof, salts thereof, acid chlorides thereof, combinations thereof in the same species and/or mixtures thereof.

[0070] Especially preferred monomers that may comprise component (b) are selected from:

[0071] acrylic acid, methacrylic acid, beta carboxy ethyl acrylate, methylene malonic acid, maleic anhydride, itaconic acid, itaconic anhydride, phosphated hydroxyl ethyl methacrylate (phosphated HEMA), phosphated hydroxylethyl acrylate (phosphated HEA), phosphated hydroxylpropyl methacrylate (phosphated HPMA), phosphated hydroxylpropyl acrylate (phosphated HPA), sulphonated styrene (and its chloride), 2-acrylamido-2-methylpropane sulfonic acid (AMPS) and ethylmethacrylate-2-sulphonic acid.

[0072] Particularly preferred acid monomers are acrylic acid, methacrylic acid, beta carboxy ethyl acrylate, itaconic acid, and/or itaconic anhydride.

[0073] For emulsion polymerization acrylic acid, methacrylic acid, beta carboxy ethyl acrylate, and/or itaconic acid may be convenient. For SAD copolymerization, acrylic acid, methacrylic acid, and/or itaconic anhydride are preferred.

[0074] The hydrophilic monomer component (b) may optionally be absent from the compositions and/or copolymers of the invention but if present is present in an amount of more than a trace amount usefully greater than or equal to 0.1 wt-%, conveniently greater than or equal to 0.5 wt-%, for example greater than 0.8 wt-% based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0075] Conveniently component (b) if present is present in the compositions and/or copolymers of the invention in an amount of less than 23 wt-%, more conveniently less than or equal to 20 wt-%, even more conveniently less than or equal to 10 wt-%, most conveniently \leq 5 wt-%, such as \leq 3 wt-%; for example 51 wt % based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0076] Preferably, component (b) may be used in a total amount from 0 to 10 wt-%, more preferably from about 0.1 to about 5 wt-%, even more preferably from about 0.1 to about 3 wt-%, most preferably from about 0.5 to about 1% by weight based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0077] Conveniently component (b) may be used in a total amount sufficient that the resultant polymer has an acid value (AV) of between 3 and 100 mg KOH per g of solid polymer, preferably from 8 to 80 mg KOH per g, more preferably from 15 to 65 mg KOH per g, and most preferably from 15 to 45 mg KOH per g.

[0078] Usefully component (b) satisfies both the acid value (AV) and weight limits herein, but it will be appreciated that depending on the monomer used the AV specified herein may

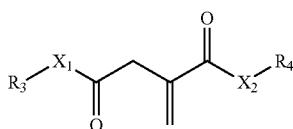
be achieved using weight percentages outside those preferred wt-% values given herein. Where there is an apparent inconsistency herein between any weight % of monomer or other component and the acid values specified it will be appreciated that satisfying the AV is generally the more desirable objective. If necessary the values for weight % of the relevant ingredients can be modified appropriately in a manner well known to a skilled person.

Component (c) (Lower Itaconate Esters and Itaconate Amides)

[0079] Component (c) comprises one or more other diester itaconate monomers other than those of Formula 1, preferably a monomer of Formula A where neither Ra nor Rb are H or an optionally substituted C₄₋₁₀hydrocarbo. More preferably component (c) comprises a lower itaconate diester. As used herein the term lower itaconate diester denotes diesters of Formula A where Ra and Rb are independently optionally substituted C₁₋₃hydrocarbo groups, such as C₁₋₃alkyl, an example of which is dimethyl itaconate (DMI).

[0080] Usefully component (c) may comprise lower itaconate diesters (i.e. diesters other than those of Formula 1), and/or higher or lower itaconate amides and thus component (c) may be represented by Formula 2

Formula 2



where R₃ and R₄ independently represent H or an optionally substituted hydrocarbo moiety having from 1 to 20 carbon atoms (e.g. from 1 to 6 carbon atoms); preferably C₁₋₂₀alkyl, preferably C₁₋₆alkyl, more preferably C₁₋₄alkyl, most preferably C₁₋₃alkyl; X₁ and X₂ independently represents O or NR₅ where R₅ denotes H or an optionally substituted hydrocarbo moiety having from 1 to 20 carbon atoms (e.g. from 1 to 6 carbon atoms); preferably C₁₋₂₀alkyl, more preferably C₁₋₆alkyl; even more preferably C₁₋₄alkyl; for example C₁₋₃alkyl;

with the proviso that when X₁ and/or X₂ are 0 then the respective R₃ and/or R₄ attached to the oxy group independently represent an optionally substituted hydrocarbo having from 1 to 3 carbon atoms, preferably C₁₋₃alkyl.

[0081] Components (a), (b), (c) and (d) are mutually exclusive. Thus compounds of Formula 2 are different from those of Formula 1 and the mono acid half itaconate esters are also excluded from Formulae 1 and 2, optionally comprising part of hydrophilic component (b).

[0082] Thus in one preferred embodiment of the invention components (a) and (b) (and optionally (c) where present) are each derived from itaconates and/or acids and/or derivatives thereof, more preferably from a biorenewable source. Thus for example component (a) may be a di(C₄₋₆dialkyl)itaconate, (e.g. DBI), component (b) may be itaconic anhydride itaconic acid, and/or C₁₋₄alkyl monoester of itaconic acid and component (c) where present may be a di(C₁₋₃dialkyl)itaconate (e.g. DMI). In such an embodiment optionally there is no component (d) so the copolymer may advantageously be obtained from monomers from the same itaconate source.

[0083] Whilst R₃ and R₄ may be different, more conveniently they represent identical moieties.

[0084] Whilst X₁ and X₂ may be different, more conveniently they represent identical moieties.

[0085] Preferably component (c) may be used in a total amount of less than 35%, more preferably from 0 to 25% by weight.

[0086] The component (c) if present may optionally be present in an amount usefully greater than or equal to 0.1 wt-%, conveniently greater than or equal to 0.5 wt-%, for example greater than 1.0 wt-% based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0087] Conveniently component (c) is present in the compositions and/or copolymers of the invention in an amount of less than 40 wt-%, more conveniently less than or equal to 35 wt-%, even more conveniently less than or equal to 25 wt-%, most conveniently ≥ 20 wt-%, for example ≥ 15 wt-% based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0088] Component (c) may be used in a total amount from 0 to 10 wt-%, preferably from 0.01 to 10 wt-%, more preferably from 0.1 to 40 wt-%, even more preferably from 0.5 to 35 wt-%, most preferably from 1.0 to 30 wt-%, for example from 1.0 to 25 wt-% by weight based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

Component (d) (Other Copolymerisable Monomers)

[0089] Preferably component (d) comprises monomers not part of components (a), (b) or (c), more preferably that are copolymerisable with them in any suitable technique such as any of those described herein (for example in a SAD and/or an emulsion polymerisation).

[0090] Component (d) may comprise a suitable activated unsaturated moiety (such as ethylenic unsaturation) where the structure(s) of component (d) do not overlap with any of components (a), (b) or (c).

[0091] Preferably component (d) is used in an amount of less than 50% and more preferably less than 40% by weight.

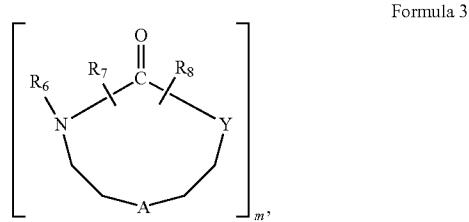
[0092] Component (d) may comprise monomers that can undergo crosslinking, that can improve adhesion of the coating to various substrates, that can enhance the colloidal stability of the polymer emulsion, or that can be used to affect T_g or polymer polarity.

[0093] Conveniently component (d) may comprise (meth)acrylate monomers having alkyl moieties comprising between 1 and 20 carbon atoms, styrene, alpha-methyl styrene, (meth)acrylonitrile, (meth)acryl amide or alkylated (meth)acryl amides, diacetone acryl amide, acetoacetoxyethyl methacrylate, hydroxyethyl (meth)acrylate, hydroxypropyl (meth)acrylate, silane functional monomers, such as 3-methacryloxypropyl trimethoxysilane (Geniosil GF31, ex Wacker), ureido functional monomers, such as Plex 6852-O (ex. Evonik), i-bornyl (meth)acrylate, polyethylene (meth)acrylate, polypropylene (meth)acrylate.

[0094] Component (d) may also comprise crosslinking monomers that can induce crosslinking of the copolymer composition. Crosslinking can occur at ambient temperatures (using for instance diacetone acryl amide combined with adipic dihydrazide), at elevated temperatures (stoving conditions in which for instance copolymerized hydroxyethyl (meth)acrylate reacts with hexamethoxy methyl melamines), as 2C composition (copolymerized hydroxyethyl (meth)

acrylate reacting with polyisocyanates, such as Bayhydur 3100), or as UV coating (when polymers or oligomers having multiple unsaturated groups are admixed. Typical examples include di- or tri-functional multifunctional acrylates such as trimethylol propane triacrylate or ethoxylated or propoxylated versions thereof).

[0095] Optionally component (d) may also comprise least one polymer precursor(s) of Formula 3



where Y denotes an electronegative group, R₆ is H, OH or an optionally hydroxy substituted C₁₋₁₀hydrocarbo

R₇ is H or a C₁₋₁₀hydrocarbo;

R₈ is a C₁₋₁₀hydrocarbo group substituted by at least one activated unsaturated moiety; and; either:

A represents a divalent organo moiety attached to both the —HN— and —Y— moieties so the —A—, —NH—, —C(=O)— and —Y— moieties together represent a ring of 4 to 8 ring atoms, and R₇ and R₈ are attached to any suitable point on the ring; or

A is not present (and Formula 3 represents a linear and/or branched moiety that does not comprise a heterocyclic ring) in which case R₇ and R₈ are attached to R₆; and

m is an integer from 1 to 4.

[0096] The ring moiety(ies) of Formula 3 are each attached to R₈ and in Formula 3 when m is 2, 3 or 4 then R₈ is multi-valent (depending on the value of m). If m is not 1 R₇ and —Y— may respectively denote the same or different moieties in each ring, preferably the same respective moieties in each ring. R₇ and R₉ may be attached at any suitable position on the ring.

[0097] Preferred monomers of Formula 3 comprise, conveniently consist essentially of, those where: A represents a optional substituted divalent C₁₋₅hydrocarbylene; and —Y— is divalent —NR₉— (where R₉ is H, OH, optionally hydroxy substituted C₁₋₁₀hydrocarbo or R₈) or divalent O,

[0098] More preferred monomers of Formula 3 comprise those where: m is 1 or 2

—Y— is —NR₈— (i.e. where Formula 2 is attached to R₉ via a ring nitrogen), A represents a divalent C₁₋₃hydrocarbylene; R₆ is H, R₇ is a C₁₋₁₀hydrocarbo; and

R₈ comprises a (meth)acryloxyhydrocarbo group or derivative thereof (e.g. maleic anhydride).

[0099] Monomers represented by Formula 3 include some monomers informally referred to as ureido monomers. Further suitable ureido monomers of Formula 3 are described in "Novel wet adhesion monomers for use in latex paints" Singh et al, Progress in Organic Coatings, 34 (1998), 214-219, (see especially sections 2.2 & 2.3) and EP 0629672 (National Starch) both of which are hereby incorporated by reference. Conveniently the monomers of Formula 3 may be used as a substantially pure compound (or mixture of compounds) or

may be dissolved in a suitable solvent such as a suitable (meth)acrylate or acrylic derivative for example methyl methacrylate.

[0100] Other and/or additional component (d) may be used in those cases where higher molecular weights are desired, such as suitable multi functional (meth)acrylates or divinyl aromatics. Typical examples include di-, tri-, or tetra-functional (meth)acrylates, especially difunctional (meth)acrylates and divinyl benzene. Typical concentrations are less than 10%, more preferred less than 5%, even more preferred between 0.05 and 4%, most preferred between 0.1 and 2.5%, and even most preferred between 0.15 and 1.5% by weight based on total monomers.

[0101] The component (d) may optionally be present in an amount usefully greater than or equal to 0.1 wt-%, conveniently greater than or equal to 0.5 wt-%, for example greater than 1.0 wt-% based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0102] Conveniently component (d) is present in the compositions and/or copolymers of the invention in an amount of less than 77 wt-%, more conveniently less than or equal to 50 wt-%, even more conveniently less than or equal to 40 wt-%, most conveniently ≤30 wt-%, for example ≤25 wt % based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0103] Preferably, component (d) may be used in a total amount from 0 to 77 wt-%, more preferably from about 0.1% to about 50 wt-%, even more preferably from about 0.5% to about 40 wt-%, most preferably from about 1.0% to about 30% by weight based on the total weight of monomers (a), (b), (c) and (d) used to prepare the copolymer being 100%.

[0104] One aspect of the invention relates to an aqueous sequential vinyl polymer dispersion comprising 30% by weight (preferably at least 40%) of polymer obtained or obtainable from one or more higher itaconate diester(s).

[0105] Other examples of suitable monomers that may comprises all or part of components (a), (b), (c), or (d) may be described in the various further aspects of the invention later in this application. It will be understood that where suitable such monomers where not already mentioned above may also be used as components in the above aspect of the invention.

Polymerisation Processes

[0106] Copolymers (optionally sequential copolymers) of the invention may be formed using a number of processes. These include emulsion polymerisation, suspension polymerisation, bulk polymerisation and solution polymerisation. Such processes are extremely well known and need not be described in great detail.

[0107] In one embodiment emulsion polymerisation is used to form copolymers of the invention.

[0108] A conventional emulsion process involves dispersing the monomers in an aqueous medium and conducting polymerisation using a free-radical initiator (normally water soluble) and appropriate heating (e.g. 30 to 120° C.) and agitation.

[0109] The aqueous emulsion polymerisation can be effected with conventional emulsifying agents (surfactants) being used such as anionic and/or non-ionic emulsifiers. The amount used is preferably low, preferably 0.3 to 2% by weight, more usually 0.3 to 1% by weight based on the weight of total monomers charged.

[0110] The aqueous emulsion polymerisation can employ conventional free radical initiators such as peroxides, persul-

phates and redox systems as are well known in the art. The amount of initiator used is generally 0.05 to 3% based on the weight of total monomers charged.

[0111] The aqueous emulsion polymerisation process may be carried out using an “all-in-one” batch process (i.e. a process in which all the components to be employed are present in the polymerisation medium at the start of polymerisation) or a semi-batch process in which one or more of the components employed (usually at least one of the monomers), is wholly or partially fed to the polymerisation medium during the polymerisation. Although not preferred, fully continuous processes could also be used in principle. Preferably a semi-batch process is employed for example power feed polymerization which is a semi-continuous emulsion copolymerization in which the instantaneous composition of the formed copolymer is the same as that of the added monomer mixture(s). Power feed polymerisation is typically used to make gradient polymers. Sequential copolymers of the invention may also be prepared from a dispersion of a first (co)polymer that is mixed with further unpolymerised polymer precursor or monomer which is then polymerised in the present of the first polymer.

[0112] The polymerisation technique employed may be such that a low molecular weight polymer is formed, e.g. by employing a chain transfer agent such as one selected from mercaptans (thiols), certain halohydrocarbons and alpha-methyl styrene; or catalytic chain transfer polymerisation using for example cobalt chelate complexes as is quite conventional. Alternatively a controlled radical polymerisation process can be used, for instance by making use of an appropriate nitroxide or a thiocarbonylthio compounds such as dithioesters, dithiocarbamates, trithiocarbonates, and xanthates in order to mediate the polymerization via for example a nitrox mediated polymerisation (NMP), a reversible addition fragmentation chain-transfer process (RAFT) or atom transfer radical polymerization (ATRP).

[0113] When the copolymer of the invention is an emulsion polymer it may be mixed with a variety of other polymer emulsions such as those that do not comprise DBI (or higher itaconate esters). Examples of such second polymer emulsions can be polyurethane emulsions, polyurethane-poly (meth)acrylate emulsions, alkyd emulsions, polyester emulsions and/or polyvinyl emulsions. This latter group of copolymer emulsions may comprise oligomer-polymer emulsions, gradient morphology emulsions, sequentially polymerized emulsions, or single phase copolymer emulsions.

[0114] The emulsions according to the description above can be produced via emulsion polymerization or via a process called solvent assisted dispersion (SAD) polymerization.

[0115] When the copolymer emulsion is produced via emulsion polymerization this can be according to a single feed process, a sequentially fed multi-phase copolymerization process, an oligomer supported emulsion polymerization process or a power feed process, resulting in a gradient particle morphology.

[0116] In the case of solvent assisted dispersion polymerization process, or SAD polymerization, the polymerization is performed in organic solvents. Next, base and/or surfactant are added and the polymer solution is emulsified. Preferably, the solvent is removed via evaporation at the end of the complete process.

[0117] SAD polymer emulsions can be produced via a single feed solution polymerization or by a sequentially fed

multi-phase polymerization. It is also envisaged that an SAD polymer emulsion, prior or after the optional removal of the solvent, is used as a seed for an emulsion polymerization stage. In this case, the polymer emulsion prepared according to the SAD process is used as seed in a batch or semi-batch polymerization process.

[0118] The preferred polymerization process is emulsion polymerization.

[0119] Preferably, the weight average molecular weight (M_w) (as determined with GPC as described herein) of the DBI containing copolymers is more than 2000 g/mol, more preferably more than 10,000 g/mol, even more preferably more than 25,000 g/mol, most preferably more than 40,000 g/mol, and even most preferably more than 100,000 g/mol.

[0120] In the case of oligomer-polymer emulsions prepared via emulsion polymerization lower molecular weights may be desired. In those cases chain transfer agents may be employed. Typical chain transfer agents can be mercaptans, such as lauryl mercaptan, i-octyl thioglycolate, or 3-mercaptopropionic acid, or halogenides, such as bromomethane, bromoethane. Typical chain transfer concentrations in these cases are enough to reduce the weight average molecular weight of the oligomer phase to between 500 and 100,000 g/mol, more preferred between 1,000 and 60,000 g/mol, even more preferred between 2,500 and 50,000 g/mol, and most preferred between 5,000 and 25,000. Typical chain transfer agent concentrations are below 5%, more preferably below 2.5%, and most preferably between 0.5 and 2.5% by weight of total monomer. In the case that the oligomer is combined with a high molecular weight polymer, the preferred molecular weights for the high molecular weight fraction will be as described earlier.

[0121] In those cases where the copolymer emulsion comprises multiple phases or is made up from multiple monomer feeds (sequential, oligomer-polymer or power feed) one of the copolymer phases preferably comprises between 10 and 80%, more preferably between 15 and 50%, and most preferably between 20 and 40% by weight of the total monomers used to prepare the sequential, power feed, and/or oligomer-polymer composition. This particular copolymer phase has a T_g , as calculated using the Fox equation, of higher than 40° C., more preferably higher than 60° C., and most preferably higher than 80° C. The other copolymer phase(s) may then comprise between 20 and 90% of the total monomers more preferably between 50 and 85%, and most preferably between 60 and 80% by weight of the total monomers used to prepare the sequential, power feed, and/or oligomer-polymer composition. These particular copolymer phase(s) have a T_g , as calculated using the Fox equation, of less than 40° C., more preferably of less than 20° C., and most preferably of less than 0° C.

[0122] The difference in T_g in such emulsions between that of the high T_g phase(s) and that of the low T_g phase(s) is preferably at least 20° C., more preferably at least 30° C., and most preferably at least 40° C.

[0123] In a special case it is envisaged that the itaconic anhydride which is copolymerized in an SAD copolymerization process can be post modified using chemicals having anhydride reactive groups. The objective in these cases is to introduce special functionalities, such as crosslinking or adhesion promoting groups, while maintaining an acid group that can be used for colloidal stabilization.

[0124] Modification of the anhydride groups can occur with any nucleophilic functionality. Preferred functionalities

include hydroxyl groups, hydrazide groups, hydrazine groups, semi-carbazide groups and amine groups. In all cases, modification will result in the introduction of the moiety attached to the hydroxyl, hydrazide, hydrazine, semi-carbazide or amine group and, simultaneously, of an acid group. The acid group can subsequently be used for emulsifying the copolymer.

[0125] The modification can be done with monofunctional hydroxyl groups, hydrazide, or hydrazine, or primary, or secondary amines, but also with di-functional or higher functional hydroxyl, hydrazine, hydrazide, semi-carbazide, or primary or secondary amines. Potential hydroxyl functionalities can include C₁-C₂₀ aliphatic, aromatic, or cycloaliphatic mono-, di-, or high functional alcohols. The aliphatic, aromatic, or cycloaliphatic groups can include other functionalities that can, for instance, be used for improved adhesion, crosslinking or other purposes. Typical examples of such functionalities can include phosphate, phosphonate, sulphate, sulphonate, ketone, silane, (cyclic) ureido, (cyclic) carbonate, hydrazide, hydrazine, semi-carbazide, urethane, urea, carbamate, and melamine.

[0126] The preferred (poly)amines, (poly)hydrazines, or (poly)hydrazides can be characterized by the same description.

[0127] In the case where the copolymer composition is prepared via emulsion polymerization, the pH of the emulsion can preferably be increased using organic or inorganic bases. Typical examples include ammonia, primary and secondary organic amines, lithium hydroxide, sodium hydroxide or potassium hydroxide, sodium carbonate or sodium bicarbonate. Typically, the pH is increased only at the end of the manufacturing process, although it can be envisaged that either at the start of the polymerization the pH of the aqueous phase is already increased (buffered) or that the pH of a polymerizing mixture is increased for instance between sequential monomer feeds. In the case of copolymers prepared via emulsion polymerization the pH is preferably increased at the end of the manufacturing process, preferably using ammonia or lithium hydroxide.

[0128] Typically, the pH is raised to values above 5, more preferred above 6, and most preferred to values of between 6 and 9.

[0129] When the copolymer emulsion is prepared via the SAD polymerization process, emulsification can be done by addition of surfactants, but is preferably done by first neutralizing the polymer acid groups. This can be done by addition of base to the solution polymerized polymer followed by the addition of water or by addition of base to an aqueous phase followed by the addition of the polymer solution. In both cases, suitable bases are the same as above. Preferred bases are ammonia, lithium hydroxide or dimethyl ethanol amine, diethanol methyl amine, diethanol ethyl amine, diethyl ethanol amine and the like. Typically, the molar ratio of base to acid groups is between 0.5 and 1.3, more preferred between 0.6 and 1.2, most preferred between 0.6 and 1.

[0130] The concentration of volatile organic compounds (VOC) in the aqueous copolymer emulsions is preferably low. In a preferred case, the VOC level is below 20 wt-%, more preferred below 10 wt-%, even more preferred below 5 wt-%, most preferred below 1 wt-%, and even most preferred below 0.5 wt-%. Intentionally, the VOC level of the copolymer emulsions, prior to formulating them into paints, is close to 0 wt-%, typically below 0.1 wt-%.

[0131] When the copolymer composition is prepared via SAD polymerization, solvents are required for the solution polymerization process. Typical solvents include organic solvents that are well known to those experienced in the field, such as acetone, methyl ethylketone, ethanol, methanol, i-propanol, i-octyl alcohol, xylene, glycol ethers, glycol esters. Preferably solvents are used that—following polymerization at elevated pressure—can be removed from the emulsion by evaporation. Preferred solvents in this respect are acetone and methyl ethylketone.

[0132] Initiators are required to start the radical polymerization. These, too, are well known to those experienced in the field. The aqueous emulsion polymerisation can employ conventional free radical initiators such as peroxides, persulphates and redox systems. Useful examples include inorganic peroxides, such as ammonium persulphate, sodium persulphate, potassium persulphate, AZO initiator, such as azobisisobutyronitrile (AIBN), 2,2'-azodi(2-methylbutyronitrile) (AMBN), and organic peroxide and hydroperoxides. (Hydro) peroxide can readily be used in combination with suitable reducing agents. Preferably, initiators are used in an amount of between 0.05 and 6%, more preferably between 0.5 and 4%, most preferably from 0.5 to 3% by weight of the total monomers.

[0133] Surfactants are used in emulsion polymerization as known to those skilled in the art. Typical surfactants have been extensively described in all kinds of patent applications. The choice and concentration of surfactants are not deemed to be critical for this invention. The aqueous emulsion polymerisation can be effected with conventional emulsifying agents (surfactants) being used such as anionic and/or non-ionic emulsifiers. The amount used is preferably low, preferably 0.3 to 2% by weight, more usually 0.3 to 1% by weight based on the weight of total monomers charged to make the polymer.

[0134] In the case of SAD copolymer emulsions, emulsification can be aided by selecting the right anionic, nonionic and mixed anionic/nonionic surfactant(s). Typically, surfactant is used in an amount of less than 5% more preferably less than 3%, and most preferably between 0.2 and 2.5% by weight of the total monomers.

[0135] Preferably (and subject to the provisos herein) in one embodiment of the invention the process of making a copolymer emulsion of the invention comprises using a chaser monomer composition as described in WO2011073417. In another embodiment a chaser monomer may optionally not be used.

[0136] In a preferred case the residual monomer content of the copolymer emulsion is below 2000 mg/L, more preferred below 1500 mg/L, most preferred below 1000 mg/L, and especially preferred below 550 mg/L.

[0137] The aqueous coating composition yields coatings with typical König hardness values of at least 30 s, more preferred at least 40 s, even more preferred at least 50 s, and most preferred at least 60 s.

[0138] In another embodiment the polymer of the invention may be made using a bulk polymerisation process. Bulk polymerisation of olefinically unsaturated monomers is described in detail in EP 0156170, WO82/02387, and U.S. Pat. No. 4,414,370 the contents of which are hereby incorporated by reference.

[0139] In general in a bulk polymerisation process a mixture of two or more monomers are charged continuously into a reactor zone containing molten vinyl polymer having the same ratio of vinyl monomers as the monomer mixture. The

molten mixture is maintained at a preset temperature to provide a vinyl polymer of the desired molecular weight. The product is pumped out of the reaction zone at the same rates as the monomers are charged to the reaction zone to provide a fixed level of vinyl monomer and vinyl polymer in the system. The particular flow rate selected will depend upon the reaction temperature, vinyl monomers, desired molecular weight and desired polydispersity.

[0140] For polymers of the invention especially those to be used in coating compositions, providing amino functional groups thereon may also be useful as such groups provide enhanced adhesion to certain substrates, such as wood and alkyl resins. Amino groups may be incorporated into a polymer by using a carboxyl functional precursor for example prepared by employing ethylenically unsaturated acid functional monomer(s) such as acrylic acid or methacrylic acid. At least some of the carboxy-functional groups may be converted to amino groups (as part of amino ester groups) by reaction with alkylene imines such as ethylene imine, propylene imine or butylene imine. Such a reaction is well established in the art, being known as an imination reaction and the details of this are for example taught in U.S. Pat. No. 7,049,352 the contents of which are hereby incorporated herein by reference. Therefore a further aspect of the invention comprises iminated versions of the all the copolymers of the present invention as described herein.

[0141] If it is desired to crosslink polymers (for example in a polymer dispersion), the relevant polymers can carry functional groups such as hydroxyl groups and the dispersion subsequently formulated with a crosslinking agent such as a polyisocyanate, melamine, or glycoluril; or the functional groups on one or both polymers could include keto or aldehyde carbonyl groups and the subsequently formulated crosslinker in step c) could be a polyamine or polyhydrazide such as adipic acid dihydrazide, oxalic acid dihydrazide, phthalic acid dihydrazide, terephthalic acid dihydrazide, isophorone diamine and 4,7-dioxadecane-1,10 diamine. It will be noted that such crosslinking agents will effect crosslinking by virtue of forming covalent bonds.

[0142] The designation of the polymer phase involved as a first phase or core material and second phase or shell material does not mean that the invention should be bound by any particular morphology of the latex particles. The term polymer phase is to be understood as meaning a portion of the emulsion polymer which is prepared during a temporally-limited segment of the emulsion polymerization and the dispersion of which differs from that of the foregoing or following phase. This is also known as a multi-stage polymerization.

[0143] The two-phase structure of the dispersions of the invention influences the properties of the film formed when the dispersion dries after coating a substrate.

[0144] This aspect of the invention provides an aqueous vinyl polymer dispersion with an advantageous combination of MFFT and anti-blocking properties which can be prepared at least in part from bio-renewable monomers (such as biorenewable DBI).

[0145] According to this aspect of the present invention there is provided an aqueous polymer dispersion having a minimum film forming temperature below 50° C., more preferably below 30° C. comprising a vinyl polymer derived from olefinically unsaturated monomers, with at least two phases comprising:

[0146] A) 40 to 90 wt-%, more preferably 50 to 85 wt-% and especially 60 to 80 wt-% of a vinyl polymer A

having a glass transition temperature in the range of from -(minus)50 to 30° C.; and

[0147] B) 10 to 60 wt-%, more preferably 15 to 50 wt-% and especially 20 to 40 wt-% of a vinyl polymer B having a glass transition temperature the range of from 50 to 130° C.; where

[0148] (i) at least one of the monomers used to prepare vinyl polymer A and/or vinyl polymer B is represented by Formula 1 as described herein (usefully a higher itaconate ester such as DBI) preferably in an amount from 20 to 80 wt-%, more preferably from 20 to 65 wt-%, most preferably 30 to 55 wt-% of the total monomers

[0149] (ii) optionally 10% by weight (preferably at least 20 wt-%) of the total amount of monomer used to form vinyl polymer A and vinyl polymer B is derived from at least one bio-renewable olefinically unsaturated monomer;

[0150] where the weight percentage of monomers in A and B are calculated in (i) and (ii) based on the total amount of olefinically unsaturated monomers used to prepare polymer A and polymer B being 100%;

[0151] (iii) vinyl polymer A comprises 0.1 to 10 wt-% of at least one acid-functional olefinically unsaturated monomer where the weight percentage of acid functional monomer is calculated based on the total amount of olefinically unsaturated monomer used to prepare polymer A being 100%.

[0152] In this aspect of the invention features (i) and (iii) correspond respectively to components (a) and (b) of the present invention and the other monomers used to prepare polymers A and B corresponding to optional components (c) and/or (d) as appropriate.

[0153] Other preferred features of this aspect of the present invention are given below and/or in the claims.

[0154] The acid-functional olefinically unsaturated monomer may be selected from the group consisting of acrylic acid, methacrylic acid, itaconic anhydride, maleic anhydride methylene malonic acid, itaconic acid, crotonic acid and fumaric acid.

[0155] Vinyl polymer A may comprise 0.1 to 20 wt-% of at least one crosslinking olefinically unsaturated monomer, preferably 0.4 to 6 wt-% of at least one olefinically unsaturated monomer with a wet-adhesion promoting functionality.

[0156] The crosslinking monomer(s) and wet adhesion promoting monomer(s) can be used together in the same polymer composition. It is, however, often desired to use either crosslinking monomer(s) or wet adhesion promoting monomer(s) in any phase. This means that vinyl polymer A can comprise crosslinking monomer(s) or wet adhesion promoting monomer(s), while vinyl polymer contains wet adhesion promoting monomer(s) or crosslinking monomer(s). In addition to this it is also possible to use wet adhesion promoting monomer(s) in either vinyl polymer A and/or vinyl polymer B or in both and no crosslinking monomer(s) or to use crosslinking monomer(s) in vinyl polymer A and/or vinyl polymer B and no wet adhesion promoting monomer(s).

[0157] Olefinically unsaturated monomer with a wet-adhesion promoting functionality contain wet-adhesion promoting functional groups such as acetoacetoxy groups and optionally substituted amine or urea groups, for example cyclic ureido groups, imidazole groups, pyridine groups, hydrazine or semicarbazide groups.

[0158] The bio-renewable olefinically unsaturated monomers may comprise bio-renewable (meth)acrylic acid and/or bio-renewable alkyl (meth)methacrylate.

[0159] The bio-renewable olefinically unsaturated monomers may also comprise bio-renewable: α -methylene butyrolactone, α -methylene valerolactone, α -methylene γ -R¹ butyrolactone (R¹ can be an optionally substituted alkyl or optionally substituted aryl); itaconates such as dialkyl itaconates and monoalkyl itaconates, itaconic acid, itaconic anhydride, crotonic acid and alkyl esters thereof, citraconic acid and alkyl esters thereof, methylene malonic acid and its mono and dialkyl esters, citraconic anhydride, mesaconic acid and alkyl esters thereof.

[0160] The bio-renewable monomers may also comprise bio-renewable: N—R², α -methylene butyrolactam (R² can be an optionally substituted alkyl or optionally substituted aryl); N—R², α -methylene γ -R¹ butyrolactam; N-alkyl itaconimids; itaconmonoamids; itacondiimids; dialkyl itaconamides, mono alkyl itaconamides; furfuryl (meth)acrylate; and fatty acid functional (meth)acrylates.

[0161] Vinyl polymer A and vinyl polymer B may comprise at least about 1.5 dpm/gC of carbon-14.

[0162] In a further aspect of the present invention provides a process for preparing the aqueous polymer dispersion (or polymer A and polymer B as described above) which process comprises steps:

[0163] a) a first polymerization step, to form a first phase vinyl polymer;

[0164] b) a second polymerization step in the presence of the resulting first phase vinyl polymer from step a) to form a second phase vinyl polymer.

[0165] Vinyl polymer A may be the first phase in which case vinyl polymer B is the second phase. Alternatively vinyl polymer B may be the first phase in which case vinyl polymer A is the second phase. Preferably vinyl polymer A is the first phase. Preferably the second phase vinyl polymer is prepared in the presence of the first phase vinyl polymer.

[0166] Optionally the process includes c) a neutralisation step before/after or during step c) to solubilise the first polymer phase.

[0167] Optionally the process includes d) the addition of a crosslinking agent after the polymerization step a) and/or step b), said crosslinking agent being reactable with any crosslinking functional groups of vinyl polymer A and for vinyl polymer B on subsequent drying of the coating dispersion to effect covalent bond crosslinking.

[0168] Optionally the process includes a post treatment imidation step e) with alkylene imines like for instance propylene imine) which can greatly improve wet adhesion.

[0169] A film, polish, varnish, lacquer, paint, ink and/or adhesive may comprise the aqueous polymer dispersion comprising polymer A and polymer B described above and these aqueous polymer dispersions may also be used protective coatings on wood, plastic, paper and/or metal substrates.

[0170] An embodiment of the invention provides an aqueous polymer dispersion where vinyl polymers A and B comprise individually at least 30 wt-%, more preferably at least 40 wt-%, most preferably at least 60 wt-%, and especially preferably at least 70 wt-% of compounds of Formula 1 such as higher itaconate diesters for example DBI. Although the concentration of itaconate monomers in polymers A and B can be similar, it is preferred that the concentrations are different. In each of the preferred cases described above, it is envisaged

that the concentration of itaconate monomers in the other phase can always be below 20 wt-% or even be 0 wt-%.

[0171] Preferably the concentration of itaconate esters according to the invention in the low Tg phase is at least 10 wt-% higher than that in the high Tg phase, more preferably at least 20 wt-%.

[0172] In yet another preferred embodiment of the invention there is provided an aqueous polymer emulsion according to the invention where the monomer feed making up polymer A or the feed making up polymer B comprise up to 20 wt-% of organic solvent, more preferably less than 10 wt-%, even more preferably less than 5 wt-%, and most preferably between 0.1 and 2.5 wt-%.

[0173] Improved properties of the copolymers of the this aspect of the invention may include heat resistance, colloidal stability, pigment compatibility, surface activity, blocking resistance and reduced MFFT depending on the monomers used.

[0174] The monomer system used for the preparation of vinyl polymer A and vinyl polymer B is any suitable combination of olefinically unsaturated monomers which is amenable to copolymerisation (including bio-renewable monomers described herein which may of course also be acid-functional, crosslinkable etc as described below).

[0175] Preferably vinyl polymer A comprises 0.5 to 9 wt-%, more preferably 1 to 8 wt-% and especially 1.5 to 5 wt-% of at least one acid-functional olefinically unsaturated monomer.

[0176] Preferably vinyl polymer B comprises less than 5 w % of any acid functional monomers and preferably less than 2 w %, and in some preferred embodiments none at all.

[0177] Other, non-acid functional, non-crosslinking monomers which may be copolymerized with the acid monomers include acrylate and methacrylate esters and styrenes; also dienes such as 1,3-butadiene and isoprene, vinyl esters such as vinyl acetate, and vinyl alkanoates. Methacrylates include normal or branched alkyl esters of C1 to C12 alcohols and methacrylic acid, such as methyl methacrylate, ethyl methacrylate, and n-butyl methacrylate, and (usually C5 to C12) cycloalkyl methacrylates acid such as isobornyl methacrylate and cyclohexyl methacrylate. Acrylates include normal and branched alkyl esters of C1 to C12 alcohols and acrylic acid, such as methyl acrylate, ethyl acrylate, n-butyl acrylate, and 2-ethylhexyl acrylate, and (usually C5-C12) cycloalkyl acrylates such as isobornyl acrylate and cyclohexylacrylate. Also included are (meth)acrylamide, and mono- or di-alkyl amides of (meth)acrylic acid. Styrenes include styrene itself and the various substituted styrenes, such as *alpha*-methyl styrene and *t*-butyl styrene. Nitriles such as acrylonitrile and methacrylonitrile may also be polymerised, as well as olefinically unsaturated halides such as vinyl chloride, vinylidene chloride and vinyl fluoride.

[0178] Functional monomers which impart crosslinkability (crosslinking monomers for short) include epoxy (usually glycidyl) and hydroxyalkyl (usually C₁-C12, e.g. hydroxyethyl)methacrylates and acrylates, as well as keto or aldehyde functional monomers such as acrolein, methacrolein and vinyl methyl ketone, the acetoxacetoxyl esters of hydroxyalkyl (usually C₁-C₁₂)acrylates and methacrylates such as acetoacetoxyethyl methacrylate and acrylate, and also keto-containing amides such as diacetone acrylamide. The purpose of using such functional monomer is to provide subsequent crosslinkability in the resulting polymer system as discussed.

In principle the functional monomer used for imparting crosslinkability could be acid-bearing monomer, but this is not usual.

[0179] Preferably vinyl polymer A comprises 0.1 to 3 wt-% of at least one crosslinking monomer containing at least two olefinically unsaturated groups.

[0180] Preferably vinyl polymer A comprises 0.1 to 20 w %, preferably 1 to 15 w %, and particularly 1 to 10 w % of crosslinking monomers.

[0181] Adhesion promoting monomers include amino, urea, or N-heterocyclic groups. As known to those skilled in the art this property can also be achieved by imination i.e. reaction of the acid groups with propylene imine.

[0182] Preferably vinyl polymer A comprises 0.4 to 6 wt-% of at least one olefinically unsaturated monomer with a wet-adhesion promoting functionality, more preferably between 0.5 and 4 wt-%.

[0183] Vinyl polymer A preferably has a weight average molecular weight (M_w) as determined with GPC of from 20,000 to 6,000,000 g/mol, preferably more than 80,000 g/mol and most preferably more than 100,000 g/mol. More preferably the upper limit does not exceed 4,000,000 g/mol.

[0184] Vinyl polymer B preferably has a weight average molecular weight (M_w) as determined with GPC of from 20,000 to 6,000,000 g/mol, preferably more than 80,000 g/mol and most preferably more than 100,000 g/mol. More preferably the upper limit does not exceed 4,000,000 g/mol.

[0185] Preferably vinyl polymer A has a glass transition temperature in the range of from -(minus)20 to 20° C.

[0186] Preferably vinyl polymer B has a glass transition temperature in the range of from 65 to 110° C.

[0187] Preferably the polymer dispersion contains latex particles having a diameter from 30 to 900 nanometres (nm), particularly 60 to 300 nm. The particle size distribution can be unimodal, bimodal, or polymodal. Dispersions having bi- or poly-modal particle size distributions can be made according to the method described in DE3147 008 or U.S. Pat. No. 4,456,726.

[0188] In a preferred embodiment there is provided an aqueous polymer dispersion having a minimum film forming temperature of below 30° C. comprising a vinyl polymer derived from olefinically unsaturated monomers, with at least two phases comprising:

[0189] A) 60 to 80 wt-% of a vinyl polymer A having a glass transition temperature in the range of from -20 to 20° C.; and

[0190] B) 20 to 40 wt-% of a vinyl polymer B having a glass transition temperature in the range of from 65 to 110° C.;

wherein vinyl polymer A comprises 2 to 5 wt-% of at least one acid-functional olefinically unsaturated monomer, and wherein at least 50 wt-% of the monomer composition used to form vinyl polymer A and vinyl polymer B comprises itaconate diesters of Formula 1, preferably from a biorenewable source.

[0191] If vinyl polymer A is made in the second phase then preferably vinyl polymer A has at least 80%, more preferably at least 100% and most preferably 110% of the acid value of vinyl polymer B being made in the first phase and this helps to affect the morphology of the particles to get good film formation.

[0192] According to an embodiment of the invention there is also provided a process to obtain an aqueous polymer dispersion as defined herein which process comprises steps:

[0193] a) a first polymerization step, to form a first phase vinyl polymer;

[0194] b) a second polymerization step in the presence of the resulting first phase vinyl polymer from step a) to form a second phase vinyl polymer.

[0195] The first phase vinyl polymer may be formed using emulsion polymerisation. Such processes are extremely well known, are described elsewhere in this specification and need not be described further great detail.

[0196] If desired the pH of the polymer emulsion can be adjusted to higher values using suitable bases. Examples of which include organic amines such as trialkylamines (e.g. triethylamine, tributylamine), morpholine and alkanolamines, and inorganic bases such as ammonia, NaOH, KOH, and LiOH.

[0197] In an embodiment of the invention it is also possible to use a gradient polymerisation process as described in for example EP1434803 to make at least part of the first and second phase. The second phase monomer feed preferably starts after 20 to 80% completion of the first phase monomer feed.

[0198] In a preferred embodiment when >30 wt-% of monomers of Formula 1 (such as DBI) are used the monomers are preferably fed into the reactor during polymerisation, with a preferred feed time >60 minutes, more preferably >120 minutes and most preferred >150 minutes.

[0199] Preferably, the concentration of unreacted monomer according to Formula 1 during the polymerisation is less than 5 wt-% on total weight of the emulsion, more preferably less than 3 wt-%, most preferably less than 1 wt-%, and typically less than 0.5 wt-% on total weight of the emulsion. The concentration of unreacted monomer(s) other than according to Formula 1 during the polymerisation is less than 5 wt-%, more preferred less than 2.5 wt-%, most preferably less than 1 wt-%, and typically less than 0.3 wt-% on total weight of the emulsion.

[0200] Preferably the dispersions of the invention have VOC levels of less than 100 g/L and more preferably less than 80 g/L, most preferably less than 50 g/L and especially less than 20 g/L of volatile organic components (VOC) such as coalescing solvents.

[0201] If crosslinking monomers are present then preferably the amount of crosslinking agent that is employed is such that the ratio of the number of crosslinker groups present in the first phase vinyl polymer and (if employed) in the second phase vinyl polymer to the number of reactive groups (for crosslinking purposes) in the crosslinking agent is within the range of from 10/1 to 1/3, preferably 2/1 to 1/1.5.

[0202] A crosslinker reactive with a copolymerised crosslinking monomer, if present, is usually combined with the aqueous dispersion by adding it thereto after the preparation of the second phase vinyl polymer (and sometimes just before use of the dispersion), although it may in principle also be combined by performing the polymerisation of the second phase vinyl polymer in the presence of the crosslinking agent. A combination of both incorporation expedients may also in principle be used.

[0203] It will be appreciated that vinyl polymer A and optionally vinyl polymer B possess functional groups for imparting latent crosslinkability to the dispersion (i.e. so that crosslinking takes place e.g. after the formation of a coating therefrom) when combined with the crosslinking agent. For example, one or both polymers could carry functional groups such as hydroxyl groups and the dispersion subsequently

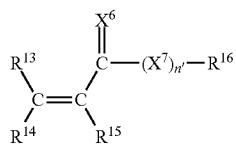
formulated with a crosslinking agent such as a polyisocyanate, melamine, or glycoluril; or the functional groups on one or both polymers could include keto or aldehyde carbonyl groups and the subsequently formulated crosslinker in step c) could be a polyamine or polyhydrazide such as adipic acid dihydrazide, oxalic acid dihydrazide, phthalic acid dihydrazide, terephthalic acid dihydrazide, isophorone diamine and 4,7-dioxadecane-1,10 diamine. It will be noted that such crosslinking agents will effect crosslinking by virtue of forming covalent bonds.

[0204] According to an embodiment of the invention there is provided a process for the production of the aqueous polymer coating dispersion, which process comprises steps: a') a first polymerization step, to form a first phase vinyl polymer; b') a second polymerization step in the presence of the resulting first phase vinyl polymer from step a') to form a second phase vinyl polymer. Optionally the process includes c') a neutralisation step before/after or during step b'). Optionally the process includes a post treatment imidation step d') with alkylene imines like for instance propylene imine) which can greatly improve wet adhesion. Optionally the process includes e') the addition of a crosslinking agent after the polymerization step a') and/or step b'), and preferably after the optional imidation step d'), said crosslinking agent being reactable with any crosslinking functional groups of vinyl polymer A and/or vinyl polymer B on subsequent drying of the coating dispersion to effect covalent bond crosslinking (as described herein).

[0205] The term "activated unsaturated moiety", is used herein to denote a species comprising at least one unsaturated carbon to carbon double bond in chemical proximity to at least one activating moiety. Preferably the activating moiety comprises any group which activates an ethylenically unsaturated double bond for addition thereon by a suitable electrophilic group. Conveniently the activating moiety comprises oxy, thio, (optionally organo substituted)amino, thiocarbonyl and/or carbonyl groups (the latter two groups optionally substituted by thio, oxy or (optionally organo substituted) amino). More convenient activating moieties are (thio)ether, (thio)ester and/or (thio)amide moiety(ies). Most convenient "activated unsaturated moieties" comprise an "unsaturated ester moiety" which denotes an organo species comprising one or more "hydrocarbylidene(thio)carbonyl(thio)oxy" and/or one or more "hydrocarbylidene(thio)-carbonyl(or-gano)amino" groups and/or analogous and/or derived moieties for example moieties comprising (meth)acrylate functionalities and/or derivatives thereof. "Unsaturated ester moieties" may optionally comprise optionally substituted generic α,β -unsaturated acids, esters and/or other derivatives thereof including thio derivatives and analogs thereof.

[0206] Preferred activated unsaturated moieties are those represented by a radical of Formula 4.

Formula 4



where n' is 0 or 1, X⁶ is oxy or, thio; X⁷ is oxy, thio or NR¹⁷ (where R¹⁷ represents H or optionally substituted organo), R¹³, R¹⁴, R¹⁵ and R¹⁶ each independently represent a bond to

another moiety in Formula 1, H, optional substituent and/or optionally substituted organo groups, where optionally any of R¹³, R¹⁴, R¹⁵ and R¹⁶ may be linked to form a ring; where at least one of R¹³, R¹⁴R¹⁵ and R¹⁶ is a bond; and all suitable isomers thereof, combinations thereof on the same species and/or mixtures thereof.

[0207] The terms "activated unsaturated moiety", "unsaturated ester moiety" and/or Formula 4 herein represents part of a formula herein and as used herein these terms denote a radical moiety which depending where the moiety is located in the formula may be monovalent or multivalent (e.g. divalent).

[0208] More preferred moieties of Formula 4 (including isomers and mixtures thereof) are those where n' is 1; X⁶ is O; X⁷ is O, S or NR⁷.

[0209] R¹³, R¹⁴, R¹⁵ and R¹⁶ are independently selected from: a bond, H, optional substituents and optionally substituted C₁₋₁₀hydrocarbo, optionally R¹⁵ and R¹⁶ may be linked to form (together with the moieties to which they are attached) a ring; and where present R¹⁷ is selected from H and optionally substituted C₁₋₁₀hydrocarbo.

[0210] Most preferably n' is 1, X⁶ is O; X⁷ is O or S and R¹³R¹⁴, R¹⁵ and R¹⁶ are independently a bond, H, hydroxy and/or optionally substituted C₁₋₁₀hydrocarbyl.

[0211] For example n' is 1, X⁶ and X⁷ are both O; and R³, R⁴, R⁵ and R⁶ are independently a bond, H, OH, and/or C₁₋₄alkyl; or optionally R⁵ and R⁶ may together form a divalent C₀₋₄alkylenecarbonylC₀₋₄alkylene moiety so Formula 4 represents a cyclic anhydride (e.g. when R¹⁵ and R¹⁶ together are carbonyl then Formula 4 represents a maleic anhydride or derivative thereof).

[0212] For moieties of Formula 4 where n' is 1 and X⁶ and X⁷ are both O then when one of (R¹³ and R¹⁴) is H and also R¹³ is H, Formula 4 represents an acrylate moiety, which includes acrylates (when both R¹³ and R¹⁴ are H) and derivatives thereof (when either R¹³ and R¹⁴ is not H). Similarly when one of (R¹³ and R¹⁴) is H and also R¹⁵ is CH₃, Formula 4 represents an methacrylate moiety, which includes methacrylates (when both R¹³ and R¹⁴ are H) and derivatives thereof (when either R¹³ and R¹⁴ is not H). Acrylate and/or methacrylate moieties of Formula 5 are particularly preferred.

[0213] Conveniently moieties of Formula 4 are those where n' is 1; X⁶ and X⁷ are both O; R¹³ and R¹⁴ are independently a bond, H, CH₃ or OH, and R¹⁵ is H or CH₃; R¹⁶ is H or R¹⁵ and R¹⁶ together are a divalent C=O group.

[0214] More conveniently moieties of Formula 4 are those where n' is 1; X⁶ and X⁷ are both O; R¹³ is OH, R⁴ is CH₃, and R¹⁵ is H and R⁶ is a bond and/or tautomer(s) thereof (for example of an acetoacetoxy functional species).

[0215] Most convenient unsaturated ester moieties are selected from: —OCO—CH=CH₂; —OCO—C(CH₃)=CH₂; acetoacetoxy, —OCOCH=CH(C(CH₃)OH) and all suitable tautomer(s) thereof.

[0216] It will be appreciated that any suitable moieties represented by Formula 4 could be used in the context of this invention such as other reactive moieties.

[0217] Whilst the term vinyl polymer is commonly used to refer to thermoplastic polymers derived by polymerization from compounds containing the vinyl group (CH₂=CH—), the term "vinyl polymer" is used herein more broadly to denote any polymer (whether thermoplastic or not) that comprises (e.g. as repeat units therein) and/or is derived from monomers and/or polymer precursors comprising one or

more of the following moieties: activated unsaturated moieties (such as acrylates and/or methacrylates); any olefinically unsaturated moieties (such as vinyl moieties); mixtures thereof; and/or combinations thereof within the same moiety.

[0218] There is an increasing demand to use bio-renewable monomers in order to improve the sustainability of the polymers used in for example coating applications. In view of concerns about depletion of fossil fuel resources or an increase in carbon dioxide in the air that poses a global-scale environmental problem in recent years, methods for producing raw materials of these polymers from biomass resources have attracted a lot of attention. Since these resources are renewable and therefore have a carbon-neutral biomass, such methods are expected to gain in particular importance in future. It is therefore a preferred feature of the present invention and the aspects described herein that where possible the monomers (especially the higher itaconate diesters such as DBI) as far as possible are biorenewable.

[0219] Preferably at least 30 wt-%, more preferably at least 50 wt-%, and especially 70 wt-% of the olefinically unsaturated monomers used to form the polymers of the invention are derived from at least one bio-renewable olefinically unsaturated monomer. Bio-renewable monomers may be obtained fully or in part from bio-renewable sources. Thus it is preferred to also measure the carbon-14 content to determine the biorenewability.

[0220] The content of carbon-14 (C-14) is indicative of the age of a bio-based material. It is known in the art that C-14, which has a half life of about 5,700 years, is found in bio-renewable materials but not in fossil fuels. Thus, "bio-renewable materials" refer to organic materials in which the carbon comes from non-fossil biological sources. Examples of bio-renewable materials include, but are not limited to, sugars, starches, corns, natural fibres, sugarcanes, beets, citrus fruits, woody plants, cellulosics, lignocellulosics, hemicelluloses, potatoes, plant oils, other polysaccharides such as pectin, chitin, levan, and pullulan, and a combination thereof.

[0221] C-14 levels can be determined by measuring its decay process (disintegrations per minute per gram carbon or dpm/gC) through liquid scintillation counting. In one embodiment of the present invention, polymer A, polymer B and/or the olefinically unsaturated monomer(s) that are used to obtain polymer A and/or polymer B may be considered sufficiently biorenewable for the purposes of this embodiment of the invention when the respective polymer A, polymer B and/or olefinically unsaturated monomer comprise an amount of carbon-14 to produce a decay of at least about 1.5 dpm/gC (disintegrations per minute per gram carbon), more preferably at least 2 dpm/gC, most preferably at least 2.5 dpm/gC, and especially at least 4 dpm/gC.

[0222] It is preferred that the higher itaconate diesters such as DBI are biorenewable, however other monomers used in the present invention may also be biorenewable. Examples of bio-renewable monomers include but are not limited to bio-based acrylics obtained by for example using bio-derived alcohols such as bio-butanol and include (meth)acrylic acid and alkyl (meth)acrylate, where alkyl is preferably selected from methyl, ethyl, butyl or 2-ethylhexyl.

[0223] Acrylic acid can be made from glycerol, as is disclosed by Arkema, or from lactic acid as described by US7687661. Methacrylic acid can be prepared from ethene, methanol and carbon monoxide (all bio-renewable), as disclosed by Lucite International Ltd.

[0224] Olefinically unsaturated bio-renewable monomers which may additionally provide a contribution to improved coating properties include α -methylene butyrolactone, α -methylene valerolactone, α -methylene γ -R³ butyrolactone (R³ can be an optionally substituted alkyl or optionally substituted aryl); itaconates such as dialkyl itaconates (including DBI) and monoalkyl itaconates, itaconic acid, itaconic anhydride, crotonic acid and alkyl esters thereof, citraconic acid and alkyl esters thereof, methylene malonic acid and its mono and dialkyl esters, citraconic anhydride, mesaconic acid and alkyl esters thereof.

[0225] Other non-acid functional, non-crosslinking monomers include diesters of itaconic acid. Preferred examples of such monomers include dimethyl itaconate, diethyl itaconate, di-n-propyl itaconate, di-1-propyl itaconate, di-n-butyl itaconate, di-1-butyl itaconate, and di-2-ethyl hexyl itaconate.

[0226] Another useful set of useful bio-renewable monomers include N—R², α -methylene butyrolactam (R² can be an optionally substituted alkyl or optionally substituted aryl); N—R², α -methylene γ -R¹ butyrolactam; N-alkyl itaconimides; itaconmonoamids; itacondiamids; ialkyl itaconamides, mono alkyl itaconamides; furfuryl (meth)acrylate; fatty acid functional (meth)acrylates such as DAPRO FX-522 from Elementis and Visiomer® MUMA from Evonik.

[0227] It is appreciated that certain features of the invention, which are for clarity described in the context of separate embodiments may also be provided in combination in a single embodiment. Conversely various features of the invention, which are for brevity, described in the context of a single embodiment, may also be provided separately or in any suitable sub-combination.

[0228] The object of the present invention is to solve some or all of the problems or disadvantages (such as identified throughout the application herein) with the prior art.

[0229] Unless the context clearly indicates otherwise, as used herein plural forms of the terms herein are to be construed as including the singular form and vice versa.

[0230] The term "comprising" as used herein will be understood to mean that the list following is non exhaustive and may or may not include any other additional suitable items, for example one or more further feature(s), component(s), ingredient(s) and/or substituent(s) as appropriate.

[0231] The terms 'effective', 'acceptable', 'active' and/or 'suitable' (for example with reference to any process, use, method, application, preparation, product, material, formulation, compound, monomer, oligomer, polymer precursor, and/or polymers described herein as appropriate) will be understood to refer to those features of the invention which if used in the correct manner provide the required properties to that which they are added and/or incorporated to be of utility as described herein. Such utility may be direct for example where a material has the required properties for the aforementioned uses and/or indirect for example where a material has use as a synthetic intermediate and/or diagnostic tool in preparing other materials of direct utility. As used herein these terms also denote that a functional group is compatible with producing effective, acceptable, active and/or suitable end products.

[0232] Preferred utility of the present invention comprises as a coating composition.

[0233] In the discussion of the invention herein, unless stated to the contrary, the disclosure of alternative values for the upper and lower limit of the permitted range of a parameter coupled with an indicated that one of said values is more

preferred than the other, is to be construed as an implied statement that each intermediate value of said parameter, lying between the more preferred and less preferred of said alternatives is itself preferred to said less preferred value and also to each less preferred value and said intermediate value.

[0234] For all upper and/or lower boundaries of any parameters given herein, the boundary value is included in the value for each parameter. It will also be understood that all combinations of preferred and/or intermediate minimum and maximum boundary values of the parameters described herein in various embodiments of the invention may also be used to define alternative ranges for each parameter for various other embodiments and/or preferences of the invention whether or not the combination of such values has been specifically disclosed herein. Thus for example a substance stated as present herein in an amount from 0 to "x" (e.g. in units of mass and/or weight %) is meant (unless the context clearly indicates otherwise) to encompass both of two alternatives, firstly a broader alternative that the substance may optionally not be present (when the amount is zero) or present only in an de-minimus amount below that can be detected. A second preferred alternative (denoted by a lower amount of zero in a range for amount of substance) indicates that the substance is present, and zero indicates that the lower amount is a very small trace amount for example any amount sufficient to be detected by suitable conventional analytical techniques and more preferably zero denotes that the lower limit of amount of substance is greater than or equal to 0.001 by weight % (calculated as described herein).

[0235] It will be understood that the total sum of any quantities expressed herein as percentages cannot (allowing for rounding errors) exceed 100%. For example the sum of all components of which the composition of the invention (or part(s) thereof) comprises may, when expressed as a weight (or other) percentage of the composition (or the same part(s) thereof), total 100% allowing for rounding errors.

[0236] However where a list of components is non exhaustive the sum of the percentage for each of such components may be less than 100% to allow a certain percentage for additional amount(s) of any additional component(s) that may not be explicitly described herein.

[0237] In the present invention, unless the context clearly indicates otherwise, an amount of an ingredient stated to be present in the composition of the invention when expressed as a weight percentage, is calculated based on the total amount of monomers in the composition being equivalent to 100% (thus for example components (a)+(b)+(c)+(d) total 100%). For convenience certain non monomer ingredients (such as for example chain transfer agents (CTA)) which fall outside the definitions of any of components (a) to (d) may also be calculated as weight percentages based on total monomer (i.e. where the weight of total monomers alone is set at 100%). As the weight % of monomers (for example for components (a) to (d)) by definition total 100% it will be seen that using monomer based weight % values for the non-monomer ingredients (i.e. those components outside (a) to (d)) will mean the total percentages will exceed 100%. Thus amounts of non-monomer ingredients expressed as monomer based weight percentages can be considered as providing a ratio for the weight amounts for these ingredients with respect to the total weight of monomers which is used only as a reference for calculation rather than as a strict percentage. Further ingredients are not excluded from the composition when (a)+(b)+

(c)+(d) total 100% and weight percentages based on total monomers should not be confused with weight percentages of the total composition.

[0238] The term "substantially" as used herein may refer to a quantity or entity to imply a large amount or proportion thereof. Where it is relevant in the context in which it is used "substantially" can be understood to mean quantitatively (in relation to whatever quantity or entity to which it refers in the context of the description) there comprises an proportion of at least 80%, preferably at least 85%, more preferably at least 90%, most preferably at least 95%, especially at least 98%, for example about 100% of the relevant whole. By analogy the term "substantially-free" may similarly denote that quantity or entity to which it refers comprises no more than 20%, preferably no more than 15%, more preferably no more than 10%, even more preferably no more than 5%, most preferably no more than 2%, especially no more than 1.5%, for example about 0% (e.g. completely absent or if present only in an undetectable amount) of the relevant whole.

[0239] The terms 'optional substituent' and/or 'optionally substituted' as used herein (unless followed by a list of other substituents) signifies the one or more of following groups (or substitution by these groups): carboxy, sulpho, formyl, hydroxy, amino, imino, nitrilo, mercapto, cyano, nitro, methyl, methoxy and/or combinations thereof. These optional groups include all chemically possible combinations in the same moiety of a plurality (preferably two) of the aforementioned groups (e.g. amino and sulphonyl if directly attached to each other represent a sulphonyl group). Preferred optional substituents comprise: carboxy, sulpho, hydroxy, amino, mercapto, cyano, methyl, halo, trihalomethyl and/or methoxy.

[0240] The synonymous terms 'organic substituent' and "organic group" as used herein (also abbreviated herein to "organo") denote any univalent or multivalent moiety (optionally attached to one or more other moieties) which comprises one or more carbon atoms and optionally one or more other heteroatoms. Organic groups may comprise organoheteraryl groups (also known as organoelement groups) which comprise univalent groups containing carbon, which are thus organic, but which have their free valence at an atom other than carbon (for example organothio groups). Organic groups may alternatively or additionally comprise organyl groups which comprise any organic substituent group, regardless of functional type, having one free valence at a carbon atom. Organic groups may also comprise heterocyclyl groups which comprise univalent groups formed by removing a hydrogen atom from any ring atom of a heterocyclic compound: (a cyclic compound having as ring members atoms of at least two different elements, in this case one being carbon). Preferably the non carbon atoms in an organic group may be selected from: hydrogen, halo, phosphorus, nitrogen, oxygen, silicon and/or sulphur, more preferably from hydrogen, nitrogen, oxygen, phosphorus and/or sulphur.

[0241] Most preferred organic groups comprise one or more of the following carbon containing moieties: alkyl, alkoxy, alkanoyl, carboxy, carbonyl, formyl and/or combinations thereof; optionally in combination with one or more of the following heteroatom containing moieties: oxy, thio, sulphinyl, sulphonyl, amino, imino, nitrilo and/or combinations thereof. Organic groups include all chemically possible combinations in the same moiety of a plurality (preferably two) of the aforementioned carbon containing and/or heteroatom

moieties (e.g. alkoxy and carbonyl if directly attached to each other represent an alkoxy carbonyl group).

[0242] The term 'hydrocarbo group' as used herein is a sub-set of a organic group and denotes any univalent or multivalent moiety (optionally attached to one or more other moieties) which consists of one or more hydrogen atoms and one or more carbon atoms and may comprise one or more saturated, unsaturated and/or aromatic moieties. Hydrocarbo groups may comprise one or more of the following groups. Hydrocarbyl groups comprise univalent groups formed by removing a hydrogen atom from a hydrocarbon (for example alkyl). Hydrocarbylene groups comprise divalent groups formed by removing two hydrogen atoms from a hydrocarbon, the free valences of which are not engaged in a double bond (for example alkylene). Hydrocarbylidene groups comprise divalent groups (which may be represented by "R₂C—") formed by removing two hydrogen atoms from the same carbon atom of a hydrocarbon, the free valences of which are engaged in a double bond (for example alkylidene). Hydrocarbylidyne groups comprise trivalent groups (which may be represented by "RC≡"), formed by removing three hydrogen atoms from the same carbon atom of a hydrocarbon the free valences of which are engaged in a triple bond (for example alkylidyne). Hydrocarbo groups may also comprise saturated carbon to carbon single bonds (e.g. in alkyl groups); unsaturated double and/or triple carbon to carbon bonds (e.g. in respectively alkenyl and alkynyl groups); aromatic groups (e.g. in aryl groups) and/or combinations thereof within the same moiety and where indicated may be substituted with other functional groups.

[0243] The term 'alkyl' or its equivalent (e.g. 'alk') as used herein may be readily replaced, where appropriate and unless the context clearly indicates otherwise, by terms encompassing any other hydrocarbo group such as those described herein (e.g. comprising double bonds, triple bonds, aromatic moieties (such as respectively alkenyl, alkynyl and/or aryl) and/or combinations thereof (e.g. aralkyl) as well as any multivalent hydrocarbo species linking two or more moieties (such as bivalent hydrocarbylene radicals e.g. alkylene).

[0244] Any radical group or moiety mentioned herein (e.g. as a substituent) may be a multivalent or a monovalent radical unless otherwise stated or the context clearly indicates otherwise (e.g. a bivalent hydrocarbylene moiety linking two other moieties). However where indicated herein such monovalent or multivalent groups may still also comprise optional substituents. A group which comprises a chain of three or more atoms signifies a group in which the chain wholly or in part may be linear, branched and/or form a ring (including spiro and/or fused rings). The total number of certain atoms is specified for certain substituents for example C_{1-N}organo, signifies a organo moiety comprising from 1 to N carbon atoms. In any of the formulae herein if one or more substituents are not indicated as attached to any particular atom in a moiety (e.g. on a particular position along a chain and/or ring) the substituent may replace any H and/or may be located at any available position on the moiety which is chemically suitable and/or effective.

[0245] Preferably any of the organo groups listed herein comprise from 1 to 36 carbon atoms, more preferably from 1 to 18. It is particularly preferred that the number of carbon atoms in an organo group is from 1 to 12, especially from 1 to 10 inclusive, for example from 1 to 4 carbon atoms.

[0246] As used herein chemical terms (other than IUAPC names for specifically identified compounds) which com-

prise features which are given in parentheses—such as (alkyl) acrylate, (meth)acrylate and/or (co)polymer—denote that that part in parentheses is optional as the context dictates, so for example the term (meth)acrylate denotes both methacrylate and acrylate.

[0247] Certain moieties, species, groups, repeat units, compounds, oligomers, polymers, materials, mixtures, compositions and/or formulations which comprise and/or are used in some or all of the invention as described herein may exist as one or more different forms such as any of those in the following non exhaustive list: stereoisomers (such as enantiomers (e.g. E and/or Z forms), diastereoisomers and/or geometric isomers); tautomers (e.g. keto and/or enol forms), conformers, salts, zwitterions, complexes (such as chelates, clathrates, crown compounds, cryptands/cryptades, inclusion compounds, intercalation compounds, interstitial compounds, ligand complexes, organometallic complexes, non-stoichiometric complexes, π -adducts, solvates and/or hydrates); isotopically substituted forms, polymeric configurations [such as homo or copolymers, random, graft, comb and/or block polymers, linear and/or branched polymers (e.g. hyperbranched, star and/or side branched), cross-linked and/or networked polymers, polymers obtainable from di and/or tri-valent repeat units, dendrimers, polymers of different tacticity (e.g. isotactic, syndiotactic or atactic polymers)]; polymorphs (such as interstitial forms, crystalline forms and/or amorphous forms), different phases, solid solutions; and/or combinations thereof and/or mixtures thereof where possible. The present invention comprises and/or uses all such forms which are effective as defined herein.

[0248] Polymers of the present invention may be prepared by one or more suitable polymer precursor(s) which may be organic and/or inorganic and comprise any suitable (co) monomer(s), (co)polymer(s) [including homopolymer(s)] and mixtures thereof which comprise moieties which are capable of forming a bond with the or each polymer precursor(s) to provide chain extension and/or cross-linking with another of the or each polymer precursor(s) via direct bond(s) as indicated herein.

[0249] Polymer precursors of the invention may comprise one or more monomer(s), oligomer(s), polymer(s); mixtures thereof and/or combinations thereof which have suitable polymerisable functionality. It will be understood that unless the context dictates otherwise term monomer as used herein encompasses the term polymer precursor and does not necessarily exclude monomers that may themselves be polymeric and/or oligomeric in character.

[0250] A monomer is a substantially monodisperse compound of a low molecular weight (for example less than one thousand daltons) which is capable of being polymerised.

[0251] A polymer is a polydisperse mixture of macromolecules of large molecular weight (for example many thousands of daltons) prepared by a polymerisation method, where the macromolecules comprises the multiple repetition of smaller units (which may themselves be monomers, oligomers and/or polymers) and where (unless properties are critically dependent on fine details of the molecular structure) the addition or removal one or a few of the units has a negligible effect on the properties of the macromolecule.

[0252] A oligomer is a polydisperse mixture of molecules having an intermediate molecular weight between a monomer and polymer, the molecules comprising a small plurality of monomer units the removal of one or a few of which would significantly vary the properties of the molecule.

[0253] Depending on the context the term polymer may or may not encompass oligomer.

[0254] The polymer precursor of and/or used in the invention may be prepared by direct synthesis or (if the polymeric precursor is itself polymeric) by polymerisation. If a polymerisable polymer is itself used as a polymer precursor of and/or used in the invention it is preferred that such a polymer precursor has a low polydispersity, more preferably is substantially monodisperse, to minimise the side reactions, number of by-products and/or polydispersity in any polymeric material formed from this polymer precursor. The polymer precursor(s) may be substantially un-reactive at normal temperatures and pressures.

[0255] Except where indicated herein polymers and/or polymeric polymer precursors of and/or used in the invention can be (co)polymerised by any suitable means of polymerisation well known to those skilled in the art. Examples of suitable methods comprise: thermal initiation; chemical initiation by adding suitable agents; catalysis; and/or initiation using an optional initiator followed by irradiation, for example with electromagnetic radiation (photo-chemical initiation) at a suitable wavelength such as UV; and/or with other types of radiation such as electron beams, alpha particles, neutrons and/or other particles.

[0256] The substituents on the repeating unit of a polymer and/or oligomer may be selected to improve the compatibility of the materials with the polymers and/or resins in which they may be formulated and/or incorporated for the uses described herein. Thus the size and length of the substituents may be selected to optimise the physical entanglement or interlocation with the resin or they may or may not comprise other reactive entities capable of chemically reacting and/or cross linking with such other resins as appropriate.

[0257] Another aspect of the invention broadly provides a coating composition comprising the polymers and/or beads of the present invention and/or as described herein.

[0258] A further aspect of the invention provides a coating obtained or obtainable from a coating composition of the present invention.

[0259] A yet other aspect of the invention broadly provides a substrate and/or article having coated thereon an (optionally cured) coating composition of the present invention.

[0260] A yet further aspect of the invention broadly provides a method of using polymers of the present invention and/or as described herein to prepare a coating composition.

[0261] A still further aspect of the invention broadly provides a method for preparing a coated substrate and/or article comprising the steps of applying a coating composition of the present invention to the substrate and/or article and optionally curing said composition in situ to form a cured coating thereon. The curing may be by any suitable means, such as thermally, by radiation and/or by use of a cross-linker.

[0262] Preferred coating compositions are solvent coating compositions or aqueous coating compositions, more preferably are aqueous coating compositions.

[0263] Optionally aqueous coating compositions may also comprise a co-solvent. A co-solvent, as is well known in the coating art, is an organic solvent employed in an aqueous composition to ameliorate the drying characteristics thereof, and in particular to lower its minimum film forming temperature. The co-solvent may be solvent incorporated or used during preparation of polymers of the invention or may have been added during formulation of the aqueous composition.

[0264] The compositions of the invention are particularly useful as or for providing the principle component of coating formulations (i.e. composition intended for application to a substrate without further treatment or additions thereto) such as protective or decorative coating compositions (for example paint, lacquer or varnish) wherein an initially prepared composition optionally may be further diluted with water and/or organic solvents, and/or combined with further ingredients or may be in more concentrated form by optional evaporation of water and/or organic components of the liquid medium of an initially prepared composition.

[0265] The compositions of the invention may be used in various applications and for such purposes may be optionally further combined or formulated with other additives and/or components, such as defoamers, rheology control agents, thickeners, dispersing and/or stabilizing agents (usually surfactants and/or emulsifiers), wetting agents, fillers, extenders, fungicides, bactericides, coalescing and wetting solvents or co-solvents (although solvents are not normally required), plasticisers, anti-freeze agents, waxes, colorants, pigments, dyes, heat stabilisers, levelling agents, anti-cratering agents, fillers, sedimentation inhibitors, UV absorbers, antioxidants, reactive diluents, neutralising agents, adhesion promoters and/or any suitable mixtures thereof.

[0266] The aforementioned additives and/or components and the like may be introduced at any stage of the production process or subsequently. It is possible to include fire retardants (such as antimony oxide) to enhance fire retardant properties.

[0267] The compositions of the invention may also be blended with other polymers such as vinyl polymers, alkyds (saturated or unsaturated), polyesters and/or polyurethanes.

[0268] The coating composition of the invention may be applied to a variety of substrates including wood, board, metals, stone, concrete, glass, cloth, leather, paper, plastics, foam and the like, by any conventional method including brushing, dipping, flow coating, spraying, and the like. The coating composition of the invention may also be used to coat the interior and/or exterior surfaces of three-dimensional articles. The coating compositions of the invention may also be used, appropriately formulated if necessary, for the provision of films, polishes, varnishes, lacquers, paints, inks and adhesives. However, they are particularly useful and suitable for providing the basis of protective coatings for substrates that comprise wood (e.g. wooden floors), plastics, polymeric materials, paper and/or metal.

[0269] The carrier medium may be removed from the compositions of the invention once they have been applied to a substrate by being allowed to dry naturally at ambient temperature, or the drying process may be accelerated by heat. Crosslinking can be developed by allowing to stand for a prolonged period at ambient temperature (several days) or by heating at an elevated temperature (e.g. 50° C.) for a much shorter period of time.

[0270] Many other variations embodiments of the invention will be apparent to those skilled in the art and such variations are contemplated within the broad scope of the present invention.

[0271] Further aspects of the invention and preferred features thereof are given in the claims herein.

Tests

Minimum Film Forming Temperature

[0272] The minimum film forming temperature (MFFT) of a dispersion as used herein is the temperature where the dispersion forms a smooth and crack free coating or film using DIN 53787 and when applied using a Sheen MFFT bar SS3000.

Spot Tests

[0273] Coating films formed by blends of the invention can be tested in well known conventional spot tests (such as ASTM D1308-02e1) to determine the resistance of the film to various liquid reagents such as water, ethanol, detergent (e.g. that available commercially from Unilever under the trade mark Andy) and coffee. In one such test a standard volume (e.g. 0.5 ml) of the liquid reagent may be applied to the film to form a spot thereon (e.g. by pipette) which is then covered with a watch glass. After the time specified (e.g. in the tables herein) the film can be assessed and rated visually on a scale of 1 to 5 as described below.

Koening Hardness

[0274] Koening hardness as used herein is a standard measure of hardness, being a determination of how the viscoelastic properties of a film formed from the dispersion slows down a swinging motion deforming the surface of the film, and is measured according to DIN 53157 NEN5319.

Glass Transition Temperature (Tg)

[0275] As is well known, the glass transition temperature of a polymer is the temperature at which it changes from a glassy, brittle state to a plastic, rubbery state. The glass transition temperatures may be determined experimentally using Differential Scanning calorimetry (DSC), taking the peak of the derivative curve as Tg, or calculated from the Fox equation. Thus the Tg, in degrees Kelvin, of a copolymer having "n" copolymerised comonomers is given by the weight fractions W of each comonomer type and the Tgs of the homopolymers (in degrees Kelvin) derived from each comonomer according to the equation:

$$\frac{1}{T_g} = \frac{W_1}{T_{g1}} + \frac{W_2}{T_{g2}} + \dots + \frac{W_n}{T_{gn}}$$

[0276] The calculated Tg in degrees Kelvin may be readily converted to ° C.

Solids Content

[0277] The solids content of an aqueous dispersion of the invention is usually within the range of from about 20 to 65 wt-% on a total weight basis, more usually 30 to 55 wt-%. Solids content can, if desired, be adjusted by adding water or removing water (e.g. by distillation or ultrafiltration).

pH Value

[0278] The pH value of the dispersion of the invention can be from 2 to 10 and mostly is from 6 to 9.5.

Blocking

Block Resistance Measurement [Includes Blocking and Early Blocking]:

Step 1: Blocking:

[0279] A 100 micron wet film of the aqueous emulsion of the invention to which 10% butyldiglycol is added is cast on to a paper substrate and dried for 16 hours at 52° C.

Step 1: Early Blocking:

[0280] A 250 micron wet film of the aqueous emulsion of the invention to which 10% butyldiglycol was added, is cast on to a paper substrate and dried for 24 hours at room temperature.

Step 2: Blocking and Early Blocking:

[0281] After cooling down to room temperature two pieces of coated film are placed with the coated side against each other under a load of 1 Kg/cm.sup.2 for 4 hours at 52° C. After this time interval the load on the samples is removed and the samples are left to cool down to room temperature (22+2° C.). When the two coatings can be removed from each other without any damage to the film (do not stick) the block resistance is very good and assessed as a 5. When they however completely stick together, block resistance is very bad and assessed as a 0.

Gas Chromatography Mass Spectrometry (GCMS)

[0282] to confirm polymerisation is substantially complete the content of free itaconate ester monomers content can be determined by GCMS. The GCMS analyses were performed on a Trace GC-DSQ MS (Interscience, Breda, the Netherlands) equipped with a CTC combi Pal robotic autosampler for head space has been used. The carrier gas was Helium and a CP Sil 5 low bleed/MS, 25 m×0.25 mm i.d., 1.0 µm (CP nr. 7862) column has been used.

[0283] The GC-oven was programmed from 50° C. (5 min) followed by different sequential temperature ramps of 5° C./min to 70° C. (0 min), 15° C./min to 220° C. (0 min), and ending with 25° C./min to 280° C. (10 min). A continuous Helium flow of 1.2 ml/min was used. A hot split injection at 300° C. was performed on a programmed temperature vaporizer (PTV). The injection volume was 1 µl. The MS transfer line and ion source were both kept at 250° C. The samples were measured with single ion monitoring (SIM). For the specific case of dibutyl itaconate (DBI) the masses 127.0 and 59.0 Da were used, for the internal standard (iso butyl acrylate) the masses 55.0 and 73.0 were applied. The sample solutions were approximately 500 mg in 3 ml of internal standard solution (iso butyl acrylate in acetone). The calibration was performed with 5 different concentration levels from 0 to 500 ppm. The calculation was performed using Microsoft Excel with a linear calibration curve.

Molecular Weight

[0284] Unless the context clearly dictates otherwise the term molecular weight of a polymer or oligomer as used herein denotes weight average molecular weight (also denoted as M_w). M_w may be measured by any suitable conventional method for example by Gas Phase Chromatography

(GPC—performed similarly to the GCMS method described above) and/or by the SEC method described below. GPC method is preferred

Determination of Molecular Weight of a Polymer Using SEC

[0285] The molecular weight of a polymer may also be determined using Size Exclusion Chromatography (SEC) with tetrahydrofuran as the eluent or with 1,1,1,3,3,3 hexafluoro isopropanol as the eluent.

1) Tetrahydrofuran

[0286] The SEC analyses were performed on an Alliance Separation Module (Waters 2690), including a pump, auto injector, degasser, and column oven. The eluent was tetrahydrofuran (THF) with the addition of 1.0 vol % acetic acid. The injection volume was 150 μ l. The flow was established at 1.0 ml/min. Three PL MixedB (Polymer Laboratories) with a guard column (3 μ m PL) were applied at a temperature of 40° C. The detection was performed with a differential refractive index detector (Waters 410). The sample solutions were prepared with a concentration of 20 mg solids in 8 ml THF (+1 vol % acetic acid), and the samples were dissolved for a period of 24 hours. Calibration is performed with eight polystyrene standards (polymer standard services), ranging from 500 to 4,000,000 g/mol. The calculation was performed with Millennium 32 software (Waters) with a third order calibration curve. The obtained molar masses are polystyrene equivalent molar masses (g/mol).

2) 1,1,1,3,3,3 Hexafluoro Isopropanol

[0287] The SEC analyses were performed on a Waters Alliance 2695 (pump, degasser and autosampler) with a Shodex RI-101 differential refractive index detector and Shimadzu CTO-20AC column oven. The eluent was 1,1,1,3,3,3 hexafluoro isopropanol (HFIP) with the addition of 0.2M potassium trifluoro acetate (KTFA). The injection volume was 50 μ l. The flow was established at 0.8 ml/min. Two PSS PFG Linear XL columns (Polymer Standards Service) with a guard column (PFG PSS) were applied at a temperature of 40° C. The detection was performed with a differential refractive index detector. The sample solutions were prepared with a concentration of 5 mg solids in 2 ml HFIP (+0.2M KTFA), and the samples were dissolved for a period of 24 hours. Calibration is performed with eleven polymethyl methacrylate standards (polymer standard services), ranging from 500 to 2,000,000 g/mol. The calculation was performed with Empower Pro software (Waters) with a third order calibration curve. The molar mass distribution is obtained via conventional calibration and the molar masses are polymethyl methacrylate equivalent molar masses (g/mol).

Standard Conditions

[0288] As used herein, unless the context indicates otherwise, standard conditions (e.g. for drying a film) means a relative humidity of 50%±5%, ambient temperature (which denotes herein a temperature of 23° C.±2°) and an air flow of ≤ (less than or equal to) 0.1 m/s.

[0289] The following examples are provided to further illustrate the processes and compositions of the present invention. These examples are illustrative only and are not intended to limit the scope of the invention in any way. Unless other-

wise specified all parts, percentages, and ratios are on a weight basis. The prefix C before an example indicates that it is comparative.

[0290] Various registered trademarks, other designations and/or abbreviations are used herein to denote some of ingredients used to prepare polymers and compositions of the invention. These are identified below by chemical name and/or trade-name and optionally their manufacturer or supplier from whom they are available commercially. However where a chemical name and/or supplier of a material described herein is not given it may easily be found for example in reference literature well known to those skilled in the art: such as: 'McCutcheon's Emulsifiers and Detergents', Rock Road, Glen Rock, N.J. 07452-1700, USA, 1997 and/or Hawley's Condensed Chemical Dictionary (14th Edition) by Lewis, Richard J., Sr.; John Wiley & Sons.

[0291] In the examples the following abbreviations/monomers may be used:

BA=n-butyl acrylate (may be biorenewable)
 BMA=n-butyl methacrylate (may be prepared using bio-renewable alkanols)
 DBI denotes di(n-butyl) itaconate (also known as dibutyl 2-methylidenebutanedioate) (may be bio-renewable)
 DDM denotes n-dodecyl mercaptane
 DMI=dimethyl itaconate (may be bio-renewable)
 DMW denotes dematerialized water
 EDTA=ethylene diamine tetraacetic acid
 HFIP denotes hexafluoro isopropanol
 KTFA denotes potassium trifluoro acetate
 MMA=methyl methacrylate (may be prepared using bio-renewable alkanols)
 MAA=methacrylic acid (may be biorenewable)
 NS denotes sodium sulfate
 PAA denotes polyacrylic acid
 STY denotes styrene;
 D(I)I denotes di(iso-butyl) itaconate (also known as di(tert-butyl)itaconate)
 DPI denotes di(pentyl) itaconate
 DHI denotes di(hexyl) itaconate
 DHPI denotes di(heptyl) itaconate
 DOI denotes di(n-octyl) itaconate
 D(EH)I denotes di(2-ethylhexyl) itaconate
 DDI denotes di(decyl) itaconate
 DBzI denotes di(benzyl) itaconate
 DPhI denotes di(phenyl) itaconate
 BPI denotes butyl pentyl itaconate
 BHI denotes butyl hexyl itaconate
 HOI denotes hexyl n-octyl itaconate
 IA denotes itaconic acid
 MSA denotes the sulphonic acid of α -methyl styrene
 DPRI denotes di(propyl) itaconate
 CEA denotes beta carboxy ethyl acrylate
 PA denotes propyl acrylate
 OA denotes n-octyl acrylate
 MBI denotes the mono acid butyl itaconate (i.e. half ester)
 IAn denotes itaconic anhydride
 MMAlA denotes methylene malonic acid,
 MalAn denotes maleic anhydride, i
 PHEMA denotes phosphated hydroxylethyl methacrylate
 AMPS denotes 2-acrylamido-2-methylpropane sulfonic acid
 URED denotes the monomer N-[2-(2-Oxo-1-imidazolidinyl)ethyl]methacrylate
 MSTY denotes alpha methyl styrene.

EXAMPLES 1 TO 3

Sequential Vinyl Polymers

Example 1

[0292] To a round-bottomed flask equipped with a condenser, thermometer and mechanical stirrer 84.853 parts of water, 0.253 parts of sodium bicarbonate, and 1.786 parts of a 30 wt-% solution of sodium lauryl sulphate in water are added and this mixture is heated to 50° C. At 50° C., 10% of a first monomer feed consisting of 20.93 parts of water, 4.285 of a 30 wt-% solution of sodium lauryl sulphate in water, 0.726 parts of sodium bicarbonate, 0.246 parts of ammonium persulphate, 1.340 parts of methacrylic acid, 26.811 parts of dibutyl itaconate, and 25.456 parts of methyl methacrylate is added and the reactor contents are heated to 90° C. After the reaction temperature has been reached, the reactor contents are stirred for 15 minutes.

[0293] Next, the remainder of the first monomer feed is added over a period of 210 minutes. When the feed is completed, the feed tank is rinsed with 1.885 parts of water.

[0294] The batch is kept at 90° C. for 30 minutes and cooled the batch to 70° C. Next, a slurry comprising 0.289 parts of a 70 wt-% solution of t-butyl hydroperoxide in water and 1.228 parts of water is added and the batch is stirred for 5 minutes. Next, a second monomer feed, comprising 2.681 parts of methacrylic acid, 4.932 parts of methyl methacrylate, 15.117 parts of butyl acrylate, and 30.877 parts of butyl methacrylate is added over a period of 240 minutes. Simultaneously, a catalyst feed comprising 11.943 parts of water, 0.120 parts of i-ascorbic acid, and 1.071 parts of a 30 wt-% solution of sodium lauryl sulphate, is fed over the same period. After the second monomer feed is finished, the feed tank is rinsed with 1.885 parts of water.

[0295] The reactor contents are stirred at 70° C. for another 30 minutes, after which the batch is cooled to 30° C. The pH of the emulsion is adjusted to 7 using 0.6 parts of a 25% solution of ammonia in water or part of it. Simultaneously, 0.623 parts of water are added. The solids content of the emulsion is adjusted to 45% using water.

[0296] The resulting emulsion has a solids content of 45%, and a pH of 7.0.

Example 2

[0297] To a round-bottomed flask equipped with a condenser, thermometer and mechanical stirrer 84.853 parts of water, 0.253 parts of sodium bicarbonate, and 1.786 parts of a 30 wt-% solution of sodium lauryl sulphate in water are added and this mixture is heated to 50° C. At 50° C., 10% of a first monomer feed consisting of 20.93 parts of water, 4.285 of a 30 wt-% solution of sodium lauryl sulphate in water, 0.726 parts of sodium bicarbonate, 0.246 parts of ammonium persulphate, 1.340 parts of methacrylic acid, 14.044 parts of butyl methacrylate, 24.123 parts of dimethyl itaconate, and 14.100 parts of methyl methacrylate is added and the reactor contents are heated to 90° C. After the reaction temperature has been reached, the reactor contents are stirred for 15 minutes.

[0298] Next, the remainder of the first monomer feed is added over a period of 210 minutes. When the feed is completed, the feed tank is rinsed with 1.885 parts of water.

[0299] The batch is kept at 90° C. for 30 minutes and cooled the batch to 70° C. Next, a slurry comprising 0.289 parts of a

70 wt-% solution of t-butyl hydroperoxide in water and 1.228 parts of water is added and the batch is stirred for 5 minutes. Next, a second monomer feed, comprising 2.681 parts of methacrylic acid, 4.932 parts of methyl methacrylate, 15.117 parts of butyl acrylate, 18.762 parts of dibutyl itaconate, and 12.115 parts of butyl methacrylate is added over a period of 240 minutes. Simultaneously, a catalyst feed comprising 11.943 parts of water, 0.120 parts of i-ascorbic acid, and 1.071 parts of a 30 wt-% solution of sodium lauryl sulphate, is fed over the same period. After the second monomer feed is finished, the feed tank is rinsed with 1.885 parts of water.

[0300] The reactor contents are stirred at 70° C. for another 30 minutes, after which the batch is cooled to 30° C. The pH of the emulsion is adjusted to 7 using 0.6 parts of a 25% solution of ammonia in water or part of it. Simultaneously, 0.623 parts of water are added. The solids content of the emulsion is adjusted to 45% using water.

[0301] The resulting emulsion has a solids content of 45%, and a pH of 7.0.

Example 3

[0302] To a round-bottomed flask equipped with a condenser, thermometer and mechanical stirrer 84.853 parts of water, 0.253 parts of sodium bicarbonate, and 1.786 parts of a 30 wt-% solution of sodium lauryl sulphate in water are added and this mixture is heated to 50° C. At 50° C., 10% of a first monomer feed consisting of 20.93 parts of water, 4.285 of a 30 wt-% solution of sodium lauryl sulphate in water, 0.726 parts of sodium bicarbonate, 0.246 parts of ammonium persulphate, 1.340 parts of methacrylic acid, 14.044 parts of butyl methacrylate, and 38.223 parts of methyl methacrylate is added and the reactor contents are heated to 90° C. After the reaction temperature has been reached, the reactor contents are stirred for 15 minutes.

[0303] Next, the remainder of the first monomer feed is added over a period of 210 minutes. When the feed is completed, the feed tank is rinsed with 1.885 parts of water.

[0304] The batch is kept at 90° C. for 30 minutes and cooled the batch to 70° C. Next, a slurry comprising 0.289 parts of a 70 wt-% solution of t-butyl hydroperoxide in water and 1.228 parts of water is added and the batch is stirred for 5 minutes. Next, a second monomer feed, comprising 2.681 parts of methacrylic acid, 4.932 parts of methyl methacrylate, 2.673 parts of diacetone acrylamide, 12.444 parts of butyl acrylate, 26.803 parts of dibutyl itaconate, and 4.074 parts of butyl methacrylate is added over a period of 240 minutes. Simultaneously, a catalyst feed comprising 11.943 parts of water, 0.120 parts of i-ascorbic acid, and 1.071 parts of a 30 wt-% solution of sodium lauryl sulphate, is fed over the same period. After the second monomer feed is finished, the feed tank is rinsed with 1.885 parts of water.

[0305] The reactor contents are stirred at 70° C. for another 30 minutes, after which the batch is cooled to 30° C. The pH of the emulsion is adjusted to 7 using 0.6 parts of a 25% solution of ammonia in water or part of it. Simultaneously, 0.623 parts of water are added. The solids content of the emulsion is adjusted to 45% using water.

[0306] The resulting emulsion has a solids content of 45%, and a pH of 7.0.

FURTHER EXAMPLES

Examples 4 to 13

[0307] Further examples for the various embodiments can be prepared according the Common method E below and with

reference to the Table 1 below. The percentages in the tables are mostly quoted to the nearest percentage and/or to 2 significant figures and thus may not total 100% due to rounding errors.

Common Method E (for Sequential Vinyl Polymers)

[0308] The total weight of monomer used in Examples below can be the same as the total amount used to prepare Example 1 and so for convenience the amount of monomers used in these examples can be expressed as a weight percent of the total monomers used in both the first and second monomer feeds. The first monomer feed (used to prepare the low Tg part of the polymer) consists of the same ingredients described in Example 1 (or with consequent modification), other than the monomers which can be: z1% of Monomer Z1, y1% of Monomer Y1, x1% of Monomer X1 and/or w1% of Monomer W1. To the equipment described in Example 1 and the pre-feed described therein the same initial amount of the first monomer feed can be added under the conditions described therein and then the remainder of the first monomer feed can be added and the reaction continued as described in Example 1 (or with consequent modification) until the second monomer feed can be added. The second monomer feed (used to prepare the high Tg part of the polymer) consists of the same ingredients described in Example 1 (or with consequent modification), other than the monomers which can be: z2% of Monomer Z2, y2% of Monomer Y2, x2% of Monomer X2 and/or w2% of Monomer W2.

[0309] The rest of the process can be followed as described in Example 1 (or with consequent modification) with reference to Table 1 to obtain vinyl sequential polymers analogous to that described in Example 1. The relative weight ratio (R) of the respective total amount of low Tg polymer A to the total amount of high Tg polymer B is also given in Table 2 and if necessary the method described in Example 1 can be modified according by adjusting the weight of the total amount of monomers used to prepare polymer B relative to the weight of the total amount of monomers used to prepare polymer A.

[0310] The total amount of monomer of Formula 1 (as a percentage T of the total amount of monomers A+B is also given in Table 1)

Examples 14 to 18 and Comparative Examples
Comp I to V

Example 14

DBI Polymer Containing Wet-Adhesion Promoting Monomer

[0311] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 559.2 parts of demineralized water, 5.5 parts of sodium bicarbonate, 29.4 parts of a 30 wt-% solution of sodium lauryl sulphate in water, and 1.1 parts of sodium persulphate. The reactor contents were heated to 70° C. At 50° C., 10% of a monomer feed consisting of 510.3 parts of demineralized water, 12.5 parts of a 30 wt-% solution of sodium lauryl sulphate in water, 516.7 parts of butyl acrylate, 33.0 parts of methacrylic acid, 494.7 parts of dibutyl itaconate, and 110.0 parts of a 50 wt-% solution of N-(2-methacryloyloxyethyl)ethylene urea in water (Plex 6852-0, ex. Evonik), was added. Due to the exothermic nature of the polymerizing monomers, the temperature increased to 85° C. (if the exotherm would be insufficient the mixture could be heated slightly to reach a temperature of 85° C.). At 85° C., the monomer feed, comprising the remaining 90% of the original feed, and the initiator feed, consisting of 124.5 parts of demineralized water, 4.4 parts of sodium persulphate, and 2.2 parts of a 30 wt-% solution of sodium lauryl sulphate in water, were started. Both feeds were added over a period of 120 minutes. At the end of the monomer feed, the feed tank was rinsed with 19.7 parts of demineralized water and the mixture was stirred at 85° C. for another 35 minutes.

[0312] Next, the emulsion was cooled to 45° C., and a solution of 0.7 parts of iso-ascorbic acid in 12.5 parts of demineralized water was added, followed by 1.0 part of a 70 wt-% solution of t-butyl hydroperoxide in water, 1.5 parts of demineralized water, and 0.3 parts of a 30 wt-% solution of sodium lauryl sulphate in water. The entire reactor contents were stirred for 30 minutes at 45° C.

[0313] The emulsion was cooled to room temperature, and 55.0 parts of an equal mixture of a 25% solution of ammonia

TABLE 1

Examples 4 to 13 - sequential polymers (see method E)																		
Ex	Low Tg polymer A (% of A)				High Tg polymer B (% of B)				R	T % (of								
	z1%	Z1	y1%	Y1	x1%	X1	W1%	W1	z2%	Z2	y2%	Y2	x2%	X2	w2%	W2	(A to B)	A + B)
4	10	MAA	40	MMA	50	DPI	—	—	5	MAA	10	MMA	30	DMI	55	BMA	40/60	20
5	0.1	AA	39.9	MA	60	DHI	—	—	10	MAA	10	MMA	20	DEI	60	BMA	45/55	27
6	0.5	MSA	20	EA	65	DOI	14.5	BA	15	MA	5	EMA	50	DPrI	30	OA	50/50	23.5
7	1	CEA	36	PA	30	DBI	33	MA	60	DBzI	30	BA	10	DEI	—	—	55/45	43.5
8	2	MBI	80	MMA	18	EMA	—	—	85	DPhI	10	EMA	5	DMI	—	—	60/40	34
9	4	IA	22	BA	74	DBI	—	—	90	DHI	10	URED	—	—	—	—	65/35	79.6
10	6	IAn	20	MMA	64	DBI	10	EA	5	MAA	10	BA	65	DMI	20	BA	70/30	44.8
11	7.5	MMaIA	40	EMA	52.5	BPI	—	—	10	AA	40	EHA	10	DEI	40	BMA	75/25	39.4
12	8	PHEMA	30	MMA	42	BHI	20	EA	1	MMA	49	OA	50	DMI	—	—	80/20	33.6
13	3	AMPS	35	PA	62	HOI	—	—	2	MSA	30	DBI	30	DEI	38	EA	90/10	58.8

in water and demineralized water were added. The solids content of the emulsion was adjusted to 45% using demineralized water.

Example 15

DBI and Styrene Containing Polymer

[0314] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 644.0 parts of demineralized water, 0.5 parts of sodium bicarbonate, 13.3 parts of a 30 wt-% solution of sodium lauryl sulphate in water, and 0.8 parts of sodium persulphate. The reactor contents were heated to 80° C. and stirred for 5 minutes at 80° C. Next, 10% of a monomer feed, consisting of 132.9 parts of demineralized water, 13.0 parts of a 30 wt-% solution of sodium lauryl sulphate in water, 23.3 parts of methacrylic acid, 280.1 parts of dibutyl itaconate, and 280.1 parts of styrene, was added, after the temperature rose to approximately 90° C. due to the exothermic nature of the polymerization. As soon as the temperature of 90° C. was reached, the remaining monomer feed and the initiator feed, consisting of 58.7 parts of demineralized water, 2.5 parts of sodium persulphate, and 3.7 parts of a 30 wt-% solution of sodium lauryl sulphate in water, were started. Both feeds were added over a period of 2 hours. At the end of the monomer feed the feed tank was rinsed with 10.4 parts of demineralized water. The temperature of the reactor contents were cooled to 80° C., after which a solution of 1.8 parts of iso-ascorbic acid dissolved in 26.5 parts of demineralized water (which was brought to a pH of 8.5 using an ammonia solution) was fed over a period of 30 minutes, during which a mixture of 2.8 parts of t-butyl hydroperoxide and 5.6 parts of demineralized water was added in two shots; one at the start of the iso-ascorbic acid feed and 15 minutes later.

[0315] At the end of the feed, the mixture was stirred at 80° C. for 30 minutes, and the pH was raised to 7.2 using a 25 wt-% solution of ammonia in water. After stirring for another 30 minutes, the batch was cooled to room temperature. The solids content was adjusted to 40% using demineralized water.

Comparative Example Comp I

BA and Styrene Containing Polymer

[0316] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 639.5 parts of demineralized water, 0.5 parts of sodium bicarbonate, and 13.3 parts of a 30 wt-% solution of sodium lauryl sulphate in water. The reactor contents were heated to 80° C., after which a solution of 0.8 parts of sodium persulphate in 4.5 parts of demineralized water were added and stirred for 5 minutes at 80° C. Next, 10% of a monomer feed, consisting of 132.9 parts of demineralized water, 13.0 parts of a 30 wt-% solution of sodium lauryl sulphate in water, 23.3 parts of methacrylic acid, 280.1 parts of butyl acrylate, and 280.1 parts of styrene, was added, after the temperature rose to approximately 90° C. due to the exothermic nature of the polymerization. As soon as the temperature of 90° C. was reached, the remaining monomer feed and the initiator feed, consisting of 58.7 parts of demineralized water, 2.5 parts of sodium persulphate, and 3.7 parts of a 30 wt-% solution of sodium lauryl sulphate in water, were started. Both feeds were added over a period of 2 hours. At the end of the monomer feed the feed tank was rinsed with 10.4 parts of demineralized water. The temperature of the reactor contents were cooled to 80° C., after which a solution of 1.8 parts of iso-ascorbic acid dissolved in 26.5 parts of demineralized water (which was brought to a pH of 8.5 using an ammonia solution) was fed over a period of 30 minutes, during which a mixture of 2.8 parts of t-butyl hydroperoxide and 5.6 parts of demineralized water was added in two shots; one at the start of the iso-ascorbic acid feed and 15 minutes later.

[0317] At the end of the feed, the mixture was stirred at 80° C. for 30 minutes, and the pH was raised to 7.2 using a 25 wt-% solution of ammonia in water. After stirring for another 30 minutes, the batch was cooled to room temperature. The solids content was adjusted to 40% using demineralized water.

Example 16

DBI and MMA Containing Polymer

[0318] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 639.5 parts of demineralized water, 0.5 parts of sodium bicarbonate, and 13.3 parts of a 30 wt-% solution of sodium lauryl sulphate in water. The reactor contents were heated to 80° C., after which a solution of 0.8 parts of sodium persulphate in 4.5 parts of demineralized water were added and stirred for 5 minutes at 80° C. Next, 10% of a monomer feed, consisting of 132.9 parts of demineralized water, 13.0 parts of a 30 wt-% solution of sodium lauryl sulphate in water, 23.3 parts of methacrylic acid, 280.1 parts of dibutyl itaconate, and 280.1 parts of methyl methacrylate, was added, after the temperature rose to approximately 90° C. due to the exothermic nature of the polymerization. As soon as the temperature of 90° C. was reached, the remaining monomer feed and the initiator feed, consisting of 58.7 parts of demineralized water, 2.5 parts of sodium persulphate, and 3.7 parts of a 30 wt-% solution of sodium lauryl sulphate in water, were started. Both feeds were added over a period of 2 hours. At the end of the monomer feed the feed tank was rinsed with 10.4 parts of demineralized water. The temperature of the reactor contents were cooled to 80° C., after which a solution of 1.8 parts of iso-ascorbic acid dissolved in 26.5 parts of demineralized water (which was brought to a pH of 8.5 using an ammonia solution) was fed over a period of 30 minutes, during which a mixture of 2.8 parts of t-butyl hydroperoxide and 5.6 parts of demineralized water was added in two shots; one at the start of the iso-ascorbic acid feed and 15 minutes later.

[0319] At the end of the feed, the mixture was stirred at 80° C. for 30 minutes, and the pH was raised to 7.2 using a 25 wt-% solution of ammonia in water. After stirring for another 30 minutes, the batch was cooled to room temperature. The solids content was adjusted to 40% using demineralized water.

Comparative Example Comp II

BA and MMA Containing Polymer

[0320] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 639.5 parts of demineralized water, 0.5 parts of sodium bicarbonate, and 13.3 parts of a 30 wt-% solution of sodium lauryl sulphate in water. The reactor contents were heated to 80° C., after which a solution of 0.8 parts of sodium persulphate in 4.5 parts of demineralized water were added and stirred for 5 minutes at 80° C. Next, 10% of a monomer feed, consisting of 132.9

parts of demineralized water, 13.0 parts of a 30 wt-% solution of sodium lauryl sulphate in water, 23.3 parts of methacrylic acid, 280.1 parts of butyl acrylate, and 280.1 parts of methyl methacrylate, was added, after the temperature rose to approximately 90° C. due to the exothermic nature of the polymerization. As soon as the temperature of 90° C. was reached, the remaining monomer feed and the initiator feed, consisting of 58.7 parts of demineralized water, 2.5 parts of sodium persulphate, and 3.7 parts of a 30 wt-% solution of sodium lauryl sulphate in water, were started. Both feeds were added over a period of 2 hours. At the end of the monomer feed the feed tank was rinsed with 10.4 parts of demineralized water. The temperature of the reactor contents were cooled to 80° C., after which a solution of 1.8 parts of iso-ascorbic acid dissolved in 26.5 parts of demineralized water (which was brought to a pH of 8.5 using an ammonia solution) was fed over a period of 30 minutes, during which a mixture of 2.8 parts of t-butyl hydroperoxide and 5.6 parts of demineralized water was added in two shots; one at the start of the iso-ascorbic acid feed and 15 minutes later.

[0321] At the end of the feed, the mixture was stirred at 80° C. for 30 minutes, and the pH was raised to 7.2 using a 25 wt-% solution of ammonia in water. After stirring for another 30 minutes, the batch was cooled to room temperature. The solids content was adjusted to 40% using demineralized water.

Comparative Example Comp III

DMI Containing Copolymer

[0322] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 639.5 parts of demineralized water, 0.5 parts of sodium bicarbonate, and 13.3 parts of a 30 wt-% solution of sodium lauryl sulphate in water. The reactor contents were heated to 80° C., after which a solution of 0.8 parts of sodium persulphate in 4.5 parts of demineralized water were added and stirred for 5 minutes at 80° C. Next, 10% of a monomer feed, consisting of 132.9 parts of demineralized water, 13.0 parts of a 30 wt-% solution of sodium lauryl sulphate in water, 23.3 parts of methacrylic acid, 414.3 parts of dimethyl itaconate, and 145.9 parts of ethyl acrylate, was added, after the temperature rose to approximately 90° C. due to the exothermic nature of the polymerization. As soon as the temperature of 90° C. was reached, the remaining monomer feed and the initiator feed, consisting of 58.7 parts of demineralized water, 2.5 parts of sodium persulphate, and 3.7 parts of a 30 wt-% solution of sodium lauryl sulphate in water, were started. Both feeds should be added over a period of 2 hours.

[0323] After 110 minutes of the monomer feed, the emulsion gelled, showing that higher itaconates, such as DBI, yield superior properties over lower itaconates, such as DMI.

Example 17

DBI Containing h/s Sequential Copolymer

[0324] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 426.6 parts of demineralized water, 0.4 parts of sodium bicarbonate, 31.3 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), and 0.4 parts of a 25 wt-% ammonia solution. The reactor contents were heated to 80° C., after which a solution of 0.4 parts of sodium persulphate in 7.9 parts of demineralized water were added,

followed by 10% of a first monomer feed consisting of 115.1 parts of demineralized water, 35.9 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), 0.6 parts of sodium bicarbonate, 15.7 parts of acrylic acid, 90.1 parts of dibutyl itaconate, and 286.0 parts of methyl methacrylate. Due to the heat formed as a result of the polymerizing monomers, the temperature rose to 90° C., after which adding the remainder of the first monomer feed was started. The first monomer feed was added over a period of 45 minutes. Simultaneously, 60% of an initiator feed, consisting of 36.3 parts of demineralized water, 0.2 parts of sodium bicarbonate, and 2.0 parts of sodium persulphate, was fed over a period of 45 minutes. At the end of the monomer feed, the feed tank was rinsed with 7.6 parts of demineralized water.

[0325] Next, a mixture of 0.9 parts of a 25 wt-% ammonia solution and 1.2 parts of demineralized water was fed over a period of 15 minutes. 45 minutes after the end of the first monomer feed, a second monomer feed, consisting of 76.7 parts of demineralized water, 23.9 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), 0.4 parts of sodium bicarbonate, 10.5 parts of acrylic acid, 198.5 parts of dibutyl itaconate, and 52.2 parts of butyl acrylate, was started. This feed, and the remainder of the initiator feed that was fed simultaneously, were added over a period of 30 minutes. After completion of the second monomer feed, the feed tank was rinsed with 15.3 parts of demineralized water and the mixture was allowed to stir at 90° C. for another 30 minutes.

[0326] Finally, the emulsion was cooled to room temperature, the solids content was corrected to 45% using demineralized water, and the pH was corrected to 7.5 using a 25 wt-% ammonia solution.

Comparative Example Comp IV

DBI Free h/s Sequential Copolymer

[0327] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 426.6 parts of demineralized water, 0.4 parts of sodium bicarbonate, 31.3 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), and 0.4 parts of a 25 wt-% ammonia solution. The reactor contents were heated to 80° C., after which a solution of 0.4 parts of sodium persulphate in 7.9 parts of demineralized water were added, followed by 10% of a first monomer feed consisting of 115.1 parts of demineralized water, 35.9 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), 0.6 parts of sodium bicarbonate, 15.7 parts of acrylic acid, 90.1 parts of butyl acrylate, and 286.0 parts of methyl methacrylate. Due to the heat formed as a result of the polymerizing monomers, the temperature rose to 90° C., after which adding the remainder of the first monomer feed was started. The first monomer feed was added over a period of 45 minutes. Simultaneously, 60% of an initiator feed, consisting of 36.3 parts of demineralized water, 0.2 parts of sodium bicarbonate, and 2.0 parts of sodium persulphate, was fed over a period of 45 minutes. At the end of the monomer feed, the feed tank was rinsed with 7.6 parts of demineralized water.

[0328] Next, a mixture of 0.9 parts of a 25 wt-% ammonia solution and 1.2 parts of demineralized water was fed over a period of 15 minutes. 45 minutes after the end of the first monomer feed, a second monomer feed, consisting of 76.7

parts of demineralized water, 23.9 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), 0.4 parts of sodium bicarbonate, 10.5 parts of acrylic acid, and 250.7 parts of butyl acrylate, was started. This feed, and the remainder of the initiator feed that was fed simultaneously, were added over a period of 30 minutes. After completion of the second monomer feed, the feed tank was rinsed with 15.3 parts of demineralized water and the mixture was allowed to stir at 90° C. for another 30 minutes.

[0329] Finally, the emulsion was cooled to room temperature, the solids content was corrected to 45% using demineralized water, and the pH was corrected to 7.5 using a 25 wt-% ammonia solution.

Example 18

DBI Containing s/h Sequential

[0330] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 426.6 parts of demineralized water, 0.4 parts of sodium bicarbonate, 31.3 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), and 0.4 parts of a 25 wt-% ammonia solution. The reactor contents were heated to 80° C., after which a solution of 0.4 parts of sodium persulphate in 7.9 parts of demineralized water were added, followed by 10% of a first monomer feed consisting of 114.3 parts of demineralized water, 37.9 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), 0.6 parts of sodium bicarbonate, 18.3 parts of acrylic acid, 420.6 parts of dibutyl itaconate, 18.3 parts of a 50 wt-% solution of N-(2-methacryloyloxyethyl)ethylene urea in water (Plex 6852-0 ex. Evonik), and 9.1 parts of methyl methacrylate. Due to the heat formed as a result of the polymerizing monomers, the temperature rose to 90° C., after which adding the remainder of the first monomer feed was started. The first monomer feed was added over a period of 45 minutes. Simultaneously, 60% of an initiator feed, consisting of 36.3 parts of demineralized water, 0.2 parts of sodium bicarbonate, and 2.0 parts of sodium persulphate, was fed over a period of 45 minutes. At the end of the monomer feed, the feed tank was rinsed with 7.6 parts of demineralized water. Next, a mixture of 0.9 parts of a 25 wt-% ammonia solution and 1.2 parts of demineralized water was fed over a period of 15 minutes.

[0331] Next, a mixture of 0.9 parts of a 25 wt-% ammonia solution and 1.2 parts of demineralized water was fed over a period of 15 minutes. 45 minutes after the end of the first monomer feed, a second monomer feed, consisting of 77.5 parts of demineralized water, 21.9 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), 0.4 parts of sodium bicarbonate, 7.8 parts of acrylic acid, 45.0 parts of dibutyl itaconate, and 143.0 parts of methyl methacrylate, was started. This feed, and the remainder of the initiator feed that was fed simultaneously, were added over a period of 30 minutes. After completion of the second monomer feed, the feed tank was rinsed with 15.3 parts of demineralized water and the mixture was allowed to stir at 90° C. for another 30 minutes.

[0332] Finally, the emulsion was cooled to room temperature, the solids content was corrected to 45% using demineralized water, and the pH was corrected to 7.5 using a 25 wt-% ammonia solution.

Comparative Example Comp V

DBI Free s/h Sequential

[0333] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer were charged 426.6 parts of demineralized water, 0.4 parts of sodium bicarbonate, 31.3 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), and 0.4 parts of a 25 wt-% ammonia solution. The reactor contents were heated to 80° C., after which a solution of 0.4 parts of sodium persulphate in 7.9 parts of demineralized water were added, followed by 10% of a first monomer feed consisting of 114.3 parts of demineralized water, 37.9 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), 0.6 parts of sodium bicarbonate, 18.3 parts of acrylic acid, 420.6 parts of butyl acrylate, 18.3 parts of a 50 wt-% solution of N-(2-methacryloyloxyethyl)ethylene urea in water (Plex 6852-0 ex. Evonik), and 9.1 parts of methyl methacrylate. Due to the heat formed as a result of the polymerizing monomers, the temperature rose to 90° C., after which adding the remainder of the first monomer feed was started. The first monomer feed was added over a period of 45 minutes. Simultaneously, 60% of an initiator feed, consisting of 36.3 parts of demineralized water, 0.2 parts of sodium bicarbonate, and 2.0 parts of sodium persulphate, was fed over a period of 45 minutes. At the end of the monomer feed, the feed tank was rinsed with 7.6 parts of demineralized water. Next, a mixture of 0.9 parts of a 25 wt-% ammonia solution and 1.2 parts of demineralized water was fed over a period of 15 minutes.

[0334] 45 minutes after the end of the first monomer feed, a second monomer feed, consisting of 77.5 parts of demineralized water, 21.9 parts of a 20 wt-% aqueous solution of a phosphate functional surfactant (Fosfodet FAZ109V, ex. KAO), 0.4 parts of sodium bicarbonate, 7.8 parts of acrylic acid, 45.0 parts of butyl acrylate, and 143.0 parts of methyl methacrylate, was started. This feed, and the remainder of the initiator feed that was fed simultaneously, were added over a period of 30 minutes. After completion of the second monomer feed, the feed tank was rinsed with 15.3 parts of demineralized water and the mixture was allowed to stir at 90° C. for another 30 minutes.

[0335] Finally, the emulsion was cooled to room temperature, the solids content was corrected to 45% using demineralized water, and the pH was corrected to 7.5 using a 25 wt-% ammonia solution.

[0336] To illustrate the invention, film properties were determined for a selection of the polymer emulsions described above. The polymer emulsions were formulated with 8% of butyl diglycol to make them film forming. The films were cast, dried at ambient temperature for 4 hours, and next dried for 34 hours at 50° C. The results are shown below in Table 4.

TABLE 4

Film properties; "S" means excellent resistance properties, no damage to the film, "1" indicated completely destroyed film							
	Water spot test		Stain resistance			König	
	16 hrs	Blocking	(16 hrs)*			hardness	
	1 hr	hrs	resistance	EtOH	Andy	Coffee	(s)
Ex 15	5	5	3	5	4	5	201
Comp I	5	4	1	4	2	5	110
Ex 16	5	5	5	4	4	5	173
Comp II	5	3	3	3	2	4	115
Comp III	Could not be prepared due to instable processing.						
Ex 17	5	5	5	3	4	5	70
Comp IV	5	5	3	3	2	4	60
Ex 18	5	5	4	3	3	5	115
Comp V	5	5	0	3	2	4	8

*Determined as spot test.

[0337] In all cases (except Comp III), the water spot was good. Blocking resistance and König hardness were in all cases better for the polymers according to the invention compared to their most similar comparative examples. While resistance to coffee and ethanol were comparable between polymers according to the invention and the comparatives, the resistance to soap (Andy) was clearly better for the polymers according to the invention.

Example 19

MMA/DMI/AA

[0338] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer are charged 394.0 parts of 2-butanone. The reactor contents are heated to 80° C. As soon as the polymerization temperature is reached, 13.3 parts of azobis(2-methyl butyronitrile) are added and the monomer feed and catalyst feed are started. The monomer feed consists of 244.4 parts of methyl methacrylate, 244.4 parts of dimethyl itaconate, and 244.4 parts of acrylic acid. The catalyst feed consists of 31.1 parts of azobis(2-methyl butyronitrile) dissolved in 125.9 parts of 2-butanone. Both feeds are added over a period of 180 minutes.

[0339] At the end of the feeds 2.5 parts of azobis(2-methyl butyronitrile) are added and the mixture is stirred at 80° C. for another 150 minutes. The mixture is cooled to room temperature.

[0340] To 615.8 parts of the polymer solution is added a mixture of 99.6 parts of a 25 wt-% of ammonia in water, and 1080.5 parts of water. Next, the 2-butanone is removed at 50° C. under reduced pressure. The solids content is corrected to 22.5% using demineralized water and the pH is corrected to 8.6-8.8 using a 25 wt-% solution of ammonia in water.

[0341] The final polymer solution has a solids content of 22.5% and a pH of 8.7.

Example 20

S/DMI/AA

[0342] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer are charged 394.0 parts of 2-butanone. The reactor contents are heated to 80° C. As soon as the polymerization temperature is reached, 13.3 parts of azobis(2-methyl butyronitrile) are added and the monomer

feed and catalyst feed are started. The monomer feed consists of 244.4 parts of styrene, 244.4 parts of dimethyl itaconate, and 244.4 parts of acrylic acid. The catalyst feed consists of 31.1 parts of azobis(2-methyl butyronitrile) dissolved in 125.9 parts of 2-butanone. Both feeds are added over a period of 180 minutes.

[0343] At the end of the feeds 2.5 parts of azobis(2-methyl butyronitrile) are added and the mixture is stirred at 80° C. for another 150 minutes. The mixture is cooled to room temperature.

[0344] To 546.1 parts of polymer solution is added a mixture of 105.4 parts of a 25 wt-% of ammonia in water, and 1144.1 parts of water. Next, the 2-butanone is removed at 50° C. under reduced pressure. The solids content is corrected to 22.5% using demineralized water and the pH is corrected to 8.6-8.8 using a 25 wt-% solution of ammonia in water.

[0345] The final polymer solution has a solids content of 22.4% and a pH of 8.6.

Example 21

MMA/DMI/AA

[0346] To a high pressure reactor equipped with a thermometer, and a stirrer are charged 500.0 parts of 2-butanone. The reactor contents are heated to 140° C. As soon as the polymerization temperature is reached, 2.9 parts of di-t-butyl peroxide and 40 parts of 2-butanone are added. 5 minutes later the monomer feed is started. The monomer feed consists of 331.8 parts of methyl methacrylate, 331.8 parts of dimethyl itaconate, 331.8 parts of acrylic acid, 5.7 parts of di-t-butyl peroxide, and 6.6 parts of t-butyl perbenzoate, and is added over a period of 180 minutes at 140° C.

[0347] At the end of the feed the feed tank is rinsed with 90.9 parts of 2-butanone. 45 minutes after completion of the monomer feed 2.5 parts of t-butyl perbenzoate dissolved in 40 parts of 2-butanone are added and the mixture is stirred at 140° C. for another 45 minutes. Next, 2.5 parts of t-butyl perbenzoate dissolved in 40 parts of 2-butanone are added and the mixture is stirred for another 135 minutes at 140° C.

[0348] The mixture is cooled to room temperature.

[0349] To 619.3 parts of the polymer solution is added a mixture of 99.3 parts of a 25 wt-% of ammonia in water, and 1077.3 parts of water. Next, the 2-butanone is removed at 50° C. under reduced pressure. The solids content is corrected to 22.5% using demineralized water and the pH is corrected to 8.6-8.8 using a 25 wt-% solution of ammonia in water.

[0350] The final polymer solution has a solids content of 22.5% and a pH of 8.6.

Example 22

S/DMI/AA

[0351] To a high pressure reactor equipped with a thermometer, and a stirrer are charged 500.0 parts of 2-butanone. The reactor contents are heated to 140° C. As soon as the polymerization temperature is reached, 4.4 parts of di-t-butyl peroxide and 40 parts of 2-butanone are added. 5 minutes later the monomer feed is started. The monomer feed consists of 331.8 parts of styrene, 331.8 parts of dimethyl itaconate, 331.8 parts of acrylic acid, 8.6 parts of di-t-butyl peroxide, and 10.0 parts of t-butyl perbenzoate, and is added over a period of 180 minutes at 140° C.

[0352] At the end of the feed the feed tank is rinsed with 90.9 parts of 2-butanone. 45 minutes after completion of the

monomer feed 2.5 parts of t-butyl perbenzoate dissolved in 40 parts of 2-butanone are added and the mixture is stirred at 140° C. for another 45 minutes. Next, 2.5 parts of t-butyl perbenzoate dissolved in 40 parts of 2-butanone are added and the mixture is stirred for another 135 minutes at 140° C.

[0353] The mixture is cooled to room temperature.

[0354] To 617.8 parts of the polymer solution is added a mixture of 99.4 parts of a 25 wt-% of ammonia in water, and 1078.6 parts of water. Next, the 2-butanone is removed at 50° C. under reduced pressure. The solids content is corrected to 22.5% using demineralized water and the pH is corrected to 8.6-8.8 using a 25 wt-% solution of ammonia in water.

[0355] The final polymer solution has a solids content of 22.5% and a pH of 8.7.

Example 23

Sequential Polymerization Using the Polymer from Example 44

[0356] To a round-bottomed flask equipped with a condenser, thermometer, and a stirrer are charged 128.9 parts of the alkaline solution obtained from Example 44. The mixture is heated to 80° C.±2° C.

[0357] As soon as the reaction temperature is reached, a mixture of 0.2 parts of sodium persulphate and 0.4 parts of demineralized water is added. After 5 minutes, the monomer feed, consisting of 43.8 parts of methyl methacrylate and 43.8 parts of butyl acrylate, and the initiator feed, consisting of 10.8 parts of demineralized water and 0.4 parts of sodium persulphate (corrected to a pH of 8 using a 25 wt-% ammonia solution) are started. Both feeds should take 120 minutes. At the end of the monomer feed, the feed tank is rinsed with 1.2 parts of water. After both feeds are completed, the batch is stirred at 80° C. for another 30 minutes, after which it is cooled to 50° C.

[0358] At 50° C., one third of a mixture consisting of 0.1 part of a 70 wt-% solution of t-butyl hydroperoxide is added followed by one third of a solution of 0.1 part of iso-ascorbic acid in 2.9 parts of water. 15 minutes later and 30 minutes later similar portions are added and the batch is stirred at 50° C. for another 15 minutes.

[0359] The pH is checked and, if necessary, adjusted to 8.4±0.1 using a 25 wt-% solution of ammonia in water. The batch is cooled to room temperature, after which the solids content is adjusted to 48.5%±1% using demineralized water.

Example 24

Sequential Polymerization Using the Polymer from Example 20

[0360] Example 24 was prepared analogously to the method described in Example 23, replacing Example 19 with the alkaline solution obtained from Example 20. The final emulsion obtained was highly viscous, requiring a dilution to a solids content of 35%.

Example 25

Sequential Polymerization Using the Polymer from Example 21

[0361] Example 25 was prepared analogously to the method described in Example 23, replacing Example 19 with the alkaline solution obtained from Example 21.

Example 26

Sequential Polymerization Using the Polymer from Example 22

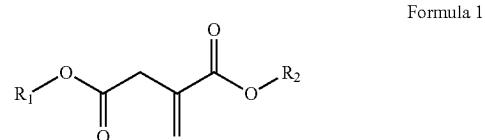
[0362] Example 26 was prepared analogously to the method described in Example 23, replacing Example 19 with the alkaline solution obtained from Example 22.

TABLE 5

Results			
	SC (%)	Viscosity (mPa · s)	pH
Example 23	47.6	208	8.4
Example 24	34.8	1006	8.4
Example 25	48.1	35	8.5
Example 26	48.1	201	8.4

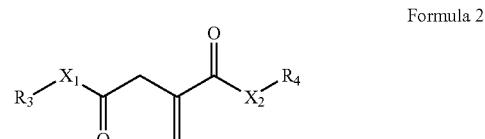
1. A vinyl sequential copolymer [optionally substantially free of styrene] (<1.5 wt-% of copolymer)] the copolymer composition comprising:

(a) at least 23% by weight of at least one monomer represented by Formula 1



where both R₁ and R₂ independently represent an optionally substituted hydrocarbo moiety having from 4 to 10 carbon atoms.

(b) optionally at least one hydrophilic monomer also in an amount sufficient that the resultant polymer has an acid value less than 150 mg KOH per g of polymer,
(c) optionally of one or more monomers represented by Formula 2



where R₃ and R₄ independently represent H or an optionally substituted hydrocarbo moiety having from 1 to 20 carbon atoms

X₁ and X₂ independently represents O or NR₅ where R₅ denotes H or an optionally substituted hydrocarbo moiety having from 1 to 20 carbon atoms with the proviso that when X₁ and/or X₂ are 0 then the respective R₃ and/or R₄ attached to the oxy group independently represent an optionally substituted hydrocarbo having from 1 to 3 carbon atoms

(d) optionally less than 77% by weight of monomers other than components (a), (b) or (c).

where the percentages or amounts of (a), (b) (c) (d) are by weight calculated as a proportion of the total weight of (a)+(b)+(c)+(d) and thus total 100%; where independently at least one of the components(a), (b) (c) and/or (d) and/or the copolymer obtained from them are biorenewable defined as comprising an amount of carbon-14 sufficient to produce a decay of at least about 1.5 dpm/gC (disintegrations per minute per gram carbon).

2. A copolymer as claimed in claim 1, in which

- (a) component (a) is from 24% to 70% by weight of one or more monomers represented by Formula 1
- (b) component (b) is one or more acid functional monomer (s) in an amount from 0.5% to 15% by weight, in an amount also sufficient that the resultant polymer has an acid value of from 3 to 100 mg KOH per g of polymer,
- (c) component (c) is from 0.01% to 10% by weight of one or more monomers represented by Formula 2 in which X_1 and X_2 are both O and R_3 and/or R_4 independently represent an optionally substituted hydrocarbo having from 1 to 3 carbon atoms.
- (d) component (d) if present is less than 75% wt-% by weight of monomer(s) other than components (a), (b) or (c) and does not contain styrene, butyl acrylate, 2-ethyl hexyl acrylate and/or mixtures thereof;

where the weight percentages or amounts of (a), (b) (c) (d) are calculated as a proportion of the total amount of (a)+(b)+(c)+(d) which thus totals 100%; with the provisos that

where the copolymer is prepared by an emulsion polymerisation a chaser monomer is not used;

the copolymer is not prepared in the presence of a seed polymer comprising a poly(itaconate ester);

the copolymer is not prepared in the presence of an initiator system comprising an organoborane amine complex.

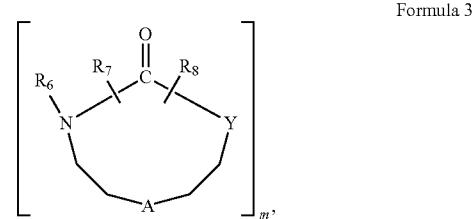
3. A copolymer as claimed in claim 1, in which component

- (a) comprises dibutyl itaconate;
- 4. A copolymer as claimed in claim 1, in which:**
- (a) component (a) is present in an amount of from 30 to 65 wt-% and is dibutyl itaconate;
- (b) optional component (b) if present is present in an amount of up to 10 wt-% and comprises an acid functional ethylenically unsaturated monomer and/or anhydride thereof;
- (c) optional component (c) if present is present in an amount of from 1 to 25 wt-% and is dimethyl itaconate and/or diethyl itaconate;
- (d) optional component (d) if present is present in an amount such that (a) and (d) [and (b) and (c) where present] total 100% by weight.

5. A copolymer as claimed in claim 1 in which: component

- (d)

comprises at least one polymer precursor(s) of Formula 3



where Y denotes an electronegative group, R₆ is H, OH or an optionally hydroxy substituted C₁₋₁₀hydrocarbo

R₇ is H or a C₁₋₁₀hydrocarbo;

R₈ is a C₁₋₁₀hydrocarbo group substituted by at least one activated unsaturated moiety; and; either:

A represents a divalent organo moiety attached to both the —HN— and —Y— moieties so the —A—, —NH—, —C(=O)— and —Y— moieties together represent a ring of 4 to 8 ring atoms, and R₇ and R₈ are attached to any suitable point on the ring; or

A is not present (and Formula 3 represents a linear and/or branched moiety that does not comprise a heterocyclic ring) in which case R₇ and R₈ are attached to R₆; and m is an integer from 1 to 4.

6. A process for preparing a copolymer as claimed in claim 1 and/or the process comprising the step of polymerising polymer precursors in a sequential polymerisation method the polymer precursors comprising component (a), component (b) and optionally components (c) and/or component (d) to obtain a sequential copolymer,

where optionally the polymerisation method is selected from aqueous emulsion polymerisation and suspension polymerisation and where the method does not comprise a chaser monomer step.

7. A copolymer obtained and/or obtainable by a process according to claim 6.

8. A coating composition comprising a copolymer as claimed in claim 1.

9. A substrate and/or article having coated thereon an (optionally cured) coating composition of claim 8.

10. A method of using a copolymer as claimed in claim 1 to prepare a coating composition.

11. A method for preparing a coated substrate and/or article comprising the steps of applying a coating composition of claim 8 to the substrate and/or article and optionally curing said composition in situ to form a cured coating thereon.

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