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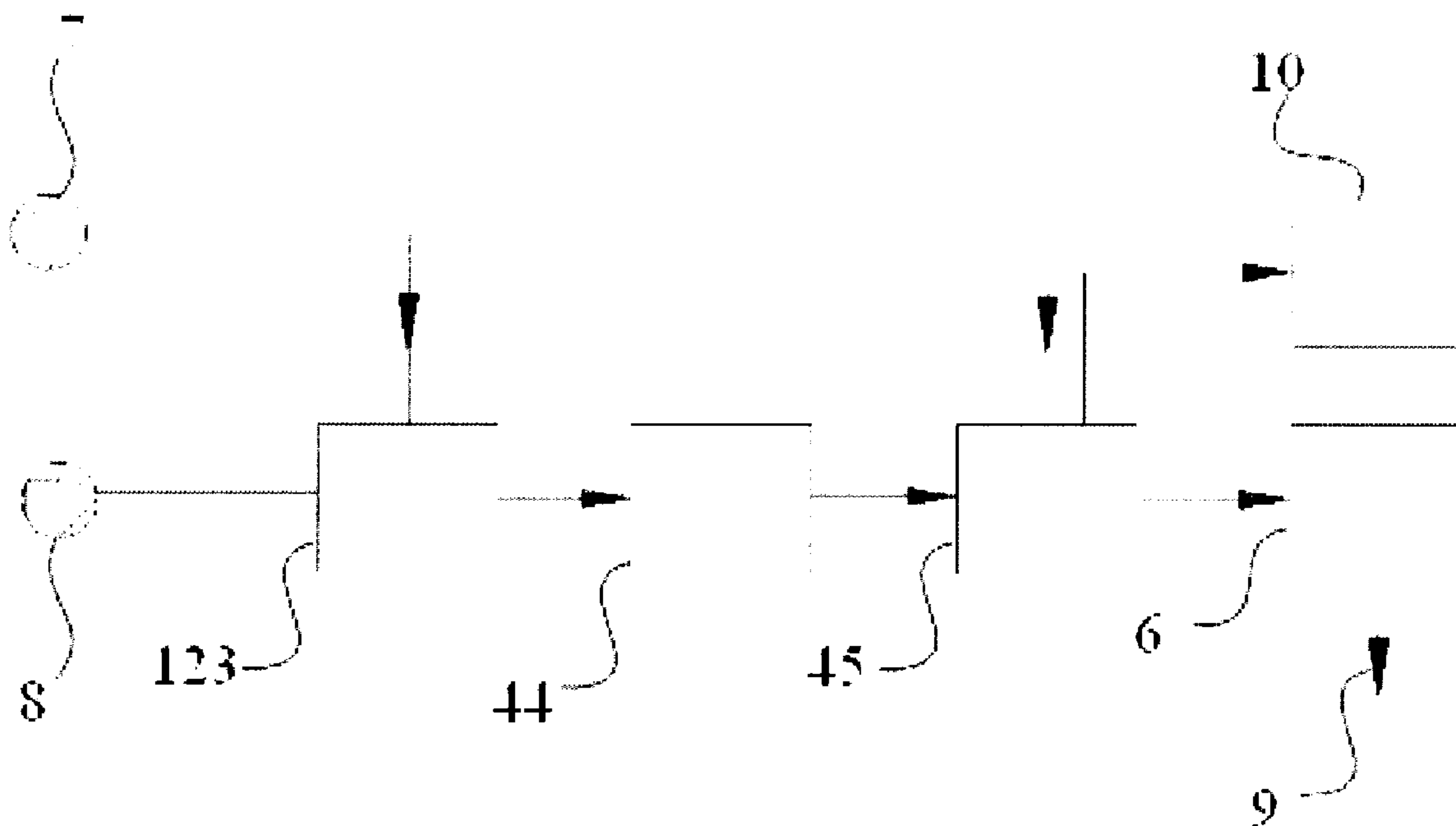
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(54) **Titre :** METHODE ET APPAREIL DE DENITRATION ET DE DESULFURISATION DE POUSSIERE ET D'ELIMINATION DE
POUSSIERE DES GAZ DE TRAINEE FCC

(54) **Title:** METHOD AND APPARATUS FOR DENITRATION AND DESULFURIZATION OF AND DUST REMOVAL FROM FCC TAIL
GAS BY AMMONIA-BASED PROCESS



(57) **Abrégé/Abstract:**

The present invention discloses an apparatus and a method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process. The apparatus comprises a first-stage waste heat recovery system, a denitration system, a dust removal and desulfurization system, a tail gas exhaust system, and an ammonium sulfate post-processing system. The dust removal and desulfurization system comprises a dedusting tower and an absorption tower disposed separately. The top and the bottom of the absorption tower are connected respectively to the tail gas exhaust system and the ammonium sulfate post-processing system. The absorption tower comprises sequentially, from bottom to top, an oxidation section, an absorption section, and a fine particulate control section. The method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process is implemented with the apparatus. The method of the present invention has the advantages of no



(57) Abrégé(suite)/Abstract(continued):

waste water discharge, no secondary pollution, synergistic control of various pollutants, recovery of sulfur dioxide by resourcelization to obtain the finished product ammonium sulfate, reduced investment and operation cost, and long-term stable operation.

Abstract

The present invention discloses an apparatus and a method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process. The apparatus comprises a first-stage waste heat recovery system, a denitration system, a dust removal and desulfurization system, a tail gas exhaust system, and an ammonium sulfate post-processing system. The dust removal and desulfurization system comprises a dedusting tower and an absorption tower disposed separately. The top and the bottom of the absorption tower are connected respectively to the tail gas exhaust system and the ammonium sulfate post-processing system. The absorption tower comprises sequentially, from bottom to top, an oxidation section, an absorption section, and a fine particulate control section. The method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process is implemented with the apparatus. The method of the present invention has the advantages of no waste water discharge, no secondary pollution, synergistic control of various pollutants, recovery of sulfur dioxide by resourcelization to obtain the finished product ammonium sulfate, reduced investment and operation cost, and long-term stable operation.

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Specification

**Method and apparatus for denitration and desulfurization of and dust removal from FCC
tail gas by ammonia-based process**

Technical Field

The present invention relates to the field of environmental protection technologies, and in particular to a method and an apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process.

Background

SO₂, NO_x, and dust are main pollutants in the atmosphere and are a significant source of smog. With the increasing total industrial pollution load and the limited environmental receptivity, the emission standards need to be further improved, to reduce the concentration of emitted pollutants. The FCC tail gas is characterized by large fine particulate level (particulates with a size of 0-10 μm account for 50% or more) and high SO₂ concentration (300-4500 mg/m³). Moreover, the dust level fluctuates greatly; particularly when the catalyst loss occurs in a regenerator during the regular "soot blowing" process and in an accident state of a high-temperature economizer, the dust level is increased dramatically. In addition to silicon, aluminum and other metal elements, the dust also contains nickel, vanadium and other heavy metal elements, thus affecting the quality of by-products, and affecting the resourcelization of sulfur. All these factors have increased the difficulty in effective management of the flue gas pollution occurring during the catalyst regeneration of a catalytic cracking unit.

After more stringent environmental protection standards and policies for the power, steel and other industries were formulated intensively in recent years, the Ministry of Environment Protection of the People's Republic of China issued the "Emission standard of pollutants for

petroleum refining industry" (GB31570- 2015) on April 16, 2015, which imposes more stringent requirements on the emission of major pollutants in the FCC regenerative flue gas (FCC tail gas), in which the specific emission limits for NO_x , SO_2 , and particulate matter are set to 100 mg/m^3 , 50 mg/m^3 and 30 mg/m^3 . Therefore, the desulfurization, desulfurization and dust removal of the FCC regenerative flue gas are a very difficult task, and it is imperative to develop a more effective deep denitrification desulfurization and dust removal process and technology with the resourcelization of sulfur, so as to meet the more stringent environmental protection requirements.

At present, the dust removal from and the desulfurization of the FCC regenerative flue gas in China mainly rely on the use of the wet washing technology; however, the investment, operation and maintenance costs are high, and the construction period of the system is long. Moreover, these technical methods also have the problems such as high consumption of lye, large volume of waste water and others. The existing popular sodium process is a disposable process, in which the desulfurization and dust removal operations have no need to be separated; however, high salt waste water is required to be treated, secondary pollution is caused, and a large amount of catalyst enters into the washing liquid under the operating condition of catalyst loss, which not only increases the treatment load of the waste solid, and also causes the waste of the catalyst, thus affecting the long-term stable operation of the system. In view of this, technologies for treating the FCC regenerative flue gas pollution are also studied and developed in China in recent years. Chinese Patent Application No. CN 104941423A disclosed a method and apparatus for denitration and desulfurization of and dust removal from an FCC regenerative flue gas by an ammonia-based process on September 30, 2015. The method includes the steps of entering the high-temperature flue gas containing the catalyst dust produced during the catalyst regeneration of a catalytic cracking unit to a waste heat recovery boiler I, where the temperature of the flue gas is reduced to $280\text{-}430^\circ\text{C}$, and the heat of the flue gas is utilized by the waste heat recovery boiler I to produce steam for output; entering the flue gas at $280\text{-}430^\circ\text{C}$ into a

denitration system for denitration; after adequate reaction on the surface of the denitration catalyst in the denitration reactor, entering the flue gas into a waste heat recovery boiler II via a flue gas vent; removing the sulfur dioxide and nitrogen oxide in the flue gas by reacting with ammonia, with ammonium sulfate being produced as a by-product, and removing the catalyst dust in the flue gas at the same time, to obtain a cleaned gas that is discharged up to standard.

In the method, an integrated desulfurization and dust removal technology by an ammonia-based process is employed. Although the process is simple, the obstacles during operation are fewer, the space occupied by the device is small, and the investment and operation costs are saved, the applicant finds during the long-term operation and practice that where the same absorption liquid is used for dust removal and desulfurization, the absorption liquid containing ammonium sulfate is hard to be separated from the dust because the particle size of the catalyst dust is small. In order to ensure the quality of the ammonium sulfate product, the separation process needs to be strengthened, resulting in an increased investment and operation cost of the separation process. The method necessitates that the dust level in the flue gas at the inlet is 30-800 mg/Nm³. The dust removal and the desulfurization are carried out at the same time, and there is mutual interference, thus affecting the long-term stable operation of the apparatus. Especially when the dust level in the flue gas at the inlet is as high as 5000 mg/Nm³, and the total amount exceeds 2 tons under an accident condition, ingredients entering the circulating absorption liquid will affect the absorption liquid, and the desulfurization and dust removal efficiencies, and the absorption liquid cannot be effectively separated from the dust, thus affecting the quality of the product ammonium sulfate.

There is an urgent need for a recovery-type deep denitration, desulfurization and dust removal technology to overcome the shortcomings existing in the prior art.

Summary of the Invention

In order to solve the technical problems in the prior art that by the existing process for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based method, only raw flue gas having a dust level of 30-800 mg/Nm³ can be treated, causing a narrowed scope of applicability of the process; the quality of the by-product ammonium sulfate is hard to be ensured, and if the separation process is strengthened, the investment and operation cost will be caused to increase; and the dust removal and the desulfurization are carried out at the same time, such that the apparatus has difficulty to operate stably for a long period of time, and a large amount of catalyst enters the washing liquid under an operation condition of catalyst loss, causing the increased treatment load of the waste solid and the waste of the catalyst, the present invention provides an apparatus and a method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process. The apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to the present invention can operate stably for a long period of time. The by-product ammonium sulfate obtained from the method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to the present invention has high quality, high desulfurization rate, high denitration rate, and high dust removal rate, and the cleaned flue gas meets the requirement as specified by GB31570-2015 "Emission standard of pollutants for petroleum refining industry".

In the present invention, the following technical solutions are employed to solve the above technical problems.

A technical solution of the present invention is to provide an apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process. The apparatus includes a first-stage waste heat recovery system, a denitration system, a dust removal and desulfurization system, a tail gas exhaust system, and an ammonium sulfate post-processing system. The denitration system has a feed port for a denitration reducing agent provided thereon.

The dust removal and desulfurization system includes a dedusting tower and an absorption tower disposed separately. The top and the bottom of the absorption tower are connected respectively to the tail gas exhaust system and the ammonium sulfate post-processing system. The dedusting tower is provided with at least 2 layers of washing liquid sprayers, and at least one layer of demisters are provided above the washing liquid sprayers in the dedusting tower. The absorption tower includes sequentially, from bottom to top, an oxidation section, an absorption section, and a fine particulate control section, where the absorption section is provided with at least 2 layers of sprayers in the absorption section, and the fine particulate control section is provided with 1 to 4 cyclically washing layers with dilute ammonium sulfate solution.

In the present invention, the first-stage waste heat recovery system, the denitration system, the dedusting tower and the absorption tower are connected in a relation that is conventional in the art; and preferably, the first-stage waste heat recovery system, the denitration system, the dedusting tower, and the absorption tower are connected in sequence.

Preferably, the apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to the present invention further includes a second-stage waste heat recovery system, where the first-stage waste heat recovery system, the denitration system, the second-stage waste heat recovery system, the dedusting tower, and the absorption tower are connected in sequence.

In the present invention, the denitration system is a denitration system for an FCC tail gas by an ammonia-based process conventionally used in the art. Preferably, the denitration system is a selective catalytic reduction (SCR) reactor, in which a rectifier is provided in an upper part of the SCR reactor, and an ammonia injection grid is provided at an inlet for the FCC tail gas of the SCR reactor.

The functions of the oxidation section, the absorption section and the fine particulate

control section in the absorption tower are similar to those described in Chinese Invention Patent Application NOs. CN103301705B entitled "Apparatus and method for controlling fine particulates in flue gas for desulfurization", and CN104524948B entitled "Ultra-low discharge method for integrated ultrasonic desulfurization and dust removal" filed by the present applicants. The present invention is advantageous in that dedusting by water washing and desulfurization by an ammonia-based process are carried out in 2 separated towers. 80% or more dust is removed in the dedusting tower, whereby the product quality and the final dust emission index are ensured. Correspondingly, no cooling and washing section needs to be provided in the absorption tower.

In the present invention, 2 to 5 layers of washing liquid sprayers are preferably provided in the dedusting tower, in which the liquid to gas ratio between each layer of the washing liquid sprayers is not less than 1.1 L/m^3 , the spray coverage rate is not less than 120%, and the total spray coverage rate of the dedusting tower is not less than 200%. The dedusting tower preferably comprises 1 to 5 layers of demisters.

The demister of the dedusting tower is a demister conventionally used in the art, and preferably one or more of a baffle demister, a roof type demister, and a wire mesh demister.

In the present invention, the bottom of the dedusting tower is preferably further connected with a washing circulation pump, which is connected to a filtering system. The filtering system is connected respectively to the top of the dedusting tower and the absorption tower. An inlet for process water to the dedusting tower is provided at an upper portion of the dedusting tower.

Fresh process water or evaporated condensed water is added to the dedusting tower via the inlet for process water to the dedusting tower, and enters a circulating washing liquid. A part of the circulating washing liquid passes through the filtering system and enters the absorption tower.

In the present invention, the absorption spray liquid is collected in the oxidation section,

and oxidized with air. Most of the slurry is recycled and, and a part of the slurry enters the ammonium sulfate post-processing system, in which a product ammonium sulfate is obtained. The slurry for recycling and the slurry entering the ammonium sulfate post-processing system for evaporation and recrystallization are drawn from different positions of the oxidation section. Preferably, the oxidation section is provided with 3 to 8 layers of gas - liquid dispersion enhancers.

In the present invention, the absorption tower preferably comprises 2 to 4 layers of sprayers in the absorption section, in which the liquid to gas ratio between each layer of the sprayers in the absorption section is not less than 1.1 L/m^3 , the spray coverage rate is not less than 120%, and the total spray coverage rate of the absorption section is not less than 300%.

In the present invention, more than 1 layer of demisters are preferably provided above the sprayers in the absorption section; and further preferably, the absorption section comprises 1 to 5 layers of demisters.

The demister of the absorption section is a demister conventionally used in the art, and preferably one or more of a baffle demister, a roof type demister, and a wire mesh demister.

In the present invention, the cyclically washing layer with dilute ammonium sulfate solution is conventional in the art. Preferably, the cyclically washing layer with dilute ammonium sulfate solution is provided with more than 1 layer of sprayers in the washing layer, and more than 1 layer of demisters are provided above the sprayers in the washing layer, in which the liquid to gas ratio between each layer of the sprayers in the washing layer is not less than 1.1 L/m^3 , the spray coverage rate is not less than 120%, and the total spray coverage rate of the fine particulate control section is not less than 300%. Further preferably, the washing layer comprises 1 to 4 layers of sprayers, and 1 to 5 layers of demisters.

The demister of the washing layer is a demister conventionally used in the art, and

preferably one or more of a baffle demister, a roof type demister, and a wire mesh demister.

In the present invention, the bottom of the absorption tower is further connected with at least one absorption circulation pump, and the absorption section of the absorption tower has an inlet for absorption spray liquid provided thereon. Preferably, 2 absorption circulation pumps are present, where several branches running from one of the absorption circulation pumps are connected respectively to the inlet for the absorption spray liquid of the absorption tower and the ammonium sulfate post-processing system; and the other absorption circulation pump is directly connected to the inlet for the absorption spray liquid of the absorption tower. An inlet for process water to the absorption tower is provided at an upper portion of the absorption tower, and an inlet for an ammonia-containing absorbent and an inlet for air as oxidant are provided at a lower portion of the absorption tower.

Fresh process water or evaporated condensed water is added to the absorption tower via the inlet for process water to the absorption tower.

After sulfur dioxide is absorbed in the absorption section, the FCC tail gas enters the fine particulate control section, and is cyclically washed with dilute ammonium sulfate solution to absorb the fine particulates (including fine particulates in dust entrained in the FCC tail gas, escaped ammonia, and aerosol), where the size of the fine particulates is $\leq 1 \mu\text{m}$.

In the present invention, the tail gas exhaust system is conventional in the art, and disposed lateral to or on the top of the desulfurization unit. The tail gas exhaust system is preferably a tail gas exhaust chimney when disposed on the top of the desulfurization unit.

In the present invention, the ammonium sulfate post-processing system is conventional in the art. Preferably, the ammonium sulfate post-processing system includes an evaporation and crystallization device, a cyclone, a centrifuge, a dryer, and a packaging machine connected in sequence, in which the evaporation and crystallization device is connected to the absorption

tower.

In the present invention, the shell, the internals, and pipes of the dedusting tower, the absorption tower, and the evaporation and crystallization device are all made with a corrosion resistant material, and preferably with a stainless-steel material of Grade 022Cr17Ni12Mo2, a dual-phase steel material of Grade 00Cr22Ni5Mo3N, a dual-phase steel material of Grade 00Cr25Ni6Mo2N, a titanium-based material, or Q235B steel lined with epoxy glass flakes.

The connection relation in the above apparatus will be further described below.

The first-stage waste heat recovery system and the denitration system are connected in a relation that is conventional in the art. Generally, an outlet of the first-stage waste heat recovery boiler is connected to a gas inlet of the denitration system; and an outlet of the denitration system is connected to the second-stage waste heat recovery system.

Another technical solution of the present invention is to provide a method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process, using the apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process. The method comprises the steps of:

(1) entering the FCC tail gas sequentially into the first-stage waste heat recovery system and the denitration system for cooling and denitration respectively, in which the temperature of the tail gas is reduced to 250-350°C;

(2) after treatment in the denitration system, entering the discharged FCC tail gas into the dust removal and desulfurization system after passing through the second-stage waste heat recovery system, for dust removal in the dedusting tower and desulfurization in the absorption tower respectively; and

(3) discharging the cleaned tail gas after desulfurization via the tail gas exhaust system, and

collecting the by-product ammonium sulfate in the ammonium sulfate post-processing system.

In the present invention, the temperature of the FCC tail gas entering the first-stage waste heat recovery system is from 580 to 950°C, the NO_x concentration is 100 to 1200 mg/Nm³, the SO₂ concentration is 200 to 30000 mg/Nm³, and the total dust level is 50 to 10000 mg/Nm³. Preferably the temperature of the FCC tail gas entering the first-stage waste heat recovery system is from 600 to 670°C, the NO_x concentration is 250 to 800mg/Nm³, the SO₂ concentration is 500 to 5000 mg/Nm³, and the total dust level is 100 to 300 mg/Nm³.

In the present invention, the denitration in Step (1) is carried out following a conventional denitration process in the art, and preferably following a selective catalytic reduction (SCR) process or a selective non-catalytic reduction (SNCR) process. The reducing agent used during denitration is conventional in the art, and preferably ammonia and/or urea.

In the present invention, the temperature of the FCC tail gas after being further cooled in the second-stage waste heat recovery system in Step (1) is preferably from 140 to 220°C.

When the second-stage waste heat recovery system is employed for further cooling the FCC tail gas, the FCC tail gas discharged after the treatment in the second-stage waste heat recovery system is fed into the dust removal and desulfurization system, where the FCC tail gas is further cooled by the second-stage waste heat recovery system in such a conventional manner in the art that a low-pressure steam of 0.3 to 0.8 MPa and a preheated soft water are preferably produced as by-products.

In the present invention, the desulfurization in Step (2) is carried out following a conventional desulfurization process in the art. During the desulfurization process in Step (2), a bottom absorption liquid is collected at the bottom of the absorption tower, a part of which is fed to the ammonium sulfate post-processing system, and the other part of which is oxidized with an oxygen-containing gas, replenished with an ammonia-containing absorbent, and then recycled to

the absorption section of the absorption tower.

Preferably, the oxygen-containing gas is preferably air.

Preferably, the ammonia-containing absorbent is preferably aqueous ammonia of 10-25% by weight and/or liquid ammonia.

Preferably, the bottom absorption liquid recycled to the absorption section accounts for 75-98% by weight of the total bottom absorption liquid.

In the cleaned flue gas obtained by the method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to the present invention, the NO_x concentration is $\leq 100 \text{ mg/Nm}^3$, the SO_2 concentration is $\leq 50 \text{ mg/Nm}^3$, the total dust level is $\leq 20 \text{ mg/Nm}^3$, and the dust removal efficiency is not less than 80%.

The quality of the by-product ammonium sulfate obtained from the method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to the present invention meets the requirement as specified by GB535-1995.

The above-described preferred conditions may be arbitrarily combined to obtain the preferred examples of the present invention, on the basis of common knowledge in the art.

The reagents and starting materials used in the present invention are commercially available.

The present invention has the following positive effects. The process of the present invention has no waste water discharge and no secondary pollution, enables the synergetic control of various pollutants and recovery of sulfur dioxide by resourcelization to obtain the finished product ammonium sulfate, and can reduce the investment and operation cost and operate stably for a long period of time.

Brief Description of Accompanying Drawings

Fig. 1 is a process flow chart of Example 1.

Fig. 2 is a schematic structural view of an apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process provided in Example 1.

List of numerals:

In Fig. 1:

6: ammonium sulfate post-processing system; 7: ammonia;

8: FCC tail gas; 9: ammonium sulfate;

10: cleaned tail gas; 123: denitration and waste heat recovery system;

44: dedusting system; 45: desulfurization system;

In Fig. 2:

1: first-stage waste heat recovery system; 2: denitration system;

3: second-stage waste heat recovery system; 4: dust removal and desulfurization system;

5: tail gas exhaust system; 6: ammonium sulfate post-processing system;

11: inlet for FCC tail gas; 21: feed port for denitration reducing agent;

41: dedusting tower; 42: absorption tower; 421: inlet for ammonia-containing absorbent;

422: inlet for air as oxidant; 61: evaporation and crystallization device;

62: cyclone; 63: centrifuge;

64: dryer; 65: packaging machine.

Detailed Description

Hereinafter, the present invention is further illustrated by way of examples; however, the present invention is not limited thereto. The experimental methods in the following examples where no specific conditions are given are implemented according to conventional methods and conditions, or selected in accordance with the product specification.

In GB535-1995, the parameters required for ammonium sulfate of the first grade are: N content $\geq 21\%$, water content $\leq 0.3\%$, and free acid content $\leq 0.05\%$.

In Example 1 below, the process flow is as follows. An FCC tail gas 8 enters a denitration and waste water recovery system 123, for the purpose of denitration under the action of ammonia 7. The FCC tail gas after denitration enters a dedusting system 44, and then enters a desulfurization system 45 for further desulfurization under the action of ammonia 7. The cleaned tail gas 10 after desulfurization is discharged via a tail gas processing system, and the remaining circulating liquid enters an ammonium sulfate post-processing system 6, where ammonium sulfate 9 is obtained. The specific process is as shown in Fig. 1.

Example 1

This example provides an apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process, which has a processing capacity of 100,0000 tons/year. The apparatus includes a first-stage waste heat recovery system 1, a denitration system 2, a second-stage waste heat recovery system 3, a dust removal and desulfurization system 4, a tail gas exhaust system 5, and an ammonium sulfate post-processing system 6. The first-stage waste heat recovery system 1 has an inlet 11 of the FCC tail gas provided thereon. The denitration system 2 is connected to the first-stage waste heat recovery

system 1, and has a feed port 21 of a denitration reducing agent thereon. The second-stage waste heat recovery system 3 is connected to the denitration system 2. The dust removal and desulfurization system 4 includes a dedusting unit and a desulfurization unit disposed separately. In this example, the dedusting unit is a dedusting tower 41 connected to the second-stage waste heat recovery system 3; and the desulfurization unit is an absorption tower 42 connected to the dedusting tower 41 and also to the tail gas exhaust system 5 and the ammonium sulfate post-processing system 6 respectively. The absorption tower 42 has an inlet 421 for an ammonia-containing absorbent and an inlet 422 for air as oxidant provided thereon, specifically as shown in Fig. 2.

In this example, the dedusting tower is provided 3 layers of washing liquid sprayer, where the liquid to gas ratio between each layer of the washing liquid sprayers is 1.5 L/m^3 , the spray coverage rate of each single layer is 140%, and the total spray coverage rate of the dedusting tower is not less than 400%. The dedusting tower is provided with 2 layers of demisters in an upper part of the dedusting tower, which are baffle and roof type demisters. The dust removal efficiency of the dedusting tower is not less than 80%. The solid-containing washing liquid obtained in the dedusting tower is fed to a filtering system for solid removal, and the washing liquid removed of the solid is recycled for washing the FCC tail gas.

In this example, an oxidation tank is provided at the bottom of the absorption tower 42, and 3 layers of absorption liquid sprayers are provided in an absorption section above the inlet for the flue gas, where the liquid to gas ratio between each layer of the washing liquid sprayers is 1.25 L/m^3 , the spray coverage rate of each single layer is 130%, and the total spray coverage rate of the dedusting tower is 320%. The absorption liquids of different oxidation rates are drawn from 2 different positions of the oxidation tank at the bottom of the absorption tower, one of which is recycled for absorption by an absorption circulation pump, and the other of which is fed to an evaporation and crystallization system. A fine particulate control section is provided above the

absorption section, and the fine particulate control section includes 2 layers of demisters provided above a sprayer layer in a washing layer, and the demisters in the washing layer are roof type and wire mesh demisters.

In this example, the ammonium sulfate post-processing system 6 includes an evaporation and crystallization device 61, a cyclone 62, a centrifuge 63, a dryer 64, and a packaging machine 65 connected in sequence.

In this example, the shell, the internals, and the pipes of the dedusting tower, the absorption tower, and the evaporation and crystallization device are all made with a stainless-steel material of Grade 022Cr17Ni12Mo2.

This example further provides a method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process, using the apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process. The method comprises the steps of:

(1) entering the FCC tail gas, where the flow rate is $262000 \text{ Nm}^3/\text{h}$, the temperature of the FCC tail gas is $600\text{-}650^\circ\text{C}$, the dust level in the flue gas is 200 mg/Nm^3 in a normal case, the SO_2 concentration is 3550 mg/Nm^3 , the NO_x concentration is 350 mg/Nm^3 , the dust level is 7500 mg/Nm^3 under the operating condition of catalyst loss, the duration of catalyst loss is 2.5 h, and the catalyst lost is 4.91 t, into the first-stage waste heat recovery system where the temperature of the FCC tail gas is reduced to 335°C , and the heat of the tail gas is utilized by the first-stage waste heat recovery system to produce steam of 4 MPa at a rate of 11.6 t/h for output;

(2) entering the flue gas at 335°C into the denitration system and denitrating with 5-15% aqueous ammonia, where after adequate reaction on the surface of the denitration catalyst in the denitration reactor, the nitrogen oxide content is decreased to 35 mg/Nm^3 , and the denitration rate is 90%.

(3) after the treatment in the denitration system, entering the flue gas into the second-stage waste heat recovery system via a flue gas vent, where steam of 0.6 MPa is produced at 3.3 t/h as a by-product, and the temperature of the flue gas is reduced to 166°C in the second-stage waste heat recovery system;

(4) after the treatment in the second-stage waste heat recovery system, entering the discharged FCC tail gas into the dedusting tower for dust removal and into the absorption tower for desulfurization, where the solid-containing washing liquid obtained in the dedusting tower is fed to a filtering system for solid removal, and the washing liquid removed of the solid is recycled for washing the FCC tail gas; and the FCC tail gas entering the absorption tower is desulfurized with 5-15% aqueous ammonia; and

(5) after the desulfurization, discharging the cleaned flue gas via the tail gas exhaust system, where the NO_x content is 35 mg/Nm³, the SO_2 content is 38 mg/Nm³, the dust level is 11.5 mg/Nm³ in a normal case and is 21mg/Nm³ under the operating condition of catalyst loss; the 40% ammonium sulfate solution produced as a by-product at about 4.7 t/h is evaporated and recrystallized, vortexed, separated by centrifugation, dried, and packaged, to obtain a finished product ammonium sulfate at 1.89 t/h, the quality of which (nitrogen content: 21.05%, water content: 0.2%, and free acid content: 0.03%) meets the requirements for ammonium sulfate of the first grade as specified by GB535-1995.

The list of the methods and main instruments for detecting various indices in this example is shown in Table 1. The parameters of main raw materials and the product are shown in Table 2.

Table 1. List of the methods and main instruments for detecting various indices

No.	Item monitored	Standard analytical method and code	Instrument and model	Instrument #
1	Flue dust	Determination of particulates and sampling methods of	Laoying 3012H model flue dust sampling instrument	8042448, 08244496 18360886,

		gaseous pollutants emitted from exhaust gas of stationary source GB/T16157-1996	Electronic balance BS224S, AB204-S	1119051201
2	SO ₂	Determination of sulphur dioxide from exhausted gas of stationary source: fixed-potential electrolysis HJ/T 57-2000	Testo 350 flue gas analytical instrument	10 [#] , 1 [#]
3	NO _x	Determination of nitrogen dioxide from exhausted gas of stationary source: fixed-potential electrolysis HJ/T 693-2014	Testo 350 flue gas analytical instrument	10 [#] , 1 [#]
4	Ammonia	Ambient air and exhaust gas-Determination of ammonia-Nessler's reagent spectrophotometry HJ 533-2009	Laoying 3072H model 722 spectrophotometer	02085809, 2c5BP363
5	Oxygen content in the flue gas	Electrochemical method - Specifications and test procedures for continuous emission monitoring systems of flue gas emitted from stationary sources (Appendix B) (HJ/T 76-2007)	Testo 350 flue gas analytical instrument	10 [#] , 1 [#]
6	Temperature of the flue gas	Platinum resistor method Determination of particulates and sampling methods of gaseous pollutants emitted from exhaust gas of stationary source (GB/T 16157-1996)	TES-1310	/
7	Humidity of the flue gas	Specifications and test procedures for continuous emission monitoring systems of flue gas emitted from stationary sources (Appendix B) (HJ/T 76-2007)	Laoying 3012H model flue dust sampling instrument	8042448, 08244496
8	Ammonium sulfate	Ammonium sulfate (GB 535-1995)	Analytical balance, PH meter and other conventional	

			laboratory instruments	
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Table 2. Parameters of main raw materials and the product

No.	Technic index	Unit	Value
1	Flow rate of FCC tail gas	Nm ³ /h	262000
2	Temperature of the flue gas at the inlet	°C	600-650
3	NO _x concentration in the flue gas	mg/Nm ³	350
4	SO ₂ concentration in the flue gas	mg/Nm ³	3550
5	Dust level in the flue gas	mg/Nm ³	200
6	NO _x concentration in the flue gas at the outlet	mg/Nm ³	35
7	SO ₂ concentration in the flue gas at the outlet	mg/Nm ³	38
8	Dust level in the flue gas at the outlet	mg/Nm ³	Normal case: 11.5; Operating condition of catalyst loss: 21
9	Absorption temperature	°C	52-54
10	Ammonia recovery rate	%	98.9
11	Quality of the product ammonium sulfate		GB535: first grade

The desulfurization efficiency in this example is 98.9%, and the denitration efficiency is 90%.

Comparative Example 1

CN104941423A is taken as a comparative example, in which the flue gas of 100,000 tons/year produced during the catalyst regeneration of a catalytic cracking unit is treated, where the flow rate of the flue gas is 135000 Nm³/h, the temperature is 950°C, the moisture content is 12%, the nitrogen oxide concentration is 360 mg/Nm³, the sulfur dioxide concentration is 2300 mg/Nm³, the dust level is 150 mg/Nm³, and the desulphurizing agent is 99.6% liquid ammonia. In a normal case, the denitration efficiency is $\geq 88.9\%$, the desulfurization efficiency is 98.5%, the NO_x concentration in the cleaned flue gas is 38 mg/Nm³, the SO₂ concentration is 32

mg/Nm³, the dust level is lower than 15 mg/Nm³, and the nitrogen content in the by-product ammonium sulfate is 20.8%.

However, the operating condition of catalyst loss is not taken into consideration. In this case, if the flue gas is treated with the apparatus according to Chinese Patent No. CN 104941423A, the following effects are finally obtained.

A large amount of dust enters the absorption liquid, such that the content of insoluble solid in the absorption liquid rises to 3% or higher. This causes the product ammonium sulfate to fail to be recrystallized and discharged. Even if the product ammonium sulfate could be discharged, the N content in the product would be decreased to 18% or below, and thus the product cannot be marketed. Moreover, the absorption circulation pump is clogged and worn, and the apparatus needs to be shut down to clean up the accumulated solids in the absorption tower.

The effects of the present invention are as follows. The denitration efficiency is $\geq 90\%$, the desulfurization efficiency is 98.9%, the NO_x concentration in the cleaned flue gas is 35 mg/Nm³, the SO₂ concentration is 38mg/Nm³, the dust level is 11.5 mg/Nm³, and the nitrogen content in the by-product ammonium sulfate is 21.06%. The apparatus of the present invention can operate normally under the operating condition of catalyst loss, and is obviously advantageous over that of the comparative example, as indicated by a dust level at the outlet of 21 mg/Nm³.

1. An apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process, comprising a first-stage waste heat recovery system, a denitration system, a dust removal and desulfurization system, a tail gas exhaust system, and an ammonium sulfate post-processing system, wherein the dust removal and desulfurization system comprises a dedusting tower and an absorption tower disposed separately, wherein the top and the bottom of the absorption tower are connected respectively to the tail gas exhaust system and the ammonium sulfate post-processing system; the dedusting tower is provided with at least 2 layers of washing liquid sprayers, and at least one layer of demisters are provided above the washing liquid sprayers in the dedusting tower; and the absorption tower comprises sequentially, from bottom to top, an oxidation section, an absorption section, and a fine particulate control section, wherein the absorption section is provided with at least 2 layers of sprayers in the absorption section, and the fine particulate control section is provided with 1 to 4 cyclically washing layers with dilute ammonium sulfate solution.

2. The apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to claim 1, wherein the first-stage waste heat recovery system, the denitration system, the dedusting tower and the absorption tower are connected in sequence.

3. The apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to claim 1 or 2, further comprising a second-stage waste heat recovery system, wherein the first-stage waste heat recovery system, the denitration system, the second-stage waste heat recovery system, the dedusting tower, and the absorption tower are connected in sequence.

4. The apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to claim 1, wherein the denitration system is a selective catalytic reduction reactor, in which a rectifier is provided in an upper part of the selective catalytic reduction reactor, and an ammonia injection grid is provided at an inlet for the FCC tail gas of the selective catalytic reduction reactor;

and/or, the tail gas exhaust system is a tail gas exhaust chimney.

5. The apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to claim 1, wherein 2 to 5 layers of washing liquid sprayers are provided in the dedusting tower, in which the liquid to gas ratio between each layer of the washing liquid sprayers is not less than 1.1 L/m^3 , the spray coverage rate is not less than 120%, and the total spray coverage rate of the dedusting tower is not less than 200%; and the dedusting tower comprises 1 to 5 layers of demisters;

and/or, the demister of the dedusting tower is one or more of a baffle demister, a roof type demister, and a wire mesh demister;

and/or, the oxidation section is provided with 3 to 8 layers of gas-liquid dispersion enhancers;

and/or, the absorption section comprises 2 to 4 layers of sprayers, in which the liquid to gas ratio between each layer of the sprayers in the absorption section is not less than 1.1 L/m^3 , the spray coverage rate is not less than 120%, and the total spray coverage rate of the absorption section is not less than 300%;

and/or, the cyclically washing layer with dilute ammonium sulfate solution is provided with more than 1 layer of sprayers in the washing layer, and more than 1 layer of demisters are provided above the sprayers in the washing layer, in which the liquid to gas ratio between each

layer of the sprayers in the washing layer is not less than 1.1 L/m^3 , the spray coverage rate is not less than 120%, and the total spray coverage rate of the fine particulate control section is not less than 300%; and preferably, the washing layer comprises 1 to 4 layers of sprayers, and 1 to 5 layers of demisters.

6. The apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to claim 1, wherein the ammonium sulfate post-processing system comprises an evaporation and crystallization device, a cyclone, a centrifuge, a dryer and a packaging machine connected in sequence, in which the evaporation and crystallization device is connected to the absorption tower.

7. A method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process, using the apparatus for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to any one of claims 1 to 6, the method comprising the steps of:

(1) entering the FCC tail gas sequentially into the first-stage waste heat recovery system and the denitration system for cooling and denitration respectively, in which the temperature of the tail gas is reduced to $250\text{-}350^\circ\text{C}$;

(2) after treatment in the denitration system, entering the discharged FCC tail gas into the dust removal and desulfurization system, for dust removal in the dedusting tower and desulfurization in the absorption tower respectively; and preferably, after treatment in the denitration system, further recovering heat from the discharged FCC tail gas in the second-stage waste heat recovery system, and then entering the discharged FCC tail gas into the dust removal and desulfurization system; and

(3) discharging the cleaned tail gas after desulfurization via the tail gas exhaust system, and collecting the by-product ammonium sulfate in the ammonium sulfate post-processing system.

8. The method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to claim 7, wherein the temperature of the FCC tail gas entering the first-stage waste heat recovery system is from 580 to 950°C, the NO_x concentration is 100 to 1200 mg/Nm³, the SO₂ concentration is 200 to 30000 mg/Nm³, and the total dust level is 50 to 10000 mg/Nm³; and preferably the temperature of the FCC tail gas entering the first-stage waste heat recovery system is from 600 to 670°C, the NO_x concentration is 250 to 800mg/Nm³, the SO₂ concentration is 500 to 5000 mg/Nm³, and the total dust level is 100 to 300 mg/Nm³.

9. The method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to claim 7, wherein the temperature of the FCC tail gas after being further cooled in the second-stage waste heat recovery system in Step (2) is from 140 to 220°C; and when the second-stage waste heat recovery system is employed for further cooling the FCC tail gas, the FCC tail gas discharged after the treatment in the second-stage waste heat recovery system is fed into the dust removal and desulfurization system, where the FCC tail gas is further cooled by the second-stage waste heat recovery system in such a manner that a low-pressure steam of 0.3 to 0.8 MPa and a preheated soft water are produced as by-products.

10. The method for denitration and desulfurization of and dust removal from an FCC tail gas by an ammonia-based process according to claim 7, wherein during the desulfurization process in Step (2), a bottom absorption liquid is collected at the bottom of the absorption tower, a part of which is fed to the ammonium sulfate post-processing system, and the other part of which is oxidized with an oxygen-containing gas, replenished with an ammonia-containing absorbent, and then recycled to the absorption section of the absorption tower, in which the oxygen-containing gas is preferably air; the ammonia-containing absorbent is preferably aqueous

ammonia of 10-25% by weight and/or liquid ammonia; and the bottom absorption liquid recycled to the absorption section preferably accounts for 75-98% by weight of the total bottom absorption liquid.

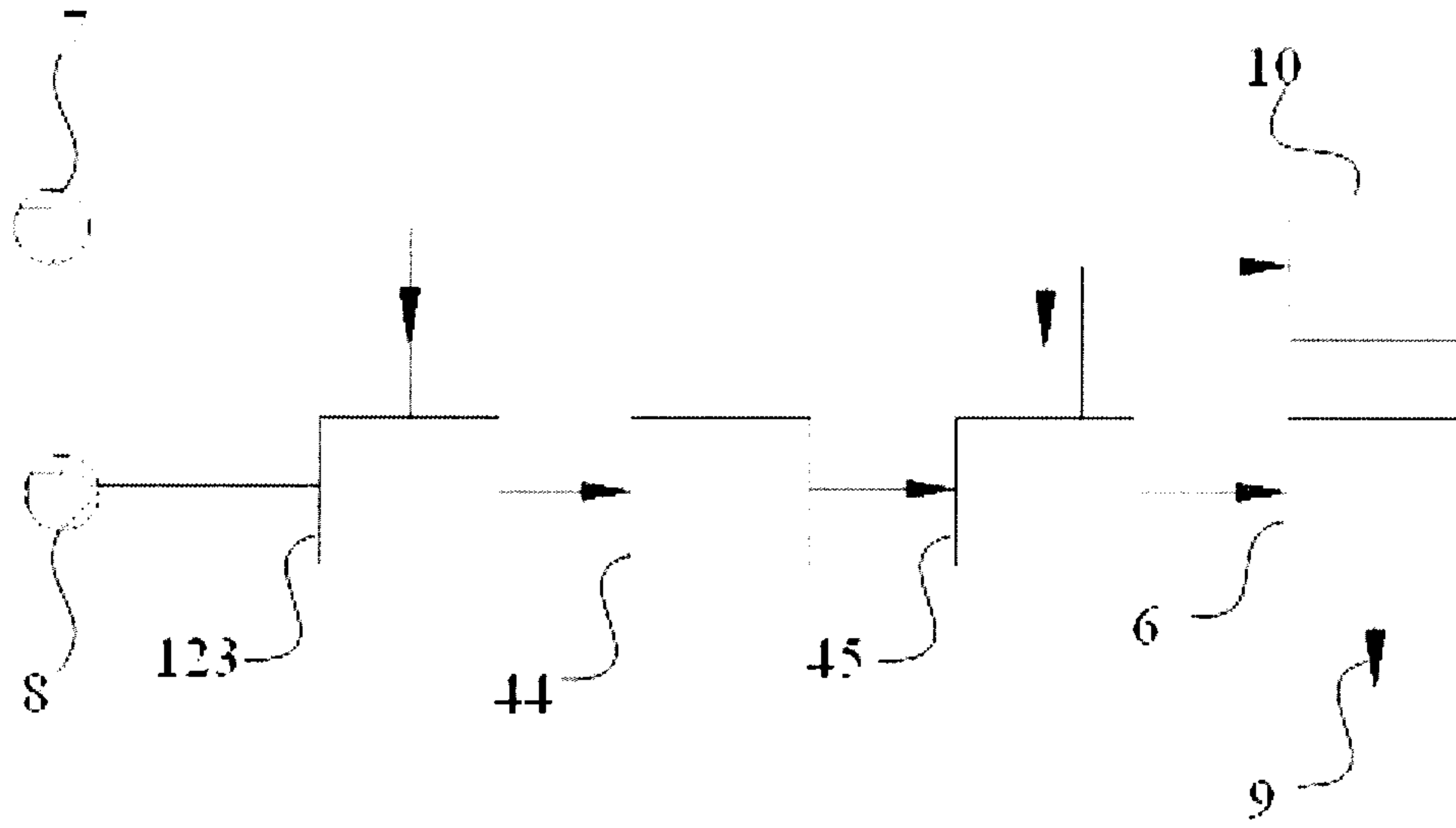


FIG. 1

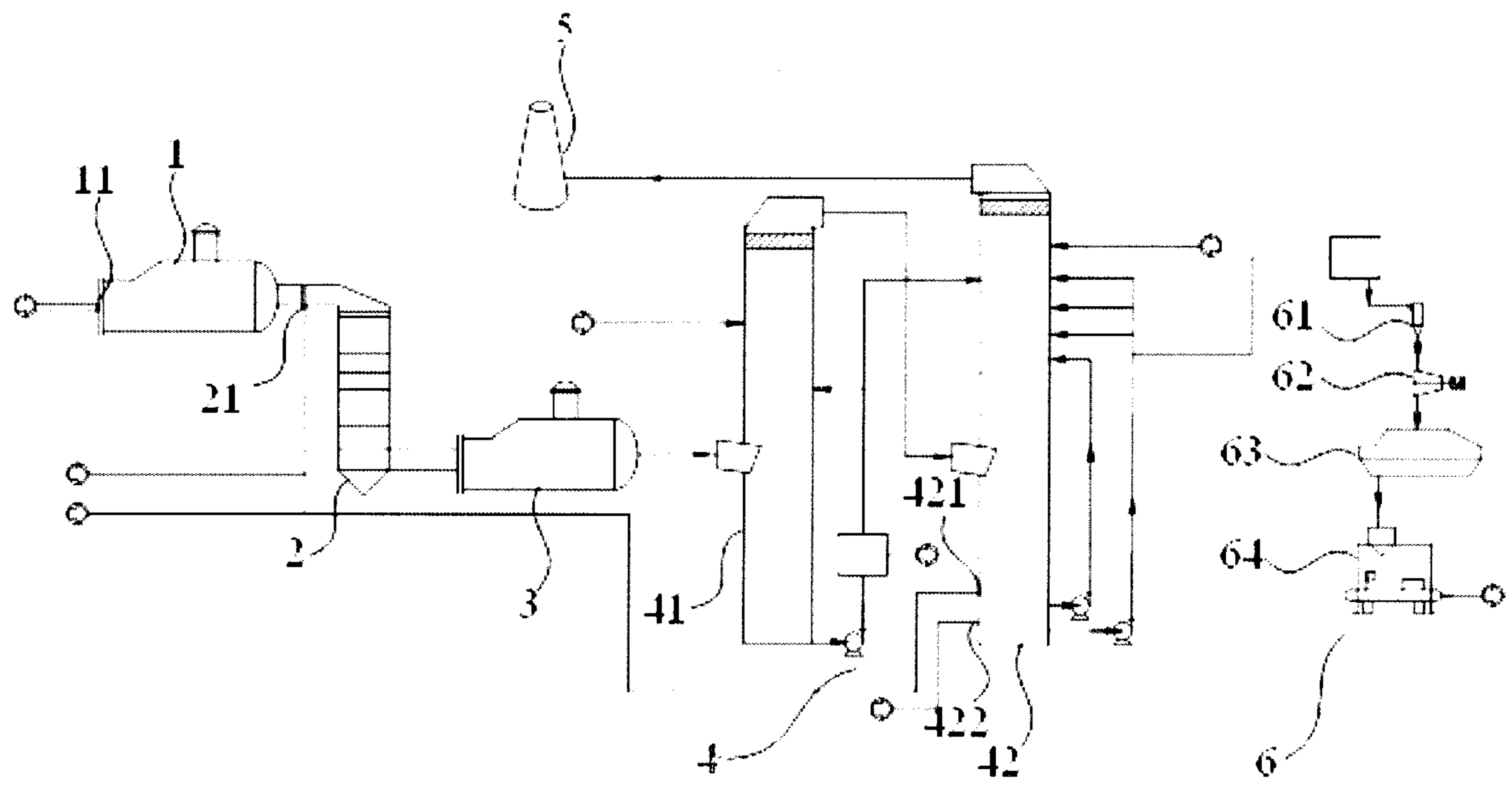


FIG. 2

