

**PCT**WORLD INTELLECTUAL PROPERTY ORGANIZATION  
International Bureau

## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

<b>(51) International Patent Classification 7 :</b> <b>C08F 4/651, 4/654, 10/00, C07C 69/38</b>		<b>A1</b>	<b>(11) International Publication Number:</b> <b>WO 00/26259</b> <b>(43) International Publication Date:</b> 11 May 2000 (11.05.00)
<b>(21) International Application Number:</b> PCT/EP99/08018			<b>(81) Designated States:</b> AU, BR, CA, CN, HU, IL, IN, JP, KR, MX, RU, SG, US, ZA, European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).
<b>(22) International Filing Date:</b> 22 October 1999 (22.10.99)			
<b>(30) Priority Data:</b> 98203733.5 4 November 1998 (04.11.98) EP			<b>Published</b> <i>With international search report.</i>
<b>(71) Applicant (for all designated States except US):</b> MONTELL TECHNOLOGY COMPANY BV [NL/NL]; Hoeksteen 66, NL-2132 MS Hoofddorp (NL).			
<b>(72) Inventors; and</b>			
<b>(75) Inventors/Applicants (for US only):</b> MORINI, Giampiero [IT/IT]; Via Giotto, 36, I-35100 Padova (IT). BALBON-TIN, Giulio [IT/IT]; Via Ugo Bassi, 17A, I-44100 Ferrara (IT). GULEVICH, Yuri, V. [RU/US]; Apartment H, 103 Deerfield Road, Elkton, MD 21921 (US).			
<b>(74) Agents:</b> ZANOLI, Enrico et al.; Montell Italia S.p.A., Intellectual Property, Patents and Trademarks, P.le G. Donegani 12, I-44100 Ferrara (IT).			
<b>(54) Title:</b> COMPONENTS AND CATALYSTS FOR THE POLYMERIZATION OF OLEFINS			
<b>(57) Abstract</b>			
The present invention relates to catalyst components for the polymerization of olefins, and to the catalyst obtained therefrom, particularly suitable for the stereospecific polymerization of olefins, comprising Ti, Mg, halogen and an electron donor compound selected from heteroatom containing esters of malonic acids (heteroatom containing malonates). Said catalyst components when used in the polymerization of olefins, and in particular of propylene, are capable to give polymers in high yields and with high isotactic index expressed in terms of high xylene insolubility.			

**FOR THE PURPOSES OF INFORMATION ONLY**

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AL	Albania	ES	Spain	LS	Lesotho	SI	Slovenia
AM	Armenia	FI	Finland	LT	Lithuania	SK	Slovakia
AT	Austria	FR	France	LU	Luxembourg	SN	Senegal
AU	Australia	GA	Gabon	LV	Latvia	SZ	Swaziland
AZ	Azerbaijan	GB	United Kingdom	MC	Monaco	TD	Chad
BA	Bosnia and Herzegovina	GE	Georgia	MD	Republic of Moldova	TG	Togo
BB	Barbados	GH	Ghana	MG	Madagascar	TJ	Tajikistan
BE	Belgium	GN	Guinea	MK	The former Yugoslav Republic of Macedonia	TM	Turkmenistan
BF	Burkina Faso	GR	Greece	ML	Mali	TR	Turkey
BG	Bulgaria	HU	Hungary	MN	Mongolia	TT	Trinidad and Tobago
BJ	Benin	IE	Ireland	MR	Mauritania	UA	Ukraine
BR	Brazil	IL	Israel	MW	Malawi	UG	Uganda
BY	Belarus	IS	Iceland	MX	Mexico	US	United States of America
CA	Canada	IT	Italy	NE	Niger	UZ	Uzbekistan
CF	Central African Republic	JP	Japan	NL	Netherlands	VN	Viet Nam
CG	Congo	KE	Kenya	NO	Norway	YU	Yugoslavia
CH	Switzerland	KG	Kyrgyzstan	NZ	New Zealand	ZW	Zimbabwe
CI	Côte d'Ivoire	KP	Democratic People's Republic of Korea	PL	Poland		
CM	Cameroon	KR	Republic of Korea	PT	Portugal		
CN	China	KZ	Kazakhstan	RO	Romania		
CU	Cuba	LC	Saint Lucia	RU	Russian Federation		
CZ	Czech Republic	LI	Liechtenstein	SD	Sudan		
DE	Germany	LK	Sri Lanka	SE	Sweden		
DK	Denmark	LR	Liberia	SG	Singapore		
EE	Estonia						

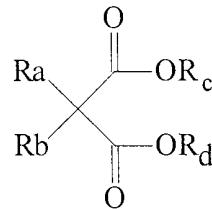
**"Components and catalysts for the polymerization of olefins"**

The present invention relates to catalyst components for the polymerization of olefins, to the catalysts obtained therefrom and to the use of said catalysts in the polymerization of olefins  $\text{CH}_2=\text{CHR}$  in which R is hydrogen or a hydrocarbyl radical with 1-12 carbon atoms. In particular the present invention relates to catalyst components, suitable for the stereospecific polymerization of olefins, comprising Ti, Mg, halogen and an electron donor compound selected from heteroatom containing esters of malonic acids (heteroatom containing malonates). Said catalyst components when used in the polymerization of olefins, and in particular of propylene, are capable to give polymers in high yields and with high isotactic index expressed in terms of high xylene insolubility.

The use of some esters of malonic acid as internal electron donors in catalysts for the polymerization of propylene is already known in the art.

In EP-A-45977 is disclosed the use of an ester of malonic acid (diethyl 2,2-diisobutylmalonate) as internal donor of a catalyst for the polymerization of olefins. EP-A-86473 discloses a catalyst for the polymerization of olefins comprising (a) an Al-alkyl compound, (b) an electron donor compound having certain reactivity features towards  $\text{MgCl}_2$  and (c) a solid catalyst component comprising, supported on  $\text{MgCl}_2$ , a Ti halide and an electron donor selected from many classes of ester compounds including malonates. None of the above-cited applications discloses malonates containing heteroatoms. The same applies to EP-A-86644 that discloses the use of diethyl 2-n-butyl malonate and diethyl 2-isopropylmalonate as internal donors in Mg-supported catalysts for the polymerization of propylene.

It is apparent from the analysis of the polymerization results reported in the above-mentioned applications that a common drawback experienced in the use of the mentioned malonates was represented by a still unsatisfactory polymerization yield and/or a not suitable isotactic index of the final polymer. This is confirmed also by the disclosure of JP-08157521. This application relates to a process for preparing a solid catalyst component for polymerization of olefins which is characterized by contacting a solid catalyst component produced by the reaction among a magnesium compound, a titanium compound and an halogen compound, with one or more electron donating compounds represented by the general formula:



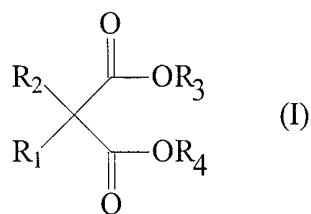
wherein  $R_c$  and  $R_d$  are, the same or different, a straight-chain or branched-chain hydrocarbon group having 1 - 10 carbon atoms, and  $R_a$  and  $R_b$  are the same or different, a saturated or cyclic saturated hydrocarbon group containing one or more secondary or tertiary carbons and having 3 - 20 carbon atoms. Although an improvement in terms of yields and isotactic index over the previously cited documents is obtained, the results are still not satisfactory for an economical use of the catalyst components disclosed therein.

It has now surprisingly been found that the polymerization yields and the isotactic index of the polymer can be improved by using catalyst components comprising heteroatom containing malonates as internal donors.

It is therefore an object of the present invention to provide a solid catalyst component for the polymerization of olefins  $CH_2=CHR$  in which R is hydrogen or a hydrocarbon radical with 1-12 carbon atoms, comprising Mg, Ti, halogen and an heteroatom containing malonate.

The term heteroatom means any atom, different from C and H, in addition to the oxygen atoms deriving from the malonic acid.

In particular, the electron donor compounds can be selected from esters of malonic acids of formula (I):



wherein  $R_1$  and  $R_2$  equal to or different from each other, are H or a  $C_1-C_{20}$  linear or branched alkyl, alkenyl, cycloalkyl, aryl, arylalkyl or alkylaryl group and said  $R_1$  and  $R_2$  can also be joined to form a cycle;  $R_3$  and  $R_4$  are independently selected from  $C_1-C_{20}$  linear or branched

alkyl, alkenyl, cycloalkyl, aryl, arylalkyl or alkylaryl group and R<sub>3</sub> and R<sub>4</sub> can also be joined to form a cycle; with the proviso that at least one of the R<sub>1</sub> to R<sub>4</sub> groups contains at least one heteroatom selected from the group consisting of halogens, N, O, Si, Ge, P, and S.

The heteroatoms, are preferably selected from the group consisting of F, Cl, Br, and Si, and, in a preferred embodiment, they are contained in the R<sub>1</sub> or R<sub>2</sub> groups.

Preferably, R<sub>3</sub> and R<sub>4</sub> are primary alkyl, arylalkyl or alkylaryl groups having from 2 to 8 carbon atoms which may contain heteroatoms. More preferably, they are primary branched alkyl groups optionally containing heteroatoms. Examples of suitable R<sub>3</sub> and R<sub>4</sub> groups not containing heteroatoms are methyl, ethyl, n-propyl, n-butyl, isobutyl, neopentyl, 2-ethylhexyl. Examples of suitable R<sub>3</sub> and R<sub>4</sub> groups containing heteroatoms are 2-chloroethyl, 1-trifluoromethylethyl, 2-trifluoromethylpropyl 2-trimethylsilylethyl, 2-bromoethyl, 2trifluoromethylpropyl, 4-chlorobenzyl, 2-fluoroethyl, 3-trimethylsilylallyl.

R<sub>2</sub> is preferably, and particularly when R<sub>1</sub> is H, a linear or branched C<sub>3</sub>-C<sub>20</sub> alkyl, cycloalkyl, arylalkyl group; more preferably R<sub>2</sub> is a C<sub>3</sub>-C<sub>20</sub> secondary alkyl, cycloalkyl, or arylalkyl. Particularly preferred are also compounds of formula (I) in which R<sub>1</sub> is H and R<sub>2</sub> is a C<sub>5</sub>-C<sub>20</sub> primary linear or branched alkyl, a C<sub>5</sub>-C<sub>20</sub> cycloalkyl, a C<sub>7</sub>-C<sub>20</sub> arylalkyl or alkylaryl group. Preferably R<sub>2</sub> contains at least one heteroatom. Specific examples of suitable monosubstituted malonate compounds are diethyl 2-(1-trifluoromethylethyl) malonate, diethyl 2-(1-trifluoromethylethylidene)malonate, bis(2-chloroethyl) 2-isopropylmalonate, diethyl 2-(trimethylsilylmethyl)malonate, diethyl 2-p-chlorobenzylmalonate, diethyl 2-piperidyl malonate, diethyl 2-(2-ethylpiperidyl)malonate, diethyl 2-(1-trifluoromethyl-1-methylethyl)malonate, diethyl 2- $\alpha$ -phenyl-p-(trifluoromethyl)benzyl malonate, bis(2-fluoroethyl) 2-isopropylmalonate, bis(2-fluoroethyl) 2-ethylmalonate.

Among disubstituted malonates preferred compounds are those in which at least one of R<sub>1</sub> and R<sub>2</sub> is a primary C<sub>3</sub>-C<sub>20</sub> alkyl, cycloalkyl, arylalkyl group.

Specific examples of suitable disubstituted malonate compounds are: diethyl-2(1-trifluoromethylethyl)-2-benzylmalonate, diethyl 2-(1-trifluoromethylethyl)-2-methylmalonate, diethyl 2-methyltrimethylsilyl-2-methylmalonate, diethyl 2-p-chlorobenzyl-2-isopropylmalonate, diethyl 2-piperidyl-2-methylmalonate, diethyl 2-(1-trifluoromethyl-1-methylethyl)-2-methylmalonate, bis(2-trimethylsilylethyl) 2-isopropyl-2-isobutylmalonate bis(p-chlorobenzyl) 2-cyclohexyl-2-methylmalonate.

It has been surprisingly found that catalyst components in which the internal donor is a heteroatom containing malonate perform better, in term of yields and isotactic index, than catalyst components comprising analogous malonates not containing heteroatoms.

As explained above, catalyst components according to the invention comprise, in addition to the above electron donor, Ti, Mg and halogen. In particular, the catalyst component comprises a titanium compound, having at least a Ti-halogen bond and the above mentioned electron donor compound supported on a Mg halide. The magnesium halide is preferably  $MgCl_2$  in active form which is widely known from the patent literature as a support for Ziegler-Natta catalysts. Patents USP 4,298,718 and USP 4,495,338 were the first to describe the use of these compounds in Ziegler-Natta catalysis. It is known from these patents that the magnesium dihalides in active form used as support or co-support in components of catalysts for the polymerization of olefins are characterized by X-ray spectra in which the most intense diffraction line that appears in the spectrum of the non-active halide is diminished in intensity and is replaced by a halo whose maximum intensity is displaced towards lower angles relative to that of the more intense line.

The preferred titanium compounds used in the catalyst component of the present invention are  $TiCl_4$  and  $TiCl_3$ ; furthermore, also Ti-haloalcohoholates of formula  $Ti(OR)_{n-y}X_y$ , where n is the valence of titanium and y is a number between 1 and n, can be used.

The preparation of the solid catalyst component can be carried out according to several methods.

According to one of these methods, the magnesium dichloride in an anhydrous state and the heteroatom containing malonate are milled together under conditions in which activation of the magnesium dichloride occurs. The so obtained product can be treated one or more times with an excess of  $TiCl_4$  at a temperature between 80 and 135°C. This treatment is followed by washings with hydrocarbon solvents until chloride ions disappeared. According to a further method, the product obtained by co-milling the magnesium chloride in an anhydrous state, the titanium compound and the heteroatom containing malonate is treated with halogenated hydrocarbons such as 1,2-dichloroethane, chlorobenzene, dichloromethane etc. The treatment is carried out for a time between 1 and 4 hours and at temperature of from 40°C to the boiling point of the halogenated hydrocarbon. The product obtained is then generally washed with inert hydrocarbon solvents such as hexane.

According to another method, magnesium dichloride is preactivated according to well known methods and then treated with an excess of  $TiCl_4$  at a temperature of about 80 to 135°C which contains, in solution, a heteroatom containing malonate. The treatment with  $TiCl_4$  is repeated and the solid is washed with hexane in order to eliminate any non-reacted  $TiCl_4$ .

A further method comprises the reaction between magnesium alcoholates or chloroalcoholates (in particular chloroalcoholates prepared according to U.S. 4,220,554) and an excess of  $TiCl_4$  comprising the heteroatom containing malonate in solution at a temperature of about 80 to 120°C.

According to a preferred method, the solid catalyst component can be prepared by reacting a titanium compound of formula  $Ti(OR)_{n-y}X_y$ , where n is the valence of titanium and y is a number between 1 and n, preferably  $TiCl_4$ , with a magnesium chloride deriving from an adduct of formula  $MgCl_2 \bullet pROH$ , where p is a number between 0.1 and 6 and R is a hydrocarbon radical having 1-18 carbon atoms. The adduct can be suitably prepared in spherical form by mixing alcohol and magnesium chloride in the presence of an inert hydrocarbon immiscible with the adduct, operating under stirring conditions at the melting temperature of the adduct (100-130°C). Then, the emulsion is quickly quenched, thereby causing the solidification of the adduct in form of spherical particles. Examples of spherical adducts prepared according to this procedure are described in USP 4,399,054 and USP 4,469,648. The so obtained adduct can be directly reacted with the Ti compound or it can be previously subjected to thermal controlled dealcoholation (80-130°C) so as to obtain an adduct in which the number of moles of alcohol is generally lower than 3 preferably between 0.1 and 2.5. The reaction with the Ti compound can be carried out by suspending the adduct (dealcoholated or as such) in cold  $TiCl_4$  (generally 0°C); the mixture is heated up to 80-130°C and kept at this temperature for 0.5-2 hours. The treatment with  $TiCl_4$  can be carried out one or more times. The heteroatom containing malonate can be added during the treatment with  $TiCl_4$ . The treatment with the electron donor compound can be repeated one or more times.

The preparation of catalyst components in spherical form is described for example in European Patent Applications EP-A-395083, EP-A-553805, EP-A-553806, EP-A-601525 and WO98/44001.

The solid catalyst components obtained according to the above method show a surface area (by B.E.T. method) generally between 20 and 500  $m^2/g$  and preferably between 50 and 400  $m^2/g$ ,

and a total porosity (by B.E.T. method) higher than 0,2 cm<sup>3</sup>/g preferably between 0,2 and 0,6 cm<sup>3</sup>/g. The porosity (Hg method) due to pores with radius up to 10.000 Å generally ranges from 0.3 to 1.5 cm<sup>3</sup>/g, preferably from 0.45 to 1 cm<sup>3</sup>/g.

A further method to prepare the solid catalyst component of the invention comprises halogenating magnesium dihydrocarbyloxide compounds, such as magnesium dialkoxide or diaryloxide, with solution of TiCl<sub>4</sub> in aromatic hydrocarbon (such as toluene, xylene etc.) at temperatures between 80 and 130°C. The treatment with TiCl<sub>4</sub> in aromatic hydrocarbon solution can be repeated one or more times, and the heteroatom containing malonate is added during one or more of these treatments.

In any of these preparation methods the desired heteroatom containing malonate can be added as such or, in an alternative way, it can be obtained *in situ* by using an appropriate precursor capable to be transformed in the desired electron donor compound by means, for example, of known chemical reactions such as esterification, transesterification etc. Generally, the heteroatom containing malonate is used in molar ratio with respect to the MgCl<sub>2</sub> of from 0.01 to 1 preferably from 0.05 to 0.5.

The solid catalyst component according to the present invention are converted into catalysts for the polymerization of olefins by reacting them with organoaluminum compounds according to known methods.

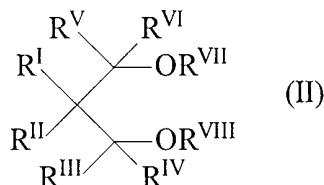
In particular, it is an object of the present invention a catalyst for the polymerization of olefins CH<sub>2</sub>=CHR, in which R is hydrogen or a hydrocarbyl radical with 1-12 carbon atoms, comprising the product of the reaction between:

- (a) a solid catalyst component comprising a Mg, Ti and halogen as essential elements and an heteroatom containing ester of malonic acids;
- (b) an alkylaluminum compound and, optionally,
- (c) one or more electron-donor compounds (external donor).

The alkyl-Al compound (b) is preferably selected from the trialkyl aluminum compounds such as for example triethylaluminum, triisobutylaluminum, tri-n-butylaluminum, tri-n-hexylaluminum, tri-n-octylaluminum. It is also possible to use mixtures of trialkylaluminum's with alkylaluminum halides, alkylaluminum hydrides or alkylaluminum sesquichlorides such as AlEt<sub>2</sub>Cl and Al<sub>2</sub>Et<sub>3</sub>Cl<sub>3</sub>.

The external donor (c) can be of the same type or it can be different from the heteroatom

containing malonate. Suitable external electron-donor compounds include silicon compounds, ethers, esters such as ethyl 4-ethoxybenzoate, amines, heterocyclic compounds and particularly 2,2,6,6-tetramethyl piperidine, ketones and the 1,3-diethers of the general formula (II):



wherein  $\text{R}^{\text{I}}$ ,  $\text{R}^{\text{II}}$ ,  $\text{R}^{\text{III}}$ ,  $\text{R}^{\text{IV}}$ ,  $\text{R}^{\text{V}}$  and  $\text{R}^{\text{VI}}$  equal or different to each other, are hydrogen or hydrocarbon radicals having from 1 to 18 carbon atoms, and  $\text{R}^{\text{VII}}$  and  $\text{R}^{\text{VIII}}$ , equal or different from each other, have the same meaning of  $\text{R}^{\text{I}}\text{-R}^{\text{VI}}$  except that they cannot be hydrogen; one or more of the  $\text{R}^{\text{I}}\text{-R}^{\text{VIII}}$  groups can be linked to form a cycle. Particularly preferred are the 1,3-diethers in which  $\text{R}^{\text{VII}}$  and  $\text{R}^{\text{VIII}}$  are selected from  $\text{C}_1\text{-C}_4$  alkyl radicals.

Another class of preferred external donor compounds is that of silicon compounds of formula  $\text{R}_a^5\text{R}_b^6\text{Si}(\text{OR}^7)_c$ , where a and b are integer from 0 to 2, c is an integer from 1 to 3 and the sum (a+b+c) is 4;  $\text{R}^5$ ,  $\text{R}^6$ , and  $\text{R}^7$ , are alkyl, cycloalkyl or aryl radicals with 1-18 carbon atoms optionally containing heteroatoms. Particularly preferred are the silicon compounds in which a is 1, b is 1, c is 2, at least one of  $\text{R}^5$  and  $\text{R}^6$  is selected from branched alkyl, cycloalkyl or aryl groups with 3-10 carbon atoms optionally containing heteroatoms and  $\text{R}^7$  is a  $\text{C}_1\text{-C}_{10}$  alkyl group, in particular methyl. Examples of such preferred silicon compounds are methylcyclohexyldimethoxysilane, diphenyldimethoxysilane, methyl-t-butylidemethoxysilane, dicyclopentyldimethoxysilane, 2-ethylpiperidinyl-2-t-butylidemethoxysilane and 1,1,1,trifluoropropyl-2-ethylpiperidinyl-dimethoxysilane. Moreover, are also preferred the silicon compounds in which a is 0, c is 3,  $\text{R}^6$  is a branched alkyl or cycloalkyl group, optionally containing heteroatoms, and  $\text{R}^7$  is methyl. Examples of such preferred silicon compounds are cyclohexyltrimethoxysilane, t-butyltrimethoxysilane and thexyltrimethoxysilane.

The electron donor compound (c) is used in such an amount to give a molar ratio between the organoaluminum compound and said electron donor compound (c) of from 0.1 to 500, preferably from 1 to 300 and more preferably from 3 to 100. As previously indicated, when used in the (co)polymerization of olefins, and in particular of propylene, the catalysts of the

invention allow to obtain, with high yields, polymers having a high isotactic index (expressed by high xylene insolubility X.I.), thus showing an excellent balance of properties. This is particularly surprising in view of the fact that, as it can be seen from the comparative examples here below reported, the use as internal electron donors of malonate compounds not containing heteroatoms gives worse results in term of yields and/or xylene insolubility.

Therefore, it constitutes a further object of the present invention a process for the (co)polymerization of olefins  $\text{CH}_2=\text{CHR}$ , in which R is hydrogen or a hydrocarbyl radical with 1-12 carbon atoms, carried out in the presence of a catalyst comprising the product of the reaction between:

- (a) a solid catalyst component comprising a Mg, Ti, halogen and a heteroatom containing malonate;
- (b) an alkylaluminum compound and, optionally,
- (c) one or more electron-donor compounds (external donor).

Said polymerization process can be carried out according to known techniques for example slurry polymerization using as diluent an inert hydrocarbon solvent, or bulk polymerization using the liquid monomer (for example propylene) as a reaction medium. Moreover, it is possible to carry out the polymerization process in the gas-phase operating in one or more fluidized or mechanically agitated bed reactors.

The polymerization is generally carried out at temperature of from 20 to 120°C, preferably of from 40 to 80°C. When the polymerization is carried out in the gas-phase the operating pressure is generally between 0.5 and 10 MPa, preferably between 1 and 5 MPa. In the bulk polymerization the operating pressure is generally between 1 and 6 MPa preferably between 1.5 and 4 MPa. Hydrogen or other compounds capable to act as chain transfer agents can be used to control the molecular weight of polymer.

The following examples are given in order to better illustrate the invention without limiting it.

## CHARACTERIZATIONS

The malonates used in the present invention were prepared by Knoevenagel condensation of halogenated ketones with diethyl malonate, see *Tetrahedron*, 29, 635, (1973), followed by selective reduction of the double bond, ( J. March in "Advanced Organic Chemistry" IV Ed. (1992) pp. 771-781). The malonates having the alcoholic moiety different from ethyl were prepared by transesterification of the corresponding diethyl malonate as described in

Example 1 of DE 2822472.

**Propylene general polymerization procedure**

In a 4-liter autoclave, purged with nitrogen flow at 70 °C for one hour, 75 ml of anhydrous hexane containing 800mg of AlEt<sub>3</sub>, 79.8 mg of dicyclopentyldimethoxysilane and 10 mg of solid catalyst component were introduced in propylene flow at 30 °C. The autoclave was closed. 1.5 Nl of hydrogen were added and then, under stirring, 1.2 Kg of liquid propylene were fed. The temperature was raised to 70°C in five minutes and the polymerization was carried out at this temperature for two hours. The non-reacted propylene was removed, the polymer was recovered and dried at 70 °C under vacuum for three hours and, then, weighed and fractionated with o-xylene to determine the amount of the xylene insoluble (X.I.) fraction at 25 °C.

**Determination of X.I.**

2.5 g of polymer were dissolved in 250 ml of o-xylene under stirring at 135°C for 30 minutes, then the solution was cooled to 25°C and after 30 minutes the insoluble polymer was filtered. The resulting solution was evaporated in nitrogen flow and the residue was dried and weighed to determine the percentage of soluble polymer and then, by difference the Xylene. Insoluble fraction. %.

**EXAMPLES**

**Examples 1-5 and Comparative Examples 6-9**

**Preparation o f solid catalyst components.**

Into a 500ml four-necked round flask, purged with nitrogen, 250 ml of TiCl<sub>4</sub> were introduced at 0°C. While stirring, 10.0 g of microspheroidal MgCl<sub>2</sub>\*2.8C<sub>2</sub>H<sub>5</sub>OH (prepared according to the method described in ex.2 of USP 4,399,054 but operating at 3,000 rpm instead of 10,000) and 7.5 mmoles of malonate were added. The temperature was raised to 100 °C and maintained for 120 min. Then, the stirring was discontinued, the solid product was allowed to settle and the supernatant liquid was siphoned off.

250 ml of fresh TiCl<sub>4</sub> were added. The mixture was reacted at 120°C for 60 min and, then, the supernatant liquid was siphoned off. The solid was washed six times with anhydrous hexane (6 x 100 ml) at 60 °C. Finally, the solid was dried under vacuum and analyzed. The type and amount of malonate (wt %) and the amount of Ti (wt %) contained in the solid catalyst component are reported in Table 1. Polymerization results are reported in Table 2.

**Table 1.**

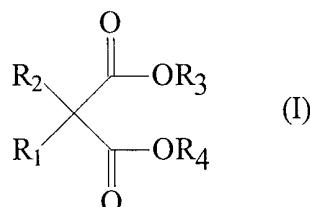
Ex.	Malonate	Ti	
n.	<i>Type</i>	Wt %	Wt %
<b>1</b>	Diethyl 2-(1-trifluoromethylethyl)-2-methylmalonate	19.3	3.4
<b>2</b>	Diethyl 2-(1-trifluoromethylethyl)malonate	12.3	3.8
<b>3</b>	Diethyl-2(1-trifluoromethylethyl)-2-benzylmalonate	16.8	3.9
<b>4</b>	Diethyl 2-(1-trifluoromethylethylidene)malonate	11.4	3.7
<b>5</b>	Bis(2-chloroethyl) 2-isopropylmalonate	13.1	3.3
<b>Comp.6</b>	Diethyl 2-isopropyl-2-methylmalonate	12.2	3.1
<b>Comp.7</b>	Diethyl 2-isopropylmalonate	10.8	3.2
<b>Comp.8</b>	Diethyl 2-isopropylidenemalonate	9.6	3.1
<b>Comp.9</b>	Diethyl 2-isopropyl-2-benzylmalonate	19.7	4.7

**Table 2.**

<b>Example</b>	<b>Yield</b>	<b>X.I.</b>
<b>n.</b>	<b>KgPP/gCat</b>	<b>Wt %</b>
<b>1</b>	50	97.6
<b>2</b>	49	97.3
<b>3</b>	45	96.2
<b>4</b>	40	94.4
<b>5</b>	38	97.1
<b>Comp.6</b>	42	97.0
<b>Comp.7</b>	30	96.9
<b>Comp.8</b>	25	93.4
<b>Comp.9</b>	38	94.9

## CLAIMS

1. A solid catalyst component for the polymerization of olefins  $\text{CH}_2=\text{CHR}$ , in which R is hydrogen or a hydrocarbyl radical with 1-12 carbon atoms, comprising Mg, Ti, halogen and an heteroatom containing malonate.
2. Catalyst component according to claim 1 in which the heteroatom containing malonate is selected from those of formula (I):



wherein R<sub>1</sub> and R<sub>2</sub> equal to or different from each other, are H or a C<sub>1</sub>-C<sub>20</sub> linear or branched alkyl, alkenyl, cycloalkyl, aryl, arylalkyl or alkylaryl group and said R<sub>1</sub> and R<sub>2</sub> can also be joined to form a cycle; R<sub>3</sub> and R<sub>4</sub> are independently selected from C<sub>1</sub>-C<sub>20</sub> linear or branched alkyl, alkenyl, cycloalkyl, aryl, arylalkyl or alkylaryl group and R<sub>3</sub> and R<sub>4</sub> can also be joined to form a cycle; with the proviso that at least one of the R<sub>1</sub> to R<sub>4</sub> groups contains at least one heteroatom selected from the group consisting of halogens, N, O, Si, Ge, P, and S.

3. Catalyst component according to claim 2 in which the heteroatoms are selected from F, Cl, Br, and Si.
4. Catalyst component according to claim 2 in which R<sub>3</sub> and R<sub>4</sub> are primary alkyl, arylalkyl or alkylaryl groups having from 2 to 8 carbon atoms
5. Catalyst component according to claim 4 in which R<sub>3</sub> and R<sub>4</sub> are primary branched alkyl groups.
6. Catalyst component according to any of the preceding claims in which R<sub>3</sub> and/or R<sub>4</sub> contain heteroatoms.
7. Catalyst component according to claim 2 in which R<sub>1</sub> is H and R<sub>2</sub> is a linear or branched C<sub>3</sub>-C<sub>20</sub> alkyl, cycloalkyl, arylalkyl group.
8. Catalyst component according to claim 7 in which R<sub>2</sub> is a C<sub>3</sub>-C<sub>20</sub> secondary alkyl,

cycloalkyl, or arylalkyl group.

9. Catalyst component according to claim 2 in which in which R<sub>1</sub> is H and R<sub>2</sub> is a C<sub>5</sub>-C<sub>20</sub> primary linear or branched alkyl, a C<sub>5</sub>-C<sub>20</sub> cycloalkyl, a C<sub>7</sub>-C<sub>20</sub> arylalkyl or alkylaryl group.
10. Catalyst components according to any of the claims 7-9 in which R<sub>2</sub> contains a heteroatom.
11. Catalyst components according to the preceding claims in which the heteroatom containing malonate is selected from the group consisting of diethyl 2-(1-trifluoromethylethyl)malonate, diethyl 2-(1-trifluoromethylethylidene)malonate, bis(2-chloroethyl) 2-isopropylmalonate, diethyl 2-(trimethylsilylmethyl)malonate, diethyl 2-p-chlorobenzylmalonate, diethyl 2-piperidyl malonate, diethyl 2-(2-ethylpiperidyl)malonate, diethyl 2-(1-trifluoromethyl-1-methylethyl)malonate diethyl 2- $\alpha$ -phenyl-p-(trifluoromethyl)benzyl malonate, bis(2-fluoroethyl) 2-isopropylmalonate, bis(2-fluoroethyl) 2-ethylmalonate.
12. Catalyst components according to claim 2 in which both R<sub>1</sub> and R<sub>2</sub> are different from H and in which at least one of R<sub>1</sub> and R<sub>2</sub> is a primary C<sub>3</sub>-C<sub>20</sub> alkyl, cycloalkyl, arylalkyl group.
13. Catalyst components according to claim 12 in which the heteroatom containing malonate is selected from the group consisting of diethyl-2(1-trifluoromethylethyl)-2-benzylmalonate, diethyl 2-(1-trifluoromethylethyl)-2-methylmalonate, diethyl 2-methyltrimethylsilyl-2-methylmalonate, diethyl 2-p-chlorobenzyl-2-isopropylmalonate, diethyl 2-piperidyl-2-methylmalonate, diethyl 2-(1-trifluoromethyl-1-methylethyl)-2-methylmalonate, bis (2-trimethylsilylethyl) 2-isopropyl-2-isobutylmalonate bis(p-chlorobenzyl) 2-cyclohexyl-2-methylmalonate.
14. A solid catalyst component according to claim 1 comprising a titanium compound having at least a Ti-halogen bond and the heteroatom containing malonate supported on a Mg halide in active form.
15. A solid catalyst component according to claim 14 in which the titanium compound is TiCl<sub>4</sub> or TiCl<sub>3</sub>.
16. A solid catalyst component according to claim 1 having a spherical form, a surface area (by B.E.T. method) between 20 and 500 m<sup>2</sup>/g, preferably between 50 and 400 m<sup>2</sup>/g, and

a total porosity (by B.E.T. method) higher than 0,2 cm<sup>3</sup>/g preferably between 0,2 and 0,6 cm<sup>3</sup>/g.

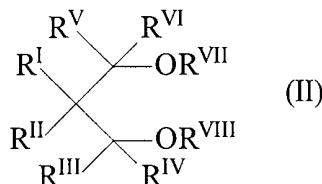
17. A catalyst for the polymerization of olefins CH<sub>2</sub>=CHR, in which R is hydrogen or a hydrocarbyl radical with 1-12 carbon atoms, comprising the product of the reaction between:

- the solid catalyst component of any of the claims 1-16;
- an alkylaluminum compound and, optionally,
- one or more electron-donor compounds (external donor).

18. Catalyst according to claim 17 in which the alkylaluminum compound (b) is a trialkyl aluminum compound.

19. Catalyst according to claim 18 in which the trialkyl aluminum compound is selected from the group consisting of triethylaluminum, triisobutylaluminum, tri-n-butylaluminum, tri-n-hexylaluminum, tri-n-octylaluminum.

20. Catalyst according to claim 17 in which the external donor (c) is selected from the 1,3-diethers of the general formula (II):



wherein R<sup>I</sup> and R<sup>II</sup>, R<sup>III</sup> R<sup>IV</sup>, R<sup>V</sup> and R<sup>VI</sup> equal or different to each other, hydrogen or hydrocarbon radicals having from 1 to 18 carbon atoms, and R<sup>VII</sup> and R<sup>VIII</sup>, equal or different from each other, have the same meaning of R<sup>I</sup>-R<sup>VII</sup> except that they cannot be hydrogen; one or more of the R<sup>I</sup>-R<sup>VIII</sup> groups can be linked to form a cycle.

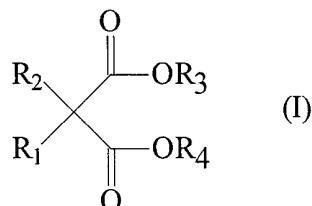
21. Catalyst according to claim 17 in which the external donor (c) is a silicon compound of formula. Ra<sup>5</sup>Rb<sup>6</sup>Si(OR<sup>7</sup>)c, where a and b are integer from 0 to 2, c is an integer from 1 to 4 and the sum (a+b+c) is 4; R<sup>5</sup>, R<sup>6</sup> and R<sup>7</sup> are alkyl, cycloalkyl or aryl radicals with 1-18 carbon atoms optionally containing heteroatoms.

22. Catalyst according to claim 21 in which a is 1, b is 1 and c is 2.

23. Catalyst according to claim 22 in which R<sup>5</sup> and/or R<sup>6</sup> are branched alkyl, cycloalkyl or

aryl groups with 3-10 carbon atoms optionally containing heteroatoms and R<sup>7</sup> is a C<sub>1</sub>-C<sub>10</sub> alkyl group, in particular methyl.

24. Catalyst according to claim 21 in which a is 0, c is 3 and R<sup>6</sup> is a branched alkyl or cycloalkyl group and R<sup>7</sup> is methyl.
25. Catalyst according to claim 23 or 24 in which the silicon compound is selected from the group consisting of methylcyclohexyldimethoxysilane, diphenyldimethoxysilane, methyl-t-butyldimethoxysilane, dicyclopentyldimethoxysilane cyclohexyltrimethoxysilane, t-butyltrimethoxysilane, thexyltrimethoxysilane, 2-ethylpiperidinyl-2-t-butyldimethoxysilane and 1,1,1,trifluoropropyl-2-ethylpiperidinyl-dimethoxysilane.
26. Process for the (co)polymerization of olefins CH<sub>2</sub>=CHR, in which R is hydrogen or a hydrocarbyl radical with 1-12 carbon atoms, carried out in the presence of the catalyst of claim 17.
27. Heteroatom containing malonates of formula (I):



wherein R<sub>1</sub> and R<sub>2</sub> equal to or different from each other, are H or a C<sub>1</sub>-C<sub>20</sub> linear or branched alkyl, cycloalkyl, aryl, arylalkyl or alkylaryl group and said R<sub>1</sub> and R<sub>2</sub> can also be joined to form a cycle; R<sub>3</sub> and R<sub>4</sub> are independently selected from C<sub>1</sub>-C<sub>20</sub> linear or branched alkyl, alkenyl, cycloalkyl, aryl, arylalkyl or alkylaryl group and R<sub>3</sub> and R<sub>4</sub> can also be joined to form a cycle; with the proviso that at least one of the R<sub>1</sub> to R<sub>4</sub> groups contains at least one heteroatom selected from the group consisting of halogens, N, O, Si, Ge, P, and S.

28. Use of the heteroatom containing malonates of formula (I) as electron donor compounds in catalysts for the polymerization of olefins.

## INTERNATIONAL SEARCH REPORT

International Application No

PCT/EP 99/08018

**A. CLASSIFICATION OF SUBJECT MATTER**  
 IPC 7 C08F4/651 C08F4/654 C08F10/00 C07C69/38

According to International Patent Classification (IPC) or to both national classification and IPC

**B. FIELDS SEARCHED**Minimum documentation searched (classification system followed by classification symbols)  
 IPC 7 C08F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category °	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 5 459 116 A (RO KI S ET AL) 17 October 1995 (1995-10-17) column 4, line 15 column 2, line 31 - line 40 example 1 ---	1-4, 14, 15, 27, 28
Y	EP 0 641 807 A (MITSUI PETROCHEMICAL IND) 8 March 1995 (1995-03-08) claim 1 page 8, line 46 -page 10, line 58 example 1 comparative example 1 page 14, line 1 -page 16, line 19 ---	1-6, 11-15, 17-26, 28
Y	EP 0 372 836 A (AMERICAN TELEPHONE & TELEGRAPH) 13 June 1990 (1990-06-13) method f; page 15 --- -/-	12, 13

 Further documents are listed in the continuation of box C. Patent family members are listed in annex.

## ° Special categories of cited documents :

- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier document but published on or after the International filing date
- "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the International filing date but later than the priority date claimed

"T" later document published after the International filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"&" document member of the same patent family

Date of the actual completion of the International search

Date of mailing of the International search report

1 February 2000

23/02/2000

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2  
 NL - 2280 HV Rijswijk  
 Tel. (+31-70) 340-2040, Tx. 31 651 epo nl  
 Fax: (+31-70) 340-3016

Authorized officer

Fischer, B

## INTERNATIONAL SEARCH REPORT

International Application No
PCT/EP 99/08018

## C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category °	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	EP 0 382 206 A (SAGAMI CHEM RES) 16 August 1990 (1990-08-16) page 24; examples 2,3; table 2	27
Y	---	1-4, 14, 15, 17-26, 28
X	CHEMICAL ABSTRACTS, vol. 76, no. 6, 7 February 1972 (1972-02-07) Columbus, Ohio, US; abstract no. 25763, SHIMA, TAKEO ET AL: "Malonic ester catalysts for the preparation of polyesters" XP002128548 abstract	27
Y	& JP 46 027180 B (TEIJIN LTD.) 5 August 1971 (1971-08-05)	1-3, 6
X	DE 43 26 918 C (HUELS CHEMISCHE WERKE AG) 19 January 1995 (1995-01-19)	27
Y	examples 1-5	1-5
X	LEHMANN, JUERG ET AL: "Regiocontrol and stereoselectivity in tungsten-bipyridine catalyzed allylic alkylation" TETRAHEDRON (1995), 51(32), 8863-74 , XP002128547 page 8866; figure 5; examples 3B,3C,7E; table 1 page 8867; figure 6; example 8E page 8872; examples 8B,8C,8E, -----	27
Y	GB 1 322 640 A (KENDALL & CO) 11 July 1973 (1973-07-11) example 23	1-4, 11

**INTERNATIONAL SEARCH REPORT**

**Information on patent family members**

International Application No

PCT/EP 99/08018

Patent document cited in search report	Publication date	Patent family member(s)		Publication date
US 5459116	A 17-10-1995	KR	123016 B	12-11-1997
		CN	1099041 A, B	22-02-1995
		JP	2680262 B	19-11-1997
		JP	7149813 A	13-06-1995
EP 0641807	A 08-03-1995	CA	2130009 A, C	14-02-1995
		CN	1111643 A	15-11-1995
		CN	1232829 A	27-10-1999
		CN	1231293 A	13-10-1999
		CN	1231295 A	13-10-1999
		CN	1231294 A	13-10-1999
		EP	0854156 A	22-07-1998
		JP	7102028 A	18-04-1995
		US	5618886 A	08-04-1997
		JP	7102029 A	18-04-1995
		JP	7109309 A	25-04-1995
		JP	7109314 A	25-04-1995
		JP	7109313 A	25-04-1995
EP 0372836	A 13-06-1990	CA	2004281 A	09-06-1990
		JP	2213132 A	24-08-1990
EP 0382206	A 16-08-1990	AT	113280 T	15-11-1994
		DE	69013528 D	01-12-1994
		JP	2918598 B	12-07-1999
		JP	3197479 A	28-08-1991
		US	5066795 A	19-11-1991
JP 46027180	B	NONE		
DE 4326918	C 19-01-1995	FR	2708928 A	17-02-1995
		JP	7053466 A	28-02-1995
		US	5463111 A	31-10-1995
		US	5569780 A	29-10-1996
GB 1322640	A 11-07-1973	AR	194578 A	31-07-1973
		AR	194697 A	31-07-1973
		AT	330200 B	25-06-1976
		AT	212374 A	15-09-1975
		AT	321937 B	25-04-1975
		AU	462551 B	26-06-1975
		AU	3549471 A	17-05-1973
		BE	775117 A	01-03-1972
		CH	568987 A	14-11-1975
		DE	2155469 A	10-05-1972
		DK	135283 B	28-03-1977
		ES	396825 A	16-06-1974
		FR	2112555 A	16-06-1972
		IL	38094 A	25-11-1975
		JP	55004099 B	29-01-1980
		LU	64226 A	29-05-1972
		NL	7115404 A, B,	12-05-1972
		NO	133497 B	02-02-1976
		SE	385887 B	26-07-1976
		US	RE28377 E	25-03-1975