

(12) PATENT
(19) AUSTRALIAN PATENT OFFICE

(11) Application No. AU 200187333 B2
(10) Patent No. 751116

(54) Title
Hydrocarbon purification system regeneration

(51)⁷ International Patent Classification(s)
C10G 031/00

(21) Application No: **200187333**

(22) Application Date: **2001.11.02**

(30) Priority Data

(31) Number	(32) Date	(33) Country
09/747710	2000.12.21	US

(43) Publication Date : **2002.06.27**

(43) Publication Journal Date : **2002.06.27**

(44) Accepted Journal Date : **2002.08.08**

(71) Applicant(s)
Phillips Petroleum Company

(72) Inventor(s)
Marvin M. Johnson; Bruce B. Randolph

(74) Agent/Attorney
PHILLIPS ORMONDE and FITZPATRICK, 367 Collins Street, MELBOURNE VIC 3000

(56) Related Art
US 5928497

ABSTRACT

A system and process for removing water and heteroatom-containing compounds from hydrocarbons and for regenerating the adsorbent used in the system and process is disclosed and includes contacting the hydrocarbon stream with a water adsorbent and a heteroatom-containing compound adsorbent. The regeneration includes passing an isoparaffin over the water-adsorbent followed by passing the isoparaffin over the heteroatom-containing compound adsorbent; and, optionally; cooling the resulting effluent; separating such into a hydrocarbon phase and a water phase in a settler; removing a portion of the hydrocarbon phase for contact with and mixing with water; returning the hydrocarbon/water mixture to the settler; removing a portion of the hydrocarbon phase from the settler to form a recycle isoparaffin stream for use as at least a portion of the stripping stream; and removal of at least a portion of the water phase from the settler to form a waste water stream containing water and heteroatom-containing compound.



AUSTRALIA

Patents Act

**COMPLETE SPECIFICATION
(ORIGINAL)**

Class Int. Class

Application Number:
Lodged:

Complete Specification Lodged:
Accepted:
Published:

Priority

Related Art:

Name of Applicant:

Phillips Petroleum Company

Actual Inventor(s):

Marvin M Johnson, Bruce B Randolph

Address for Service:

PHILLIPS ORMONDE & FITZPATRICK
Patent and Trade Mark Attorneys
367 Collins Street
Melbourne 3000 AUSTRALIA

Invention Title:

HYDROCARBON PURIFICATION SYSTEM REGENERATION

Our Ref : 655803
POF Code: 1422/50647

The following statement is a full description of this invention, including the best method of performing it known to applicant(s):

HYDROCARBON PURIFICATION SYSTEM REGENERATION

The present invention relates to the field of hydrocarbon purification. In another aspect, the invention relates to a method for regenerating a purification system suitable for removing water and heteroatom-containing compounds from hydrocarbons.

5 The phrases "consists essentially of" and "consisting essentially of" do not exclude the presence of other steps, elements, or materials that are not specifically mentioned in this specification, as long as such steps, elements, or materials, do not affect the basic and novel characteristics of the invention. Additionally, they do not exclude impurities normally associated with the elements and materials used.

10 The above terms and phrases are intended for use in areas outside of U.S. jurisdiction. Within the U.S. jurisdiction the above terms and phrases are to be applied as they are construed by U.S. courts and the U.S. Patent Office.

 The discussion of the background to the invention herein is included to explain the context of the invention. This is not to be taken as an admission that any of the material
15 referred to was published, known or part of the common general knowledge in Australia as at the priority date of any of the claims.

 Throughout the description and claims of the specification the word "comprise" and variations of the word, such as "comprising" and "comprises", is not intended to exclude other additives, components, integers or steps.

20 BACKGROUND OF THE INVENTION

 The presence of water and/or heteroatom-containing compounds can pose a problem in various hydrocarbon conversion processes. Included among these processes is the alkylation of olefins with saturated hydrocarbons, such as isoparaffins, by contacting the reactants with an acid catalyst to form a reaction mixture, settling the reaction mixture
25 to separate the catalyst from the hydrocarbons and further separating the alkylation reactor effluent to recover the separate product streams. In typical alkylation units, the unreacted isoparaffin and olefin feeds are recycled to the alkylation reactor for recontact with the acid catalyst. An undesirable result of such recycle is the buildup of water and/or heteroatom-containing compounds in the isoparaffin and olefin streams.

30 The presence of water and/or heteroatom-containing compounds in the olefin or isoparaffin streams can cause lower alkylate octane and phase separation problems in the acid recovery section of the alkylation unit.

 Therefore, development of a more efficient process for regenerating a hydrocarbon purification system suitable for removing water and heteroatom-containing compounds
35 from hydrocarbons would be a significant contribution to the art and to the economy.

BRIEF SUMMARY OF THE INVENTION

 It is desirable to provide an improved method/system for regenerating a hydrocarbon purification system suitable for removing water and/or a heteroatom-

containing compound from a hydrocarbon stream, which is economical in construction and efficient in operation.

Again it is desirable to provide a method of treating a hydrocarbon stream containing at least one heteroatom-containing compound and water using a purification system, wherein the method includes an improved method for regenerating the
5 purification system by removing accumulated water and heteroatom-containing compound.

In accordance with the present invention, a method of regenerating a hydrocarbon purification system is provided and includes the steps of:

- 10 (a) introducing a stripping stream comprising an isoparaffin into the contacting zone of a treatment system containing (1) a water adsorbent containing water, and (2) a heteroatom-containing compound adsorbent containing a heteroatom-containing compound; such that the stripping stream contacts the water adsorbent prior to contacting the heteroatom-containing compound adsorbent;
- 15 (b) withdrawing a spent stripping stream comprising isoparaffin, heteroatom-containing compound and water from the contacting zone; and, optionally, further including the steps of:
 - (c) cooling the spent stripping stream to form a cooled spent stripping stream;
 - (d) introducing the cooled spent stripping stream to a settler for separation into
20 a hydrocarbon phase and a water phase;
 - (e) removing a portion of the hydrocarbon phase from the settler to form a circulating hydrocarbon stream;
 - (f) mixing the circulating hydrocarbon stream with water to form a
hydrocarbon/water mixture;
 - 25 (g) introducing the hydrocarbon/water mixture to the settler for separation into the hydrocarbon phase and the water phase;
 - (h) removing a portion of the hydrocarbon phase from the settler to form a recycle isoparaffin stream, wherein the recycle isoparaffin stream contains less water and less heteroatom-containing compound as compared to the cooled spent stripping stream;
30 and
 - (i) using at least a portion of the recycle isoparaffin stream as at least a portion of the stripping stream.

Other objects and advantages of the invention will be apparent from the detailed description of the invention and the appended claims.

35 BRIEF DESCRIPTION OF THE DRAWING

The Figure is a schematic flow diagram presenting an embodiment of the present invention.

DETAILED DESCRIPTION OF THE INVENTION

The hydrocarbon purification system suitable for use in the present invention contains an adsorption system within a contacting zone which can comprise, consist of, or consist essentially of a water adsorbent and a heteroatom-containing compound adsorbent.

Any material suitable for use in removing water from a hydrocarbon stream can be used as the water adsorbent in the present invention. Suitable water adsorbents include, but are not limited to, aluminas, silicates, aluminosilicates, carbons, and mixtures of any two or more thereof. Preferred water adsorbents include molecular sieves, silica gel, chabazite and clay. The most preferred water adsorbents are molecular sieves which have an average pore diameter in the range of from about 3 to about 4 Å.

Any material suitable for use in removing a heteroatom-containing compound from a hydrocarbon stream can be used as the heteroatom-containing compound adsorbent in the present invention. Suitable heteroatom-containing compound adsorbents include aluminas, zeolites, and combinations thereof. The most preferred heteroatom-containing compound adsorbent is a composition comprising an alumina and a zeolite.

The hydrocarbon stream suitable for treatment (purification) in the purification system can be any hydrocarbon stream requiring treatment to remove water and/or a heteroatom-containing compound. Typical hydrocarbon streams include, but are not limited to, alkylation unit feeds such as an olefin and/or an isoparaffin.

Referring to the Figure, therein is illustrated the inventive purification process/system 10 wherein the hydrocarbon stream, as described above, is introduced to the purification system 12, for contact with the water adsorbent 14 and the heteroatom-containing compound adsorbent 16, via conduit 18 which is connected in fluid flow communication with purification system 12. An effluent stream can be withdrawn from purification system 12 via conduit 20, which is connected in fluid flow communication with purification system 12, wherein the effluent stream generally contains less heteroatom-containing compound and less water than the hydrocarbon stream. The purification system can be operated in this manner until the adsorbents are saturated with water and/or heteroatom-containing compound or until the levels of water and/or heteroatom-containing compound in the effluent stream exceed acceptable levels.

At such time, the introduction of the hydrocarbon stream to the purification system 12 via conduit 18 is blocked.

Regeneration of the purification system 12 using the inventive regeneration method is accomplished by introducing a stripping stream comprising an isoparaffin to the contacting zone of purification system 12 via conduit 18 and conduit 22, which is connected in fluid flow communication with conduit 18. The stripping stream contacts the water adsorbent 14 prior to contact with the heteroatom-containing compound

adsorbent 16. The isoparaffin useful as a stripping stream in the present invention can contain in the range of from 3 to 5 carbon atoms per molecule, and can be mixtures thereof. In addition, the isoparaffin useful as a stripping stream is preferably substantially free of a heteroatom-containing compound and water.

5 The temperature of the stripping stream is generally in the range of from about 350°F to about 500°F; preferably from about 375°F to about 450°F, and most preferably from 390°F to 425°F. The time period for contacting the stripping stream with the water adsorbent and the heteroatom-containing compound adsorbent is generally in the range of from about 0.2 to about 4 hours; preferably from about 0.3 to about 3 hours; and most
10 preferably from 0.5 to 2 hours. Time for stripping depends on how rapidly the bed reaches 400 + °F which varies with the inlet temperature and space velocity of the stripping stream.

 A spent stripping stream comprising isoparaffin, heteroatom-containing compound and water is withdrawn from the contacting zone of purification system 12 via
15 conduit 20 and conduit 24, which is connected in fluid flow communication with conduit 20 and with a cooler 26. The spent stripping stream is optionally sent to cooler 26 for cooling to form a cooled spent stripping stream. The cooling of the spent stripping stream is preferably such that substantial portions of the water and of the heteroatom-containing compound contained in the spent stripping stream are condensed.

20 The cooled spent stripping stream is withdrawn from cooler 26 via conduit 28, which is connected in fluid flow communication to cooler 26 and a settler 30. The cooled spent stripping stream is introduced to settler 30 via conduit 28 and is separated into a hydrocarbon phase 32 and a water phase 34.

 The hydrocarbon phase 32 can comprise vaporous and/or liquid isoparaffin.

25 A portion of the hydrocarbon phase 32 can be removed from settler 30 via conduit 36, which is connected to settler 30 in fluid flow communication, to form a circulating hydrocarbon stream which can comprise isoparaffin and heteroatom-containing compound. The circulating hydrocarbon stream is then mixed with a water stream, introduced to conduit 36 via conduit 38, which is connected in fluid flow communication
30 with conduit 36, to form a hydrocarbon/water mixture.

 Conduit 36 is connected in fluid flow communication with conduit 28, and the hydrocarbon/water mixture is introduced to settler 30 via conduit 36 and conduit 28 for separation into the hydrocarbon phase 32 and into the water phase 34.

35 A portion of the hydrocarbon phase 32 is removed from settler 30 via conduit 40, which is connected in fluid flow communication with settler 30, to form a recycle isoparaffin stream. The recycle isoparaffin stream generally contains less water and less heteroatom-containing compound as compared to the cooled spent stripping stream. At least a portion of the recycle stream is used as at least a portion of the stripping stream

and is introduced to purification system 12 via conduit 18 and conduit 40, which is connected in fluid flow communication with conduit 18.

In addition, at least a portion of water phase 34 can be removed from settler 30 via conduit 42, which is connected in fluid flow communication with settler 30, to form a waste water stream comprising water and heteroatom-containing compound.

After regeneration of the purification system is complete, such as when sufficient water and/or heteroatom-containing compound has been removed from purification system 12, the introduction of the stripping stream to the contacting zone of purification system 12 via conduits 22, 40 and 18 is blocked and the introduction of the hydrocarbon stream to the contacting zone of purification system 12, via conduit 18, is restarted. The withdrawing of the effluent stream from the contacting zone of purification system 12, via conduit 20, is also restarted, thus returning the purification system back to normal operation (that is, water and/or heteroatom-containing compound removal).

The heteroatom-containing compound can be any heteroatom-containing compound typically present in hydrocarbon streams. More particularly, the heteroatom-containing compound can contain an element selected from the group consisting of sulfur, nitrogen, oxygen, and combinations of any two or more thereof. More typically, the heteroatom-containing compound is a compound selected from the group consisting of acetonitrile, acetone, and combinations thereof.

The following example is provided to further illustrate this invention and is not to be considered as unduly limiting the scope of this invention.

EXAMPLE

A tubular reactor was charged with 6.1 g (8.5 mL) of molecular sieve 3A, (obtained from Aldrich Chemical Co. under product designation Molecular Sieves 3A) and 6.26 g (8.5 mL) of Selexsorb adsorbent, obtained from Alcoa Corp., Pittsburgh, PA, under product designation Selexsorb CD. The two adsorbants were separated from each other with Alundum alumina (inert, low surface area alumina) and the remainder of the reactor was charged with Alundum alumina. The molecular sieve and Selexsorb adsorbent were then heated to 425°F under N₂ gas purge for 1 hour.

A feed blend was prepared containing 54.6g propylene, 245.2g 2-butenes, 0.40g acetonitrile and 0.11 g water. This feed was then shaken and charged to a syringe pump. A 28.69g portion was pumped into a cylinder and was extracted with 26.54g distilled water. The water extract was analyzed by gas chromatography for acetonitrile. By correction, the feed, as charged, contained 605 ppm acetonitrile. Results are given in the Table.

The reactor was held at ~90°F and the feed was pumped through the reactor at a rate of 130 mL/hour. System pressure was constant at 100 psig (N₂). Samples of reactor effluent were captured at 2 and 4 hours time on stream (TOS). These samples were

extracted with a known amount of water and the water extracts analyzed by GC for acetonitrile. Results are given in the Table.

5 The feed was then stopped and the system purged with N₂ from the pump inlet to the liquid collector for 3 hours. The N₂ was bubbled through distilled water (25.0 mL) placed in the liquid collector.

10 At this time, pure isopentane (iC₅) was charged to the feed pump. The reactor heater control was set initially to 425°F. The iC₅ was then charged to the reactor (0 psig N₂) and samples of condensed iC₅ in the liquid receiver were collected, extracted with water, and the water analyzed for acetonitrile. The results are given in the Table. The temperature set point had to be continually raised to maintain reactor temperature, since the iC₅ was at room temperature upon entering the top of the reactor.

This was followed by another regeneration, with the temperature of the Selexsorb adsorbent held above 400°F. Much less acetonitrile was observed in these samples. The data are given in the Table.

TABLE
RESULTS OF ADSORPTION/REMOVAL OF ACETONITRILE (ACN)

				REGENERATION #1				REGENERATION #2			
	Feed	2 Hr. Effluent	4 hr. Effluent	15 min.	30 min.	45 min.	60 min.	15 min.	30 min.	45 min.	60 min.
5	ACN (ppm) in Reactor Outlet	605	42	140	588	79	33	24	36	3	<1
	Sample Weight (g)	28.7	25.35	28.43	25.26	25.56	25.80	25.45	25.21	25.24	25.18
	Temp. (°F)	Ambient	90.5	90.5	399.4	316.8	369.4	372.5	497.7	408.0	413.7
10	Total ACN Charged to Reactor (g)	----	0.091	0.091	----	----	----	----	----	----	----
	Total ACN in Reactor Outlet (g)	----	0.006	0.042	0.046	0.006	0.003	0.002	0.003	0	0
	Cumulative ACN Adsorbed on Adsorbent (g)	----	0.085	0.132	----	----	----	----	----	----	----
15	iC ₅ Added During ACN Removal (g)	----	----	----	78.1	78.1	78.1	78.1	78.1	78.1	78.1
	Cumulative Total ACN Removed from Adsorbent (g)	----	----	----	0.046	0.052	0.055	0.057	0.060	0.060	0.060
20	Cumulative % ACN Removed from Adsorbent During Regeneration	----	----	----	35	39	42	43	45	45	45

The amount of ACN recovered in the isopentane stripping stream was less than that adsorbed by the Selexsorb adsorbent. It is likely that some of the adsorbed ACN was converted to acetic acid and ammonia by reaction with the adsorbed water from the molecular sieve 3A during the regeneration step.

5 Following the second regeneration, the adsorbent was subjected to a combustion analysis wherein the combustion products were analyzed for carbon, hydrogen, nitrogen and sulfur and showed no detectable nitrogen (<0.15 wt. %). This indicates even better ACN removal (~100%) than was determined using the GC method.

10 The data indicate that Selexsorb adsorbent can remove acetonitrile from olefinic feedstocks and that regeneration of the Selexsorb adsorbent with iC5 at temperatures of up to about 500°F can remove all of the adsorbed acetonitrile from spent Selexsorb.

Whereas this invention has been described in terms of the preferred embodiments, reasonable variations and modifications are possible by those skilled in the art. Such modifications are within the scope of the described invention and appended claims.

The claims defining the invention are as follows:

1. A method of treating a hydrocarbon stream containing at least one heteroatom-containing compound and water, said method comprising the steps of:
 - (a) introducing a hydrocarbon stream containing at least one heteroatom-containing compound and water to a contacting zone containing a water adsorbent and a heteroatom-containing compound adsorbent;
 - (b) withdrawing an effluent stream from said contacting zone, said effluent stream containing less heteroatom-containing compound and less water than said hydrocarbon stream;
 - (c) blocking the introduction of said hydrocarbon stream to said contacting zone;
 - (d) introducing a stripping stream comprising an isoparaffin to said contacting zone such that said stripping stream contacts said water adsorbent prior to contacting said heteroatom-containing compound adsorbent; and
 - (e) withdrawing a spent stripping stream comprising isoparaffin, heteroatom-containing compound and water from said contacting zone.
2. A method in accordance with claim 1, wherein said stripping stream contacts said water adsorbent and said heteroatom-containing compound adsorbent at a temperature in the range of from about 177°C to about 260°C (about 350°F to about 500°F).
3. A method in accordance with any preceding claim, wherein said stripping stream contacts said water adsorbent and said heteroatom-containing compound adsorbent for a time period in the range of from about 0.2 to about 2 hours.
4. A method in accordance with any preceding claim, further characterized to include the steps of:
 - (f) cooling said spent stripping stream to form a cooled spent stripping stream;
 - (g) introducing said cooled spent stripping stream to a settler for separation into a hydrocarbon phase and a water phase;
 - (h) removing a portion of said hydrocarbon phase from said settler to form a circulating hydrocarbon stream;
 - (i) mixing said circulating hydrocarbon stream with water to form a hydrocarbon/water mixture;
 - (j) introducing said hydrocarbon/water mixture to said settler for separation

into said hydrocarbon phase and said water phase;

(k) removing a portion of said hydrocarbon phase from said settler to form a recycle isoparaffin stream, wherein said recycle isoparaffin stream contains less water and less heteroatom-containing compound as compared to said cooled spent stripping stream; and

(l) using at least a portion of said recycle isoparaffin stream as at least a portion of said stripping stream.

5. A method in accordance with claim 4, further characterized to include:

removing at least a portion of said water phase from said settler to form a waste water stream comprising water and heteroatom-containing compound.

6. A method in accordance with any one of preceding claims 4-5, wherein the cooling of step (f) is such that substantial portions of the water and of the heteroatom-containing compound contained in said spent stripping stream are condensed.

7. A method in accordance with any one of preceding claims 4-6, wherein said circulating hydrocarbon stream comprises isoparaffin and heteroatom-containing compound.

8. A method in accordance with any preceding claim, further characterized to include the steps of:

blocking the introduction of said stripping stream to said contacting zone in step (d);

reintroducing said hydrocarbon stream to said contacting zone; and

withdrawing said effluent stream from said contacting zone.

9. A method in accordance with any preceding claim, wherein said heteroatom-containing compound contains sulfur.

10. A method in accordance with any one of preceding claims 1-8, wherein said heteroatom-containing compound contains nitrogen.

11. A method in accordance with any one of preceding claims 1-8, wherein said heteroatom-containing compound contains oxygen.

12. A method in accordance with any preceding claim, wherein said heteroatom-containing compound is a compound selected from the group consisting of acetonitrile, acetone, and combinations thereof.

13. A method in accordance with claim 12, wherein said heteroatom-containing compound is acetonitrile.

14. A method in accordance with claim 12, wherein said heteroatom-containing compound is acetone.
15. A method in accordance with any preceding claim, wherein said water adsorbent comprises a molecular sieve.
16. A method in accordance with claim 15 wherein said water adsorbent has an average pore diameter in the range of from about 3 to about 4 Å.
17. A method in accordance with any preceding claim, wherein said heteroatom-containing compound adsorbent comprises an alumina and a zeolite.
18. A method in accordance with any preceding claim, wherein said hydrocarbon stream is further characterized to comprise a compound selected from the group consisting of an olefin, an isoparaffin, and combinations thereof.
19. A method in accordance with any preceding claim, wherein said isoparaffin of said stripping stream contains in the range of from 3 to 5 carbon atoms per molecule, and mixtures thereof.
20. A method of regenerating a hydrocarbon purification system suitable for removing water and at least one heteroatom-containing compound from a hydrocarbon stream, said method for regenerating comprising:
 - (a) introducing a stripping stream comprising an isoparaffin into the contacting zone of a treatment system containing (1) a water adsorbent containing water, and (2) a heteroatom-containing compound adsorbent containing a heteroatom-containing compound; such that said stripping stream contacts said water adsorbent prior to contacting said heteroatom-containing compound adsorbent; and
 - (b) withdrawing a spent stripping stream comprising isoparaffin, heteroatom-containing compound and water from said contacting zone.
21. A method in accordance with claim 20 wherein said stripping stream contacts said water adsorbent and said heteroatom-containing compound adsorbent at a temperature in the range of from about 177°C to about 260°C (about 350°F to about 500°F).
22. A method in accordance with any one of preceding claims 20-21, wherein said stripping stream contacts said water adsorbent and said heteroatom-containing compound adsorbent for a time period in the range of from about 0.2 to about 2 hours.
23. A method in accordance with any one of preceding claims 20-22, further characterized to include the steps of:
 - (c) cooling said spent stripping stream to form a cooled spent stripping

stream;

(d) introducing said cooled spent stripping stream to a settler for separation into a hydrocarbon phase and a water phase;

(e) removing a portion of said hydrocarbon phase from said settler to form a circulating hydrocarbon stream;

(f) mixing said circulating hydrocarbon stream with water to form a hydrocarbon/water mixture;

(g) introducing said hydrocarbon/water mixture to said settler for separation into said hydrocarbon phase and said water phase;

(h) removing a portion of said hydrocarbon phase from said settler to form a recycle isoparaffin stream, wherein said recycle isoparaffin stream contains less water and less heteroatom-containing compound as compared to said cooled spent stripping stream; and

(i) using at least a portion of said recycle isoparaffin stream as at least a portion of said stripping stream.

24. A method in accordance with claim 23, further characterized to include:

removing at least a portion of said water phase from said settler to form a waste water stream comprising water and heteroatom-containing compound.

25. A method in accordance with any one of preceding claims 23-24, wherein the cooling of step (c) is such that substantial portions of the water and of the heteroatom-containing compound contained in said spent stripping stream are condensed.

26. A method in accordance with any one of preceding claims 23-25, wherein said circulating hydrocarbon stream comprises isoparaffin and heteroatom-containing compound.

27. A method in accordance with any one of preceding claims 20-26, wherein said heteroatom-containing compound contains sulfur.

28. A method in accordance with any one of preceding claims 20-26, wherein said heteroatom-containing compound contains nitrogen.

29. A method in accordance with any one of preceding claims 20-26, wherein said heteroatom-containing compound contains oxygen.

30. A method in accordance with any one of preceding claims 20-29, wherein said heteroatom-containing compound is a compound selected from the group consisting of acetonitrile, acetone, and combinations thereof.

31. A method in accordance with claim 30, wherein said heteroatom-containing compound is acetonitrile.
32. A method in accordance with claim 30, wherein said heteroatom-containing compound is acetone.
33. A method in accordance with any one of preceding claims 20-32, wherein said water adsorbent comprises a molecular sieve.
34. A method in accordance with claim 33 wherein said water adsorbent has an average pore diameter in the range of from about 3 to about 4 Å.
35. A method in accordance with any one of preceding claims 20-34, wherein said heteroatom-containing compound adsorbent comprises alumina and a zeolite.
36. A method in accordance with any one of preceding claims 20-35, wherein said hydrocarbon stream is further characterized to comprise a compound selected from the group consisting of an olefin, an isoparaffin, and combinations thereof.
37. A method in accordance with any one of preceding claims 20-36, wherein said isoparaffin contains in the range of from 3 to 5 carbon atoms per molecule, and mixtures thereof.
38. A method of treating a hydrocarbon stream containing at least one heteroatom-containing compound and water as more particularly described herein with particular reference to the Figure and the Example.
39. A method of regenerating a hydrocarbon purification system suitable for removing water and at least one heteroatom containing compound from a hydrocarbon stream as more particularly described herein with particular reference to the Figure and the Example.

Dated: 1st November 2001

PHILLIPS ORMONDE & FITZPATRICK

Attorneys for:

PHILLIPS PETROLEUM COMPANY

David B Fitzpatrick

