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- (73) Patenthaver: **Clariant International Ltd, Rothausstrasse 61, 4132 Muttenz, Schweiz**
- (72) Opfinder: **WYLDE, Jonathan, 54 N Turtle Rock Court, The Woodlands, Texas 77382, USA**
- (74) Fuldmægtig i Danmark: **Zacco Denmark A/S, Arne Jacobsens Allé 15, 2300 København S, Danmark**
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DESCRIPTION

FIELD OF THE INVENTION

[0001] The invention relates to a process for scavenging hydrogen sulfide from liquids and/or gas by use of metal carboxylates in combination with a solvating agent and emulsion breaker package as part of a multifunctional formulation. The formulations containing the inventive mixture have particular applicability in scavenging hydrogen sulfide and/or mercaptans yet at the same time prevent the formation of unwanted emulsions and/or deposition of unwanted by products often associated with using chemistries and/or formulations of the prior art.

BACKGROUND OF THE INVENTION

[0002] The presence of sulfhydryl compounds and particularly hydrogen sulfide pose challenges in many industries. Their presence can create a significant health, safety and environmental challenge. There are many different types of sulfhydryl compounds, but the most commonly encountered molecules include hydrogen sulfide (H_2S), organo-sulfur compounds containing S-H groups (also called mercaptans), thiol carboxylic acids $RC(O)SH$, dithio acids $RC(S)SH$, and related compounds.

[0003] In the oil and gas industry the H_2S content of crude oil and natural gas in many areas of the world is high enough to present environmental and safety hazards. Hydrogen sulfide is a flammable, corrosive, and highly toxic gas. H_2S is the most reduced form of sulfur and is produced by sulfate reducing bacteria (SRB) that are often found in the anaerobic conditions encountered in oil reservoirs and is highly soluble in crude oil. As oil is produced, it is depressurized and the H_2S is released and can then be transferred to, for example, oil based drilling fluid during the drilling process and this can become a hazard as the drilling fluid is recirculated from the well to the surface. During the production phase H_2S gas can create a significant integrity risk where it is present at as little as >0.01 psig partial pressure as it is an acid gas and upon dissolving into produced water creates a very corrosive environment and requires to somehow be removed in order for the fluids to be safely processed.

[0004] The odor of sulfhydryl compounds is also a challenge in, for example, metal working environments, but equally in water treatment processes, either municipal (e.g. waste water treatment) or industrial (recycling of mining water). SRB are often present in the recirculating fluid systems, and though the bacteria can usually be controlled by the use of biocidal compositions, it is easy to lose control of the biology in the system which results in the production of hazardous H_2S in the system. Furthermore biocides are inefficient at removing H_2S after it forms and only anecdotally scavenge, via either oxidation (e.g. sodium hypochlorite application) or due to the release of low levels of aldehyde during their breakdown (e.g. with

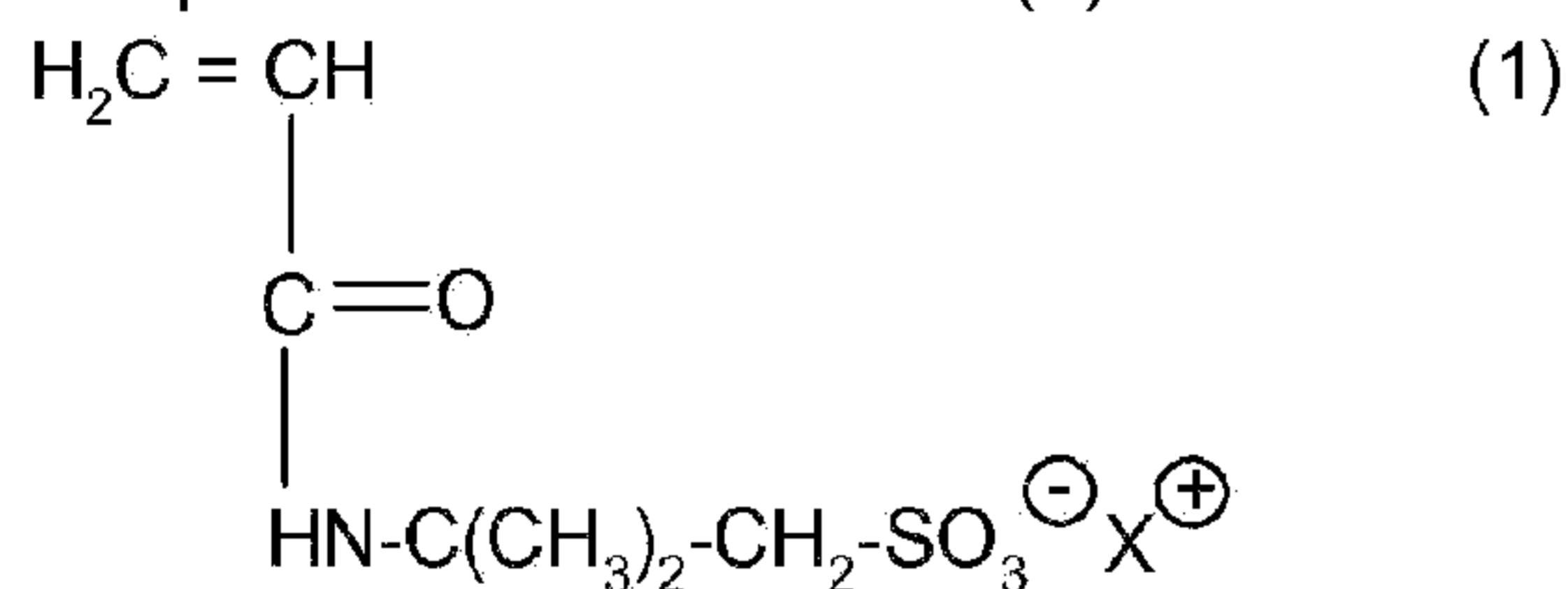
glutaraldehyde). Sulfhydryl compounds and particularly H₂S can present environmental, toxicity and integrity challenges in gaseous phases in confined spaces, as for instance in sewage treatment facilities and particularly in shipping and storage containers for moisture sensitive materials that may emit H₂S which can sit in the gaseous headspace. It would be desirable to have a scavenger that could reduce the H₂S concentrations in such locations. It would be particularly advantageous to have such a scavenger that is active in the absence of an aqueous phase. Furthermore it is desirable to have a scavenger that does not produce unwanted by-products or form emulsions that can inadvertently contaminate the very systems they are treating.

[0005] A number of methods have been proposed to scavenge hydrogen sulfide and control sulfhydryl odors in hydrocarbon containing systems:

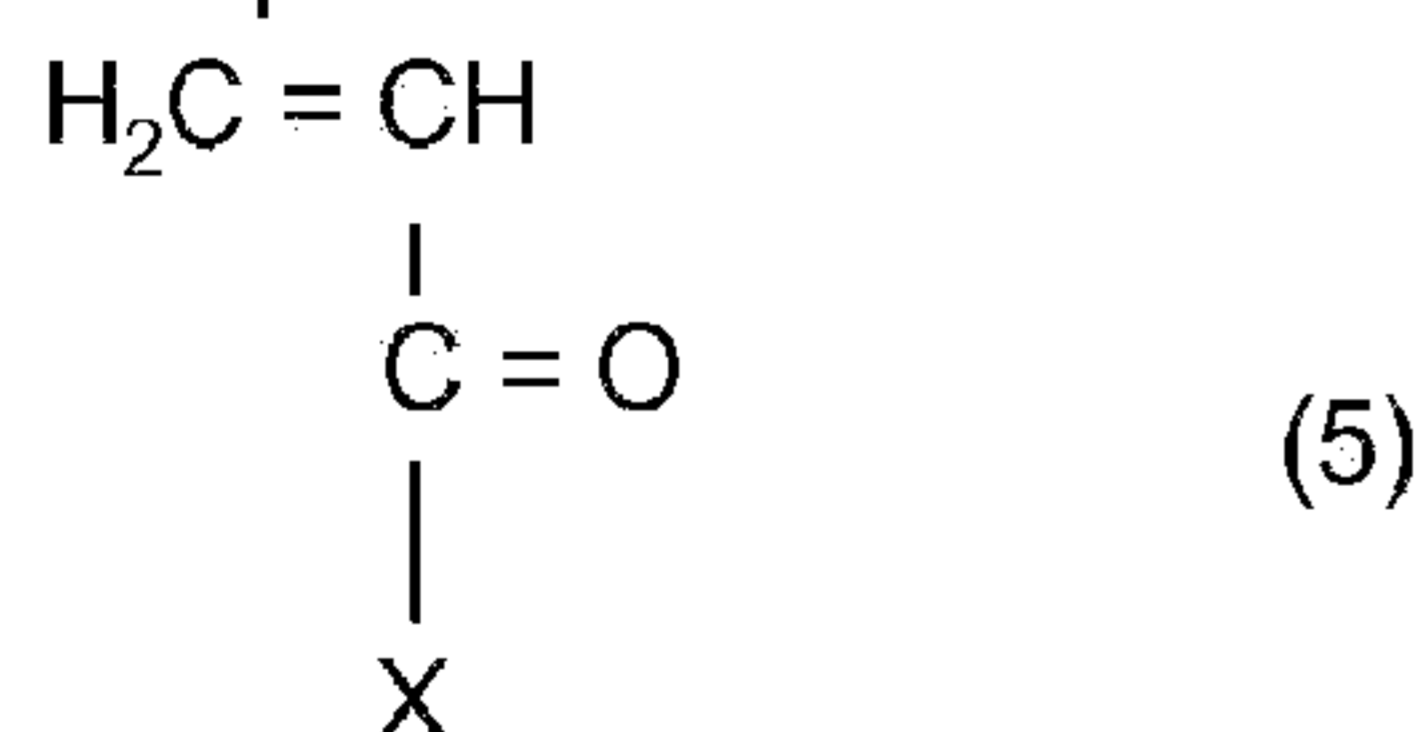
WO-98/02501 describes the use of bisoxazolidines prepared by the reaction of 1, 2 or 1, 3 amino alcohols containing 3 to 7 carbon atoms with aldehydes containing 4 or fewer carbon atoms. The relative oil and water solubility of these products can be controlled through the correct choice of starting materials. These bisoxazolidines react with sulfhydryl compounds present in oil and gas streams to neutralize and therefore scavenge them.

[0006] EP-A-2650314 teaches the use of a copolymer, comprising

1. a) 0.1 to 10 mol-%, based on the weight of the copolymer, of structural units derived from vinylphosphonic acid or of a salt thereof,
2. b) 40 to 80 mol-%, based on the weight of the copolymer, of structural units derived from compounds of the formula (1)



3. c) 1 to 50 mol-%, based on the weight of the copolymer, of structural units derived from compounds of the formula (5)



in which X is OH or NR³R⁴, and R³ and R⁴, independently of one another, are H or C₁-C₄-alkyl,

for the inhibition and/or dispersion of inorganic sulphide scales.

[0007] US-6239081 teaches a water-based drilling fluid which comprises at least one alkali metal carboxylate and at least one soluble boron compound. It further relates to the use of

boron compounds in drilling fluids which comprise alkali metal carboxylates to decrease the corrosivity of these drilling fluids.

[0008] US-5347004 teaches the use of reaction products of alkoxyalkylene amine, ammonia, and dialkylamines with aldehydes. These products are used to remove H₂S from gas streams which are sparged into water solutions of the products.

[0009] There are multiple patents published in the art that teach the use of triazine chemistry for the control of H₂S in the oilfield environment. US-4978512 teaches a method for reducing H₂S and organic sulfides from gaseous and/or liquid hydrocarbon streams by using a reaction product of a lower alkanolamine comprising 1 to about 6 carbons with a lower aldehyde comprising 1 to about 4 carbons. A preferred embodiment is the reaction product of monoethanolamine and formaldehyde which is perhaps one of the most ubiquitously used triazine chemistries in the oil and gas industry today to scavenge H₂S.

[0010] US-5128049 teaches a unique application method for scavenging agents whereby a dilute solution of a scavenging agent, such as triazine, is injected into an H₂S containing fluid, followed by equilibration and a second injection of dilute solution of scavenging agent to further reduce the H₂S content of the treated fluid.

[0011] EP-0636675 teaches the further use of a scavenging compound comprising a substantially formaldehyde free 1,3,5-trimethyl-hexahydro-1,3,5-triazine to scavenge gas or liquid hydrocarbon streams containing H₂S and/or mercaptans. The compound described is preferably prepared by the reaction of methylamine and formaldehyde.

[0012] US-8512449 teaches a method for formulating an oil-soluble triazine sulfide scavenger comprising a liquid sulfide-scavenging composition comprising from about 25 to 80 % by volume of a triazine, from about 15 to 50 % by volume of a glycol ether, and from about 5 to 40 % by volume of an alcohol, with a maximum water content of about 15 % by volume, and being oil soluble. The triazine used is a reaction product of a C₁ to C₆ alkanolamine and a C₁ to C₆ aldehyde, where the C₁ to C₆ moiety in each instance is a straight or branched chain alkyl group.

[0013] WO-2014/031537 teaches the use of an aldehyde releasing compound, preferably hydantoins, to remove sulfhydryl compounds from hydrocarbon fluids.

[0014] US-3928211 describes the use of inorganic zinc salts (most preferably zinc carbonate) preferably dispersed into aqueous or non-aqueous oil well drilling fluids with an organic dispersant such as lignin containing materials.

[0015] US-4147212 teaches the use of a water soluble zinc ammonium carbonate complex used to remove hydrogen sulfide from oils and gases by contact with aqueous solutions of the complex.

[0016] US-6599472 discloses the use of metal salt carboxylic acids that are soluble in hydrocarbon oils and are used to inactivate odor producing sulfhydryl compounds. Preferred embodiments are zinc neodecanoic acid but equally claimed are carboxylic acids of naphthenic acids, neoacids, isoacids and Guerbet acids and mixtures thereof.

[0017] WO-2014/130503 teaches the use of zinc carboxylates, preferably zinc octoate or zinc 2-ethyl hexanoic acid in combination with viscosity improver selected from the group consisting of glycol ethers having from about 4 to about 15 carbon atoms, and/or alkyl alcohols having from about 1 to about 10 carbons, and/or with additional hydrocarbons from about 7 to about 30 carbons. The resultant formulations are used to scavenge hydrogen sulfide gas.

[0018] WO-2013/181056 teaches the synergistic hydrogen sulfide scavenging obtained when use of a metal salt, preferably selected from zinc chloride, zinc acetate, zinc octanoate, and zinc salts containing at least one hydrocarbyl group of at least 4 carbon atoms in combination with an oil soluble amine formaldehyde reaction product (triazine).

[0019] US-2015/0025258 discloses the use of particulate zinc oxide salts blended in a mixture of two or more carboxylic acids selected from the group consisting of acetic acid, oleic acid, isobutyric acid, lineoleic acid and neodecanoic acid, for the scavenging of hydrogen sulfide.

[0020] The object of the invention was to provide formulations which can be used for scavenging of sulfhydryl compounds in crude oil, preferably, but not limited to H₂S and/or mercaptans. The formulations of the invention should have particular applicability in scavenging sulfhydryl compounds and should be notable for improved performance compared to the formulations and chemistries of the prior art.

[0021] It has been found that a ternary composition that comprises a metal carboxylate, an organic solvent and an emulsion breaker molecule will scavenge sulfhydryl compounds very effectively, while at the same time not induce any emulsion challenges due to the precipitation of insoluble byproducts. Deposits of sulfide scales can be a significant challenge during the use of metal carboxylate scavengers. Typically carboxylates of zinc are used which results in the deposition of ZnS. This can create significant challenges as ZnS is highly insoluble and can create flow assurance challenges due to blockages in pipes and process equipment as well as exacerbate water in oil emulsions and therefore dehydration of the crude oil.

[0022] In a first aspect, the present invention provides a composition, useful as a sulfhydryl scavenger for application in oilfield operations, comprising

1. 1.) a metal carboxylate, wherein the metal M is selected from the group consisting of Fe and Zn, those metals being present as ions in a +2 or +3 charge state, and wherein the carboxylate anion is derived from a hydrocarbyl monocarboxylic acid having 5 to 20 carbon atoms, or a mixture of such acids,
2. 2.) a solvent selected from the group consisting of water, glycol ethers having from 4 to

15 carbon atoms, alkyl alcohols having from 1 to 10 carbons, and aromatic hydrocarbon solvents having from 6 to 30 carbons, and

3. 3.) an emulsion breaker which is selected from the group consisting of a polymeric nonionic surfactant and dodecylbenzene sulfonic acid.

[0023] In a second aspect, the present invention provides the use of the composition of the first aspect as a sulfhydryl scavenger for application in oilfield operations and process systems.

[0024] In a third aspect, the present invention provides a process for scavenging sulfhydryl molecules in oilfield operations and process systems, the process comprising adding to a system susceptible to production of sulfhydryl compounds the composition of the first aspect.

[0025] In a preferred embodiment, the composition comprises additionally at least one additional hydrogen sulfide scavenger as component from group 4.

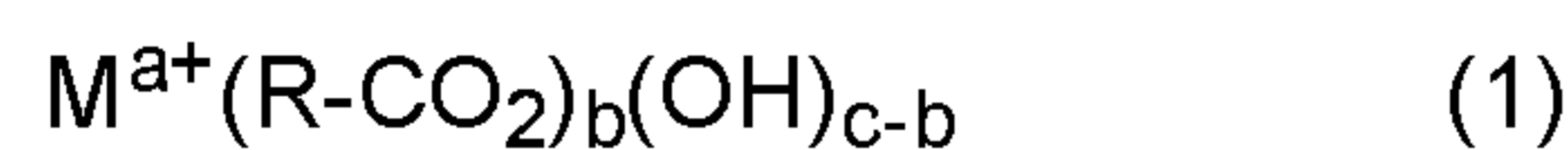
[0026] In another preferred embodiment, the composition comprises additionally at least one scale inhibitor and/or at least one corrosion inhibitor as component from group 5.

[0027] In another preferred embodiment, the composition comprises additionally both at least one additional hydrogen sulfide scavenger as component from group 4 and at least one scale inhibitor and/or at least one corrosion inhibitor as component from group 5.

Group 1

[0028] In group 1, the carboxylates are the ones of the metals Fe and Zn in their +2 or +3 charge state which means that the metals are present as respectively charged ions.

[0029] The compounds of group 1 comprise oil soluble sulfhydryl compound scavengers which in a preferred embodiment are salt compositions of the formula (1)



wherein

M

is iron

a

is 2 or 3,

b

is 1, 2 or 3,

c

is (a-b), and

R

is a hydrocarbyl radical containing from 4 to 19 carbon atoms, or mixtures of such carboxylates.

[0030] The metal ions used to prepare the carboxylate salts of this invention are chosen on the basis that the sulfide salts of the said metal ions are water insoluble or sparingly soluble. Preferably the metal sulfides have solubility in water less than 0.01 wt.-% meaning less than 0.01 g salt/ 100 cm³ water. The metal sulfides are the sulfides of zinc and iron, and most preferred is zinc sulfide.

[0031] The most preferred embodiment for the metal carboxylate is thus a zinc carboxylate. It is known that zinc carboxylates may occur as cyclic structures that correspond to the formula $(Zn)_n(O_2CR)_{(2n-2)}(O)_{[n]/4}$ instead of $Zn(R-CO_2)_b(OH)_{(c-b)}$. Mostly, zinc carboxylate will correspond to the formula $Zn_4(O_2CR)_6O$.

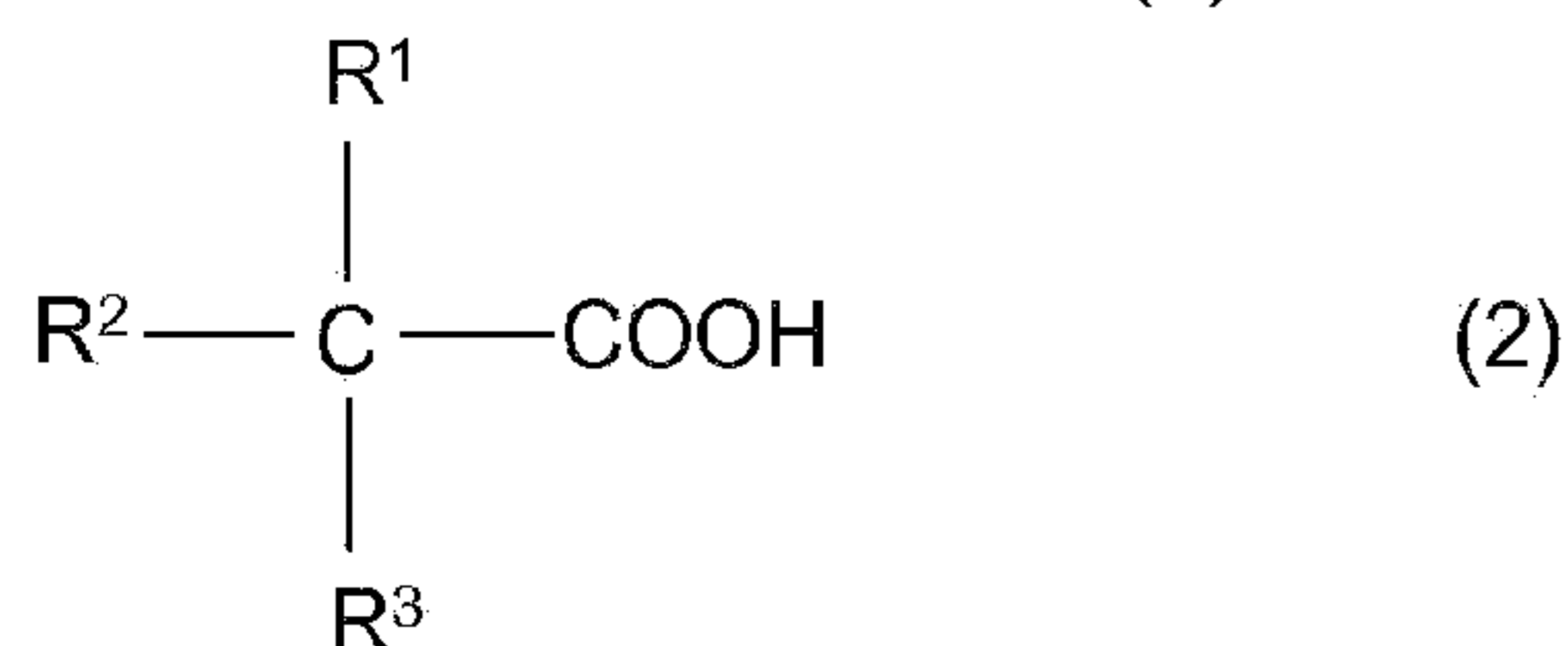
[0032] The carboxylic acids used to prepare the compositions of this invention contain from 5 to 20 carbon atoms, and are preferably chosen from those which form oil soluble salts with the metal ions of this invention. The preferred oil solubility is a log Pow of >1 but more preferably >2 where log Pow is measured using the OECD 117 method.

[0033] In one preferred embodiment, the acids from which the metal salts of group 1 are formed are liquid below 100 °C, more preferably below 50 °C, most preferably below 25 °C.

[0034] In another preferred embodiment, the metal salts according to formula (1) have a viscosity of less than 20,000 cP at standard room temperature and pressure (STP), more preferably below 15,000 cP, most preferably below 10,000 cP. All viscosity measurements were performed at STP using a Brookfield viscometer and a constant rotational speed and spindle type.

[0035] The formation of low melting salts typically requires that the carboxylic acids used to synthesize the final product have highly branched structures. Examples of suitable acids include:

1. 1. Neoacids of the formula (2)



wherein

R^1 , R^2 , and R^3 are each independently alkyl groups containing 1 to 16 carbon atoms,

with the total number of carbon atoms contained in R¹, R², and R³ being from 3 to 18. Readily available and suitable neoacids include, but are not limited to, neopentanoic acid, neoheptanoic acid, neo-octanoic acid, neononanoic acid, neodecanoic acid, and neotridecanoic acid. Neoacids with up to a total average of 20 carbon atoms are also available as mixtures of chain lengths and isomers, and are also suitable, as are mixtures of any of the described neoacids in any proportions. A preferred neoacid is neodecanoic acid as it is readily available and forms low viscosity salts.

2. 2. Isoacids of formula (3)

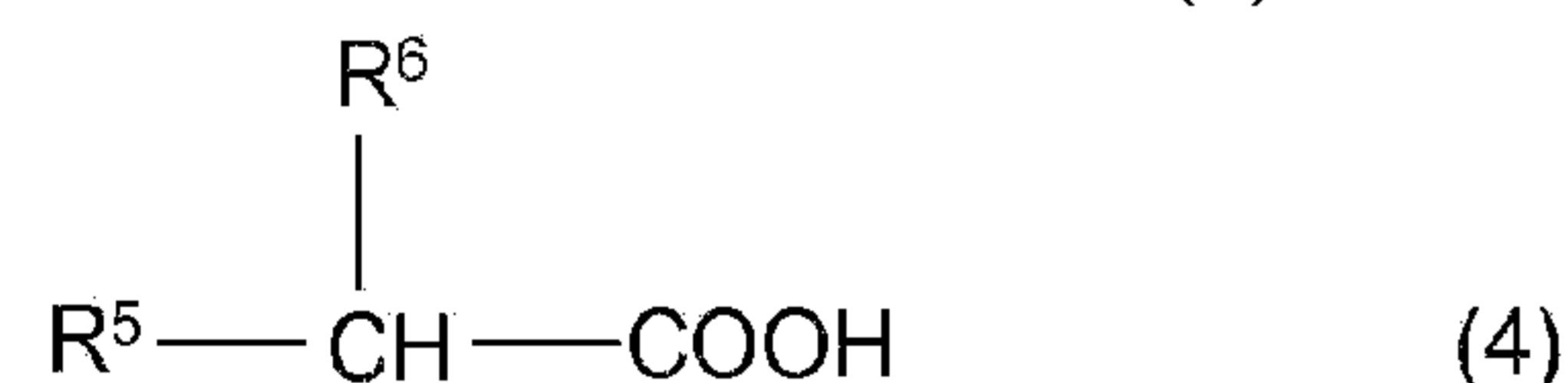


wherein

R⁴ is an aliphatic, branched hydrocarbyl group containing from 2 to 20 carbon atoms, wherein branched means that R⁴ includes at least one methyl group at a position other than the terminal carbon atom.

Readily available isoacids are usually mixtures of isomers which differ in the number and position of the methyl substitutions. Preferred isoacids include isopentanoic acid, isoheptanoic acid, iso-octanoic acid, isononanoic acid, isodecanoic acid, and isotridecanoic acid.

3. 3. Guerbet acids of formula (4)



wherein

R⁵

is a hydrocarbyl group containing from 2 to 8 carbon atoms, and

R⁶

is a hydrocarbyl group containing from 4 to 10 carbon atoms.

[0036] Preferred Guerbet acids include 2-ethylhexanoic acid, 2-butyloctanoic acid, 2-hexyldecanoic acid, and 2-octyldodecanoic acid. Most preferred is 2-ethylhexanoic acid.

Group 2

[0037] This group comprises hydrocarbon solvents used to deliver the Group 1 metal carboxylate component. The metal carboxylate is delivered as a composition having the metal carboxylate and a solvent. The solvent may be any solvent suitable, for example, for dissolving or suspending the metal carboxylate. In preferred embodiments, the solvent is water, alcohol, a non-alcoholic organic solvent, and/or any combination thereof. The alcohol may include any

alcohol suitable as a solvent and for use with oil recovery operations. Preferred are alkyl alcohols having from 1 to 10 carbon atoms, e.g. isopropyl alcohol, methanol, ethanol, propanol, butanol. Another preferred type of alcohols is glycol ethers having from 4 to 15 carbon atoms. Examples of suitable glycol ethers include ethylene glycol, propylene glycol, butylene glycol, oligoethylene glycols, oligopropylene glycols, isopropyl alcohol or any combination thereof. Oligoethylene glycols and oligopropylene glycols preferably have a number average molecular weight between 200 and 1000 g/mol.

[0038] According to another preferred embodiment, the organic solvent includes aromatic compounds, either alone or in any combination with the foregoing. In an embodiment, the aromatic compounds have a molecular weight from about 70 to about 400, preferably from about 100 to about 200 g/mol. Examples of suitable aromatic compounds include toluene, xylene, naphthalene, ethylbenzene, trimethylbenzene, and aromatic naphtha (AN), other suitable aromatic compounds, and any combination of the foregoing. It is to be understood that the amount of metal carboxylate in the composition in relation to the solvent may vary in some embodiments depending upon factors such as temperature, time, and type of metal carboxylate. For instance a higher ratio of metal carboxylate to solvent may be used if a faster reaction time is desired.

Group 3

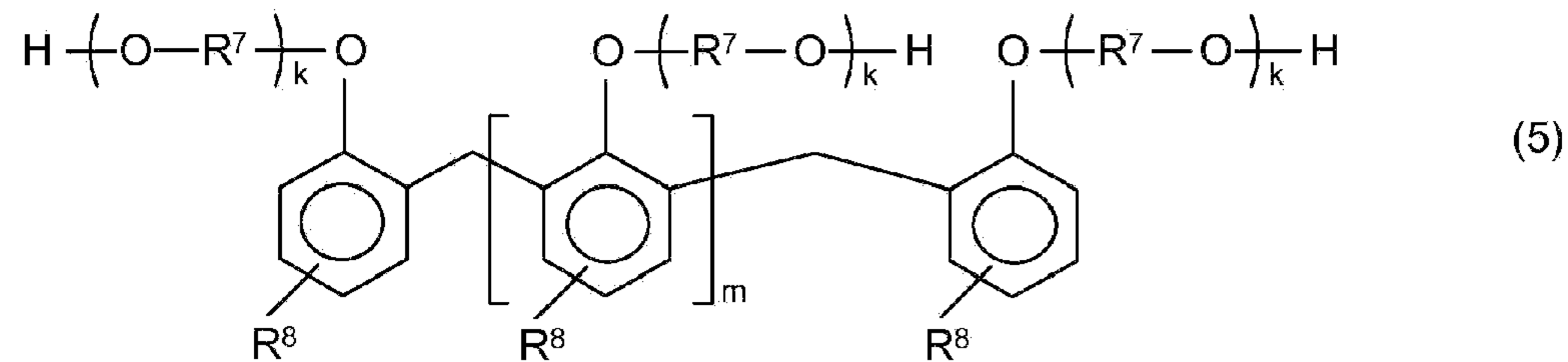
[0039] This group comprises emulsion breakers, or demulsifiers or non-emulsifiers. The purpose of having these compounds present is to prevent the formation of emulsions caused by the reaction products of metal carboxylate from Group 1. The metal carboxylate reaction product with sulfhydryl compounds is the corresponding metal sulfide. These metal sulfides are highly oil wetting and as a result they are attracted to the oil/water interface and cause emulsion stability. The purpose of the demulsifier molecule is to break the oil/water emulsion by creating a preferentially water wet surface on the metal sulfide and also to modify the surface tension at the oil/water interface which is stabilized by the metal sulfides to one allowing coalescence of the emulsion.

[0040] Examples of suitable polymeric nonionic surfactants include polysorbates, fatty alcohols such as cetyl alcohol and oleyl alcohol, polymers comprising ethylene oxide, polymers comprising propylene oxide, ethylene oxide-propylene oxide copolymers, alkyl polyglucosides such as decyl maltoside, alkylphenol polyethylene oxide, alkyl polyethylene oxide, and ethoxylated and/or propoxylated alkyl phenol-formaldehyde resins.

[0041] In preferred embodiments, the emulsion breaker components refer to components or additives that may be added as part of the composition comprising the instant invention and can be described as polymeric nonionic surfactants. Without limitation, examples of suitable polymeric nonionic surfactants include polysorbates, fatty alcohols such as cetyl alcohol and oleyl alcohol, polymers comprising ethylene oxide, polymers comprising propylene oxide, ethylene oxide-propylene oxide copolymers, alkyl polyglucosides such as decyl maltoside,

alkylphenol polyethylene oxide, alkyl polyethylene oxide, dodecylbenzenesulfonic acid, and ethoxylated and/or propoxylated alkyl phenol-formaldehyde resins.

[0042] In a preferred embodiment, the emulsion breaker is a compound according to the formula (5)



wherein

R^7
is C_2 to C_4 alkylene

R^8
is C_1 to C_{18} alkyl

k
is a number from 1 to 200

m
is a number from 1 to 100

[0043] In a preferred embodiment R^7 is an ethylene or a propylene group. R^7 may respect mixtures of different C_2 to C_4 alkylene groups, preferably ethylene and propylene groups.

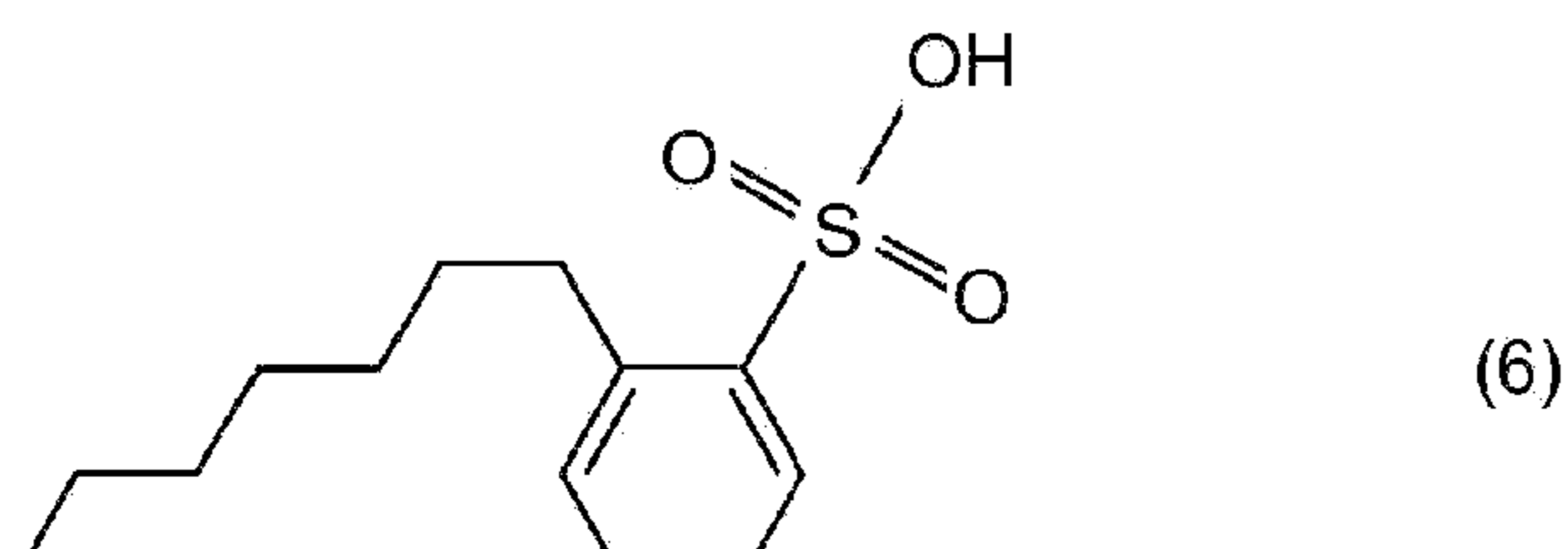
[0044] In another preferred embodiment, R^8 is a C_4 to C_{12} alkyl group, more preferably a tertiary butyl group or an iso-nonyl group.

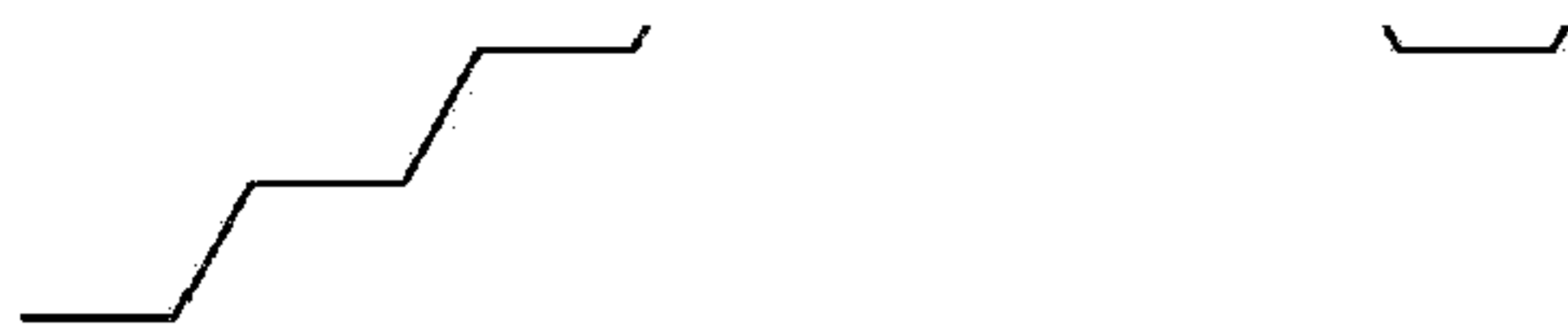
[0045] In formula (5), R^7 , R^8 and k may be the same in each of the repeating units, or they may differ from unit to unit.

[0046] In another preferred embodiment k is a number from 1 to 20.

[0047] In another preferred embodiment m is a number from 3 to 20.

[0048] In another specific preferred embodiment the emulsion breaker is dodecylbenzenesulfonic acid:





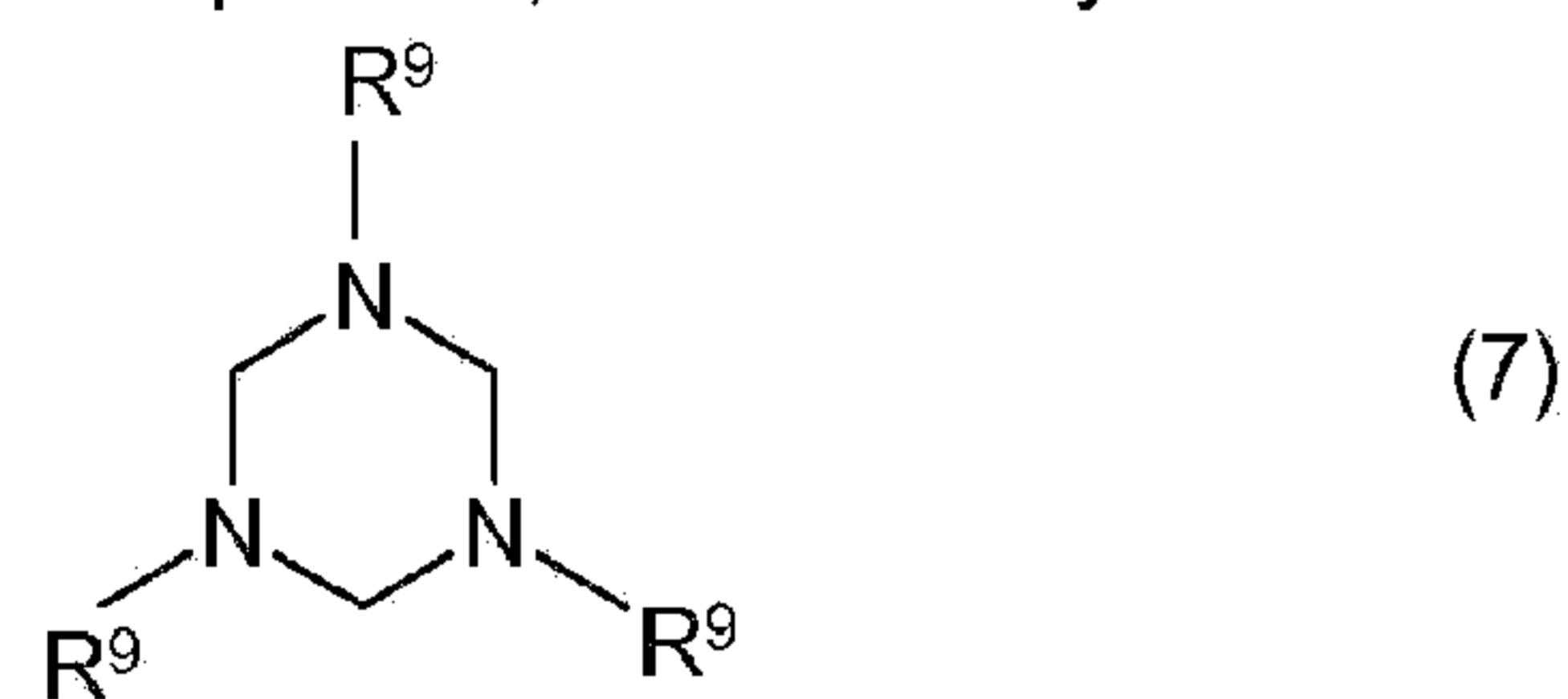
[0049] In another preferred embodiment, the demulsifier is a mixture of at least one compound of formula (5) and at least one compound of formula (6). Such mixture preferably contains (5) and (6) in a weight ratio of from 5:1 to 1:5, more preferably in a weight ratio of from 3:1 to 1:3.

[0050] The polymeric nonionic surfactant is preferably dissolved or suspended in a solvent. Any solvent suitable for dissolving or suspending a polymeric nonionic surfactant may be used. Examples of suitable solvents include water, butylglycol, ethylene glycol, propylene glycol, butylene glycol, oligoethylene glycols, oligopropylene glycols, ethers, alcohols, toluene, xylene, aromatic naphtha, or any combination thereof. The alcohol may include any alcohol suitable for use with oil recovery and for dissolving the polymeric nonionic surfactant and is preferably selected from the group consisting of isopropyl alcohol, methanol, ethanol, propanol, butanol or any combination thereof.

Group 4

[0051] The addition of a further hydrogen sulfide scavenger serves a two-fold purpose. Firstly it scavenges any residual H₂S not scavenged by the Group 1 components, and secondly, there may be a synergy created in scavenging in terms of rate of H₂S uptake.

[0052] Additional scavengers that can be included in the formulation include triazine compounds, described by the formula (7):



wherein

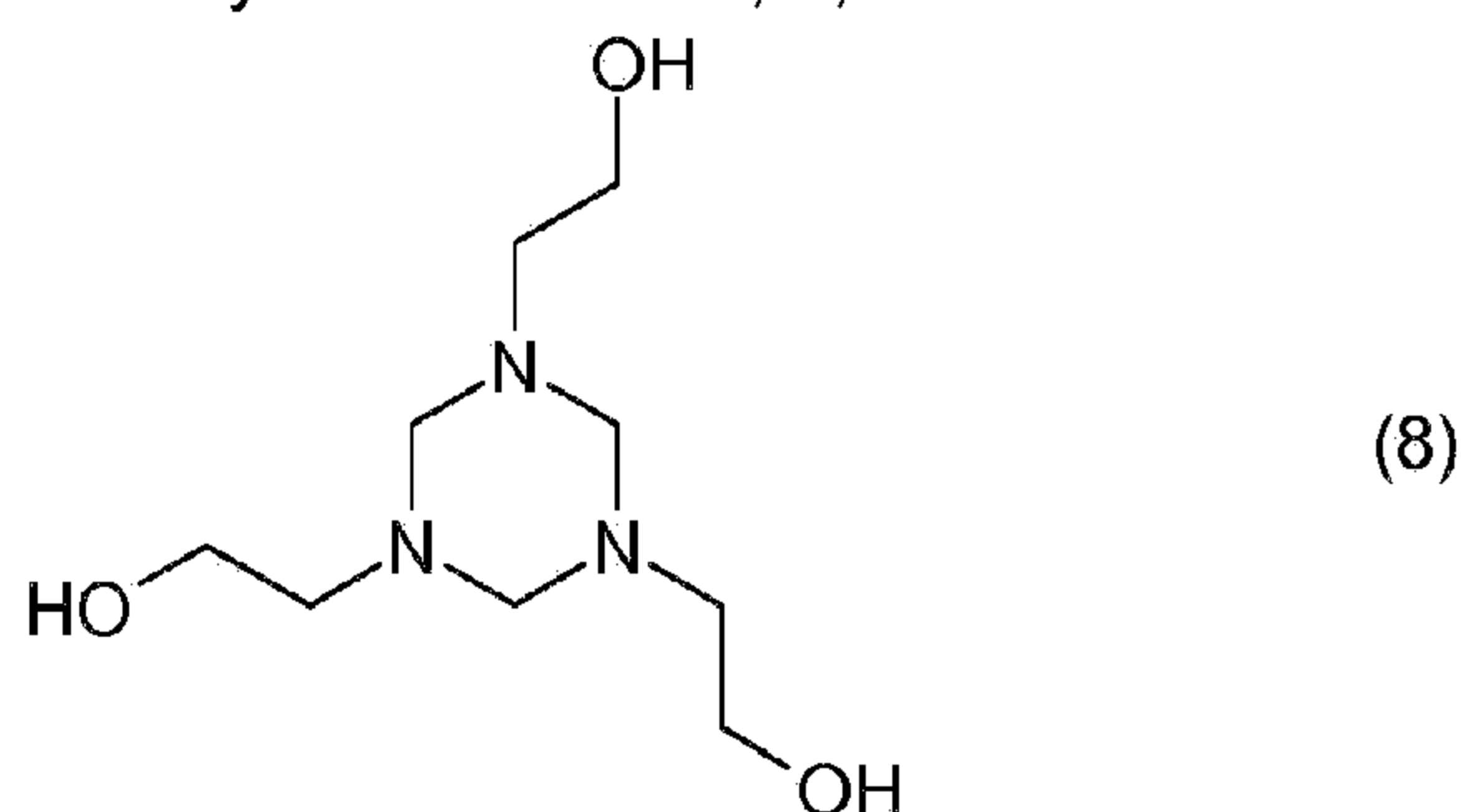
each R⁹ is independently selected from the group consisting of C₁ to C₂₀ straight or branched alkyl groups, or -R¹⁰OH, where R¹⁰ is a C₁ to C₂₀ straight or branched alkylene group. Preferably, at least one R⁹ group is a C₁ to C₂₀ straight or branched alkyl group and at least one R⁹ group is -R¹⁰OH.

[0053] Further, the scavenger can be selected from a range of hemi-acetal compounds, described by the general formula R¹¹R¹²C(OH)OR¹³ wherein R¹¹, R¹² or R¹³ are hydrogen and/or C₁ to C₂₀ straight or branched alkyl group. In a preferred embodiment, R¹¹, R¹², R¹³ all are C₁ to C₂₀ straight or branched alkyl groups.

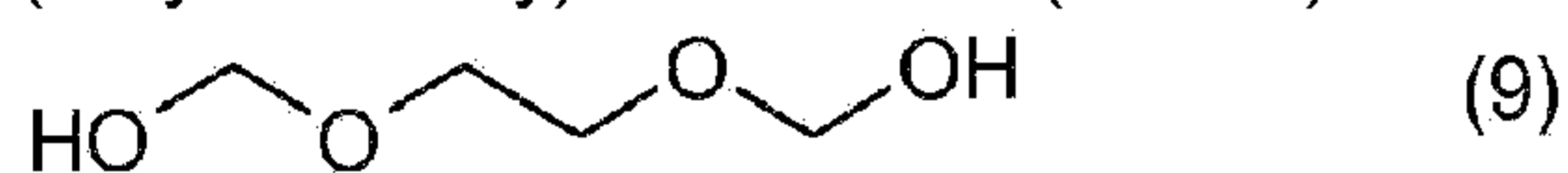
[0054] Further, the scavenger compound may be selected from hydantoins. Exemplary hydantoins include, but are not limited to hydroxyalkylhydantoins, bis(hydroxyalkyl)hydantoins, and dialkylhydantoins, where the alkyl group is generally a C₁ to C₆ alkyl group. Exemplary hydroxyalkylhydantoins useable as the aldehyde-releasing compound include, but are not limited to, 1-hydroxymethyl-5,5-dimethyl-hydantoin also known as monomethyloldimethylhydantoin (MDMH), 3-hydroxymethyl-5,5-dimethylhydantoin. Exemplary bis (hydroxyalkyl) hydantoins useable as the aldehyde-releasing compound include, but are not limited to, 1,3-bis(hydroxymethyl)-5,5-dimethylhydantoin as known as dimethyloldimethylhydantoin (DMDMH). Exemplary dialkylhydantoins useable as the aldehyde-releasing compound include, but are not limited to, 5,5-dimethylhydantoin. In addition, mixtures of the hydantoins may also be used.

[0055] Glyoxal (or ethandial) is a dialdehyde that has been shown in the art to scavenge hydrogen sulfide gas (e.g. US-4,680,127) and may also be used in the present invention to scavenge any hydrogen sulfide when contained in a formulation comprising group 1, group 2 and group 3 components.

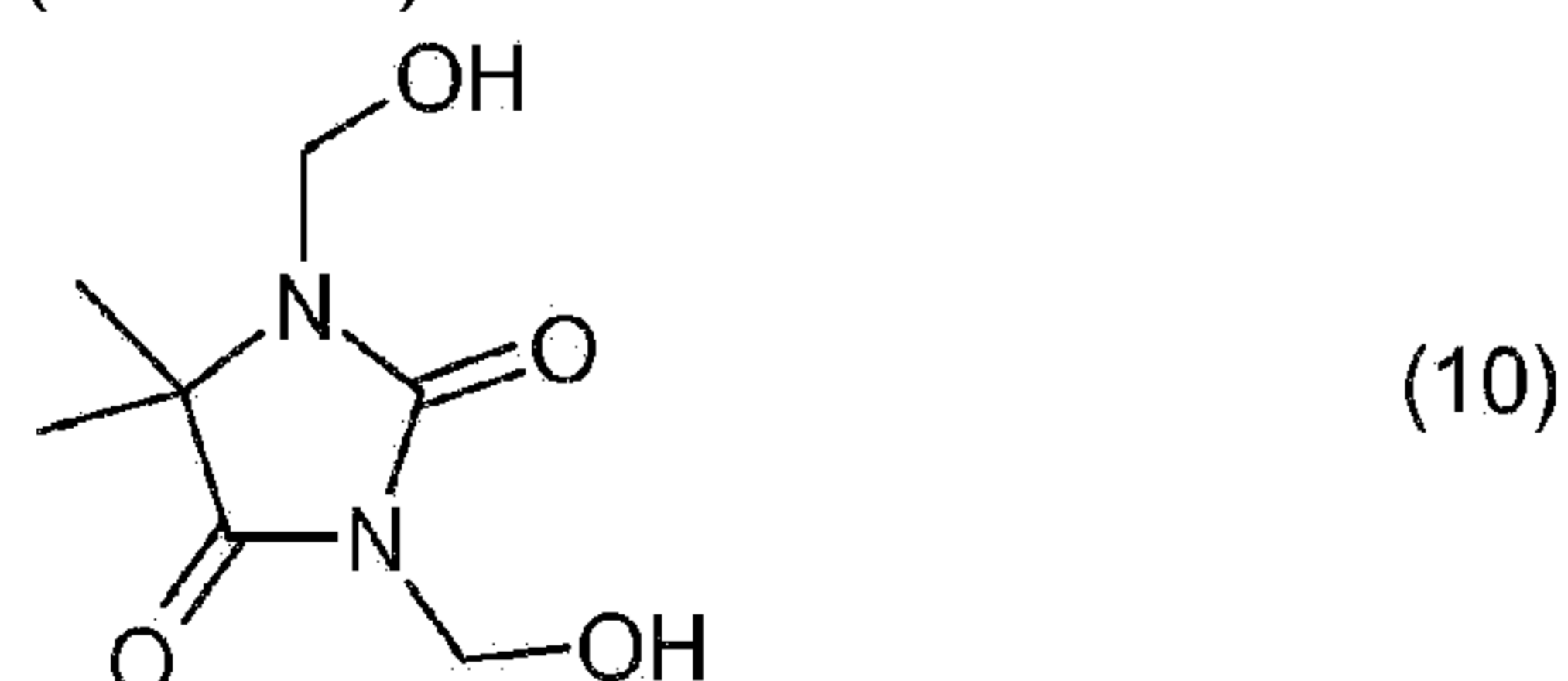
[0056] One preferred embodiment of the current invention is to use 1, 3, 5 Hexahydrotriethanol-1, 3, 5 Triazine to scavenge hydrogen sulfide gas:



[0057] Another preferred embodiment of the current invention is to use the hemiacetal (ethylenedioxy) dimethanol (EDDM):



[0058] Yet another preferred embodiment of the current invention is to use 1,3-bis(hydroxymethyl)-5,5-dimethylhydantoin as known as dimethyloldimethylhydantoin (DMDMH):



Group 5

[0059] Scale and/or corrosion inhibitors may be added to the target system separately and/or in association with the compounds described in group 1, 2 and 3. The addition of these Group 5 components serves to add functionality to the overall product.

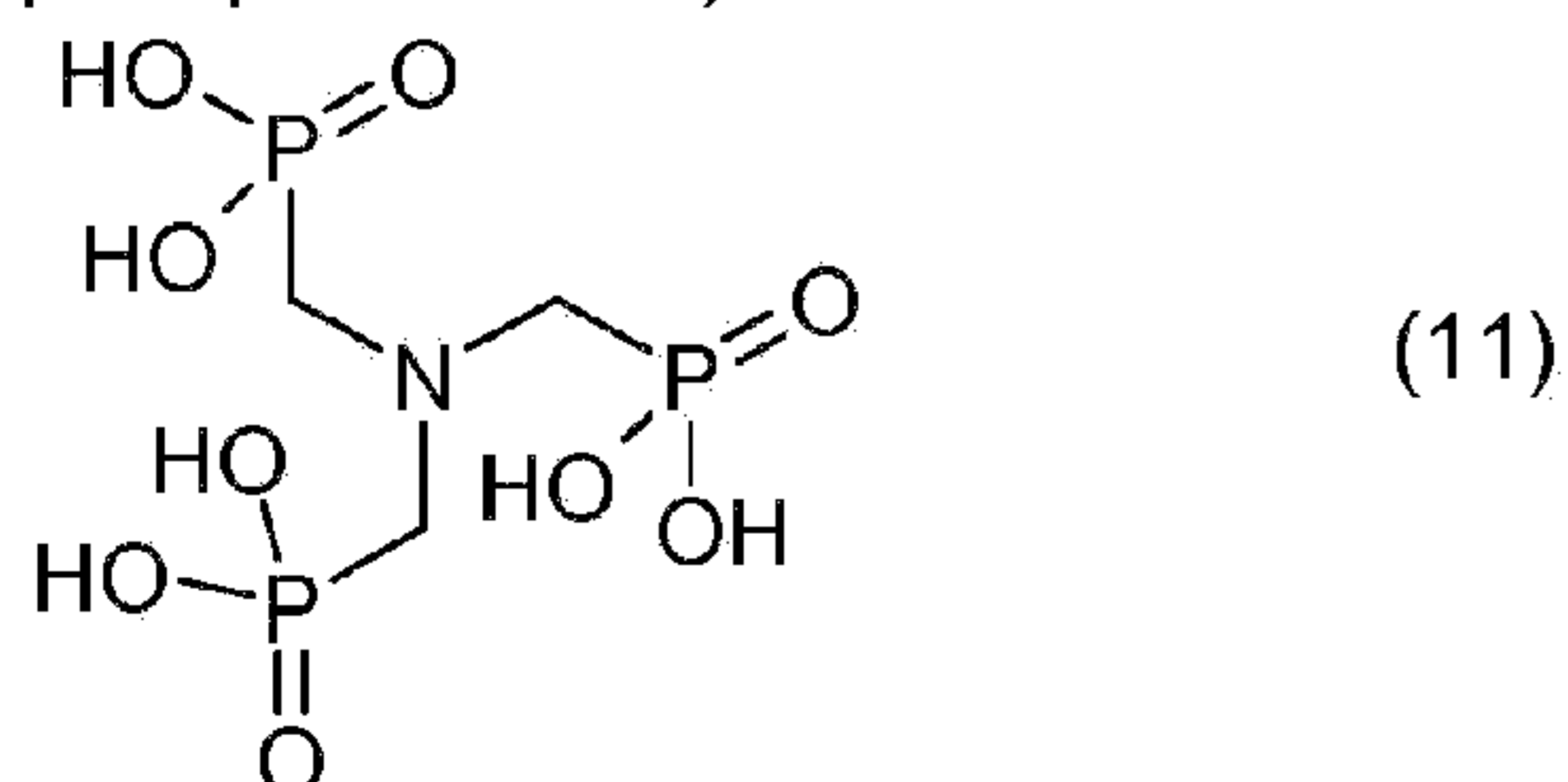
[0060] Adding a scale inhibitor can prevent either the deposition of unwanted solids that may result from mixing of incompatible waters. Furthermore, the reaction of metal carboxylates with sulfhydryl compounds very often leads to the precipitation of insoluble sulfide scale, for example the reaction of zinc neodecanoate will inevitably lead to the precipitation of highly water insoluble zinc sulfide.

[0061] The corrosion inhibitor serves to reduce the overall corrosivity of the treatment, protecting the tubulars and production equipment that oilfield fluids into which the instant invention is deployed into.

[0062] Conventional scale inhibitors which may be added to the water to be treated in conjunction with the present invention include, but are not limited to, 1-hydroxyethane-1,1-diphosphonates, diethylenetriamine penta(methylene phosphonic acid), nitrilo(methylene phosphonic acid), methacrylic diphosphonate homopolymer, polymaleates, polyacrylates, polymethacrylates, polyphosphates, phosphate esters, acrylic acid-allyl ethanolamine diphosphonate copolymer, sodium vinyl sulfonate-acrylic acid-allyl ammonia diphosphonate terpolymer, acrylic acid-maleic acid-diethylene triamine) allyl phosphonate terpolymer and polycarboxylates, all added to the formulation so that the conventional scale inhibitor present in the water to be treated ranges from 20 to 50 mg/L.

[0063] Conventional corrosion inhibitors which may be added to the water to be treated in conjunction with the present invention include, but are not limited to soluble zinc salts, nitrates, sulfites, benzoate, tannin, lignin sulfonates, benzotriazoles and mercapto-benzothiazoles amines, imidazolines, quaternary ammonium compounds, resins and phosphate esters, all added to the formulation so that the conventional corrosion inhibitor present in the water to be treated ranges from 50 to 100 mg/L.

[0064] One preferred embodiment of the current invention is to use amino tris(methylene phosphonic acid) as scale inhibitor



R¹⁷ are both hydrogen.

[0069] In all embodiments of the invention, monomers comprising an olefinically unsaturated hydrocarbon substituted ammonium salt group, wherein the expression hydrocarbon encompasses groups containing oxygen, are present in the copolymer in an amount of preferably below 1 mol-%, particularly 0.001 to 1 mol-%, especially 0.001 to 0.1 mol-%. They are particularly preferably completely absent.

[0070] In all embodiments of the invention, the molar proportion of vinylphosphonic acid or salts thereof is preferably from 0.8 to 6, especially from 1 to 4 mol-%. Suitable salts of vinylphosphonic acid are preferably the alkali metal or ammonium (NH₄⁺) salts thereof.

[0071] In a preferred embodiment, the molar proportion of structural units which are derived from compounds of the formula (12) in all embodiments of the invention is preferably from 45 to 70, especially from 50 to 65 mol-%.

[0072] The molar proportion of structural units which are derived from compounds of the formula (13) is preferably from 5 to 45 mol-%, especially from 10 to 40 mol-%. Formula (13) preferably represents acrylic acid and/or acrylamide. If formula (13) represents only acrylamide, the proportion thereof is preferably from 5 to 45 mol-%, especially from 10 to 40 mol-%. If formula (13) represents a mixture of acrylic acid and acrylamide, the proportion of acrylic acid is preferably from 1 to 10 mol-%, especially from 2 to 5 mol-%, and the proportion of acrylamide provides for the difference up to the total molar amount as described above.

[0073] The molar proportion of structural units which are derived from compounds of the formula (15) is preferably from 1 to 10 mol-%, particularly from 2 to 8 mol-%, especially from 3 to 7 mol-%.

[0074] The molar proportion of structural units which are derived from compounds of the formula (14) is preferably from 1 to 10 mol-%, particularly from 2 to 8 mol-%, especially from 3 to 7 mol-%.

[0075] Particular examples of suitable copolymers comprise (molar %).

[0076] 58 % AMPS, 38 % Acrylic Amide, 2 % n-Vinyl Formamide, 2 % Vinyl Phosphonic Acid.

[0077] 68 % AMPS, 28 % Acrylic Amide, 2 % n-Vinyl Formamide, 2 % Vinyl Phosphonic Acid.

[0078] 83 % AMPS, 5 % n-Vinyl Pyrrolidone, 5 % n-Vinyl Formamide, 5 % Acrylic Amide, 2 % Vinyl Phosphonic Acid.

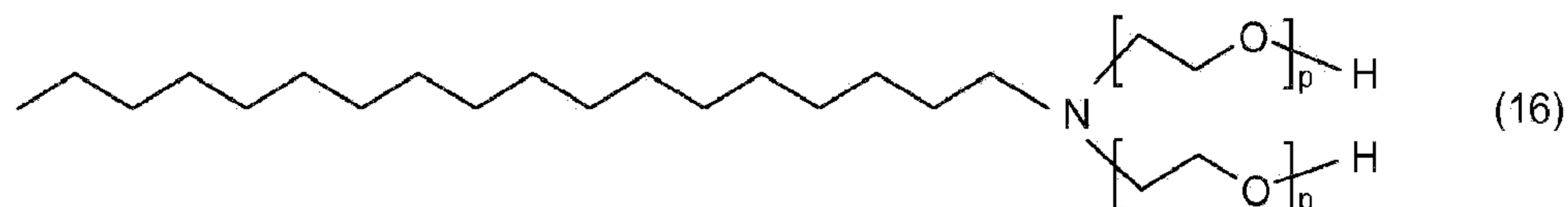
[0079] The monomer units may be in any sequence in the copolymers. They may be either random polymers or block polymers.

[0080] The molecular weights (number average) of the copolymers according to the invention are preferably from 100,000 to 10,000,000 g/mol, in particular from 500,000 to 5,000,000 g/mol. Molecular weight is to be determined by GPC against polyacrylic acid as standard.

[0081] The copolymers according to the invention can be prepared by copolymerization of vinyl phosphonic acid and compounds of the formulae (12), (13) and optionally (14), (15) in the stated molar ratios.

[0082] The copolymers according to the invention can be prepared by the conventional polymerization methods, such as solution polymerization, mass polymerization, emulsion polymerization, inverse emulsion polymerization, precipitation polymerization or gel polymerization. They are preferably the product of a free-radical copolymerization of vinyl phosphonic acid and the compounds of the formulae (12), (13) and optionally (14), (15).

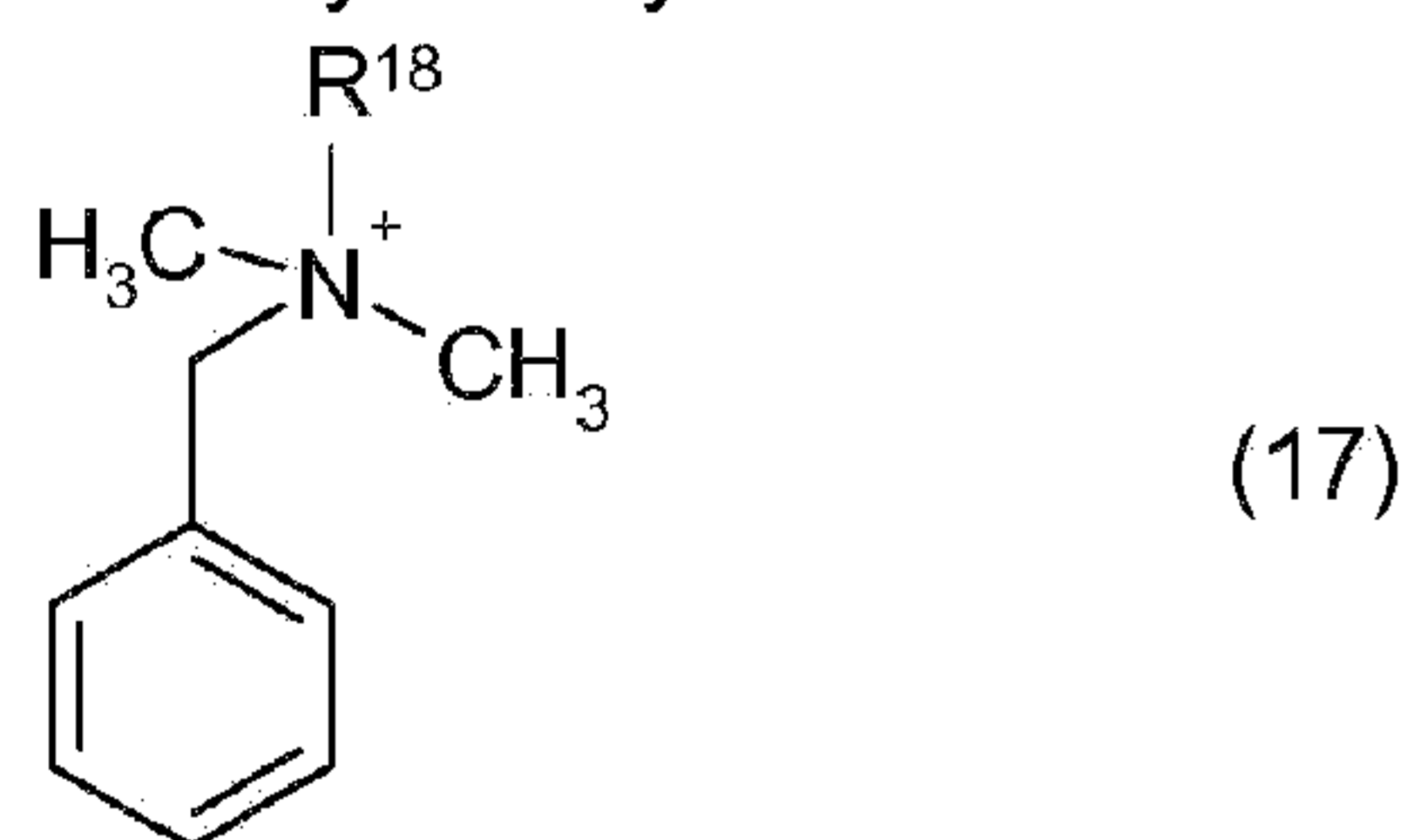
[0083] Yet another preferred embodiment of the current invention is to use tallow alkyl amine ethoxylate as corrosion inhibitor



wherein

p is a number from 4 to 10.

[0084] Yet another preferred embodiment of the current invention is to use coconut alkyl dimethyl benzyl ammonium chloride as corrosion inhibitor



wherein

R¹⁸ is C₈ to C₁₈ alkyl.

[0085] The composition may additionally contain biocides, for example, formaldehyde or glutaraldehyde, water dispersants, antifoams, oxygen scavengers and/or flocculants. There may also be added to the water to be treated oxygen scavengers, flocculants such as polyacrylamide dispersants, antifoams such as acetylenic diols, silicones or polyethoxylated antifoams.

[0086] The composition of one embodiment of the present invention is preferably prepared by combining:

0.1 to 80 wt.-% of the metal carboxylate species described above in group 1, preferably between 60 and 80 wt.-%,

1 to 50 wt.-% of the solvent species described above in group 2, preferably between 5 and 25 wt.-%,

0.1 to 10 wt.-% of at least one emulsion breaker species described above in group 3, preferably between 0.5 and 2 wt.-%,

1 to 20 wt.-% of the scavenger species described above in Group 4, preferably between 5 and 15 wt.-%, and

0.1 to 5 wt.-% of the scale and/or corrosion inhibitor species described above in Group 6, preferably between 0.2 and 2 wt.-%.

[0087] Furthermore, any balance remaining after addition of the 5 components described above is preferably made up with water and/or glycol and/or alcohol based solvents. The alcohols and solvents are preferably selected from, but not limited to, methanol, ethanol, propan-1-ol, propan-2-ol, monoethylene glycol, triethylene glycol, propylene glycol and / or 2-butoxyethanol.

[0088] The inventive composition is preferably applied to a production system where significant sulfhydryl compounds are present in concentrations between 0.1 and 10,000 mg/L based on oil production. The exact concentration will preferably depend on the formulation activity itself, the type of sulfhydryl compounds required to be scavenged, static conditions, materials of construction of the medium being treated, quality of the materials being used to make up the inventive solution, temperature of the system and salinity of the system. At this concentration range, the inventive system can provide substantial scavenging of sulfhydryl compounds from the produced liquids in order to maintain the flowability of hydrocarbon production and the quality of the hydrocarbon produced product as it is transported to market.

[0089] The present invention also includes a process for applications using the compositions above for application to be deployed in scavenging of sulfhydryl compounds present in the drilling and the production cycle, particularly as a component of well work-over, well intervention, production enhancement and flow assurance packages.

[0090] The injection fluid containing the composition of the instant invention may additionally contain other ingredients known to those familiar with the art. Such other ingredients include acids, dispersants, viscosifiers, lubricity agents, scale inhibitors, friction reducers, crosslinker, surfactants, scavenger, pH adjuster, iron control agents, breakers; this is especially true if any produced water (or recycled water) is in contact with the compositions of the instant invention.

[0091] Employing the embodiments of the instant invention improves the scavenging of sulfhydryl compounds while not causing formation of complex and difficult to treat emulsions. Furthermore the embodiments of the instant invention will not corrode the oilfield equipment that it comes into contact with, nor will it allow the deposition of unwanted solids, such as metal

sulfide scales, so often found with applications of the prior art. Other applications of the embodiments of the instantaneous invention include treating water for downhole injection for pressure support, treatment of drilling and work-over operations, wettability alteration and well cleanout.

EXAMPLES

[0092] In the whole specification, all references to percentages are meant to be weight percent relative to the respective whole composition, except if noted otherwise.

Example 1: Scavenger performance

[0093] In order to demonstrate the efficiency of the instant invention in removing sulfhydryl compounds as exhibited by components comprising Group 1, testing was performed focusing on removal of H₂S from an oil/water mixture. All testing was performed at 117 °F (47 °C) by sparging 200 ppm and 1,000 ppm H₂S gas (in a nitrogen matrix) at 0.15 liters per minute through 300 mL of oil (Eagle Ford condensate) and water (in a 50:50 volume ratio of oil to water) while magnetically stirring at 400 rpm. Five different dose rates of the various scavenger chemicals tested were added to the oil/water mixture at 250, 500, 1,000, 2,000 and 4,000 mg/L.

[0094] Efficacy was determined as the time required to measure the same concentration of H₂S exiting the test fluid than that entering, i.e. the time required for the scavenger to be 100 % spent and loaded with H₂S. The longer the time the more efficient the scavenger. The results have been summarized in Table 1.

Table 1: H₂S scavenger efficiency testing of components that comprise the instant invention and comparative examples from the prior art

Example	Chemical	200 ppm H ₂ S (min-sec)			1,000 ppm H ₂ S (min-sec)	
		250 ppm	500 ppm	1000 ppm	2000 ppm	4000 ppm
1 (C)	1,3,5 Hexahydrotriethanol-1, 3, 5 Triazine	1'50"	3'42"	11'22"	2'12"	5'17"
2 (C)	1, 3, 5-trimethylhexahydro-1, 3, 5-triazine	1'45"	3'37"	11'05"	2'03"	5'03"
3 (C)	α, α, α -Trimethyl-1, 3, 5-triazine-1, 3, 5(2H, 4H, 6H)-triethanol	1'48"	3'40"	11'15"	2'07"	5'10"
4 (C)	1, 6-dihydroxy-2, 5-dioxahexane	2'15"	4'58"	14'24"	2'44"	6'31"

Example	Chemical	200 ppm H ₂ S (min-sec)			1,000 ppm H ₂ S (min-sec)	
		250 ppm	500 ppm	1000 ppm	2000 ppm	4000 ppm
5 (C)	1,3-Dimethylol-5,5-dimethylhydantoin	2'04"	4'32"	12'49"	2'24"	5'53"
6 (C)	Zinc neodecanoate	3'21"	8'21"	25'50"	3'04"	7'48"
7 (C)	Zinc 2-ethylhexanoate	3'15"	8'05"	24'58"	2'52"	7'31"
8	Instant Invention Formulation	3'25"	8'29"	26'02"	3'17"	7'59"

[0095] The inventive formulation of example 8 was as follows: 75 % zinc-neodecanoate, 24.3 % heavy aromatic naphtha, 0.3 % of DDBSA (as described in formula (6)), 0.2 % Nonyl acid catalyzed resin with up to 5 mol ethylene oxide (EO) per OH group and an approximate molecular weight of 3,500 g/mol as described in formula (5), and 0.2 % Group 5 Copolymer (58 % AMPS, 38 % Acrylic Amide, 2 % n-Vinyl Formamide, 2 % Vinyl Phosphonic Acid).

[0096] It can be seen that all the triazine compounds that comprised comparative examples 1 (C), 2 (C), and 3 (C) performed very similarly. Comparative examples 4 (C) and 5 (C) performed better than the triazine examples but the raw scavengers of this instant invention in examples 6 and 7 outperformed the comparative examples in terms of H₂S loading efficacy.

Example 2: Viscosity profiles

[0097] The purpose of this testing was to determine the effect that Group 2 components had on the viscosity of compositions of the instant invention. Viscosity was measured using a Brookfield viscometer at a constant of 71 °F (22 °C) and ambient pressure. The results have been displayed in Table 2.

Table 2: Viscosity measurements of the instant invention and comparative examples

Example	Chemistry / Formulation	Viscosity (cP)
1 (C)	Zinc neodecanoate	9,000
2 (C)	Zinc 2-ethylhexanoate	8,500
3 (C)	75 % Zinc neodecanoate + 25 % MEG	732
4 (C)	75 % Zinc 2-ethylhexanoate + 25 % MEG	711
5 (C)	75 % Zinc neodecanoate + 25 % 2-BE	766
6 (C)	75 % Zinc 2-ethylhexanoate + 25 % 2-BE	728

Example	Chemistry / Formulation	Viscosity (cP)
7 (C)	75 % Zinc neodecanoate + 25 % HAN	93
8 (C)	75 % Zinc 2-ethylhexanoate + 25 % HAN	86
9 (C)	75 % Zinc neodecanoate + 25 % butanol	624
10 (C)	75 % Zinc 2-ethylhexanoate + 25 % butanol	586
11 (C)	75 % Zinc neodecanoate + 25 % toluene	137
12 (C)	75 % Zinc 2-ethylhexanoate + 25 % toluene	124
13	Instant Invention Formulation	139

[0098] The inventive formulation of example 13 was 1 as follows: 75 % zinc-neodecanoate, 24.3 % heavy aromatic naphtha, 0.3 % of DDBSA (as described in formula (6)), 0.2 % Nonyl acid catalyzed resin with up to 5 mol ethylene oxide (EO) per OH group and an approximate molecular weight of 3,500 g/mol as described in formula (5), and 0.2 % Group 5 Copolymer (58 % AMPS, 38 % Acrylic Amide, 2 % n-Vinyl Formamide, 2 % Vinyl Phosphonic Acid).

[0099] In Table 2 MEG is monoethylene glycol, 2-BE is 2-butoxyethanol, and HAN is heavy aromatic naphtha. It can be seen that viscosity can be dramatically reduced by adding relatively low amounts of solvent compared to the two comparative Group 1 examples. The most effective Group 2 components to add to the Group 1 components for viscosity reduction were heavy aromatic naphtha and/or toluene.

Example 3: Emulsion testing

[0100] It is well known to one skilled in the art that solids in an oil/water mixture can cause significant emulsion stability especially if those solids are liable to oil wet and sit on the oil/water interface. This is the case with zinc sulfide and as this is a reaction product of preferred embodiments of the instant invention, the test work presented here shows how Group 3 emulsion breaker components assist with the resolution of emulsions caused by use of the Group 1 components.

[0101] The testing was performed using the standard bottle test, well known to one skilled in the art. This involved taking 100 mL of different ratios of crude oil and synthetic brine in a prescription bottle and agitating them on a mechanical shaker in order to induce emulsions. All tests were performed at a temperature of 140 °F (60 °C) and separation observed for 10 minutes. For tests that contained ZnS, the ZnS was added as a substance in a known concentration. The time taken for emulsion resolution was recorded as water drop rate, crude

oil dehydration and interface quality. Water drop rate is the rate at which water volumetrically separates from the crude oil. It is desirable for this to be as quick as possible, achieving a maxima in under 5 minutes is more desirable in oilfield operations. The crude oil dehydration is measured as base sediment and water % (BS&W %) which in this test is the water content that remains in the oil at the end of the test. This gives a secondary indication of performance because while water drop is one desirable feature of a good demulsifier, the remaining water left in the crude oil is ideally <2 %, more desirable is <1 %. Finally the quality of the interface is important. A clean interface, i.e. a very uniform layer existing between the oil and water, rather than a baggy, or inhomogeneous interface is most desirable. This is because the way oilfield separation process equipment works requires a clean interface to be most efficient. These tests were performed using comparative components and preferred embodiments of the instant invention to show how inclusion of Group 3 components significantly enhanced the resolution of emulsions and that examples from the known art cause substantial challenges with respect to emulsion formation. The results have been summarized in Tables 3 and 4 which show formulations and performance data respectively.

Table 3: Formulations tested for emulsion resolution

Example	Formulation
1 (C)	Zinc-neodecanoate
2 (C)	75 % zinc-neodecanoate, 25 % HAN
3	75 % zinc-neodecanoate, 24 % HAN, 1 % DDBSA as described in formula (6)
4	75 % zinc-neodecanoate, 24 % HAN, 1 % Nonyl acid catalyzed resin with up to 5 mol ethylene oxide (EO) per OH group and an approximate molecular weight of 3,500 g/mol as described in formula (5)
5	75 % zinc-neodecanoate, 24 % HAN, 0.5 % DDBSA as described in formula (6) and 0.5 % Nonyl acid catalyzed resin with up to 5 mol ethylene oxide (EO) per OH group and an approximate molecular weight of 3,500 g/mol as described in formula (5)

Table 4: Emulsion resolution testing of the instant invention and comparative examples

Ex. (from Table 3)	Oil (vol.-%) ¹	ZnS content (wt.-%)	Water Drop (mL)						BS&W (%)	Interface Quality
			1 min	2 min	3 min	4 min	5 min	10 min		
1 (C)	50	0	35	41	48	50	50	50	3.2	Good, sharp
	50	0.5	21	24	27	31	33	41	6.3	Poor, baggy
	70	0	12	18	26	30	30	30	2.8	Good, sharp
	70	0.5	6	8	10	13	14	19	5.9	Poor, baggy

Ex. (from Table 3)	Oil (vol.-%) ¹	ZnS content (wt.-%)	Water Drop (mL)						BS&W (%)	Interface Quality
			1 min	2 min	3 min	4 min	5 min	10 min		
2 (C)	50	0	37	42	50	50	50	50	2.9	Good, sharp
	50	0.5	22	23	29	34	36	44	6.1	Poor, baggy
	70	0	14	19	28	30	30	30	2.4	Good, sharp
	70	0.5	7	8	12	14	16	21	5.7	Poor, baggy
3	50	0	43	48	50	50	50	50	1.4	Good, sharp
	50	0.5	34	38	42	44	47	50	2.3	Good, sharp
	70	0	22	29	30	30	30	30	0.9	Good, sharp
	70	0.5	16	21	27	29	30	30	1.9	Good, sharp
4	50	0	42	47	49	50	50	50	1.6	Good, sharp
	50	0.5	32	36	40	43	46	50	2.7	Good, sharp
	70	0	21	28	30	30	30	30	1.0	Good, sharp
	70	0.5	14	20	26	28	30	30	2.1	Good, sharp
5	50	0	48	50	50	50	50	50	0.3	Good, sharp
	50	0.5	46	49	50	50	50	50	0.3	Good, sharp
	70	0	27	29	30	30	30	30	0.1	Good, sharp
	70	0.5	24	28	30	30	30	30	0.2	Good, sharp

¹The remainder of the 100 % is brine

[0102] It can be seen that the presence of ZnS in the oil/water mixtures causes separation issues via emulsion formation. The presence of small concentrations of emulsion breaker bases helps to resolve these emulsions, in Example 5 which is a preferred embodiment of the instant invention, a formulated emulsion breaker package was used to show how complete

emulsion resolution can be obtained that could be used as a field solution in order to resolve the challenges caused by the prior art examples.

Example 4: Breakdown product inhibition

[0103] A further preferred embodiment of the instant invention is to inhibit the formation of undesirable solids. An example is the inhibition of ZnS solids caused by the reaction of preferred embodiments from Group 1 with H₂S. Preferred embodiments from Group 5 were included with a preferred embodiment formulation comprising components from Group 1, 2 and 3 and tested for inhibition of undesirable solid formation.

[0104] The various formulations were tested at various concentrations in a 50:50 oil/water mixture (as described in Example 1). At the end of the test the total fluids were filtered through a 0.45 µm filter and the solids captured weighted and characterized. A high amount of solids measured indicated poor inhibition of ZnS, and the composition confirmed using x-ray diffraction. The results of this testing has been summarized in Table 5 and 6 which show the formulations tested and performance of these formulations respectively.

Table 5: Formulations tested for ZnS solids deposition potential

Example	Formulation
1 (C)	Zinc-neodecanoate
2 (C)	75 % zinc-neodecanoate, 25 % HAN
3	75 % zinc-neodecanoate, 24 % HAN, 1 % DDBSA as described in formula (6)
4	75 % zinc-neodecanoate, 24 % HAN, 1 % Nonyl acid catalyzed resin with up to 5 mol ethylene oxide (EO) per OH group as described in formula (5)
5	75 % zinc-neodecanoate, 24 % HAN, 0.5 % DDBSA as described in formula (6) and 0.5 % Nonyl acid catalyzed resin with up to 5 mol ethylene oxide (EO) per OH group and an approximate molecular weight of 3,500 g/mol as described in formula (5)
6	75 % zinc-neodecanoate, 24.3 % heavy aromatic naphtha, 0.3 % of DDBSA (as described in formula (6)), 0.2 % Nonyl acid catalyzed resin with up to 5 mol ethylene oxide (EO) per OH group and an approximate molecular weight of 3,500 g/mol as described in formula (5), and 0.2 % Group 5 Copolymer (58 % AMPS, 38 % Acrylic Amide, 2 % n-Vinyl Formamide, 2 % Vinyl Phosphonic Acid).

Table 6: Results of ZnS solids deposition control

Example (from table 5)	Table 5 Formulation Concentration (ppm)	Mass of Solids (g)	Composition of Inorganic Component of Solids
1 (C)	1,000	0.0171	Zinc sulfide
	5,000	0.0867	Zinc sulfide
	10,000	0.1682	Zinc sulfide

Example (from table 5)	Table 5 Formulation Concentration (ppm)	Mass of Solids (g)	Composition of Inorganic Component of Solids
2 (C)	1,000	0.0160	Zinc sulfide
	5,000	0.0649	Zinc sulfide
	10,000	0.1269	Zinc sulfide
3	1,000	0.0127	Zinc sulfide
	5,000	0.0627	Zinc sulfide
	10,000	0.1247	Zinc sulfide
4	1,000	0.0149	Zinc sulfide
	5,000	0.0635	Zinc sulfide
	10,000	0.1245	Zinc sulfide
5	1,000	0.0148	Zinc sulfide
	5,000	0.0630	Zinc sulfide
	10,000	0.1252	Zinc sulfide
6	1,000	0.0027	Zinc sulfide
	5,000	0.0131	Zinc sulfide
	10,000	0.03468	Zinc sulfide

[0105] It can be seen that the amount of zinc sulfide byproduct formed upon sparging through excess H₂S in the comparative examples is significant when compared to the inventive example number 6 which shows clear dispersion of ZnS solids.

REFERENCES CITED IN THE DESCRIPTION

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Patentkrav**1. Sammensætning omfattende**

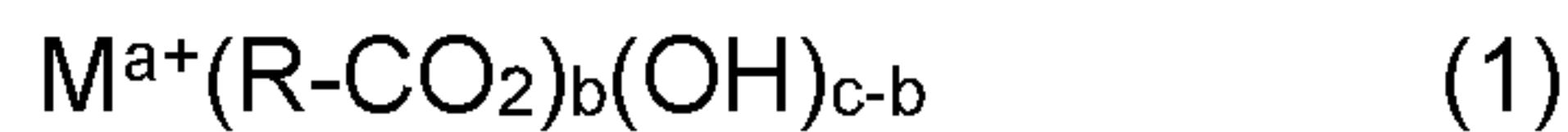
5 1.) et metalcarboxylat, hvor metallet M er udvalgt fra gruppen bestående af Fe og Zn, hvor de metaller foreligger som ioner i en +2- eller +3 ladningstilstand, og hvor carboxylatanionen er afledt af en hydrocarbylmonocarboxylsyre med 5 til 20 carbonatomer, eller en blanding af sådanne syrer,

10 2.) et opløsningsmiddel udvalgt fra gruppen bestående af vand, glycolethere med fra 4 til 15 carbonatomer, alkylalkoholer med fra 1 til 10 carbonatomer, og aromatiske carbonhydridopløsningsmidler med fra 6 til 30 carbonatomer,

3.) en emulsionsbryder, som er udvalgt fra gruppen bestående af et polymert ikke-ionisk overfladeaktivt middel og dodecylbenzensulfonsyre.

2. Sammensætning ifølge krav 1, hvor metalcarboxylatet svarer til formel (1)

15



hvor

20 M er iron,
a er 2 eller 3,
b er 1, 2 eller 3,
c er (a-b), og

R er et hydrocarbylradikal indeholdende fra 4 til 19 carbonatomer, eller blandinger af sådanne carboxylater.

25

3. Sammensætning ifølge krav 1, hvor metalcarboxylatet er zinkcarboxylat.

30 **4. Sammensætning ifølge krav 3, hvor zinkcarboxylatet svarer til formel $Zn_4(O_2CR)_6O$, hvor R er et hydrocarbylradikal indeholdende fra 4 til 19 carbonatomer, eller blandinger af sådanne carboxylater.**

5. Sammensætning ifølge et eller flere af kravene 1-4, hvor metalcarboxylatet er olie-opløseligt.

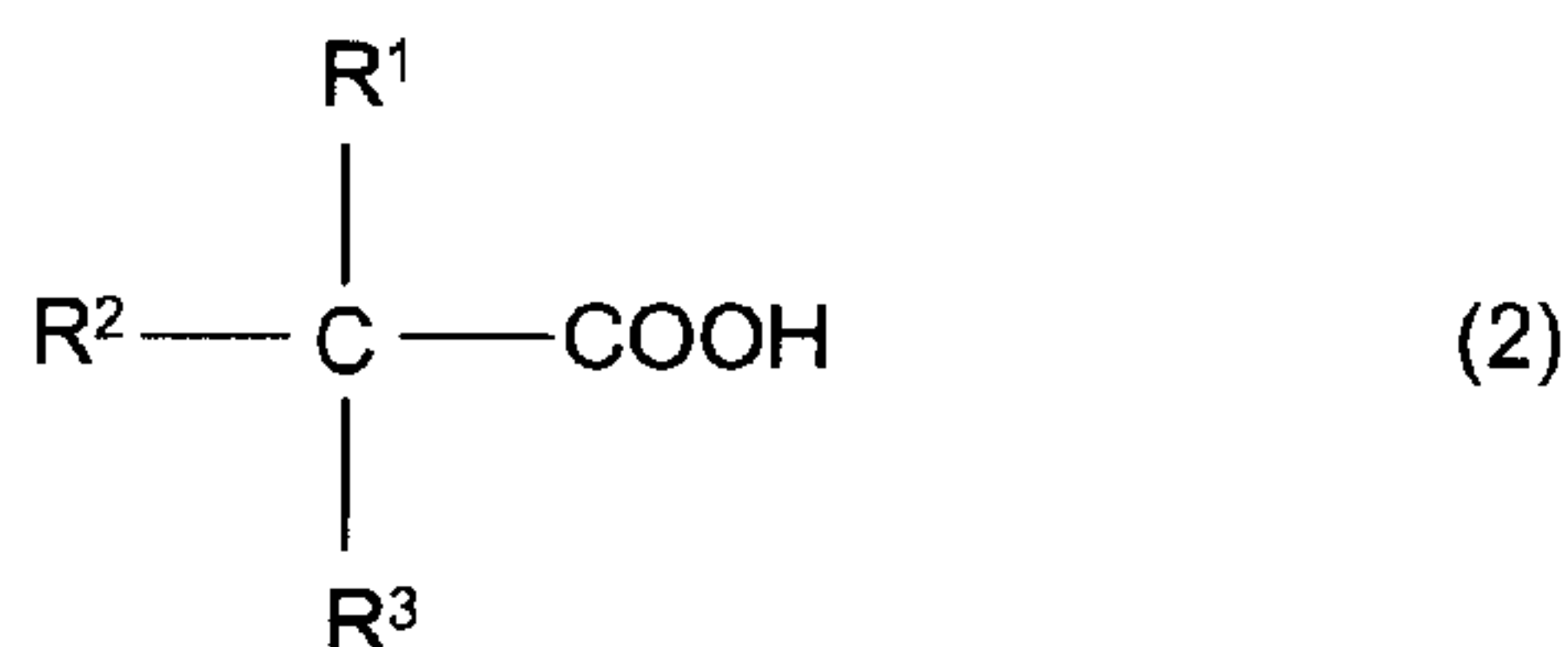
6. Sammensætning ifølge et eller flere af kravene 1 - 5, hvor syrerne R-COOH, som metalcarboxylatet er afledt af, er flydende under 100 °C.

5

7. Sammensætning ifølge et eller flere af kravene 1, 2, 5 og/eller 6, hvor M er Fe.

8. Sammensætning ifølge et eller flere af kravene 1 - 7, hvor metalcarboxylatet med formel (1) er saltet af en neosyre med formlen (2)

10



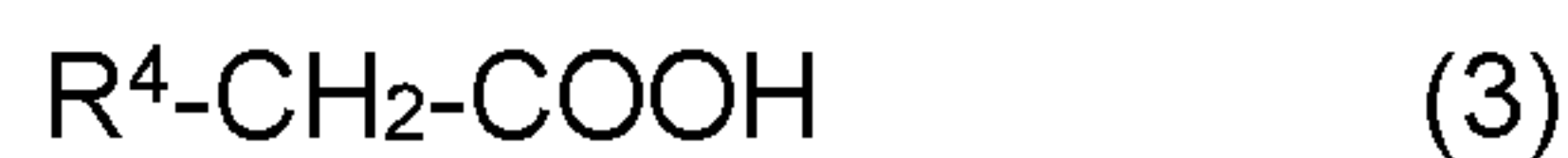
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R¹, R² og R³ hver især uafhængigt er alkylgrupper indeholdende 1 til 16 carbonatomer, hvor det samlede antal af carbonatomer indeholdt i R¹, R² og R³ er fra 3 til 18.

9. Sammensætning ifølge et eller flere af kravene 1 - 7, hvor metalcarboxylatet med formel (1) er et salt af en isosyre med formel (3)

20



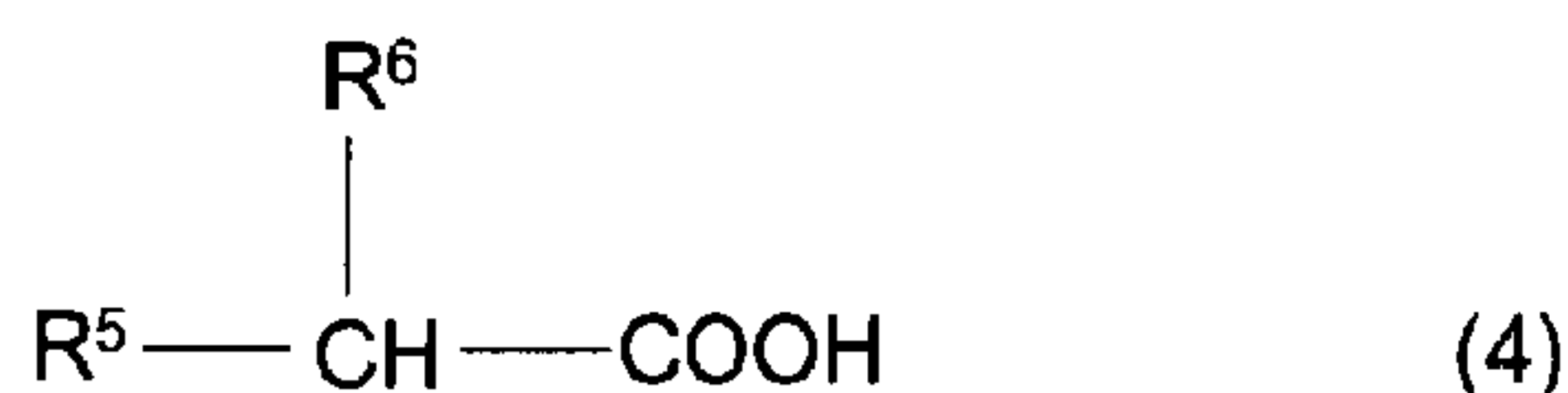
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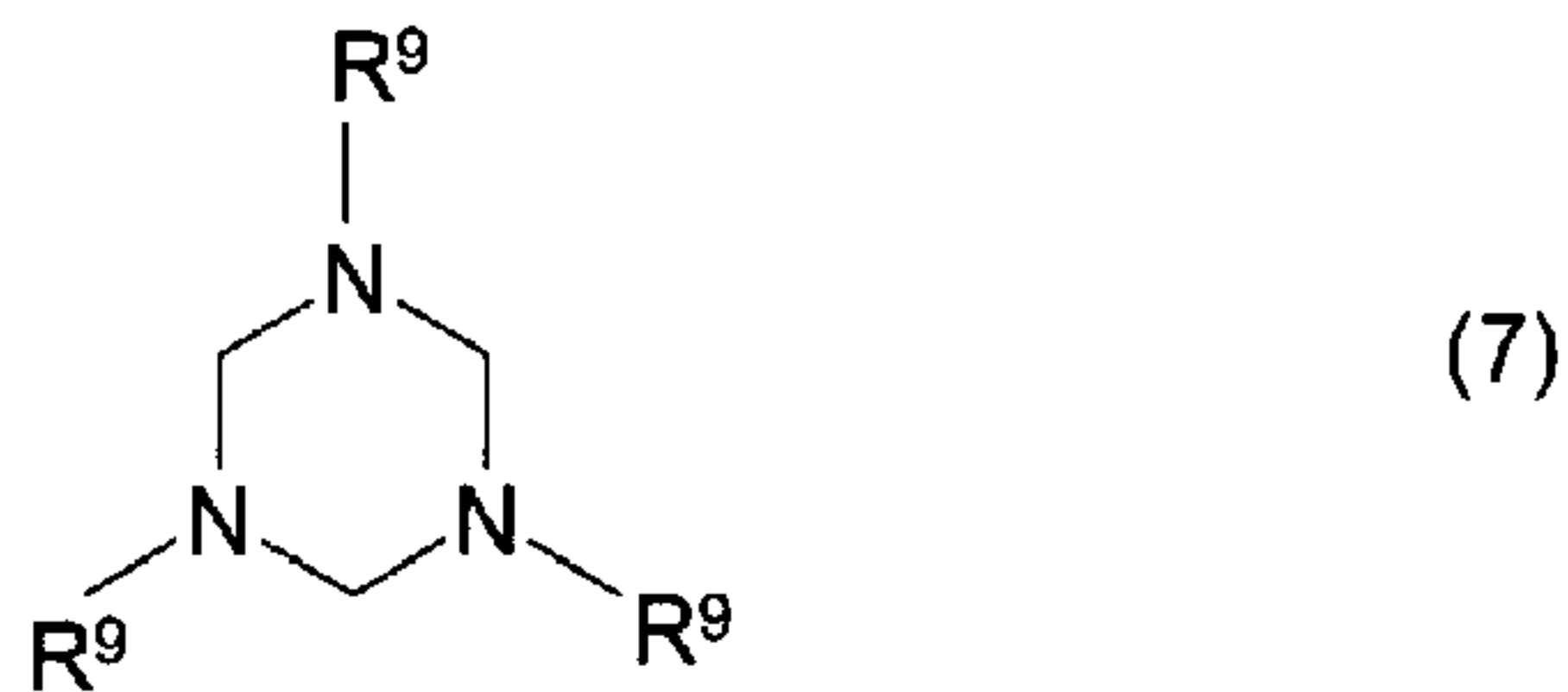
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R⁴ er en alifatisk, forgrenet hydrocarbylgruppe indeholdende fra 2 til 20 carbonatomer.

10. Sammensætning ifølge et eller flere af kravene 1 - 7, hvor metalcarboxylatet med formel (1) er et salt af en guerbetsyre med formel (4)

30



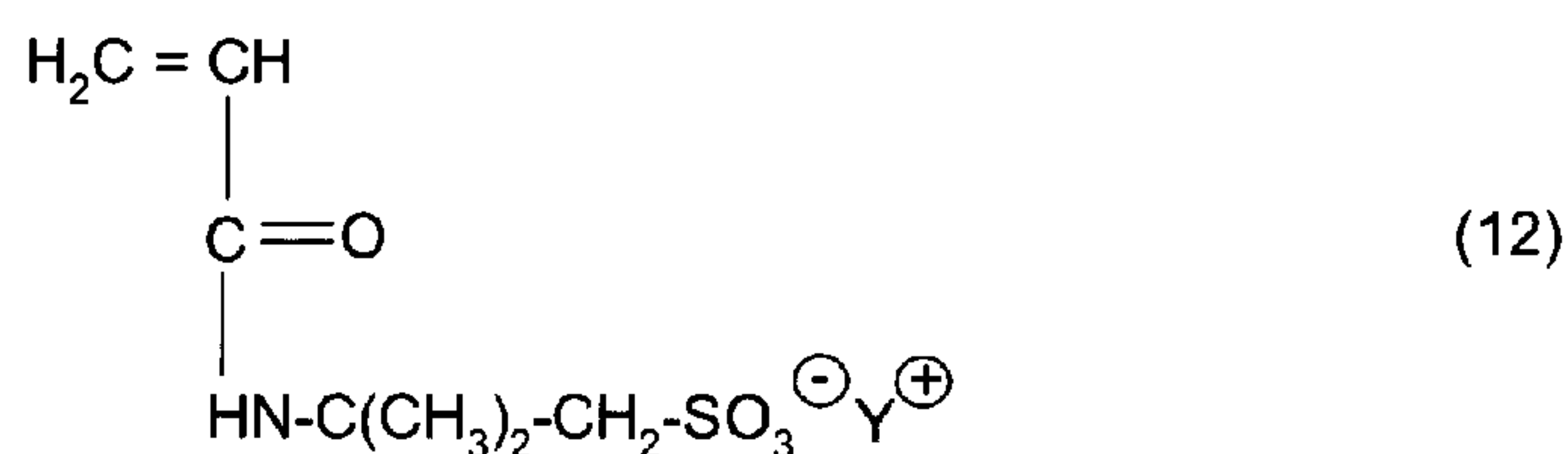


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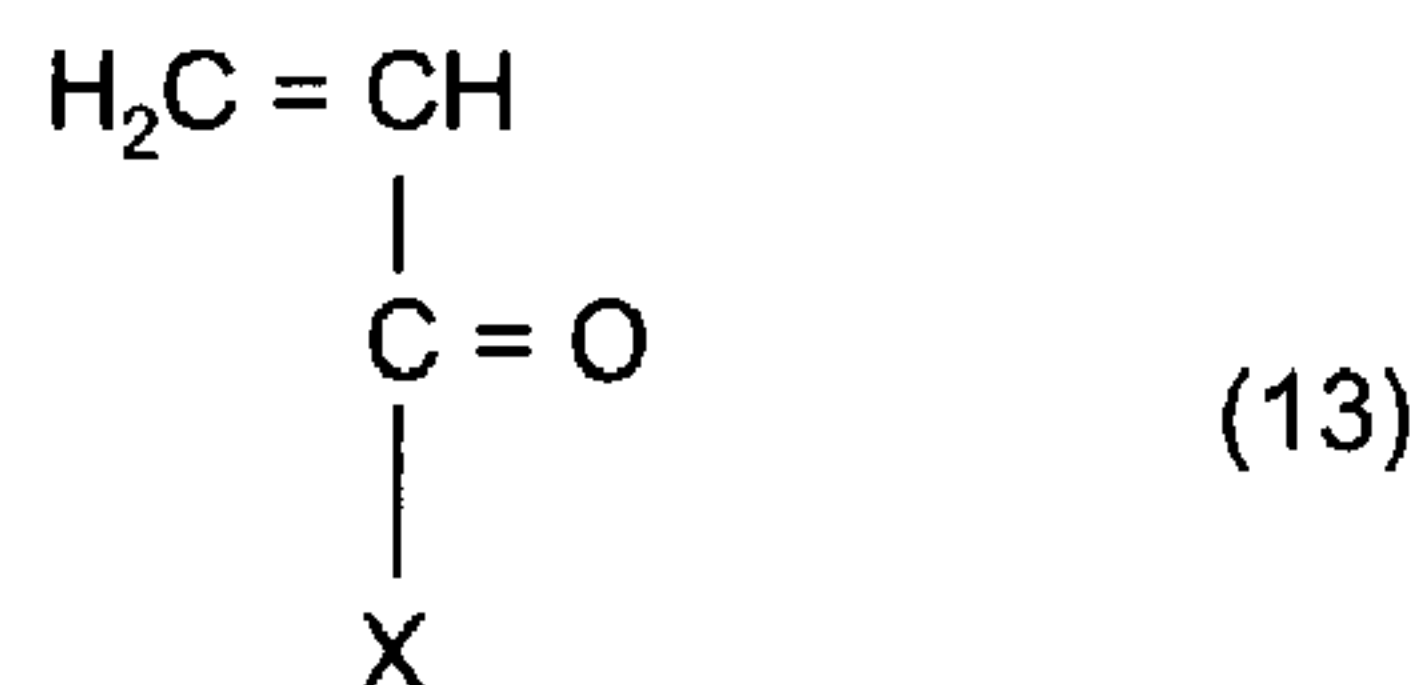
- 5 hver R⁹ er uafhængigt udvalgt fra gruppen bestående af ligekædede eller for-
 grenede C₁- til C₂₀-alkylgrupper, eller -R¹⁰OH, hvor R¹⁰ er en ligekædet eller
 forgrenet C₁- til C₂₀-alkylengruppe,
 hemiacetalforbindelser med den almene formel R¹¹R¹²C(OH)OR¹³, hvor R¹¹,
 R¹² eller R¹³ er hydrogen og/eller ligekædet eller forgrenet C₁- til C₂₀-alkyl-
 10 gruppe, hydroxyalkylhydantoiner, bis(hydroxyalkyl)hydantoiner og dialkyl-
 hydantoiner, hvor alkylgruppen er en C₁- til C₆-alkylgruppe, og
 glyoxal er foreliggende.

- 15 **15.** Sammensætning ifølge et eller flere af kravene 1 - 14, hvor en aflejnings-
 hæmmer udvalgt fra gruppen bestående af 1-hydroxyethan-1,1-diphosphonat,
 diethylentriaminpenta(methylenphosphonsyre), nitrilo(methylenphosphonsy-
 re), methacryldiphosphonathomopolymer, polymaleater, polyacrylater, poly-
 methacrylater, polyphosphater, phosphatestere, acrylsyre-allylethanolamin-
 diphosphonatcopolymer, natriumvinylsulfonat-acrylsyre-allylammoniakdiphos-
 20 phonatterpolymer, acrylsyre-maleinsyre-diethylentriamin)allylphosphonatter-
 polymer og polycarboxylater er foreliggende.

- 25 **16.** Sammensætning ifølge et eller flere af kravene 1 - 14, hvor en aflejnings-
 hæmmer er foreliggende, som er copolymer, omfattende
 a) 0,1 til 10 mol-% af strukturelle enheder afledt af vinylphosphonsyre og/eller
 et salt deraf,
 b) 40 til 90 mol-% af strukturelle enheder afledt af forbindelser med formel (12)



c) 1 til 50 mol-% af strukturelle enheder afledt af forbindelser med formelen (13)



5 i hvilken
X er OH eller NR¹⁴R¹⁵, og R¹⁴ og R¹⁵, uafhængigt af hinanden, er H eller C₁-C₄-alkyl.

10 **17.** Sammensætning ifølge et eller flere af kravene 1 - 16, omfattende
0,1 til 80 vægt-% af metalcarboxylatet,
1 til 50 vægt-% af opløsningsmidlet
0,1 til 10 vægt-% af mindst en emulsionsbryder.

15 **18.** Sammensætning ifølge et eller flere af kravene 11 - 17, omfattende den
yderligere H₂S-opfanger i en mængde på 1 til 20 vægt-%.

19. Sammensætning ifølge et eller flere af kravene 15 - 18, omfattede aflej-
ringshæmmeren i en mængde på 0,1 til 5 vægt-%.

20 **20.** Anvendelse af sammensætningen ifølge et eller flere af kravene 1 - 19 som
en sulfhydrylopfanger til anvendelse til oliefeltdrifts- og oliefeltforarbejdnings-
systemer.

25 **21.** Fremgangsmåde til opfangning af sulfhydrylmolekyler inden for oliefeltdrifts-
og oliefeltforarbejdningsystemer, hvor fremgangsmåden omfatter at tilsætte
sammensætningen ifølge et eller flere af kravene 1 - 19 til et system, der er
modtageligt over for produktion af sulfhydrylforbindelser.